

Ammonia as a carrier for hydrogen production by using Perovskites

M. Pinzón*, P. Sánchez, A. de Lucas-Consuegra, A.R. de la Osa, A. Romero

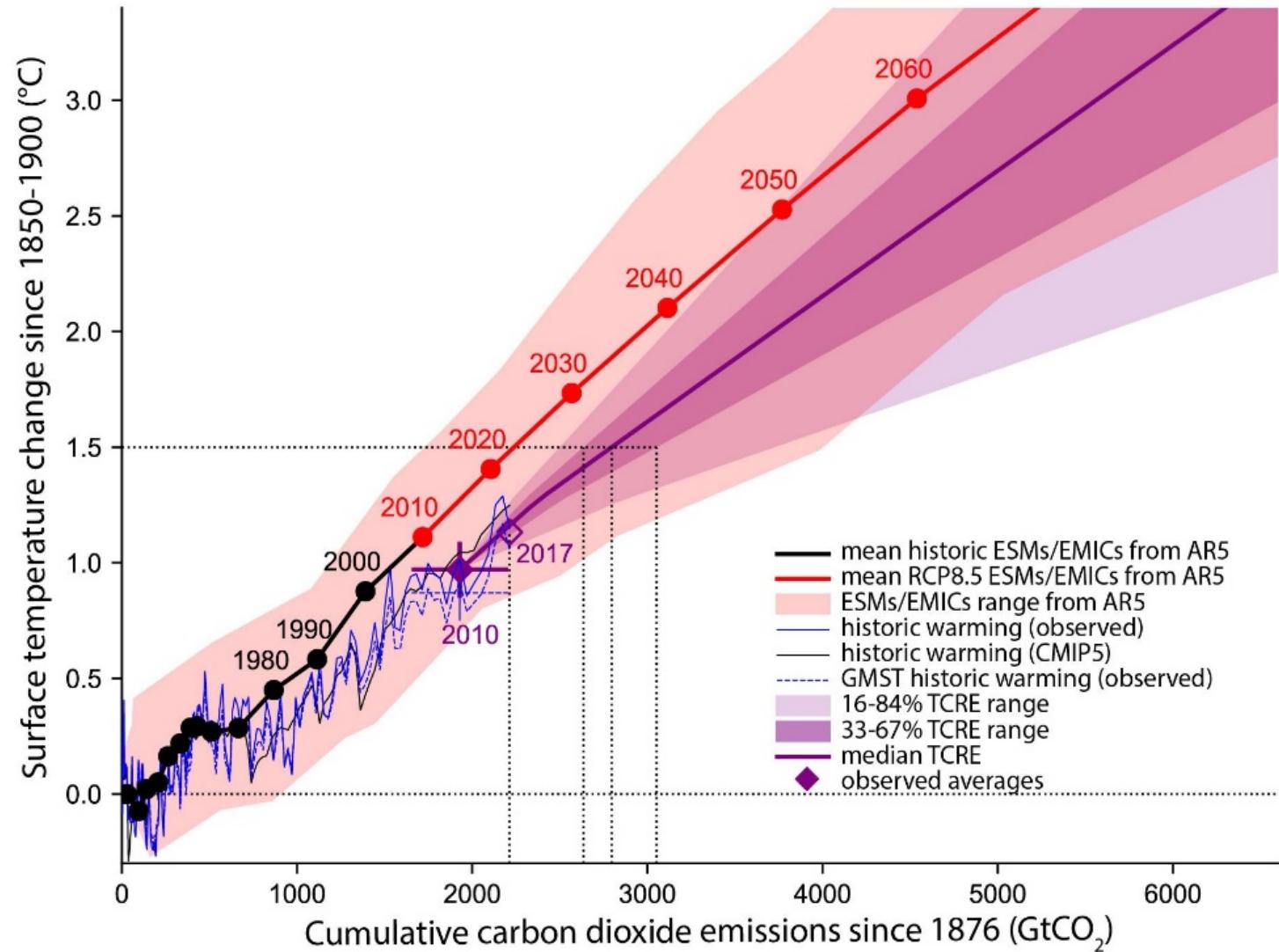
Department of Chemical Engineering, University of Castilla-La Mancha, Ciudad Real (Spain)

*Marina.PGarcia@uclm.es

8TH INTERNATIONAL CONFERENCE
ON SUSTAINABLE SOLID WASTE MANAGEMENT

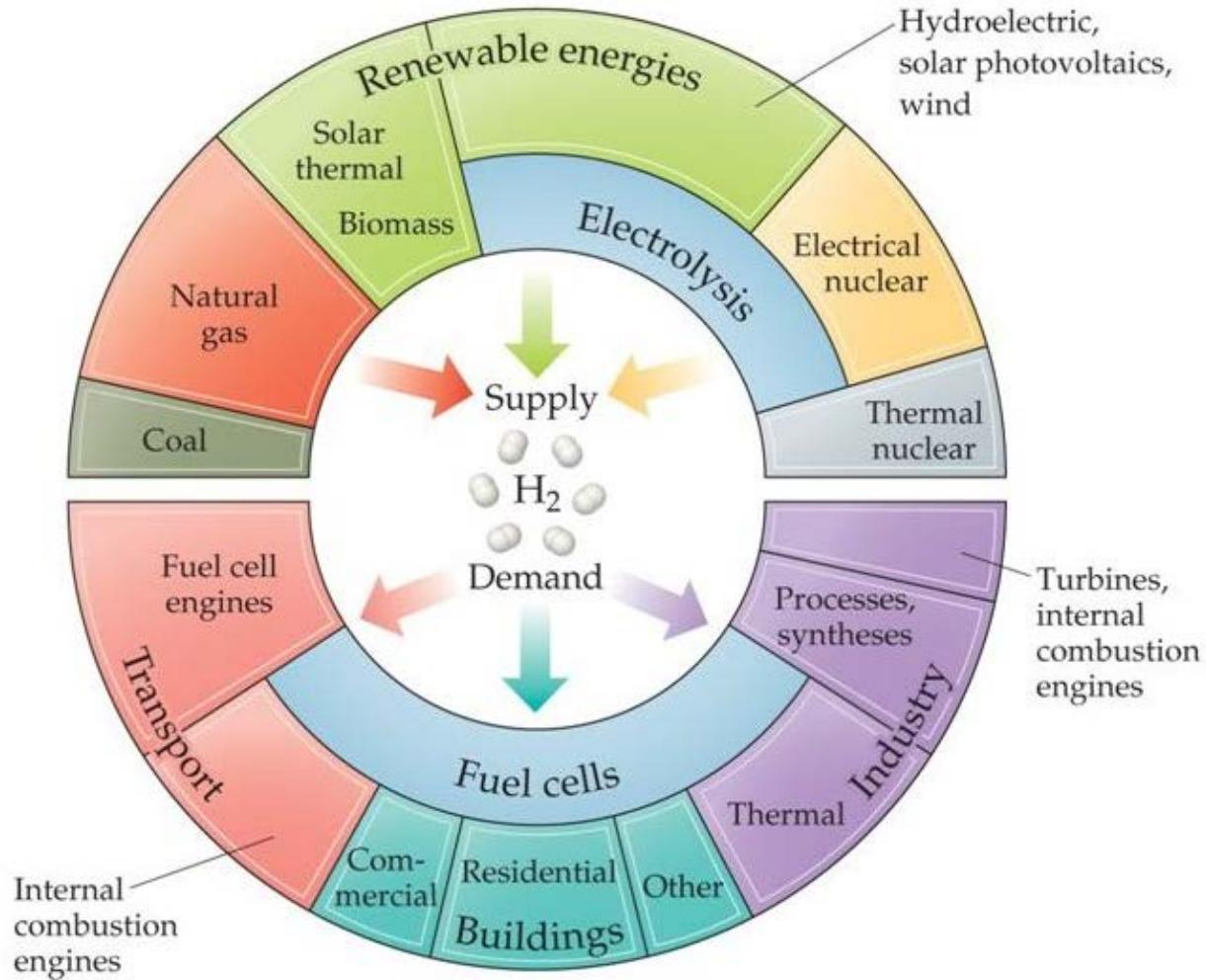
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Environmental issues





