



Conversion of winery wastes into a sugar-rich hydrolysate for the biotechnological production of succinic acid

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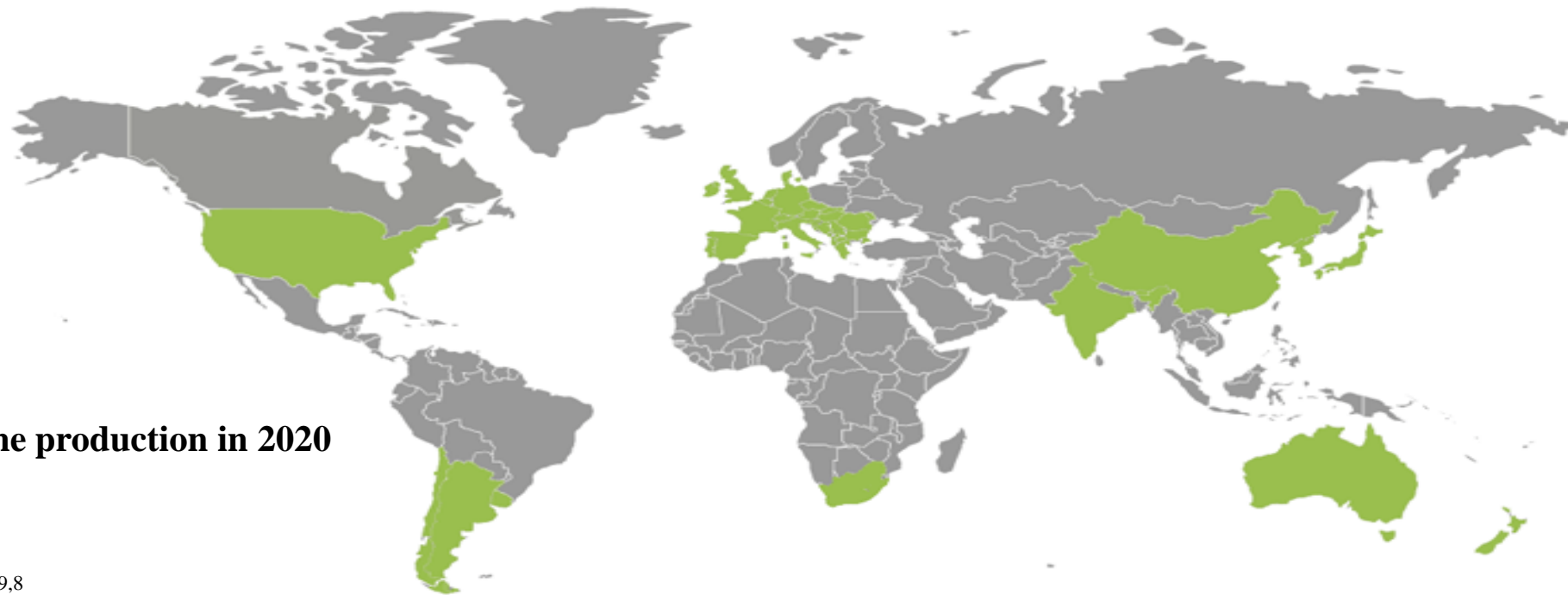
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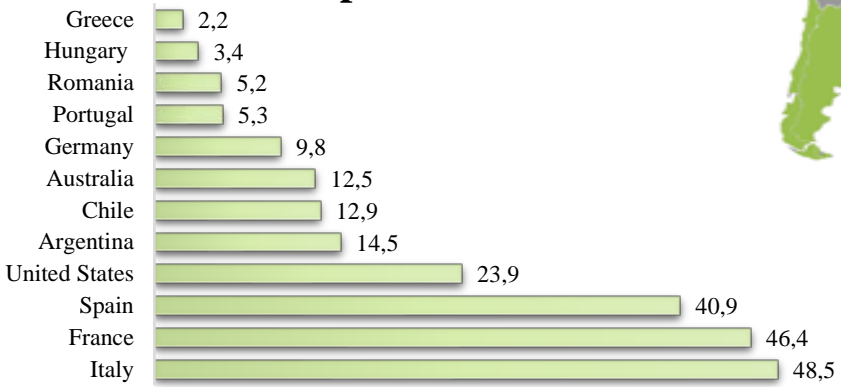


