

Evaluating the suitability of co-processing gardening residues and the organic fraction of municipal solid wastes via thermal and catalytic pyrolysis

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WHAT IS A URBAN BIOWASTE?



GARDEN AND PARK WASTES



FOOD WASTES



RESIDUES FROM FOOD
PROCESSING PLANTS



SEWAGE SLUDGE



MORE THAN 1,100,000 TONS OF URBAN BIO-WASTES ARE GENERATED EVERY YEAR¹

URBAN BIOWASTES DISPOSAL

URBAN MANAGEMENT AND TREATMENT OPTIONS



**TO EXPLOTE THE POTENTIAL RESOURCES CONTAINED IN
THOSE BIORESIDUES**

URBAN BIORESIDUES

FOOD WASTES
GARDEN RESIDUES
SEWAGE SLUDGE
PAPER



FAST PYROLYSIS

DECOMPOSITION IN THE
ABSENCE OF OXYGEN

REACTION CONDITIONS:

- ✓ TEMPERATURE: 400-500 °C
- ✓ HEATING RATE: 10³-10⁴ K/s
- ✓ VAPORS RESIDENCE TIME: 1-2s

GAS (10-30 %)

CO CO₂
H₂ C₁-C₃

BIOCHAR (10-35 %)

BIO-OIL (10-75 %)

HIGH HETEROGENEITY

BIOFUEL PRECURSOR
SOURCE OF CHEMICAL COMPOUNDS

STUDY ABOUT THE CO-PYROLYSIS OF MIXTURES OF TWO BIO-WASTES:
GARDENING PRUNING RESIDUES (GP) AND FOOD WASTES (FW)

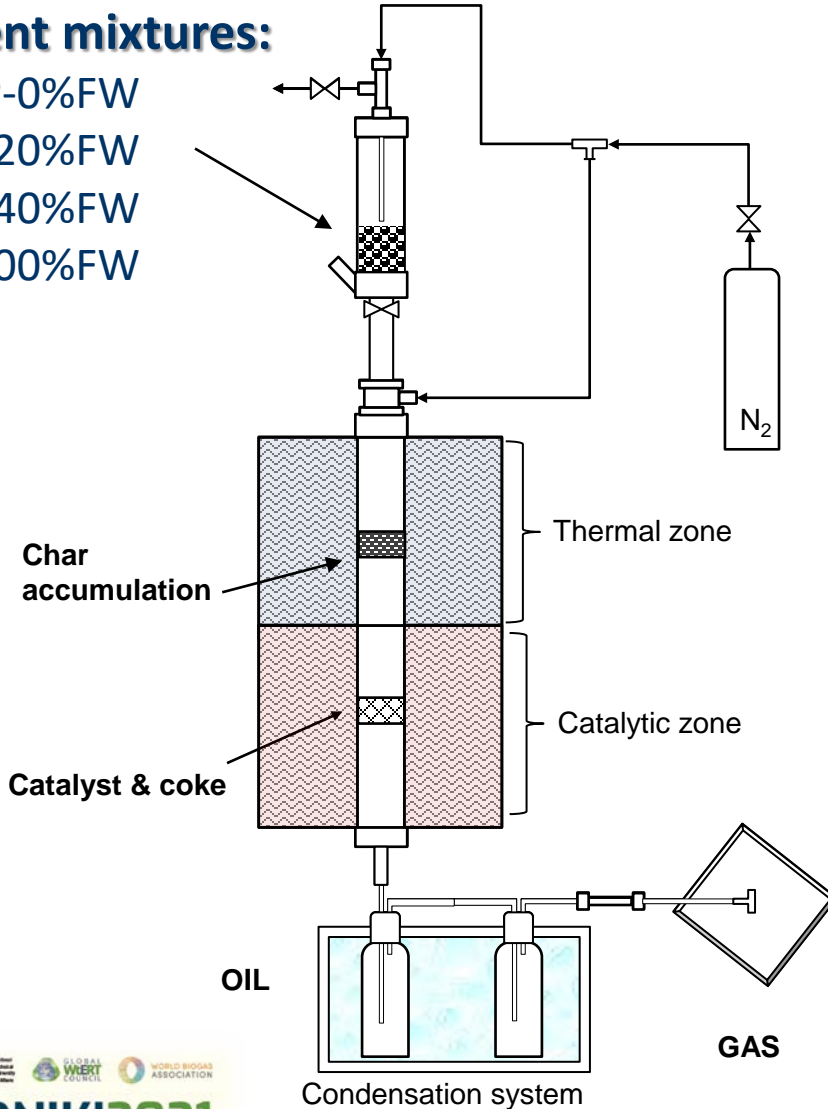


THERMAL PYROLYSIS
CATALYTIC PYROLYSIS



Four different mixtures:

- 100%GP-0%FW
- 80%GP-20%FW
- 60%GP-40%FW
- 0%GP-100%FW



Reaction conditions:

- Thermal zone: 500 °C
- Catalytic zone: 450 °C
- Pressure: 1 atm
- N₂ flow: 100 Nml/min
- Feed: 5 g of biowaste mixture
- Catalyst/feedstock: 0.4

Analytical techniques:

- **ICP-OES:** Metal content
- **Karl-Fisher:** water content
- **Elemental analysis:** CHNS/O
- **GC-MS:** molecular composition bio-oil
- **GC:** Gas composition



