THESSALONIKI 2021

8th International Conference on Sustainable Solid Waste Management Thessaloniki, Greece, 23-26 JUNE 2021



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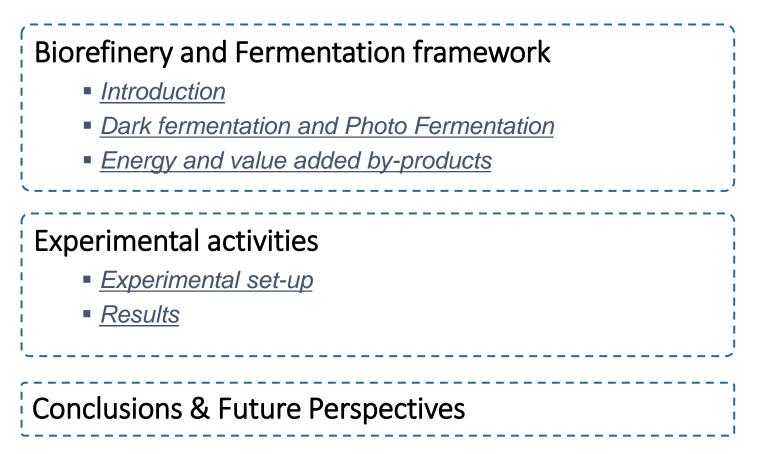


Fermentative hydrogen and PHAs production by microbial community selection and enrichment via bioaugmentation

Grazia Policastro, University of Naples Federico //

Thessaloniki (Greece), June 23-26, 2021

Outlines





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INTRODUCTION

What is a biorefining system

Biorefining is the sustainable processing of biomass into a spectrum of bio-based products (food, feed, chemicals, materials) and bioenergy (biofuels, power and/or heat)... facility that integrates biomass conversion processes and equipment to produce fuels, power, heat, and value-added chemicals from biomass.



- Anaerobic processes?
 - Costs (O₂ not used as electron acceptor)
 - Energy/Value-added chemicals
 - GHG emission mitigation