Hydrogen economy



Production from
renewable energy
sources



Clean, sustainable
and renewable
energy carrier



Storage and
transport issues



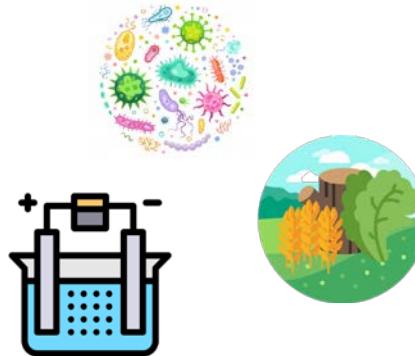
Hydrogen economy

- Thermochemical process
- CO_x emissions

Grey and blue H₂

Green H₂

- Water electrolysis
- From biomass





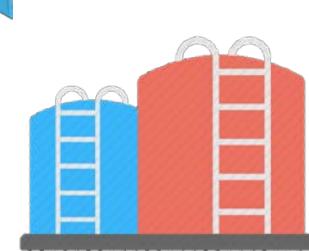
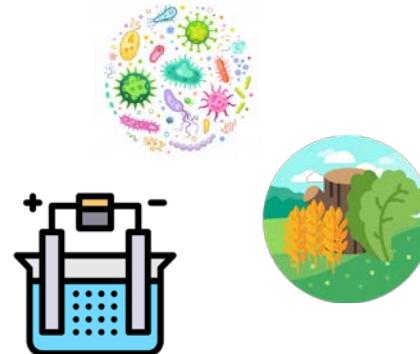
Hydrogen economy

- Thermochemical process
- CO_x emissions

Grey and blue H₂

Green H₂

- Water electrolysis
- From biomass

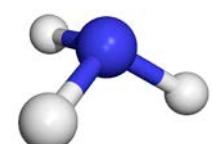


- Liquid (low temperatures) or compressed (high pressure)

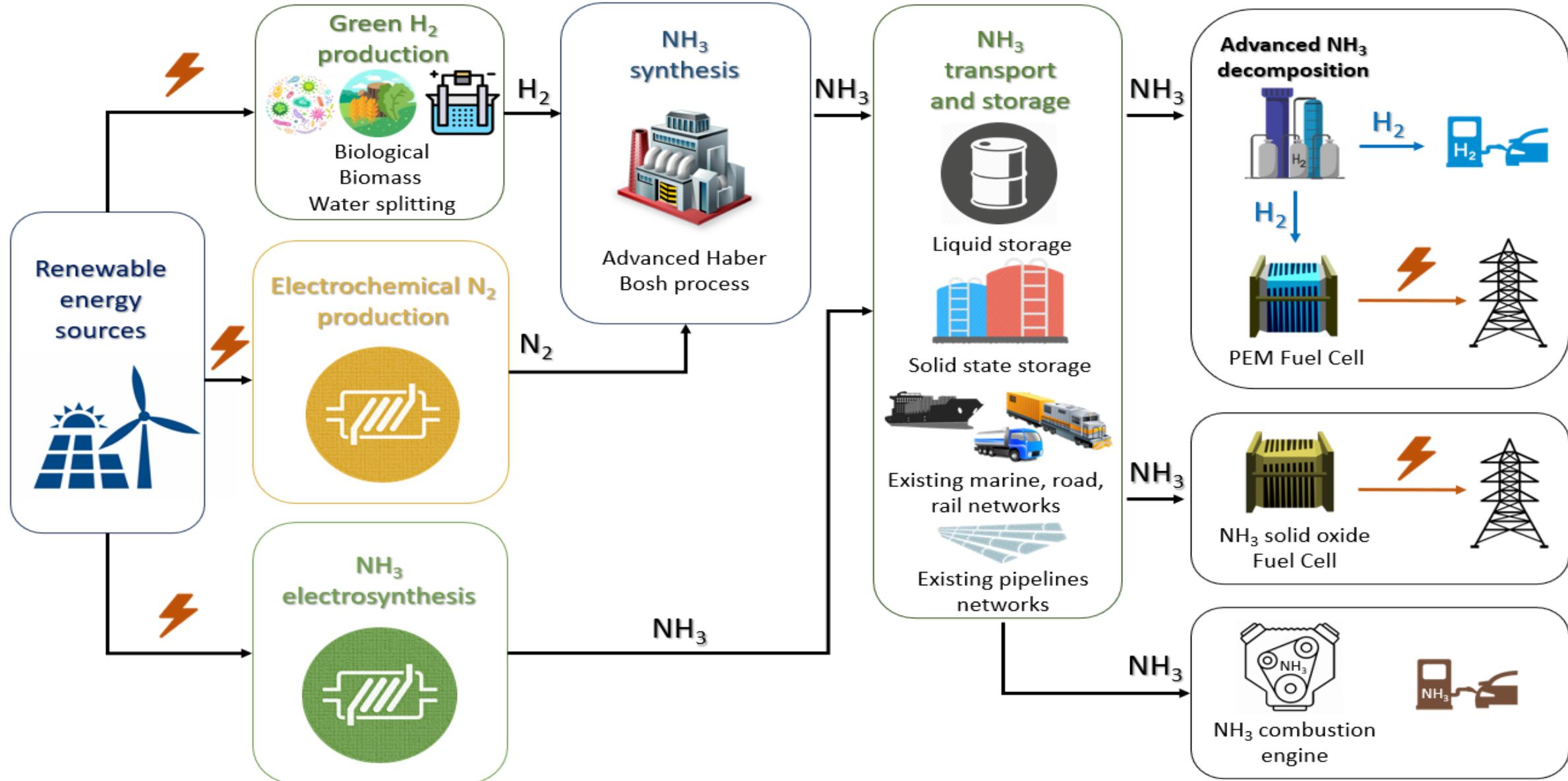
Conventional transport

Modern transport

- Adsorption
- H₂-rich molecules



👍 NH₃ as hydrogen carrier

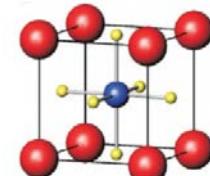


Perovskite-type
oxides (LaBO_3) by
the self-
combustion
method

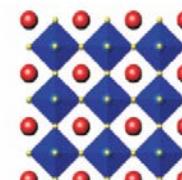
Self-combustion method



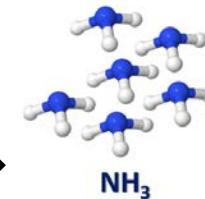
Perovskites
(LaNiO_3 and LaCoO_3)