FW AND GP CHARACTERIZATION

CHEMICAL AND STRUCTURAL PROPERTIES

	FOOD WASTES	GARDEN PRUNING
MOISTURE (WT.%)	1.1	1.2
PROXIMATE ANALYSES (WT.% DB)		
VOLATILE MATTER	70.5	82.5
ASH	5.6	3.3
FIXED CARBON	24.0	14.2
ELEMENTAL ANALYSES (WT.% DAF)		
C	51.5	50.1
H	6.3	6.1
N	1.3	1.4
O	40.9	42.4
HHV (MJ/KG)	19.9	19.5
STRUCTURAL COMPONENTS (WT.%)		
EXTRACTIVES	60.2	9.3
CELLULOSE	9.2	37.2
HEMICELLULOSE	6.7	14.0
LIGNIN	15.6	29.1
ACETYL GROUPS	1.6	4.8
OTHERS	1.1	2.3

IMPORTANT EFFECT IN BIO-OIL YIELD

GP: MAINLY COMPOSED BY CELLULOSE, HEMICELLULOSE AND LIGNIN

FW: SIGNIFICANT EXTRACTIVES CONTENT (WAX/FAT, PROTEINS, AMINO ACIDS AND PECTIN)

^a db: dry basis

^b daf: dry and ash-free basis

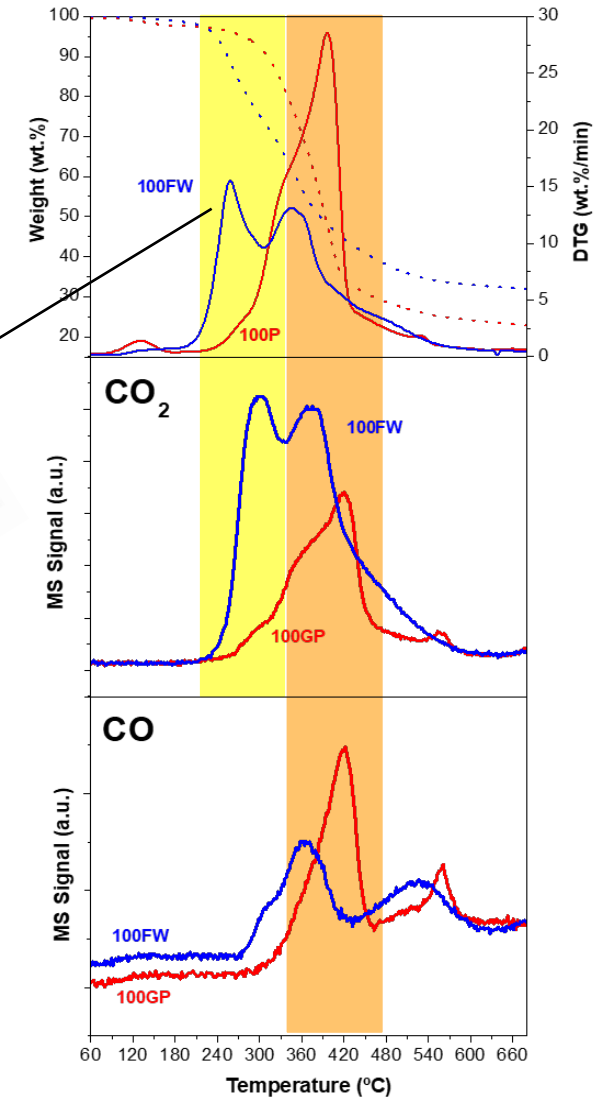
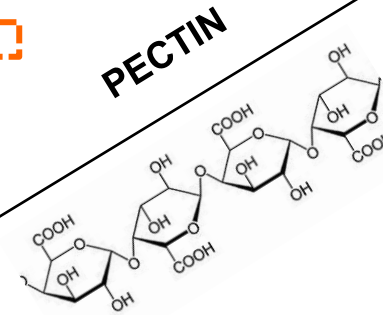
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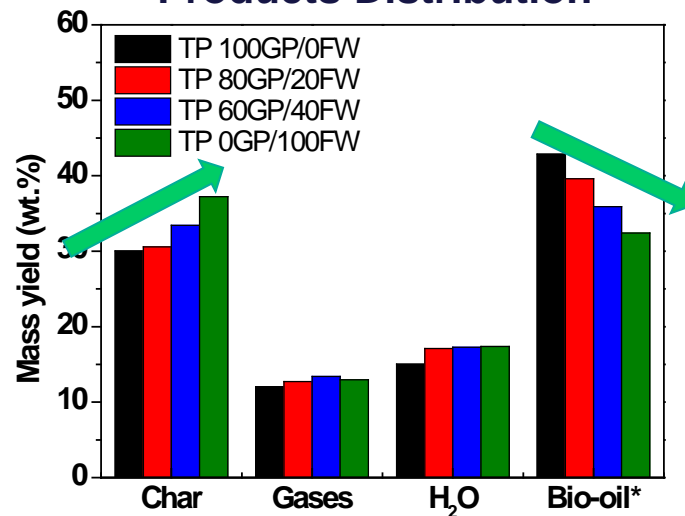
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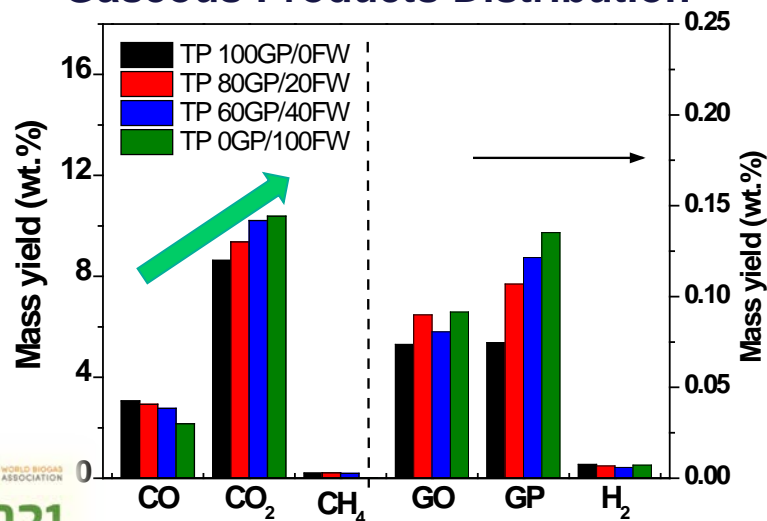
THERMAL PYROLYSIS