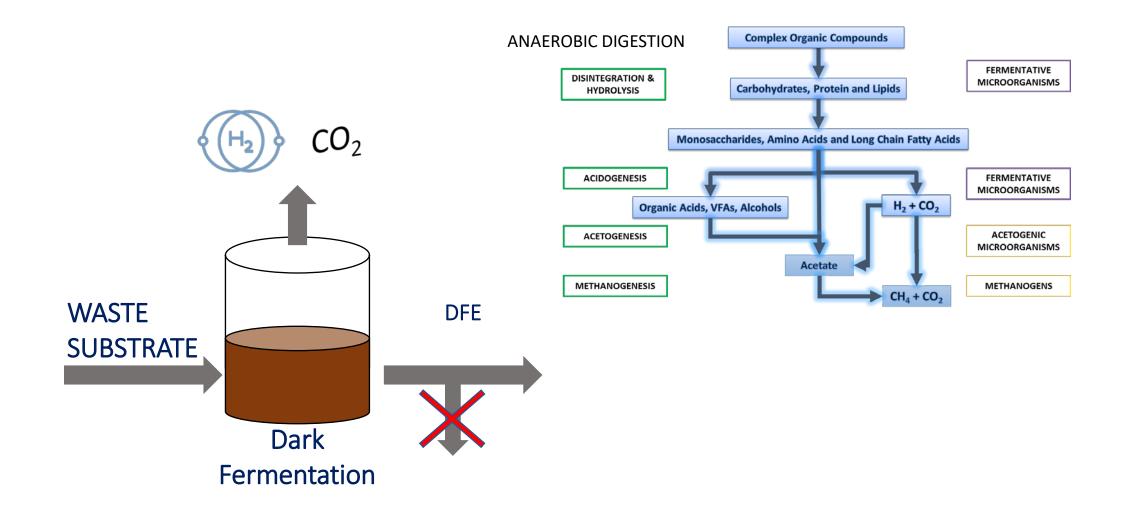


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DARK AND PHOTO FERMENTATION



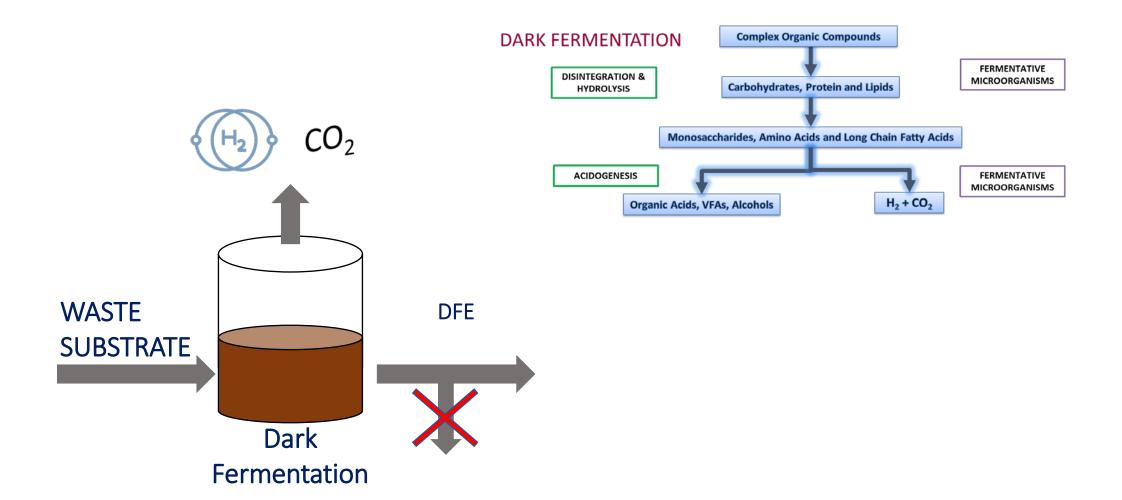


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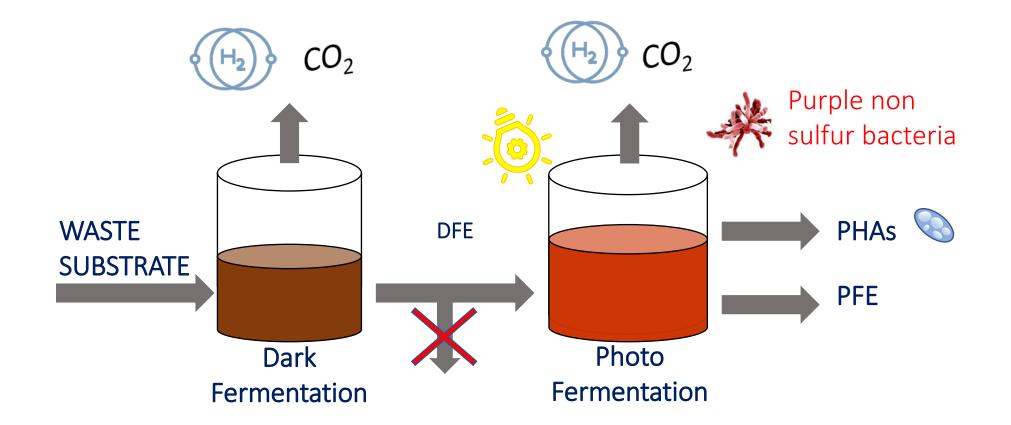


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DARK AND PHOTO FERMENTATION





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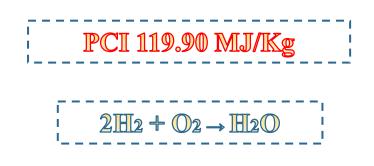
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ENERGY AND VALUE ADDED BY-PRODUCTS

H₂ production





- Efficiency conversion in internal combustion engines 50-60%
- Efficiency conversion (fossil fuels) ~25%



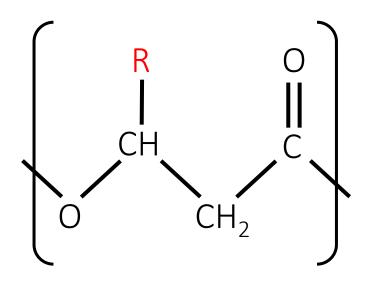
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ENERGY AND VALUE ADDED BY-PRODUCTS