● A^{2+}
● B^{4+}
● O^{2-}

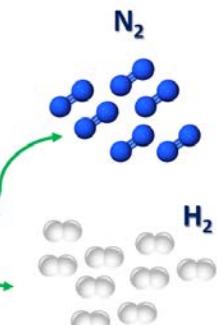


Reduction



$\text{Ni/La}_2\text{O}_3$
 $\text{Co/La}_2\text{O}_3$

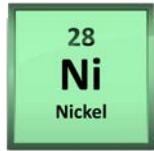
Catalyst



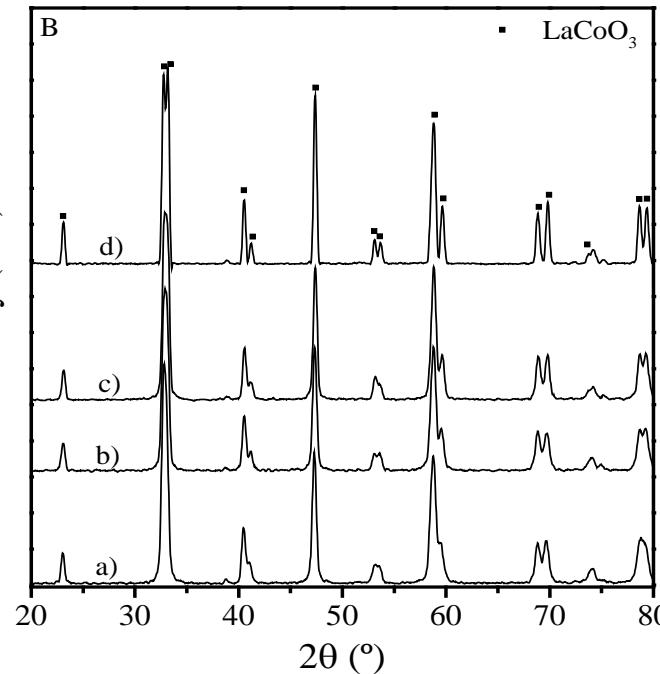
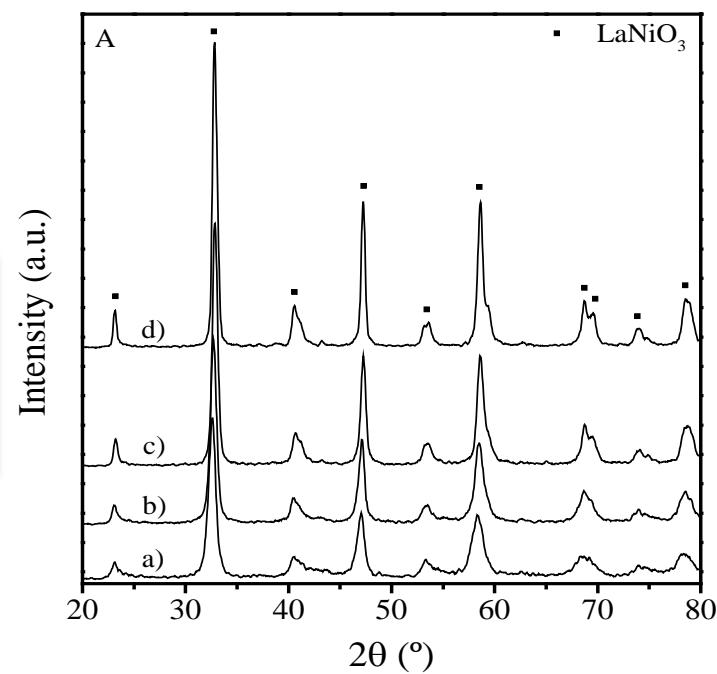
Perovskite-type
oxides (LaBO_3) by
the self-
combustion
method

Influence of
metal (Ni or Co)

Influence of
calcination
temperature



Rhombohedral
 LaNiO_3
(R-3m, 33-0711)

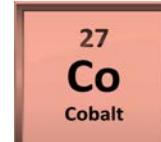
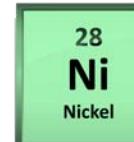


XRD pattern of A) LaNiO_3 y B) LaCoO_3 perovskites calcined at
a) 650, b) 700, c) 750 and d) 900 °C

Perovskite-type oxides (LaBO_3) by the self-combustion method

Influence of metal (Ni or Co)

Influence of calcination temperature

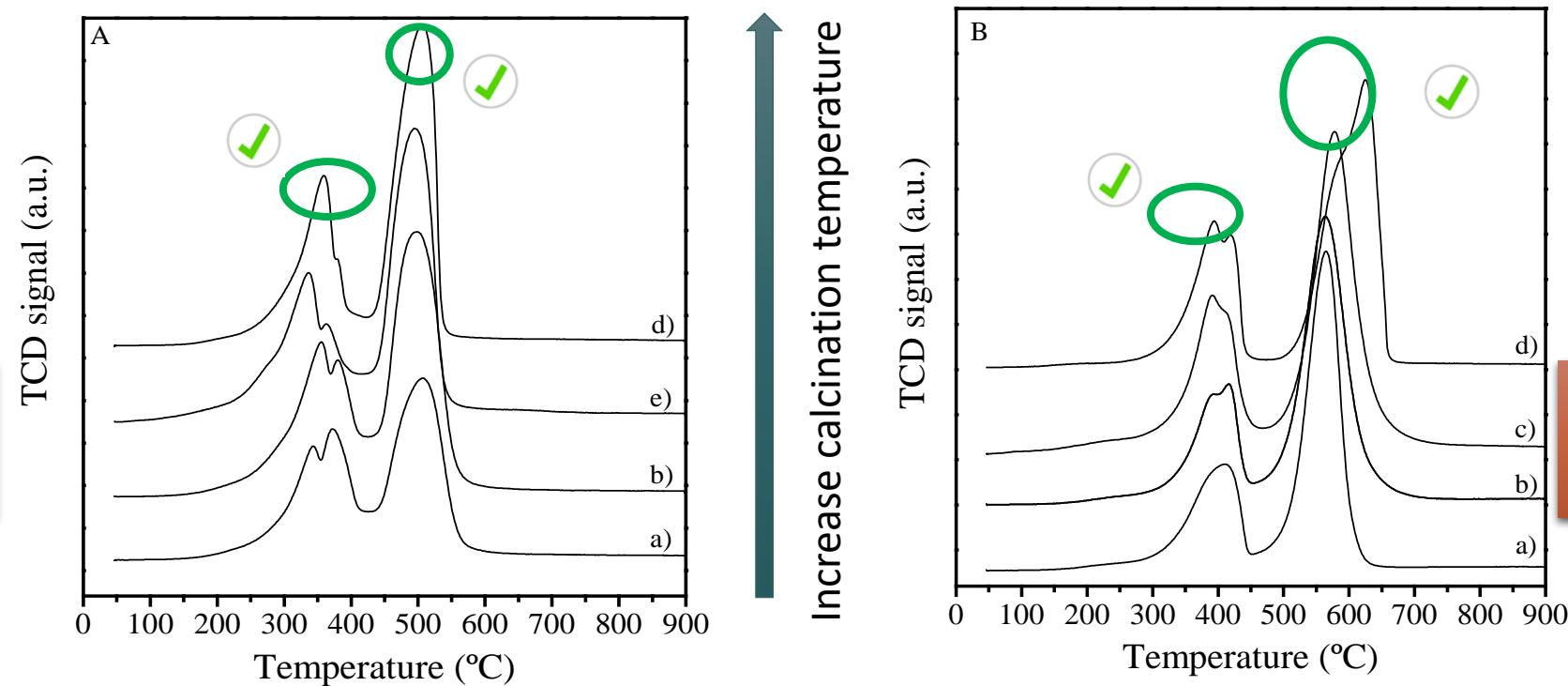
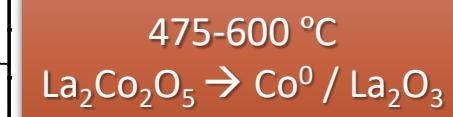
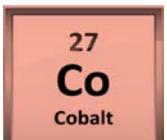
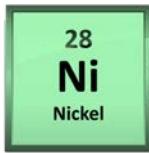