Products Distribution



- LOWER BIO-OIL YIELD AND HIGHER BIOCHAR PRODUCTION WITH INCREASING FW AMOUNT → LOWER VOLATILE MATTER.
- SLIGHT INCREASE IN WATER AND GAS FRACTION YIELDS.

Gaseous Products Distribution



- FW FAVOURS THE DEOXYGENATION OF THE PYROLYSIS VAPOURS VIA DECARBOXYLATION → PREFERRED TO DECARBONYLATION IN TERMS OF MASS AND ENERGY EFFICIENCY



THERMAL PYROLYSIS

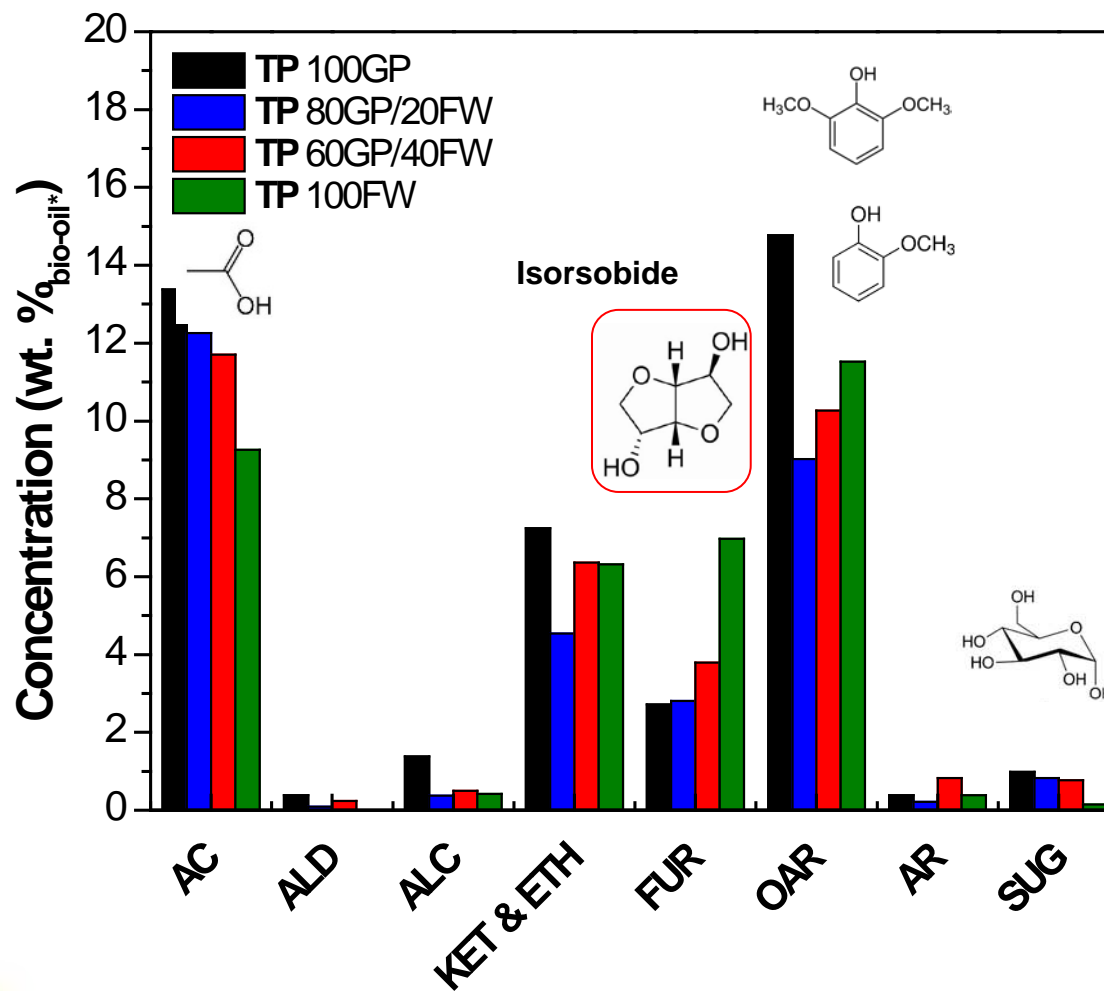
Bio-oil* chemical composition



Experiment	Water content (wt.% liquid fraction)	Elemental composition (wt.% _{bio.oil} db)					HHV (MJ/kg _{bio-oil} db)
		C	H	N	S	O	
TP 100GP	27.2	57.6	7.3	1.1	0.0	34.0	25.2
TP 80GP/20FW	29.7	60.2	7.4	1.5	0.0	31.0	26.5
TP 60GP/40FW	31.8	60.9	7.7	1.9	0.0	29.5	27.3
TP 100FW	35.7	66.5	8.3	2.8	0.0	22.4	30.7



