



The sequential biorefinery approach for biodiesel and glucose production from Spent Coffee Grounds

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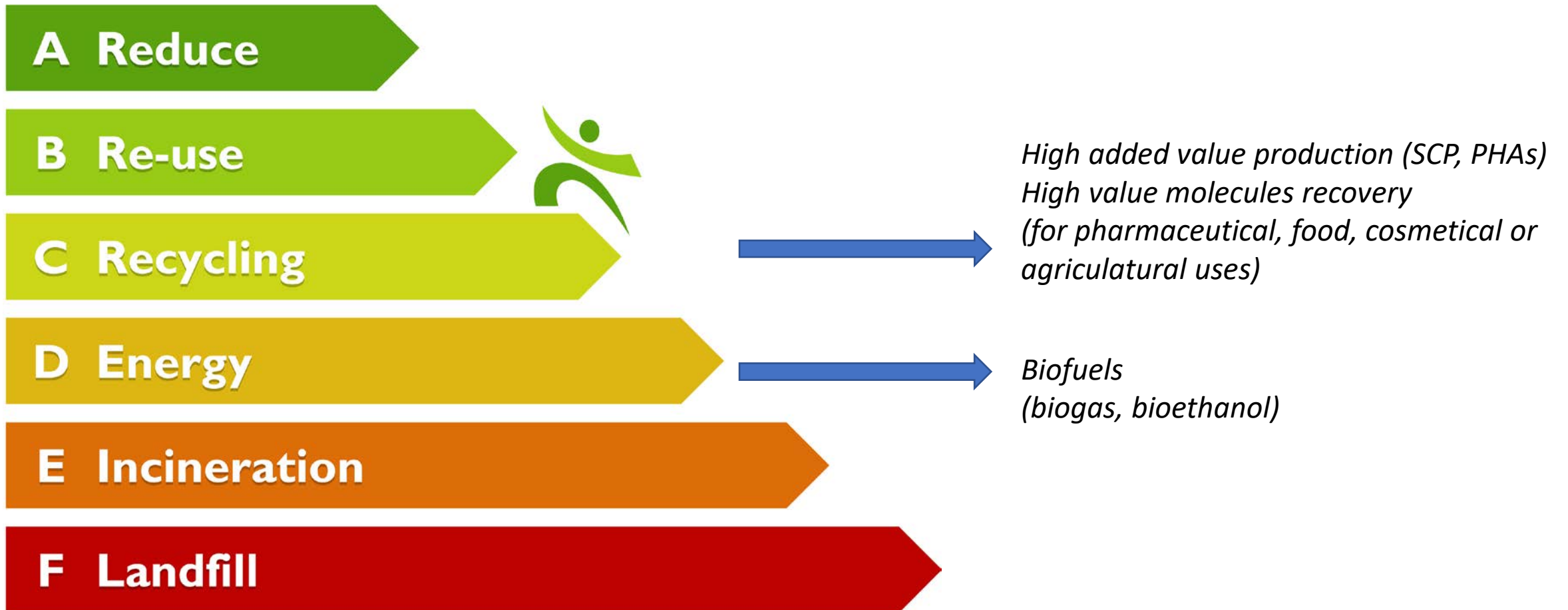
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The Waste Hierarchy approach





Coffee is one of the most appreciated beverage around the world with a global annual consumption of 9.3 Mtons.

Spent Coffee Grounds (SCG), annual amount of 6M tons generated at international level.

Currently SCG are mainly incinerated or simply collected with the Organic Fraction of the Municipal Solid Wastes (OFMSW) and disposed in landfill.