- Renewable raw materials – winery by-products
 - Grape pomace
 - Grape stalks
- Development of an integrated biorefinery for the valorisation of grape pomace and stalks generated after the winemaking process of the Greek variety Agiorgitiko for:
 - The production of bio-based succinic acid
 - The extraction of value-added fractions (lipids and phenolic compounds)
- Optimisation of enzymatic hydrolysis of pretreated grape pomace and stalks
- Evaluation of different feeding strategies in the fermentation process

Wine making worldwide production of 260 million hectoliters in 2020



World wine production in 2020



Million Hectoliters (mhl)

International organization of vine and wine



National Technical University of Athens





By-products produced from the wine making process **INVALOR**

Wine making process



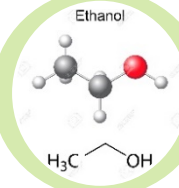
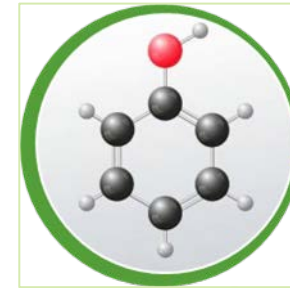
Vinification by-products



Process development



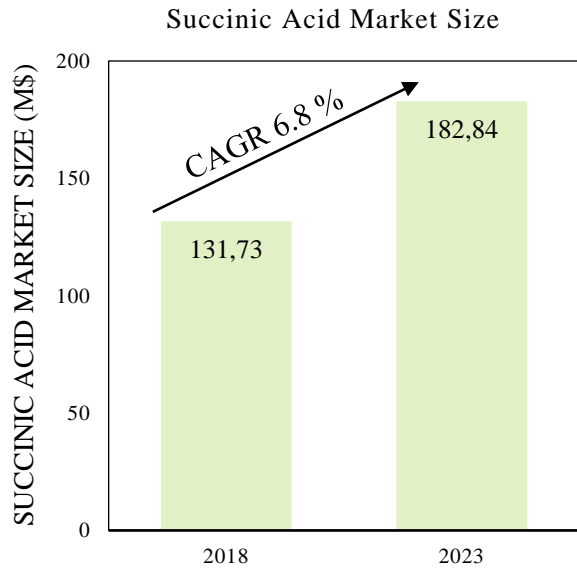
Products & Applications



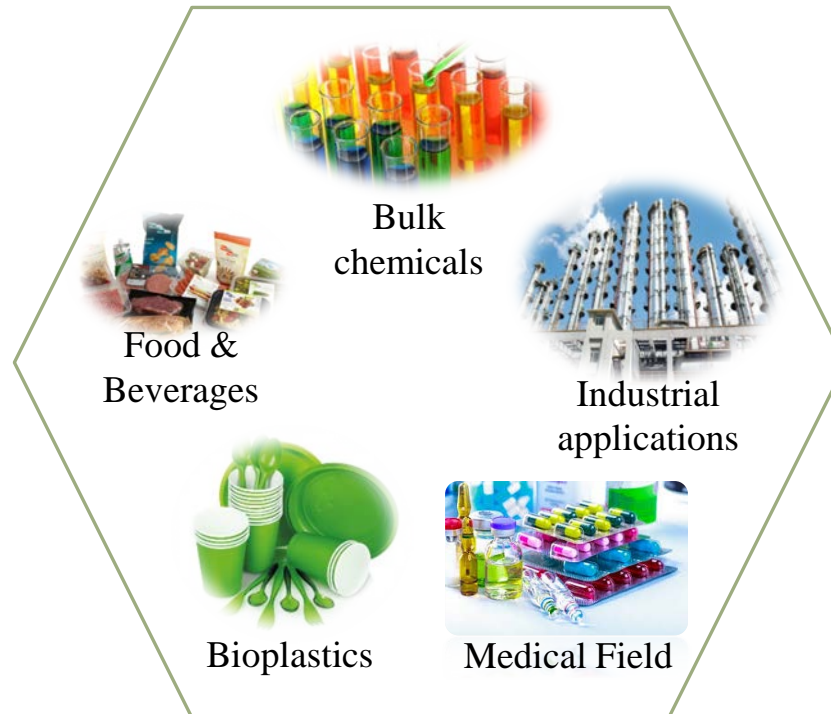


Bio-based Succinic Acid

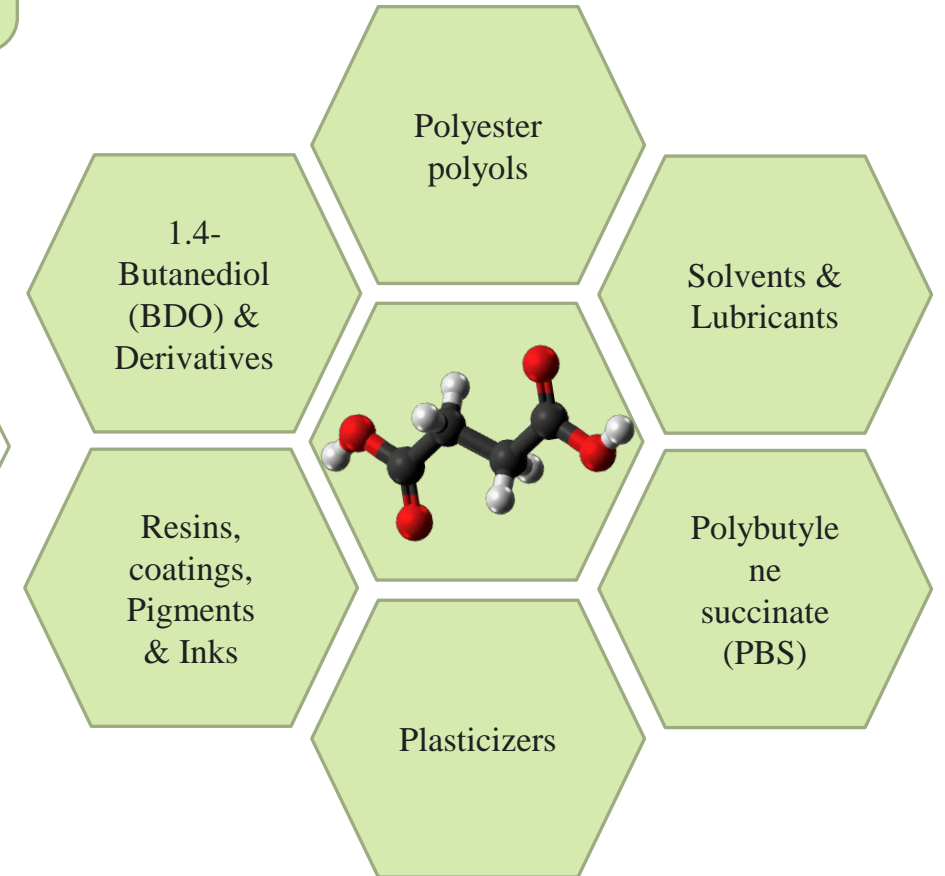
Succinic acid is one of the top 12 high-value-added bio-based chemicals
Intermediate in several chemical processes