Bio-oil* molecular composition (GC-MS)





CATALYTIC PYROLYSIS

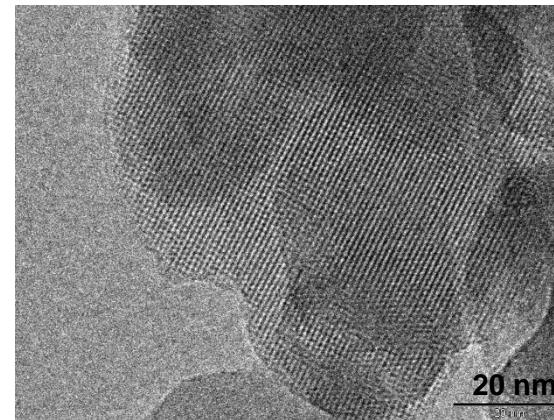
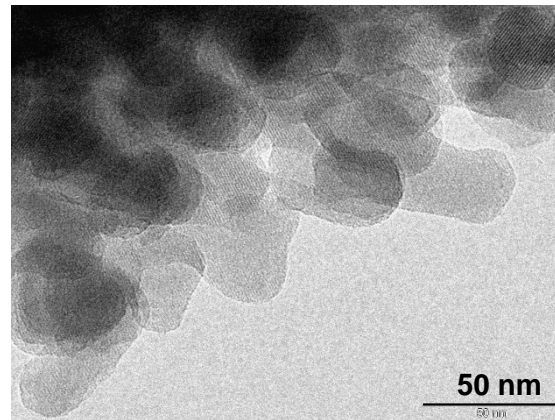
CATALYST: nanocrystalline ZMS-5 zeolite

Physicochemical properties of n-ZSM-5 zeolite

Catalyst	[Si/Al] _{MOL} ^a	S _{BET} ^b (m ² /g)	S _{MIC} ^c (m ² /g)	S _{EXT} ^c (m ² /g)	V _T ^d (cm ³ /g)	Acidity ^e (mmol/g)
n-ZSM-5	42	445	312	133	0.512	0.28

^a Measured by ICP-OES., ^b BET surface area. ^c Micropore surface area (S_{MIC}) and External surface area (S_{EXT}), calculated from NL-DFT., ^d Total pore volume at P/P₀ ≈ 0.98. ^e Measured by TPD-NH₃.

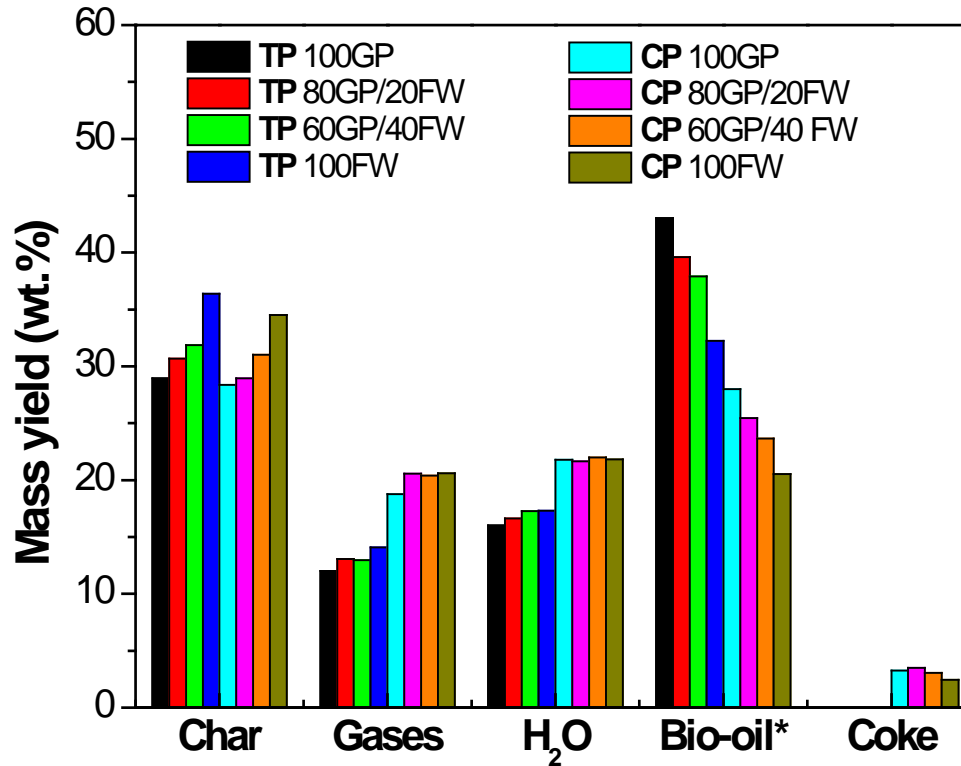
TEM





CATALYTIC PYROLYSIS

Products Distribution



- SIMILAR CHAR YIELDS TO THOSE OBTAINED FOR THERMAL TESTS.
- A CARBONACEOUS RESIDUE (COKE) IS DEPOSITED OVER THE CATALYST SURFACE.
- SIGNIFICANT INCREASE OF GASES PRODUCTION
- HIGHER WATER PRODUCTION → OXYGEN REMOVAL VIA DEHYDRATION AND CONDESATION REACTIONS.