Polyhydroxyalacanoates





3-hydroxyalcanoate

R alcaly group



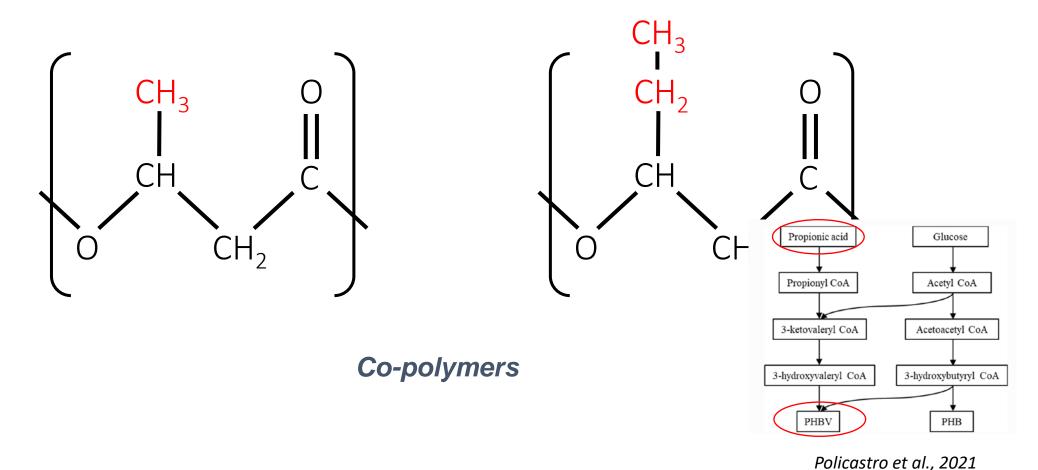
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ENERGY AND VALUE ADDED BY-PRODUCTS

Polyhydroxyalacanoates



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EXPERIMENTAL SET-UP

Aims

Hydrogen and PHAs production via two stage Dark and Photo Fermentation

Propionic acid production via Dark Fermentation

Microbial community enrichment



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EXPERIMENTAL SET-UP



| | CHEESE WHEY | INOCULUM |
|-----------------------|-------------|----------|
| Total Solids [g/L] | 64,29 | 4,67 |
| Volatile Solids [g/L] | 60,23 | 2,79 |
| COD [g/L] | 89,28 | 26,87 |
| Carbohydrates [g/L] | 39,08 | |
| Proteins [g/L] | 15,80 | |
| Lipids [g/L] | 4,12 | |



➢ COD 50-102 mg/L

➤ 180-190×10⁶ t/YEAR

 \succ Only the 50% is used for

further processes!



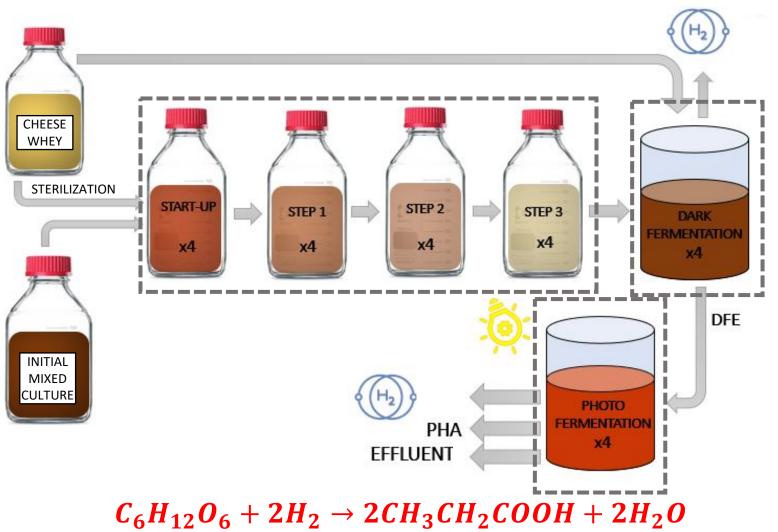


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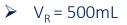
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EXPERIMENTAL SET-UP