Source: Markets and Markets



Industrial Applications



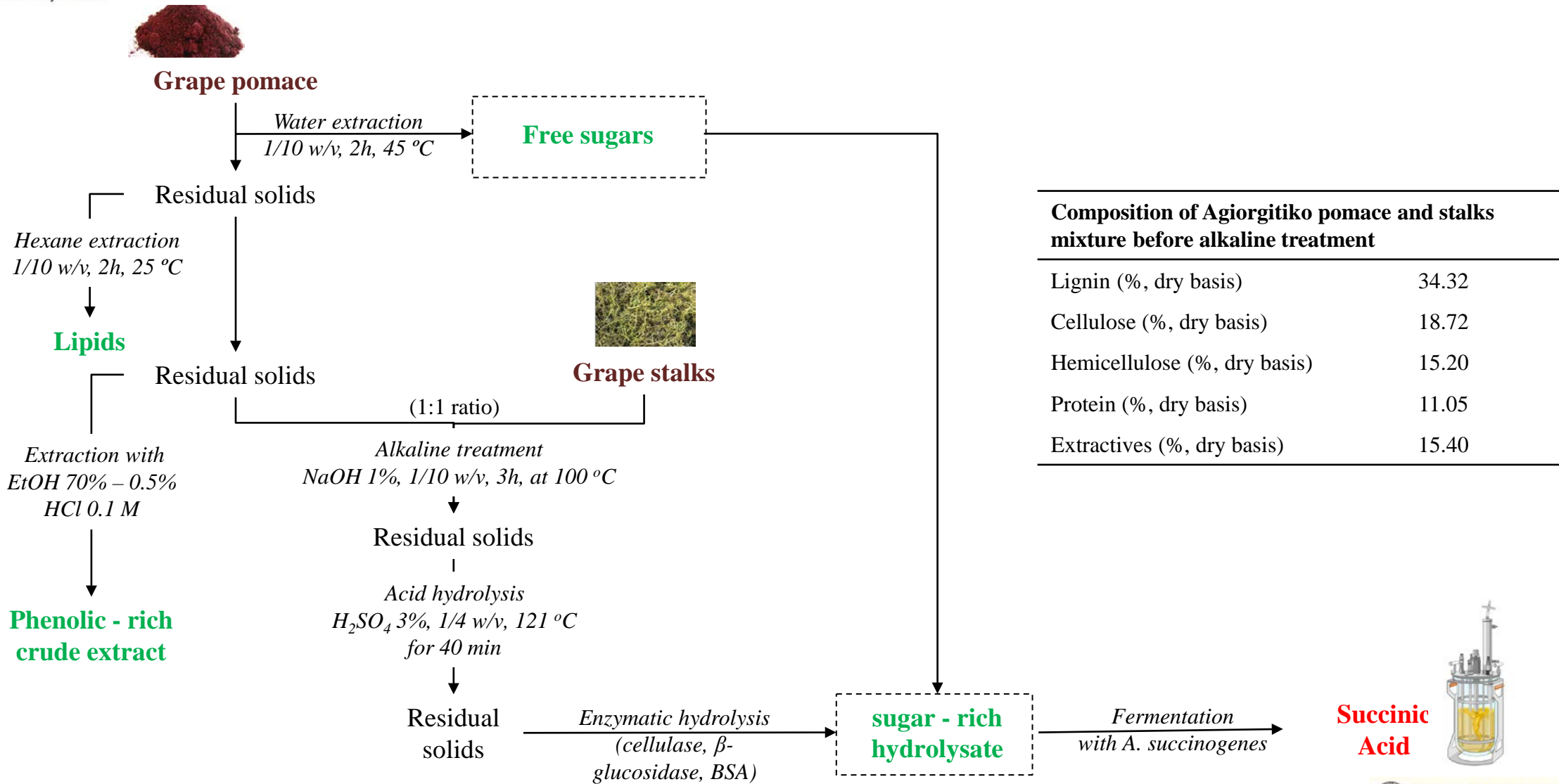
*CAGR: Compound annual growth rate

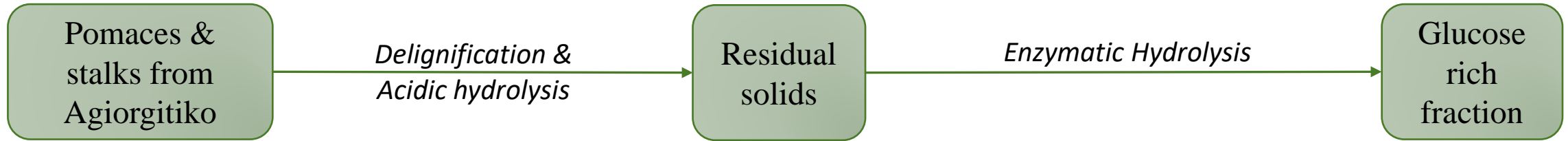
Components (%, dry basis)	Pomace	Stalks
Free sugars	2.55 ± 0.03	5.44 ± 1.17
Protein	9.36 ± 0.50	7.12 ± 0.26
Lipids	8.20 ± 0.07	8.07 ± 0.73
Ash	4.79 ± 0.13	6.76 ± 0.10
Lignin	34.79 ± 0.70	29.73 ± 0.59
Cellulose	20.90 ± 0.75	21.65 ± 0.01
Hemicellulose	13.31 ± 0.53	15.25 ± 0.88
Tannins	2.62 ± 0.02	0.74 ± 0.09
TPC (g GAE)	2.47 ± 0.05	1.36 ± 0.07
Ethanollic extract presents:		
TPC (mg GAE/ g extract)	185.75 ± 3.75	57.34 ± 4.71
Antioxidant Activity Index	1.03 ± 0.12	0.47 ± 0.02

Free sugars, cellulose and hemicellulose may provide carbon sources for succinic acid production

TPC: Total Phenolic Content
GAE: Gallic Acid Equivalents

Process flow diagram





Alkaline pretreatment (1% (w/v) NaOH, 100 °C for 3 h):

✓ Lignin removal 52% (w/w)

Dilute acid pretreatment (3% (v/v) H₂SO₄, 121 °C for 40 min):

✓ Hemicellulose solubilisation 53% (w/w)