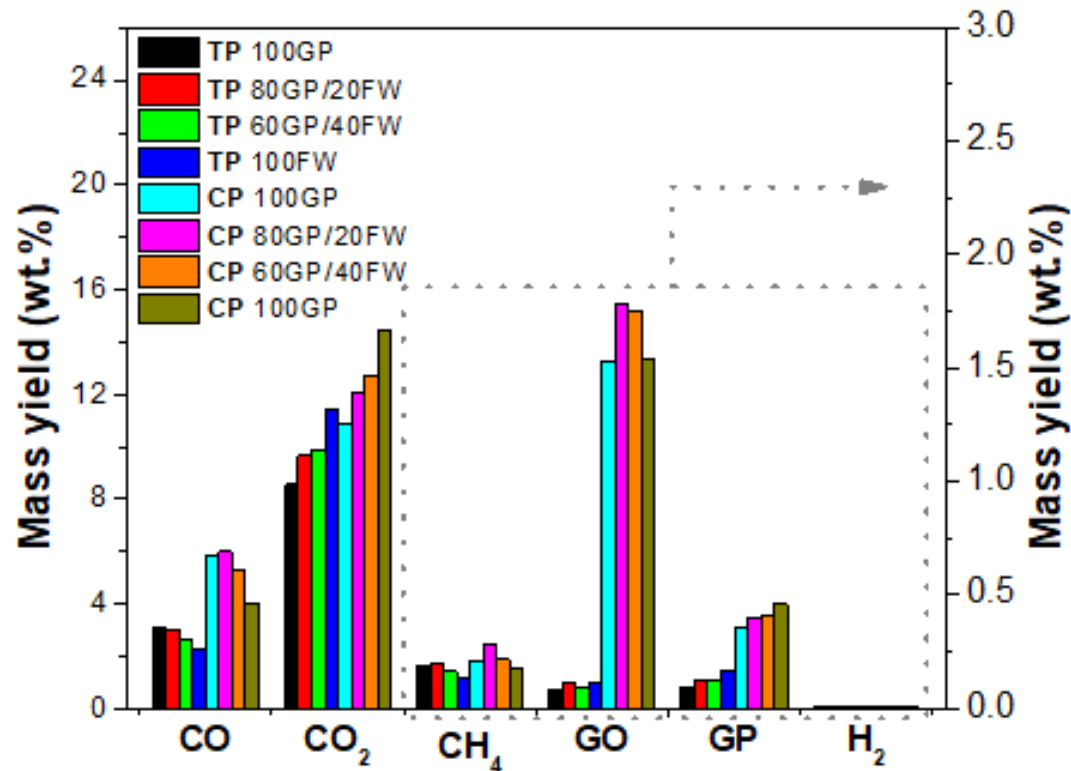
→ AQUEOUS PHASE

→ ORGANIC PHASE



CATALYTIC PYROLYSIS

Gaseous Products Distribution



- INCREASE OF CO₂ and CO YIELDS → PROMOTION OF DECARBOXYLATION AND DECARBONYLATION.
- HIGHER PRODUCTION OF GO AND GP → DEOXYGENATION AND CRACKING REACTIONS.