<i>Calcination temperature (°C)</i>	LaNiO_3			LaCoO_3		
	<i>Crystal size (nm) (2θ=47.4°)</i>	S_{BET} ($\text{m}^2 \cdot \text{g}^{-1}$)	V_p ($\text{cm}^3 \cdot \text{g}^{-1}$)	<i>Crystal size (nm) (2θ=47.5°)</i>	S_{BET} ($\text{m}^2 \cdot \text{g}^{-1}$)	V_p ($\text{cm}^3 \cdot \text{g}^{-1}$)
650	11.3	11.1	0.062	26.1	10.3	0.059
700	14.4	9.7	0.059	25.1	13.4	0.094
750	16.8	7.8	0.057	28.7	13.2	0.077
900	23.8	3.2	0.025	40.7	3.5	0.012

Perovskite-type
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Influence of
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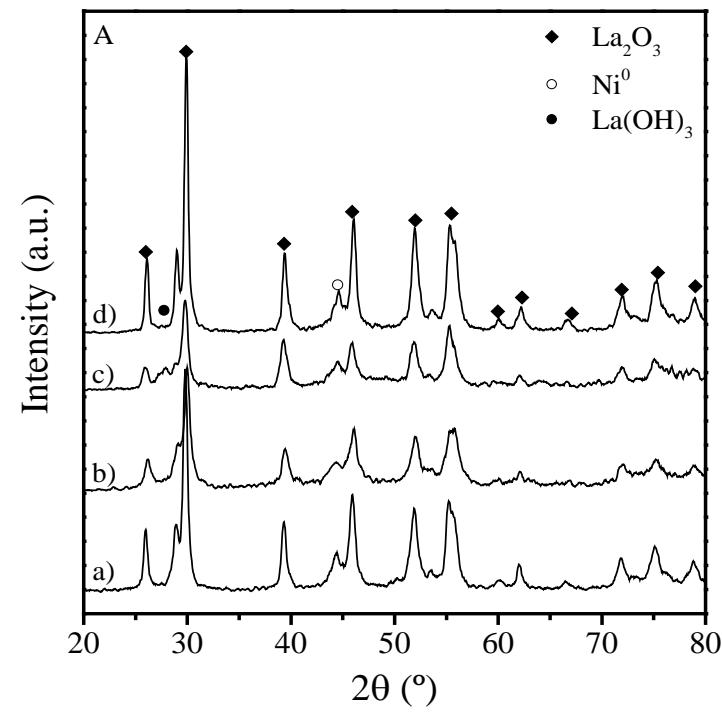
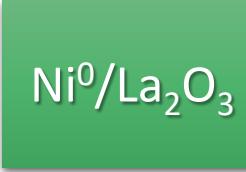
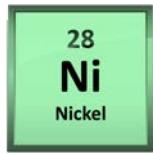


H₂-TPR profiles of A) LaNiO₃ y B) LaCoO₃ perovskites calcined
at a) 650, b) 700, c) 750 and d) 900 °C

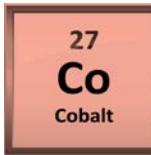
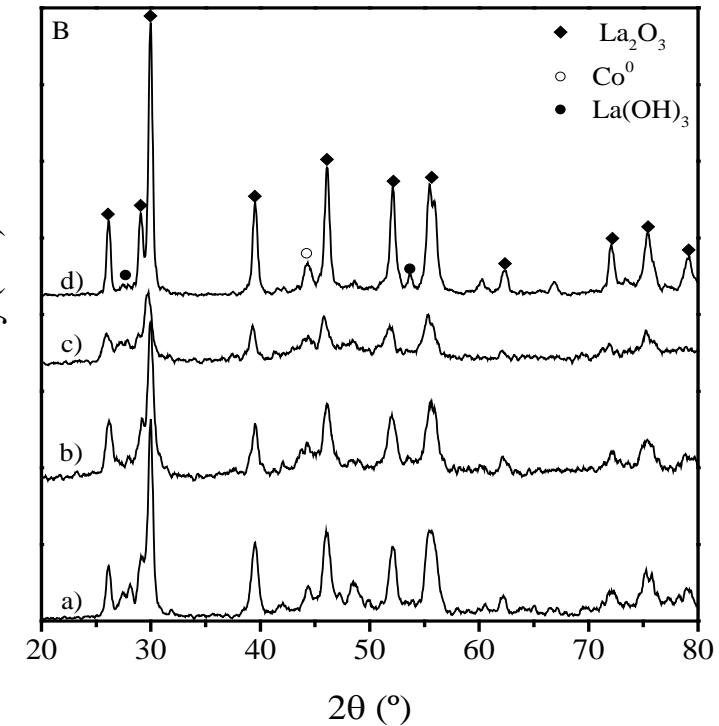
Perovskite-type
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Influence of
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Influence of
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Increase calcination temperature

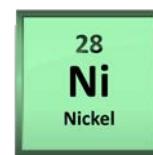


XRD pattern of A) LaNiO_3 and B) LaCoO_3 perovskites calcined at **a) 650, b) 700, c) 750 and d) 900 °C** and reduced at 550 °C and 600 °C, respectively.

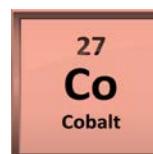
Perovskite-type oxides (LaBO_3) by the self-combustion method

Influence of metal (Ni or Co)

Influence of calcination temperature



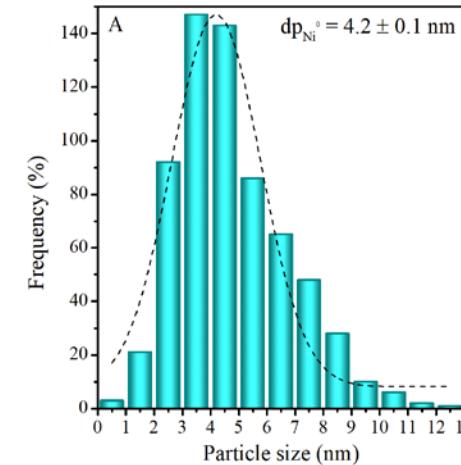
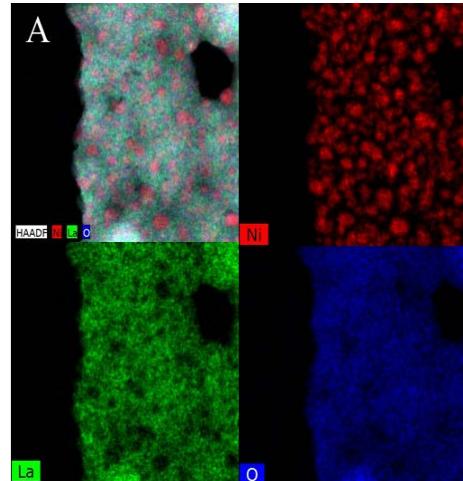
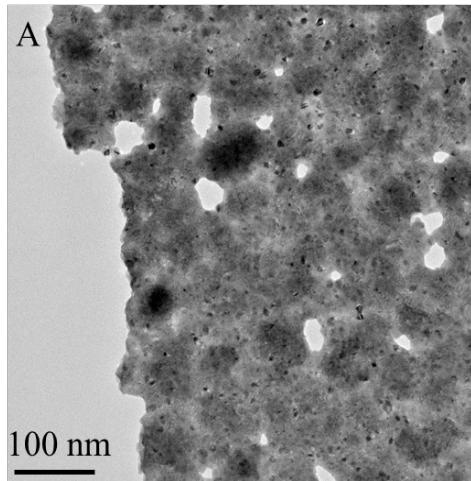
Samples	Crystal size (nm)		
	La_2O_3 ($2\theta = 29.9^\circ$)	Ni^0 ($2\theta = 44.5^\circ$)	Co^0 ($2\theta = 44.3^\circ$)
LaNiO_3 650 °C	15.6	5.5	-
LaNiO_3 700 °C	14.4	8.1	-
LaNiO_3 750 °C	14.0	9.7	-
LaNiO_3 900 °C	22.6	10.7	-
LaCoO_3 650 °C	22.5	-	9.8
LaCoO_3 700 °C	18.9	-	8.5
LaCoO_3 750 °C	11.1	-	9.0
LaCoO_3 900 °C	23.3	-	11.9