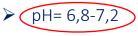


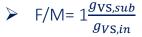
DF OPERATIONAL PARAMETERS:



 \succ V_w = 400mL







PF OPERATIONAL PARAMETERS:

➤ T= 23±2°C

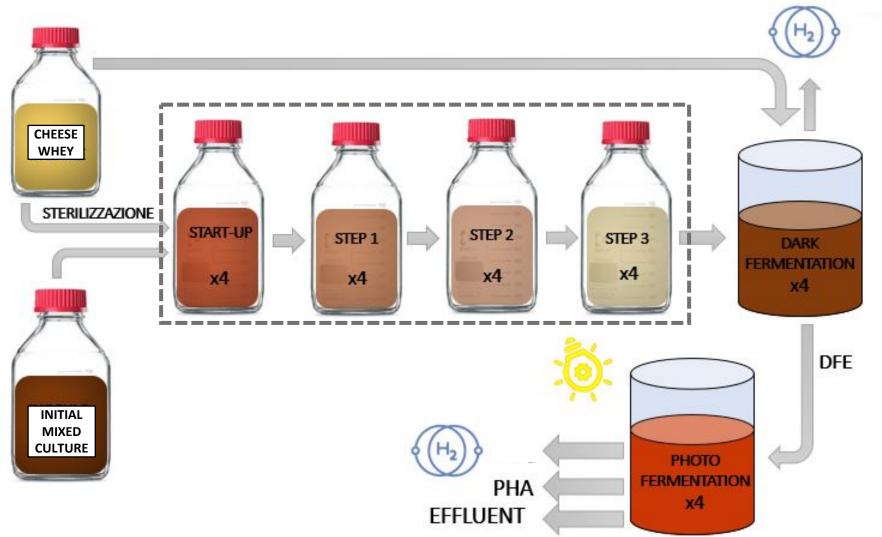
- Agitation= 250 rpm
- ➤ I= 3000 lux
- \succ CODIN= 1 $\frac{g_{\text{COD}}}{L}$

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RESULTS: Bioaugmentation cycle



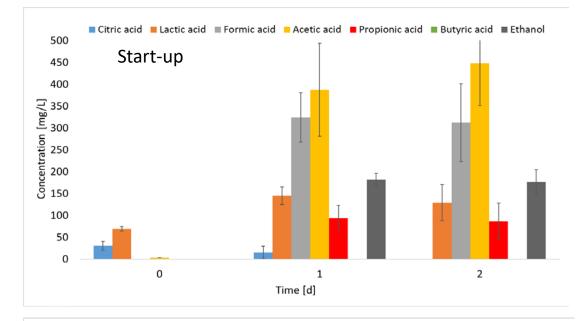


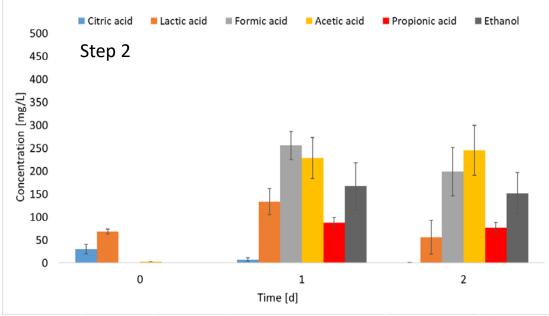
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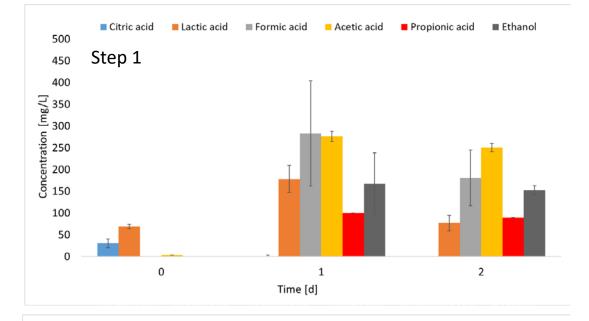
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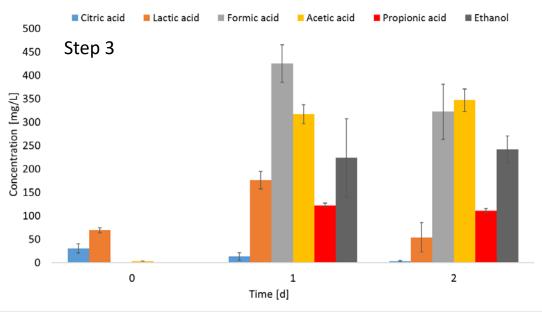
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RESULTS: Bioaugmentation cycle