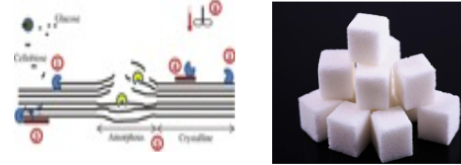




6 Mtons of SCG



Residual solid
fraction



Acid/Enzymatic Hydrolysis for
Fermentable Sugars production



Residual solid
fraction



Biogas by anaerobic
digestion

Coffee oil extraction by Soxhlet



Coffee oil



Transesterification for
biodiesel production

Based on this configuration, SCG will be used for:

- the extraction of **high economic value molecules** (tocopherols, linoleic acid, chlorogenic acid, Cafestol and Kahweol);
- **biodiesel production** by transesterification reactions of the extracted coffee oil ;
- **Sugars production** from the remaining solid matrix of SCG
- **biogas production**

Coffee oil extraction

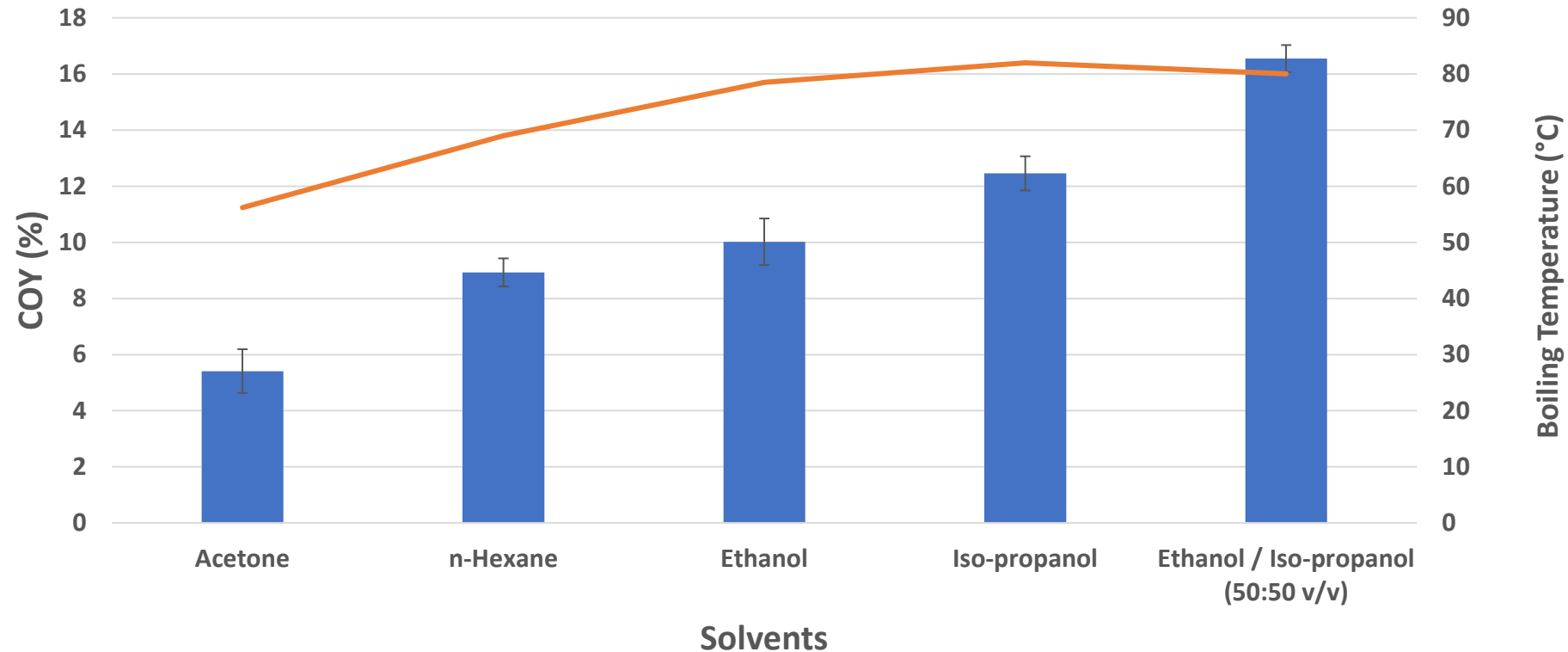
10 g of dried was located in a Soxhlet extractor.
300 mL of polar and no-polar solvents (acetone, ethanol, iso-propanol and n-hexane and a 50:50 (v/v) mixture of the ethanol and iso-propanol, were tested).