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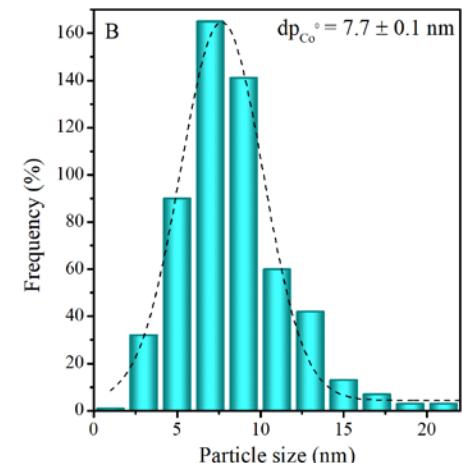
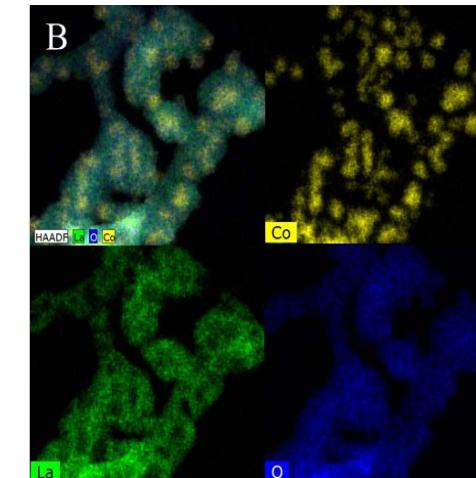
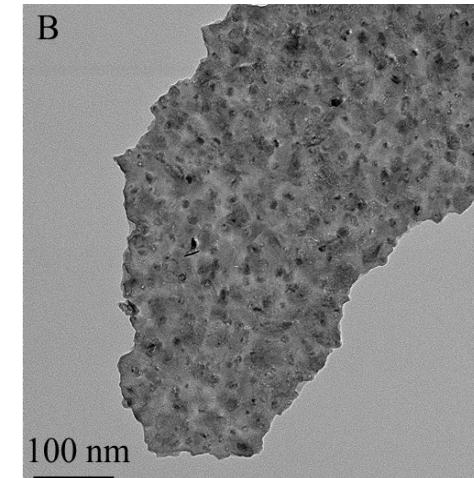
Influence of
calcination
temperature



$\text{Ni}^0/\text{La}_2\text{O}_3$

Lower particles size (4.2 nm)

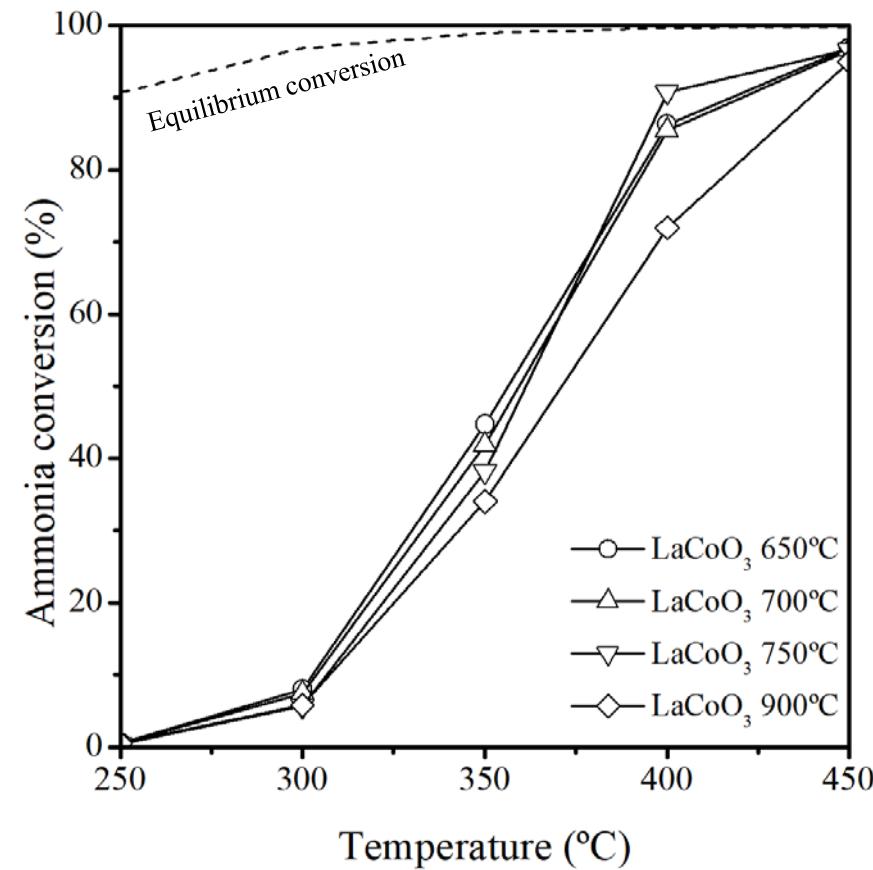
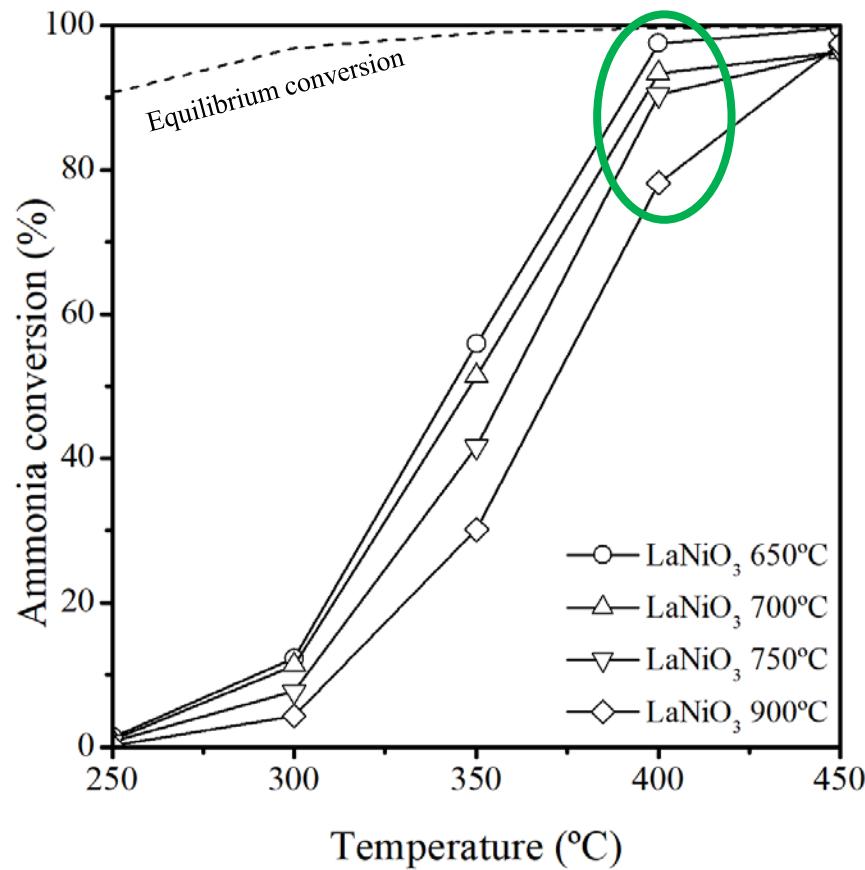
$\text{Co}^0/\text{La}_2\text{O}_3$