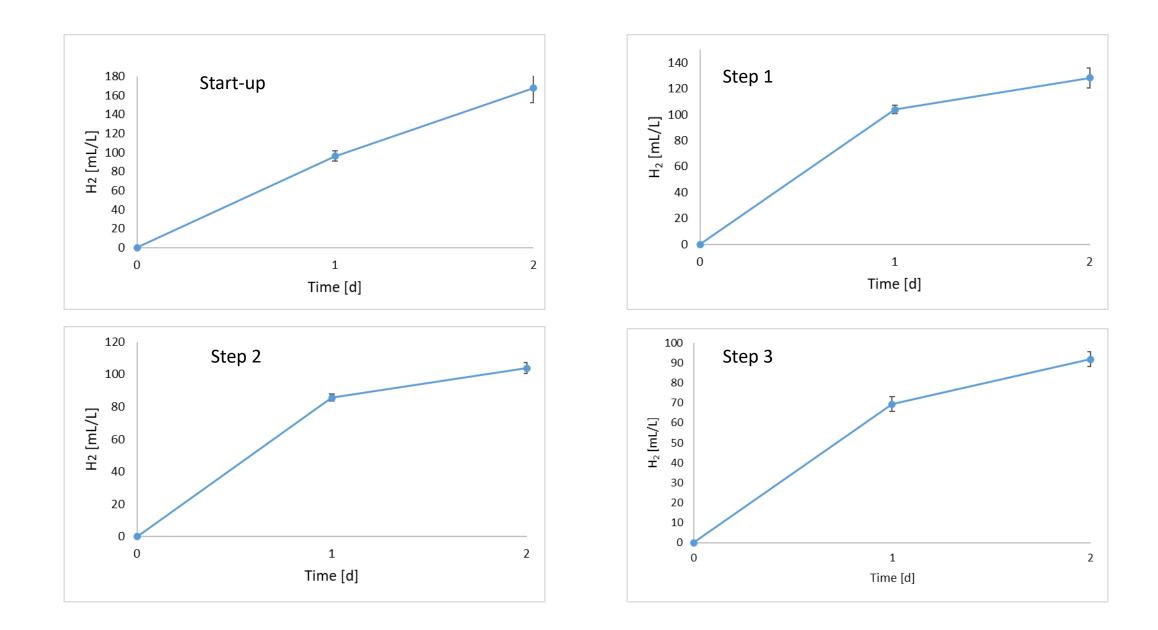


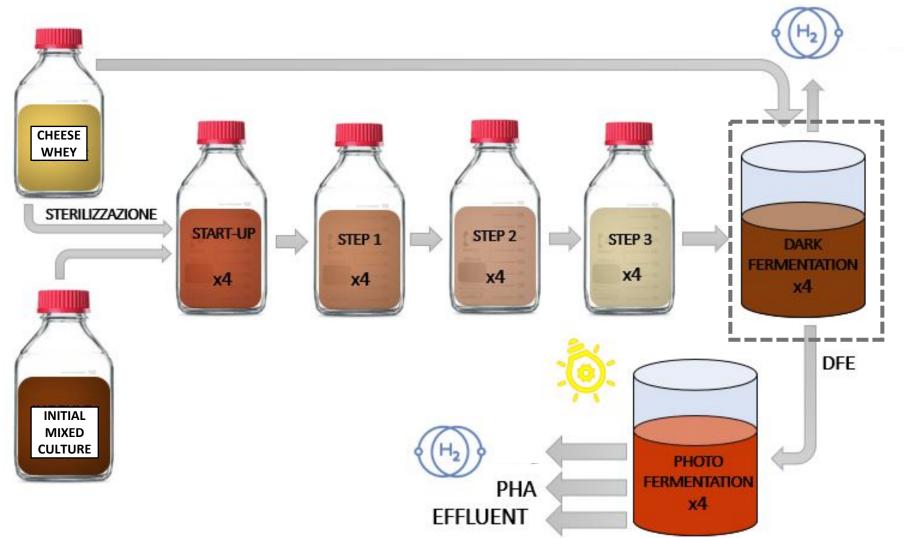






RESULTS: Bioaugmentation cycle







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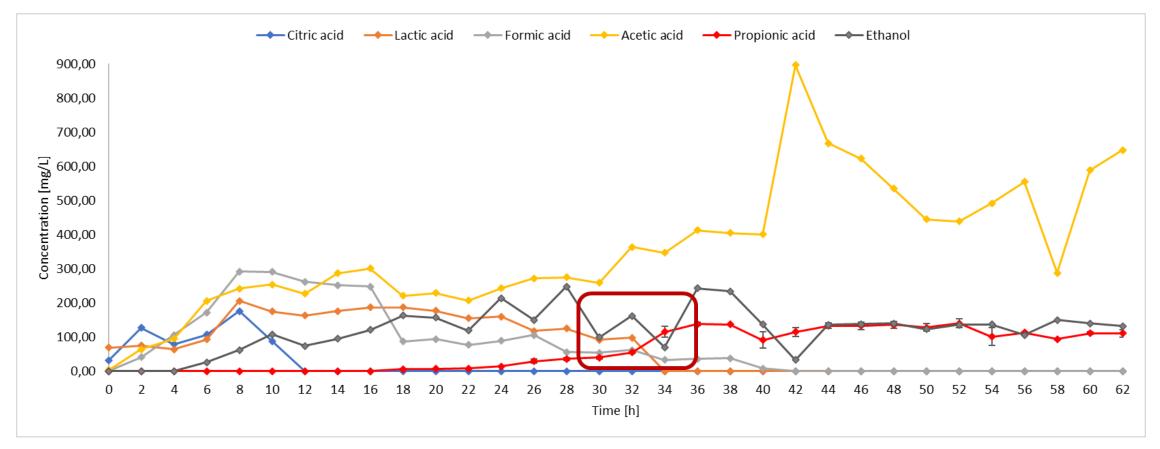
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← Citric acid ← Lactic acid ---- Formic acid ---- Acetic acid Propionic acid 900,00 800,00 700,00 Concentration [mg/l] 200,000 200,000 300,000 200,00 100,00 0,00 Time [h]