All the solvents were tested at 85°C, value higher than boiling temperature of the different solvents



$$\text{COY (\% w/w)} = \frac{M_{oil}}{M_{SCG}} \times 100$$

Coffee oil extraction yield (COY)

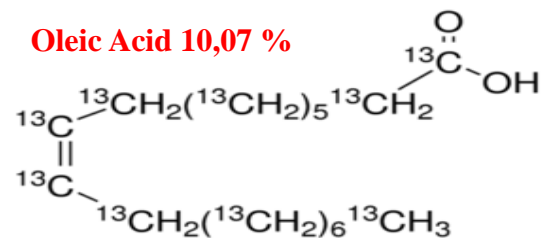
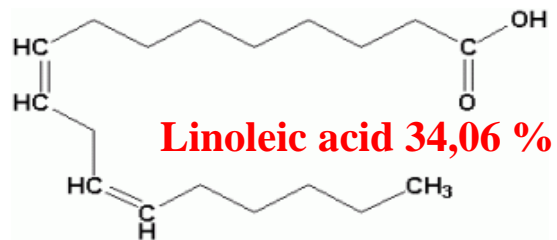
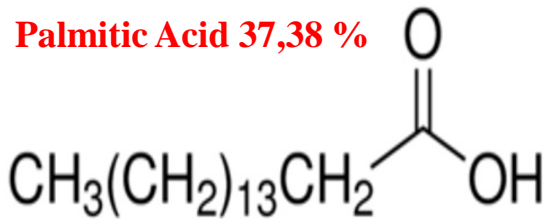


n-hexane is characterized by high value, $K_{ow} = 4.5 \times 10^4$, revealing its hydrophobic nature.

Instead, iso-propanol ($K_{ow} = 0.64$) and ethanol ($K_{ow} = 0.54$) have partition coefficients close to one, which means that these solvents, even if are more hydrophilic, are also able to extract hydrophobic components during Soxhlet extraction