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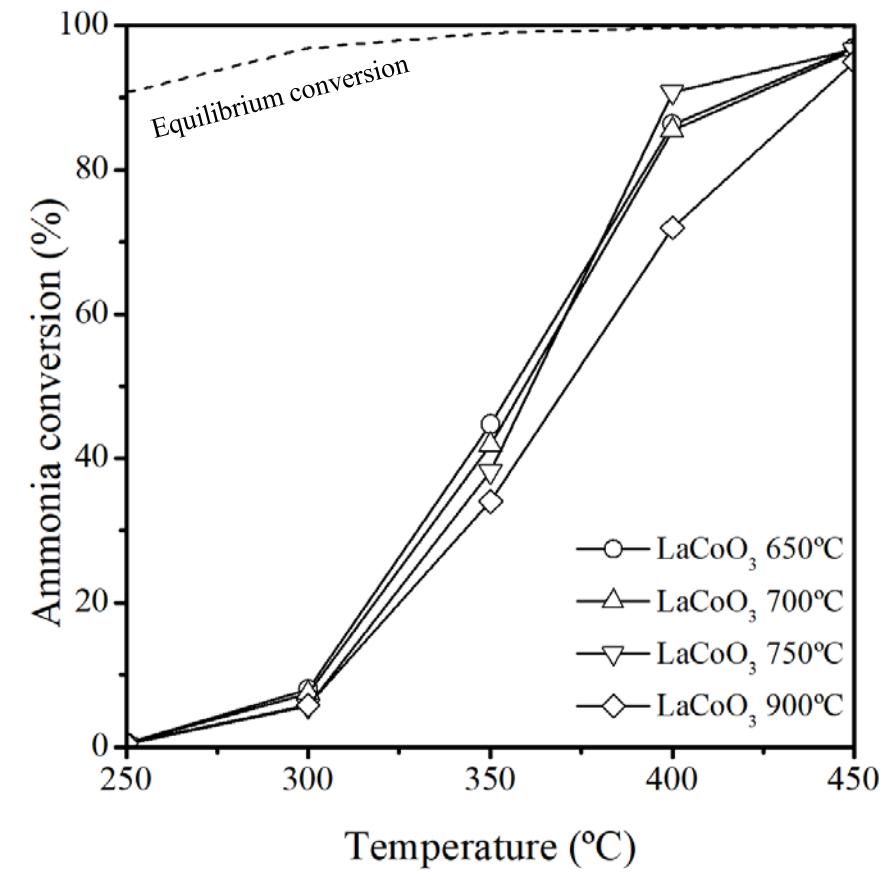
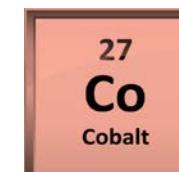
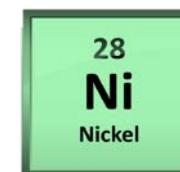
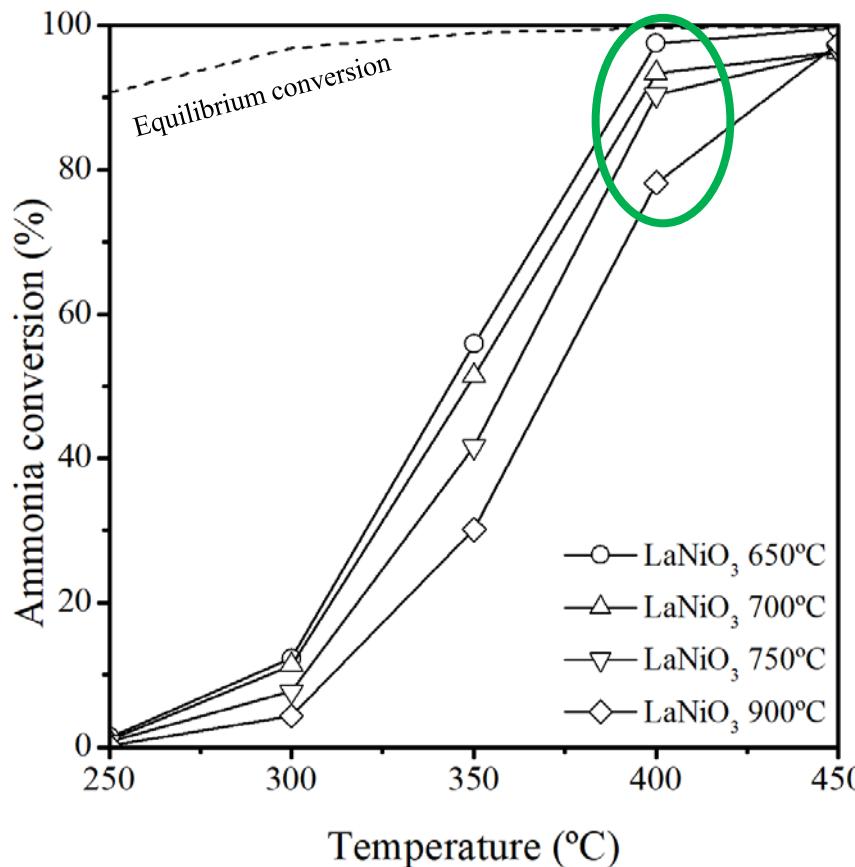
Fixed-bed reactor. P=1 atm; 5 v/v% NH_3 -Ar; GHSV=75.000 mL·g_{cat}⁻¹·h⁻¹

Reaction products were analysed on-line by using gas chromatograph (Agilent 7820A)

Perovskite-type
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Influence of
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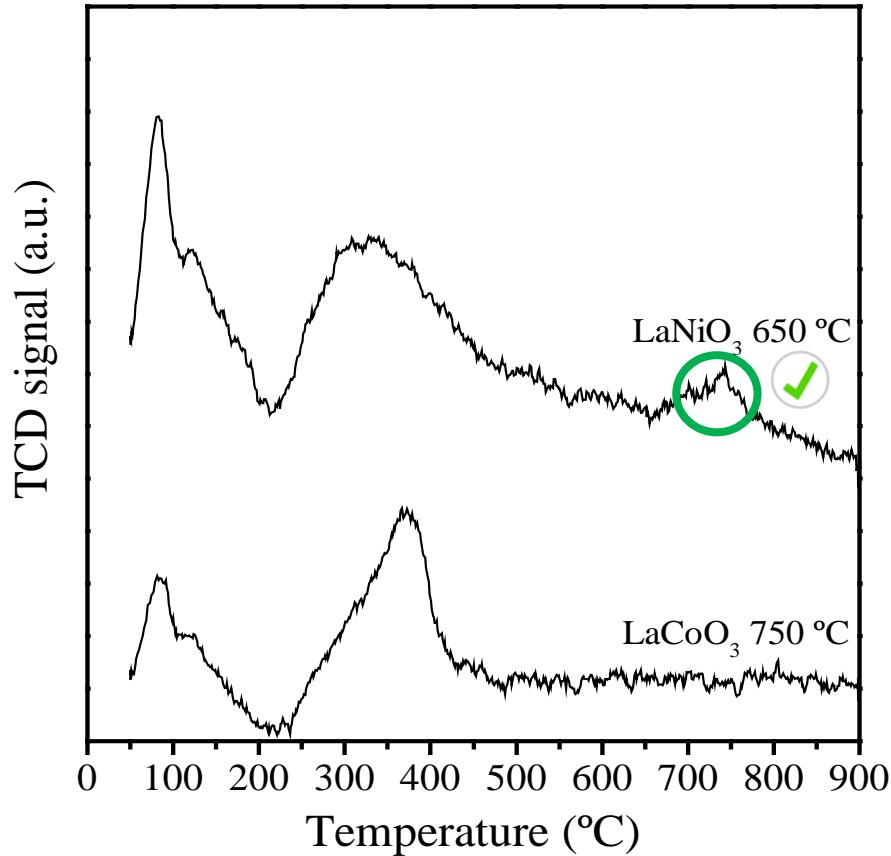
Fixed-bed reactor. $P=1 \text{ atm}$; $5 \text{ v/v\%NH}_3\text{-Ar}$; $\text{GHSV}=75.000 \text{ mL}\cdot\text{g}_{\text{cat}}^{-1}\cdot\text{h}^{-1}$