CATALYTIC PYROLYSIS

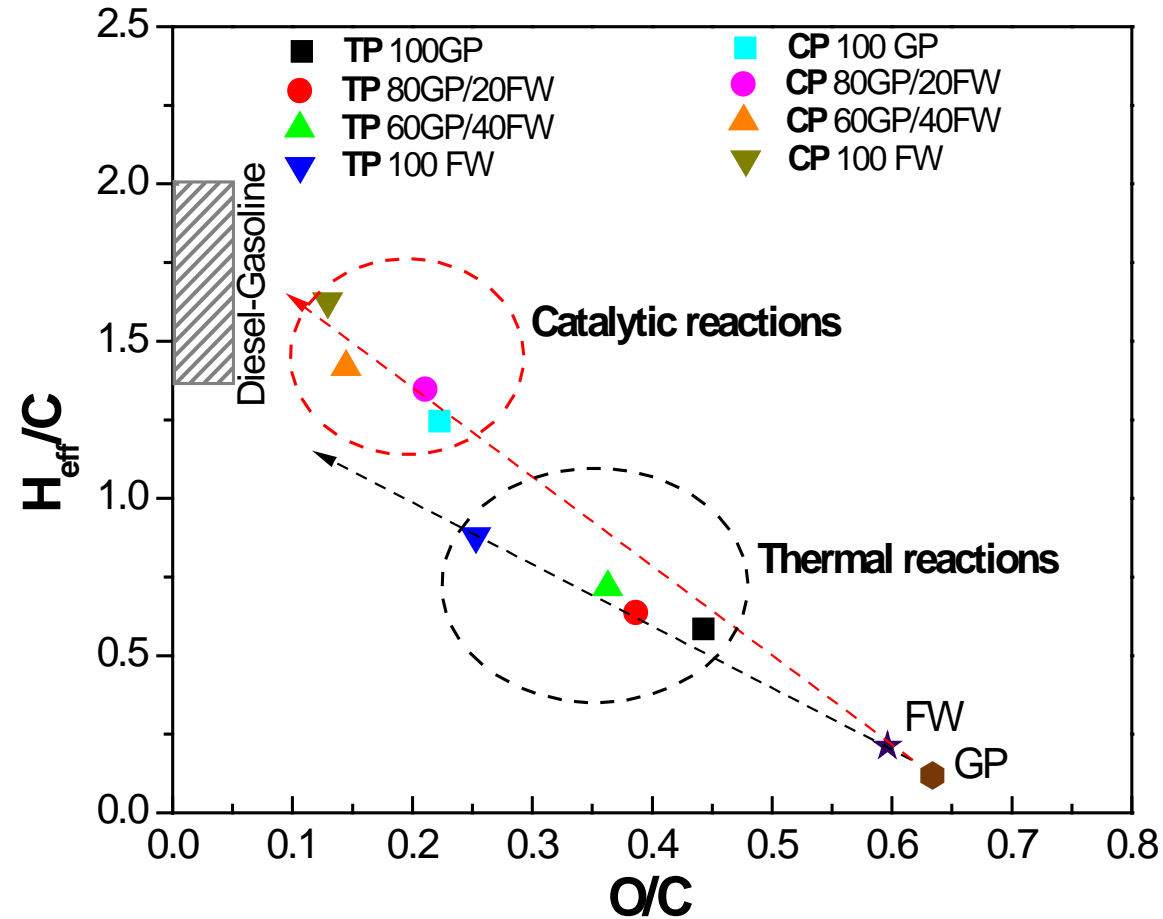
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TP 60GP/40FW	31.8	60.9	7.7	1.9	0.0	29.5	27.3
TP 100FW	35.7	66.5	8.3	2.8	0.0	22.4	30.7
CP 100GP	43.9	69.4	8.3	1.7	0.0	20.6	31.9
CP 80GP/20FW	46.5	69.4	8.8	2.4	0.0	19.5	32.5
CP 60GP/40FW	47.2	74.8	8.9	2.0	0.0	14.4	35.0
CP 100FW	51.2	74.5	9.8	3.0	0.0	12.7	36.2