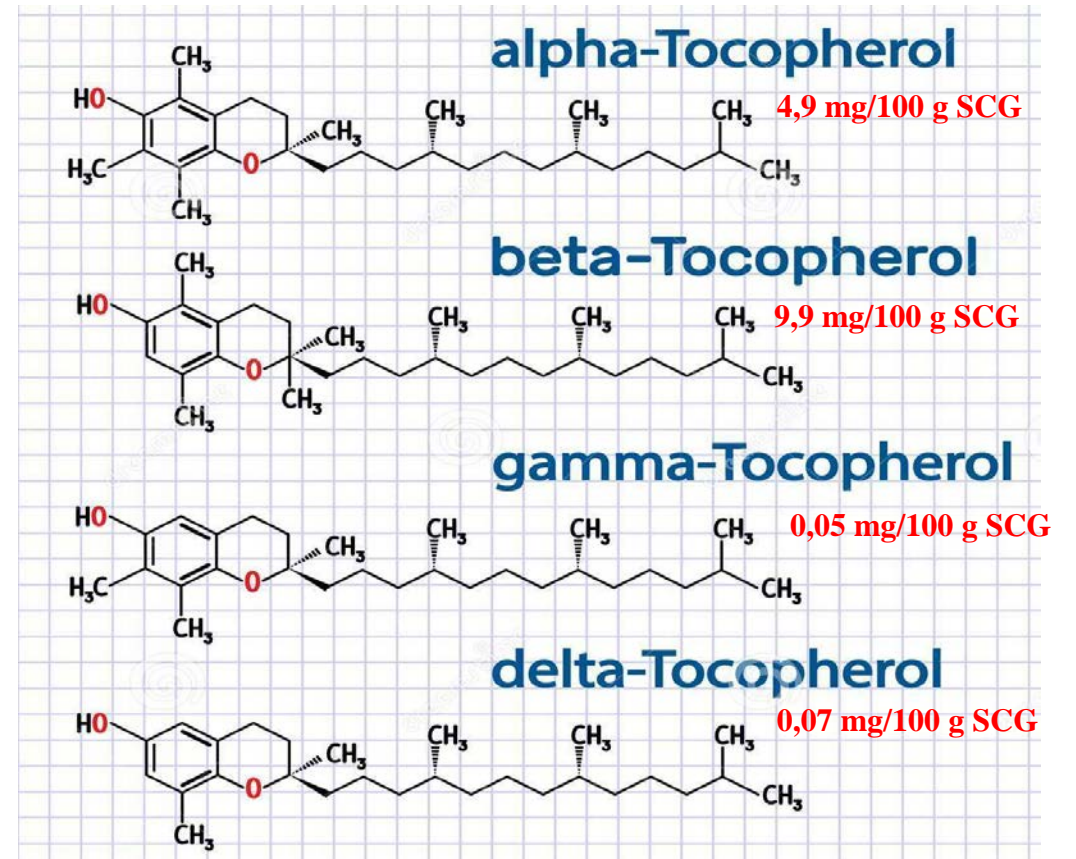
Coffee oil compounds

Fatty Acids

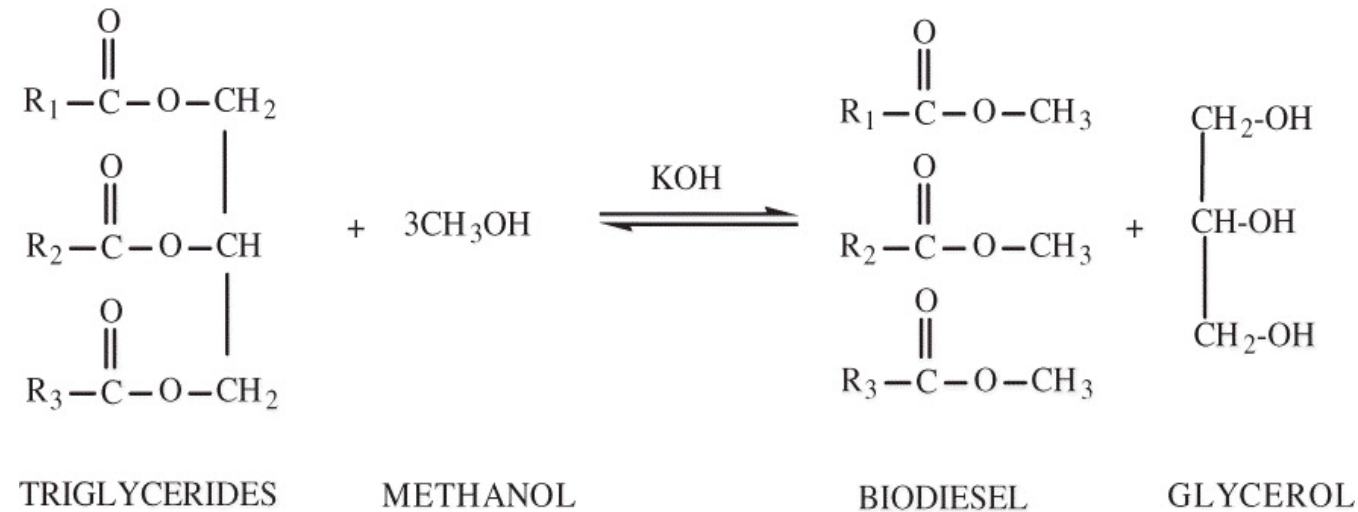


Tocopherols

About 15 mg/100 g SCG
Literature range: 6,5-30 mg/100 SCG



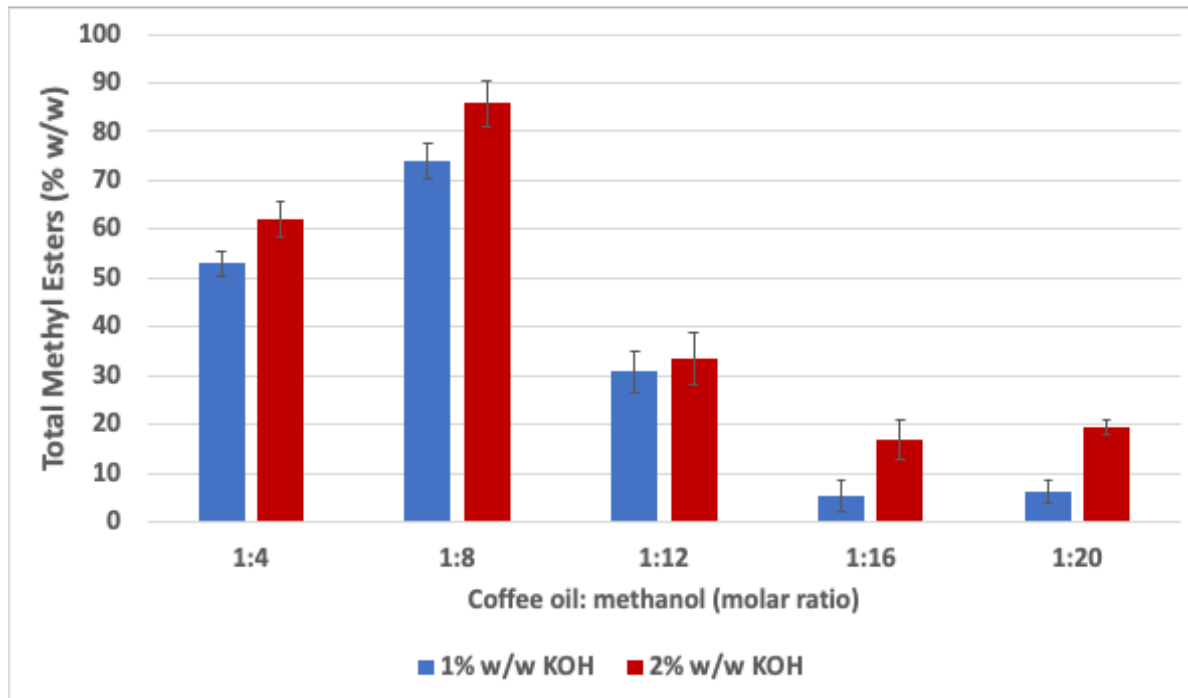
Transesterification of the coffee oil for biodiesel production



Transesterification tests at:

- different molar ratios of coffee oil: methanol of 1:4; 1:8; 1:12; 1:16; 1:20
- Two different potassium hydroxide (KOH) of 1 and 2% w/w, referred to the coffee oils content.

Transesterification of the coffee oil for biodiesel production



Content of Methyl ester from the transesterification of	% w/w
Myristic acid	0.1
Palmitic acid	30.0
Palmitoleic Acid	0.1
Heptadecanoic acid	0.2
Stearic acid	5.8
Oleic acid	8.7
Linoleic acid	37.6
Arachidic acid	1.8
Gadoleic acid	0.2
Behenic acid	0.3