Reaction products were analysed on-line by using gas chromatograph (Agilent 7820A)

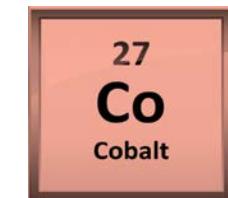
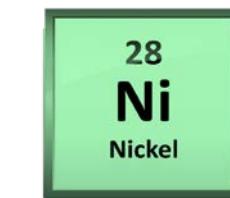
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CO₂-TPD desorption profiles



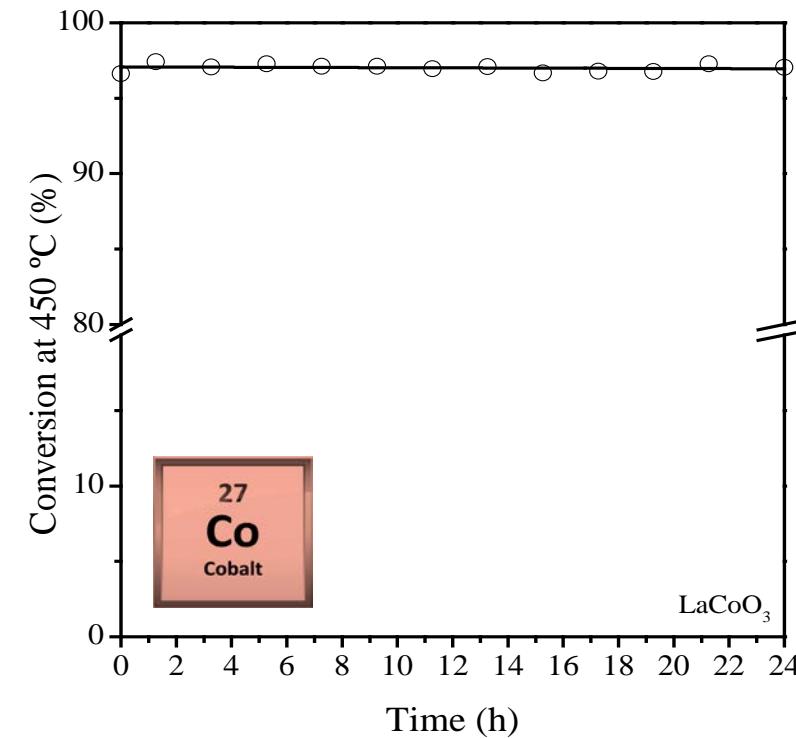
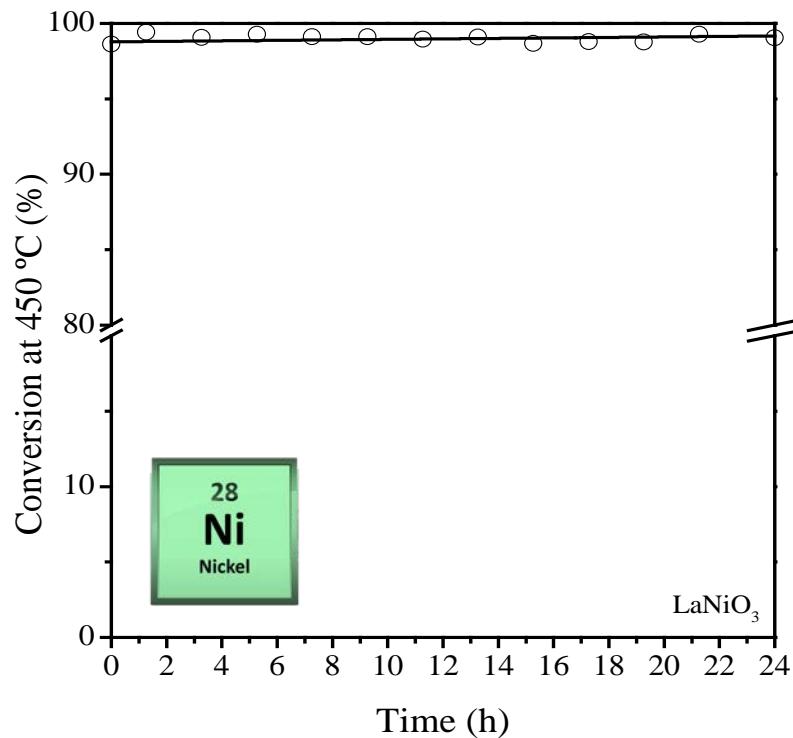
$18 \mu\text{mol CO}_2 \cdot \text{g}_{\text{cat}}^{-1}$
↑ Basicity

$9.6 \mu\text{mol CO}_2 \cdot \text{g}_{\text{cat}}^{-1}$

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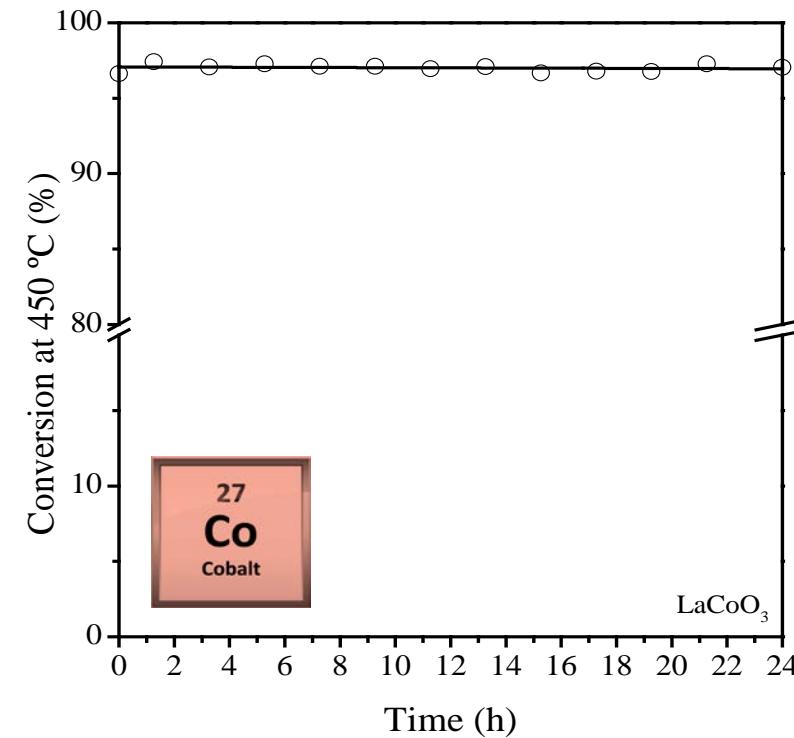
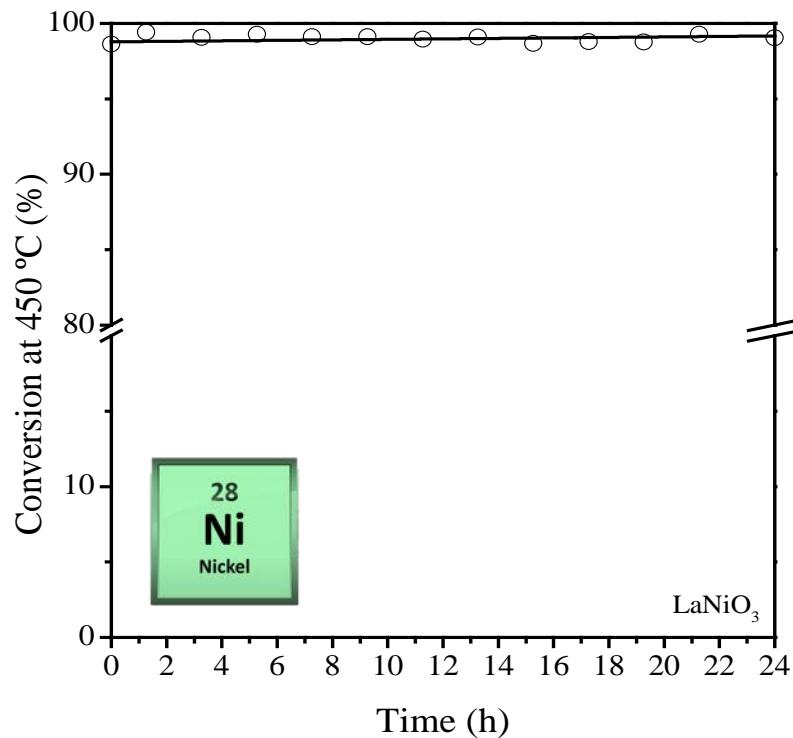