↓ +
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↓ +



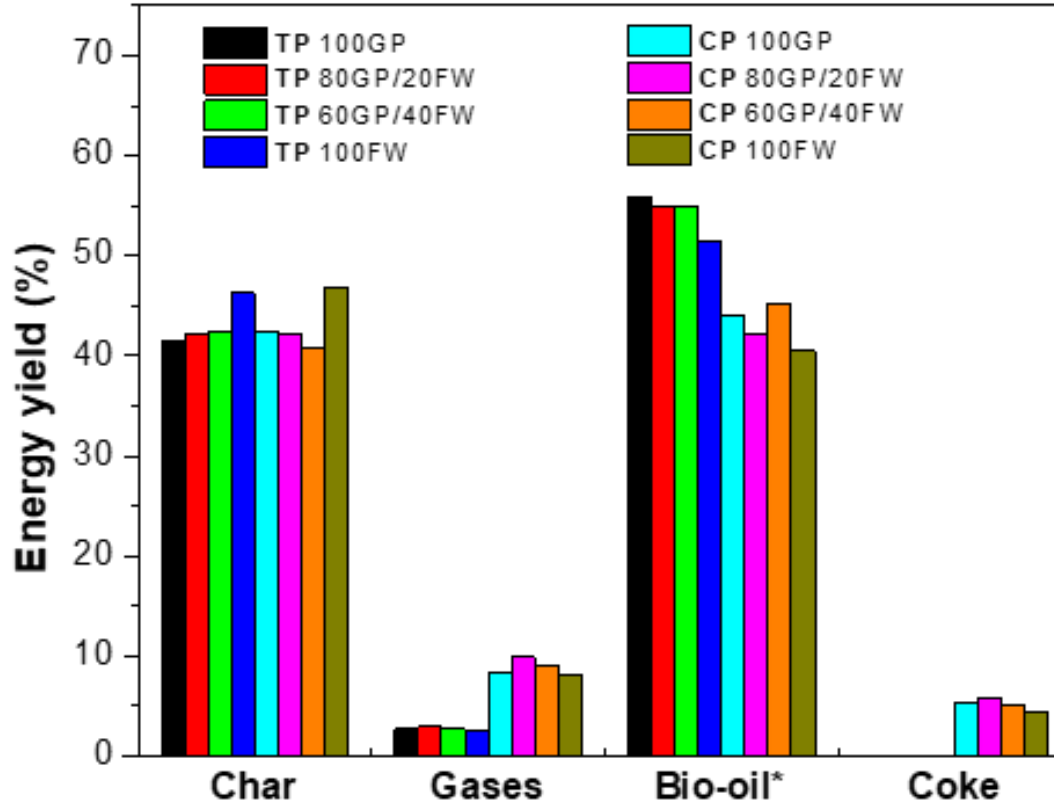
Van Krevelen Graph





CATALYTIC PYROLYSIS

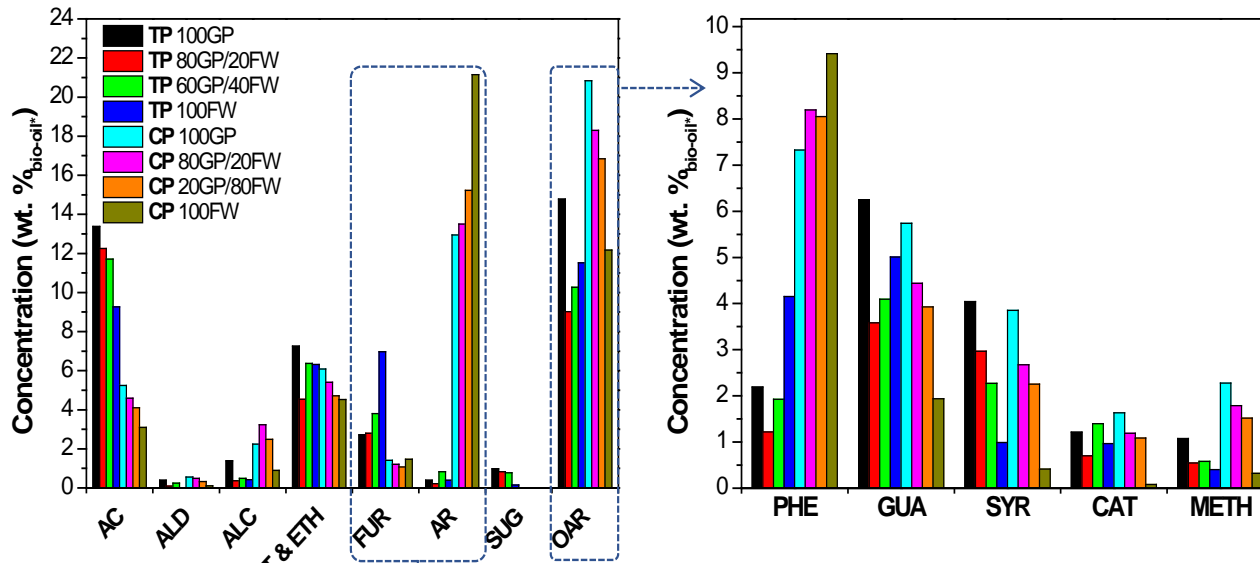
Energy yield



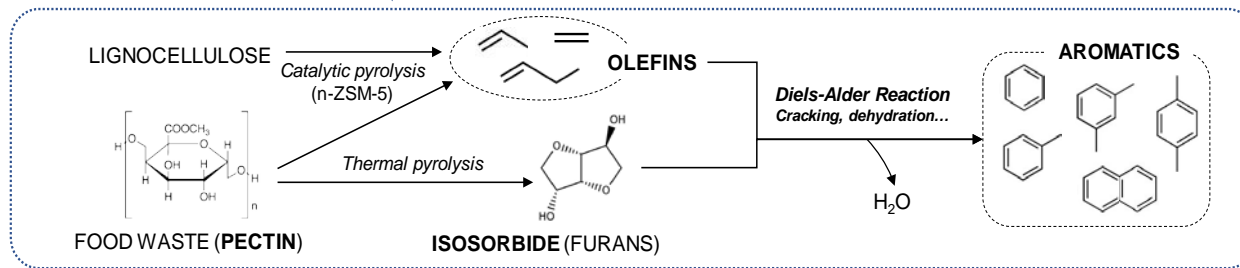
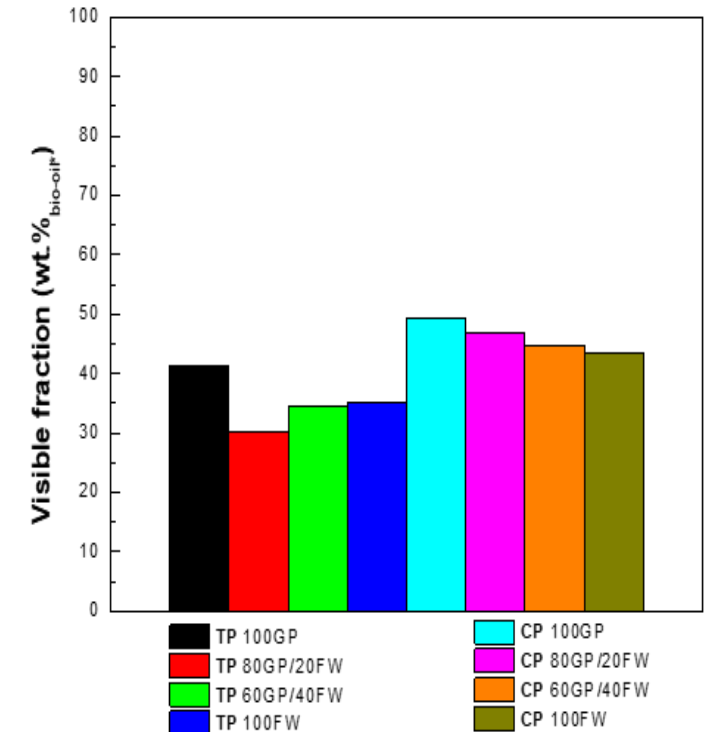
THE ENERGY YIELD REDUCTION IS LESS MARKED THAN THAT PRODUCED IN THE BIO-OIL* MASS YIELDS → LOWER OXYGEN CONTENT EXHIBITED IN THE CATALYTIC BIO-OIL.