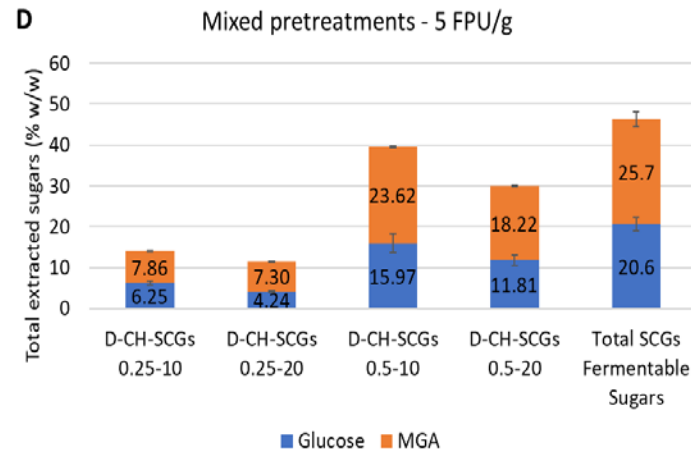
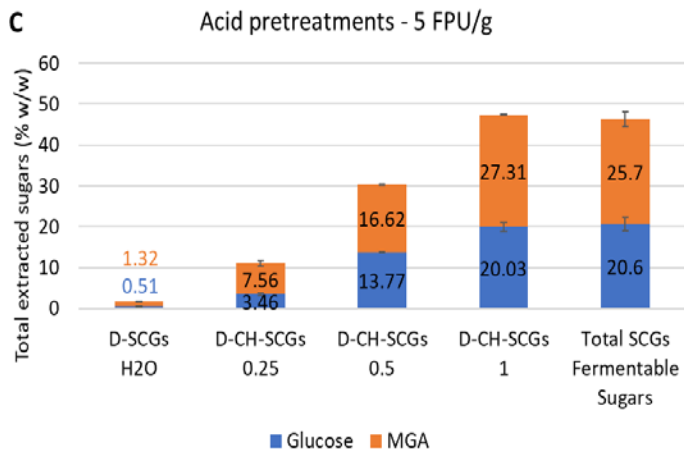
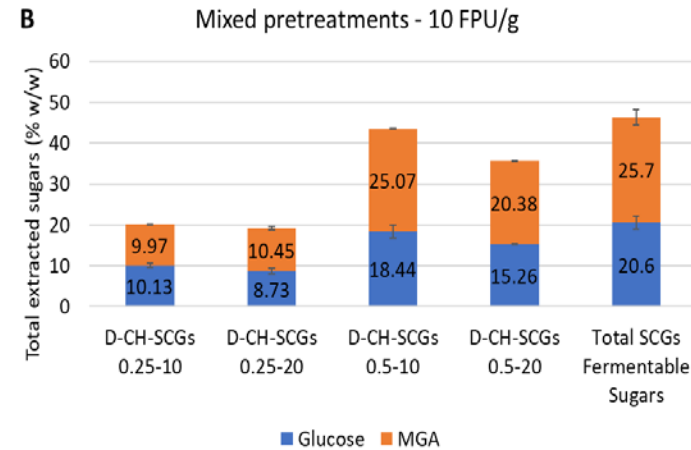
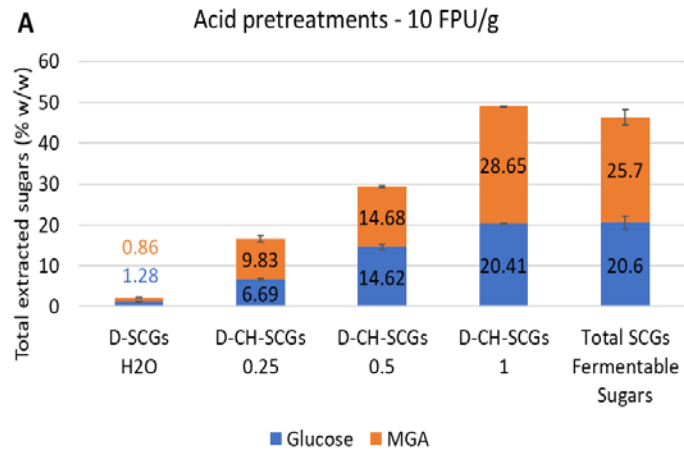


Enzymatic hydrolysis for sugars production

Sample name	H ₂ SO ₄ % (v/v)	Glycerol % (v/v)
D-SCGs-H ₂ O	-	-
D-CH-SCGs-0.25	0.25	-
D-CH-SCGs-0.5	0.50	-
D-CH-SCGs-1	1.00	-
D-CH-SCGs-10	-	10
D-CH-SCGs-20	-	20
D-CH-SCGs-40	-	40
D-CH-SCGs-80	-	80
D-CH-SCGs-0.25-10	0.25	10
D-CH-SCGs-0.25-20	0.25	20
D-CH-SCGs-0.5-10	0.50	10
D-CH-SCGs-0.5-20	0.50	20

After the pretreatment SCG were carried out using the commercial enzyme cocktail Cellic CTec 2 (Novozymes). Enzyme activity, expressed as filter paper units (FPU), was set at 5 and 10 FPU/g_{SCG}, while the TS concentration was of 15% w/v.