Stability test for reduced samples of LaNiO_3 calcined at 650 °C and LaCoO_3 calcined at 750 °C
(0.08 g catalyst, $75000 \text{ mL}\cdot\text{h}^{-1}\cdot\text{g}_{\text{cat}}^{-1}$, atmospheric pressure).

Perovskite-type
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Influence of
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Excellent catalytic stability after 24 h

Perovskite-type
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Conclusion



1

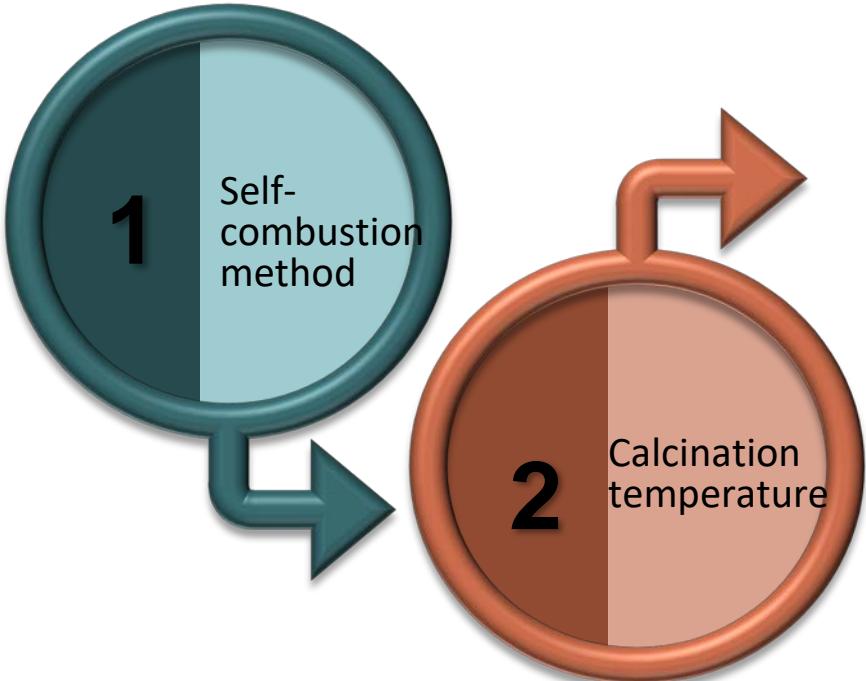
LaNiO_3 and LaCoO_3 perovskites are adequate catalytic precursors in the catalytic ammonia decomposition reaction.

Perovskite-type
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Conclusion



2

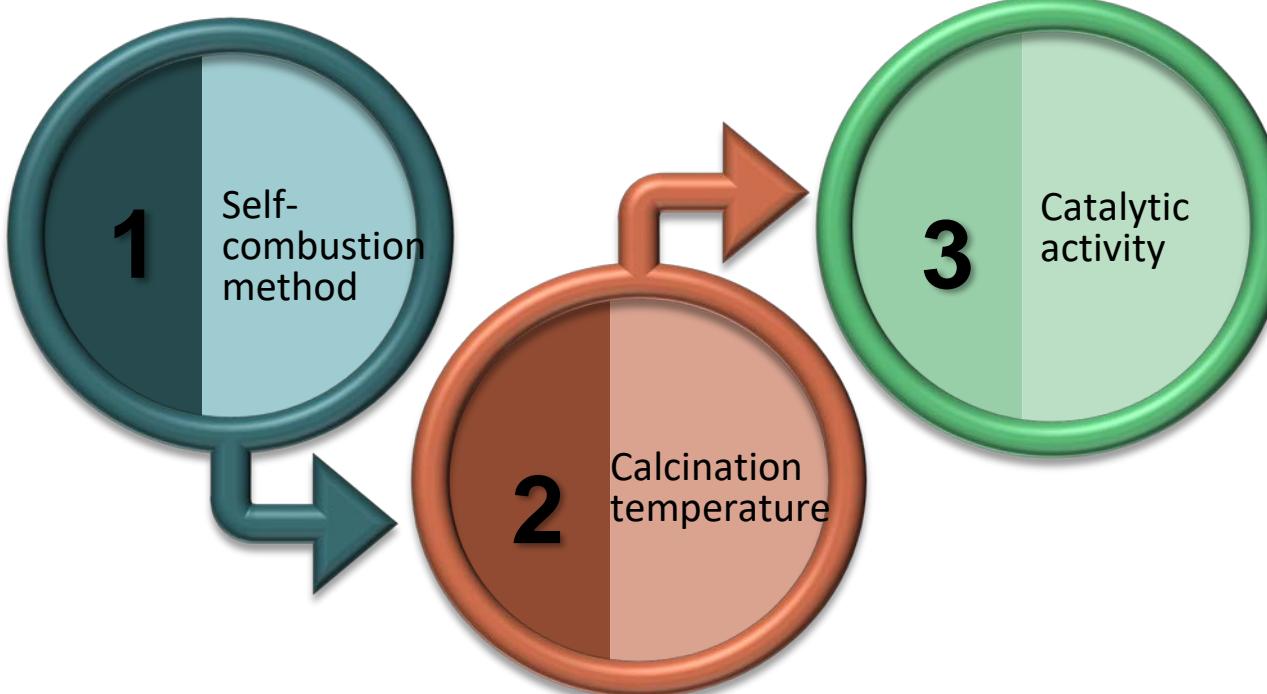
Small and well-dispersed Ni^0 particles after reduction obtained with LaNiO_3 . For cobalt perovskites, calcination temperatures below 900 °C had no significant influence on metallic cobalt crystal size.

Perovskite-type
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Conclusion



3

The nickel and cobalt perovskite-derived catalysts yielded excellent H_2 production from ammonia decomposition. In particular, at 450 °C almost 100% of the ammonia was converted over the LaNiO_3 calcined at 650 °C.

Ammonia as a carrier for hydrogen production by using Perovskites

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