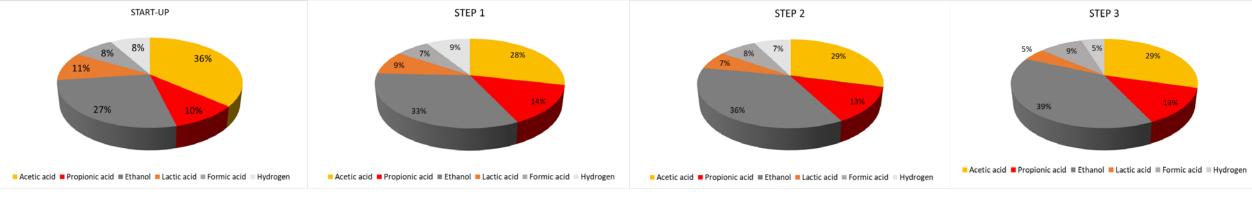
Hydrogen availability

Hydrogen limiting conditions



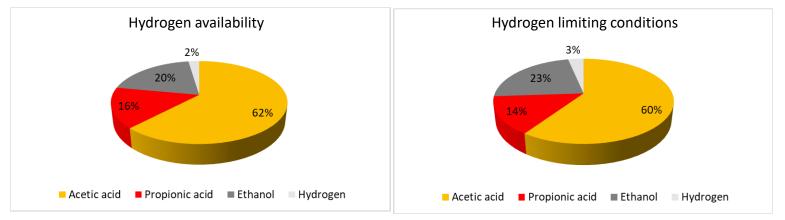


 $3CH_3CHOHCOOH \rightarrow 2CH_3CH_2COOH + CH_3COOH + CO_2 + H_2O$



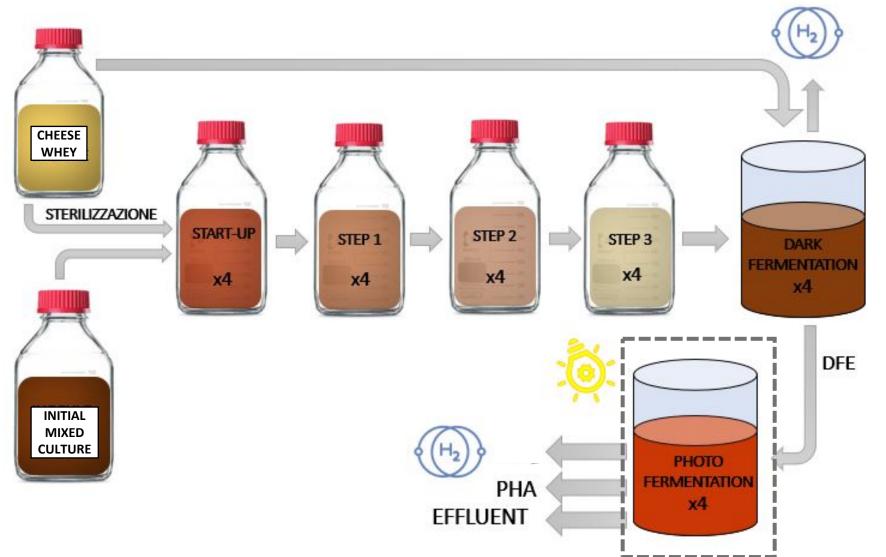
Bioaugmentation cycle

Final Dark Fermentation



Optimal propionic acid range for high performance PHAs production: **10-30%** *Kim et al., 1994*

RESULTS: Photo Fermentation



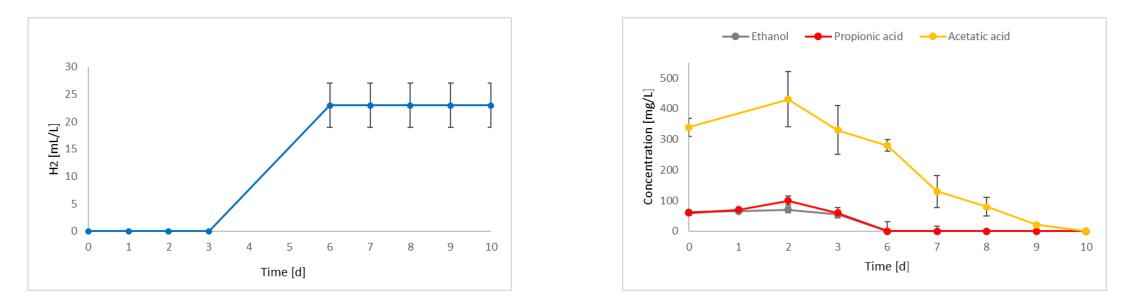


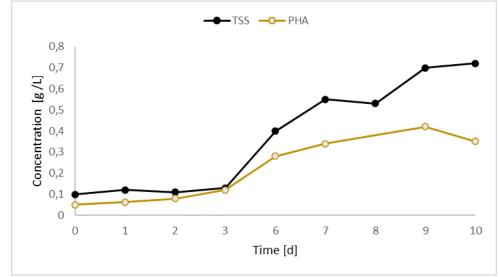
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RESULTS: Photo Fermentation





CONCLUSIONS

DF of cheese whey was effective for the production of DFEs containing propionic acid.

Mixed cultures were effective both for the DF stage and the PF one.

PHAs production was satisfactory



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FUTURE PERSPECTIVES

➢ Further enhancement of the propionic acid percentage $3CH_3CHOHCOOH → 2CH_3CH_2COOH + CH_3COH + CO_2 + H_2O$

> Analysis of the PHA structure and properties

> Analysis of microbial communities



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