Enzymatic hydrolysis for sugars production



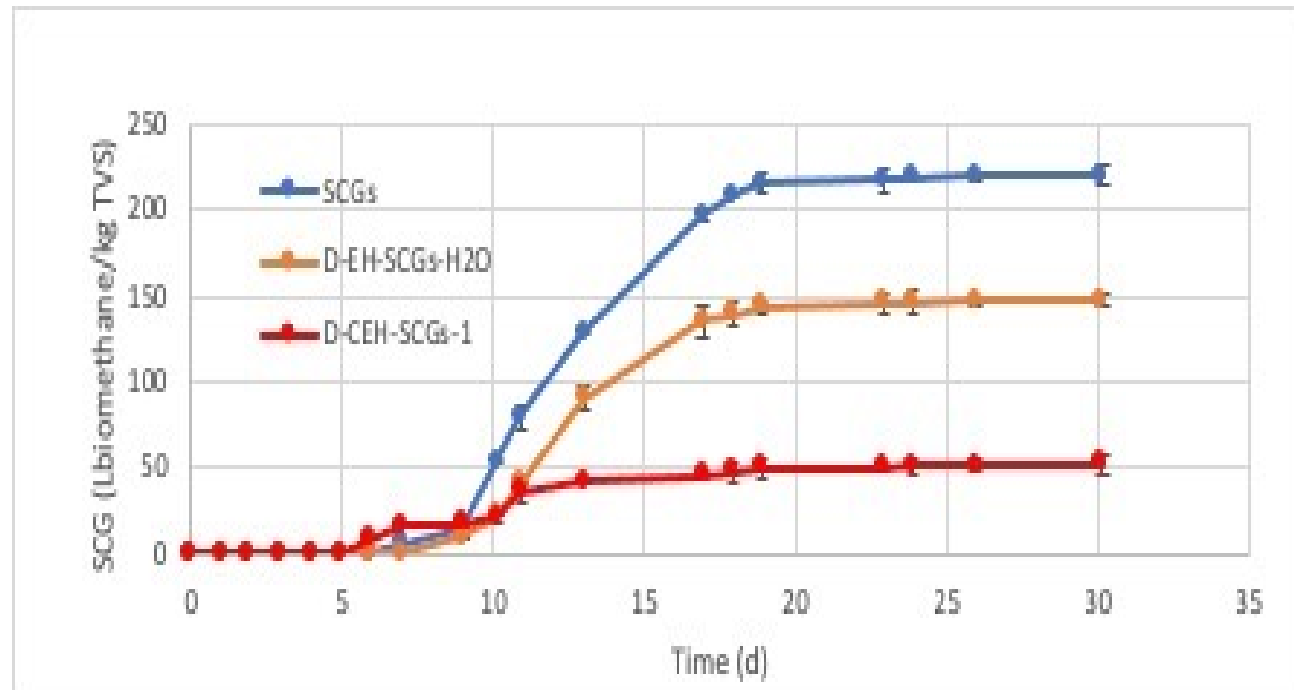
- 5 FPU/g_{SCG} allowed to have the same sugars productions than 10 FPU/g_{SCG};
- Glycerol, the by-product from biodiesel production, had a good effect on the pretreatment allowing the reduction sulfuric acid concentration.
- **The better fermentable sugars content was around 40-45% w/w**

Biogas production from the solid fraction

The remaining solid fraction of SCG, after enzymatic saccharification, was performed for the biogas production by AD in mesophilic conditions.



Biogas production from the solid fraction





Thank you for
the attention



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