Bio-oil* molecular composition (GC-MS)

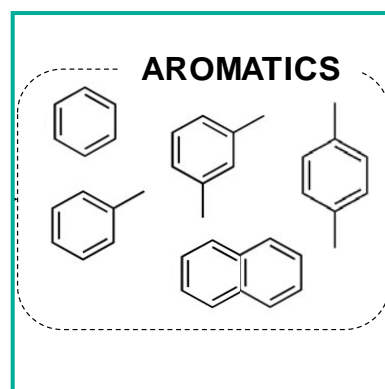


Percentage of mass detected by GC-MS in bio-oil*





- CO-PROCESSING OF **GARDEN PRUNING** AND **FOOD BIO- RESIDUES** VIA CATALYTIC PYROLYSIS IS A PROMISING VALORISATION ROUTE TO AVOID INCINERATION OR LANDFILL DISPOSAL.
- THE CO-UTILISATION OF **FOOD WASTES** WITH **GARDEN PRUNING RESIDUES** FACILITATES THE BIO-OIL* DEOXYGENATION, ENHANCING ITS QUALITY.
- THIS EFFECT IS BOOSTED IN PRESENCE OF n-ZSM-5 ZEOLITE.



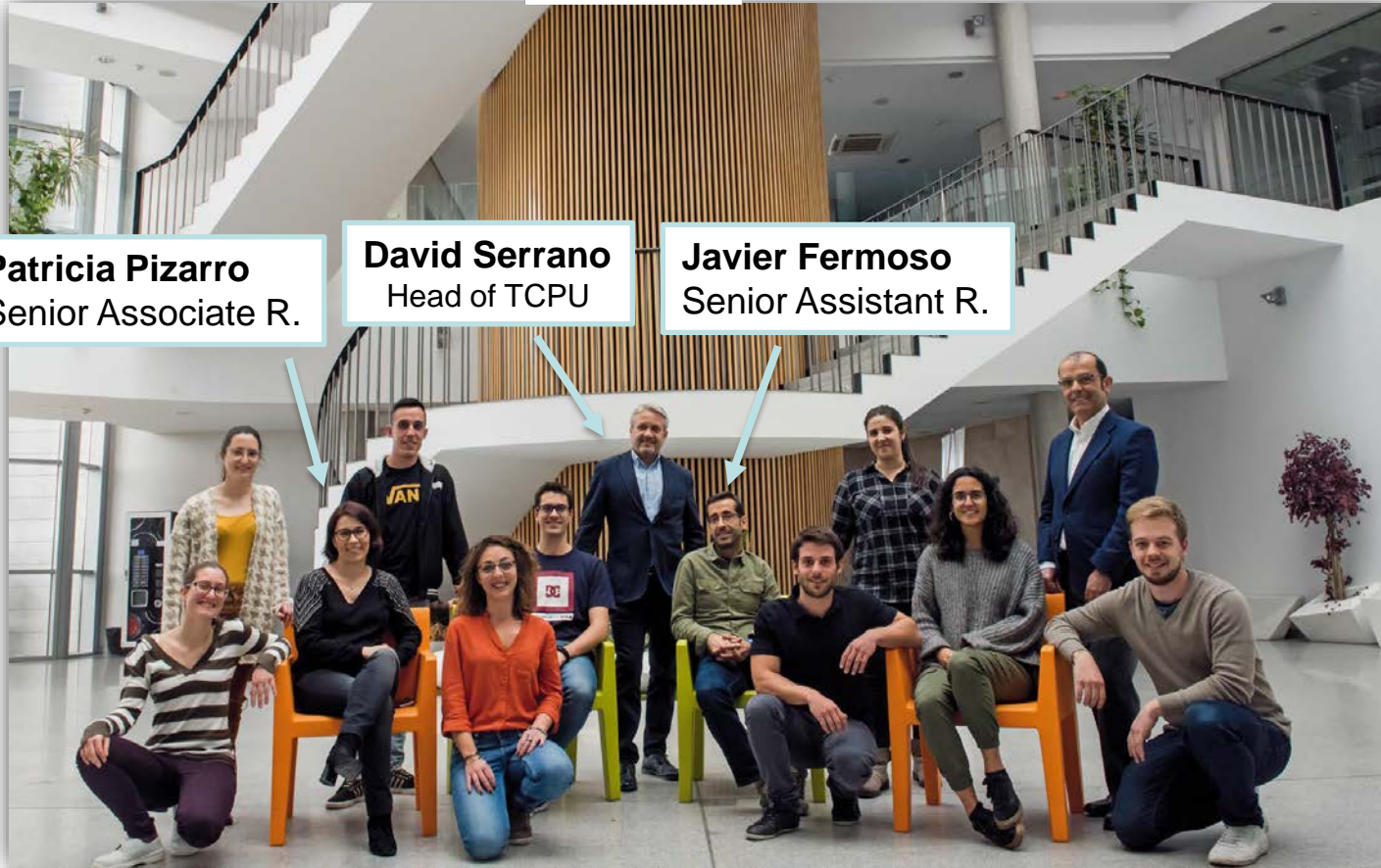
- THE SIGNIFICANT FORMATION OF VALUABLE **AROMATIC HYDROCARBONS** (ESPECIALLY BENZENE AND ALKYL BENZENES) BY CATALYTIC PYROLYSIS INCREASE THE **COMMERCIAL VALUE** OF THIS PROCESS.



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