Composition of the remaining solids (on dry basis):

✓ Cellulose: 42.38 %

✓ Hemicellulose: 10.89 %

✓ Lignin: 29.79 %

Enzymes and enzyme activities (Units / g substrate)

20 FPU Celluclast* & 80 U β-glucosidase

20 FPU Celluclast & 40 U β-glucosidase

10 FPU Celluclast & 10 FPU Viscozyme & 80 U β-glucosidase

10 FPU Celluclast & 10 FPU Viscozyme & 40 U β-glucosidase

* Cellulase from *Trichoderma reesei*

Conditions:

- ❖ 50 mM sodium citrate buffer (pH 5)
- ❖ Temperature: 50 °C
- ❖ Solid to liquid ratio: 10%
- ❖ Under mechanical stirring for 72 h

The addition of 8 mg BSA/g dry sample was also tested using all of these enzyme combinations

BSA: Bovine Serum Albumin





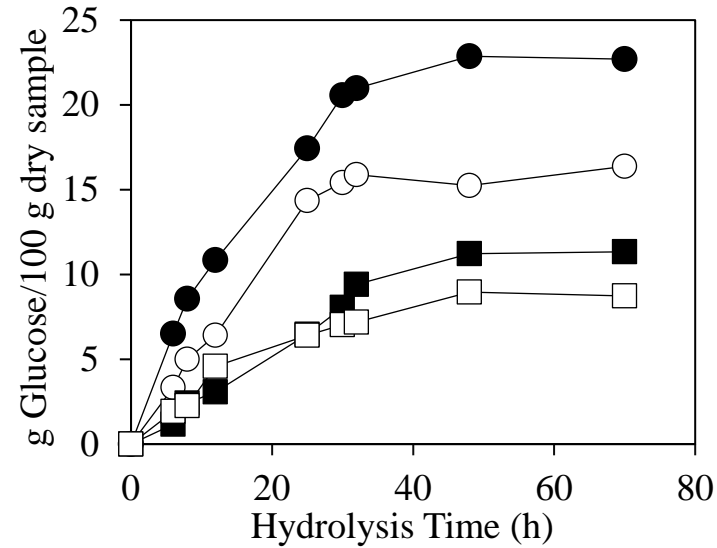
Optimisation of Enzymatic Hydrolysis

Composition (% , dry basis): 42.38 Cellulose, 10.89 Hemicellulose, 29.79 Lignin

20 FPU/g substrate Celluclast

and

- 80 U β -glucosidase /g substrate & BSA
- 80 U β -glucosidase /g substrate
- 40 U β -glucosidase /g substrate & BSA
- 40 U β -glucosidase /g substrate



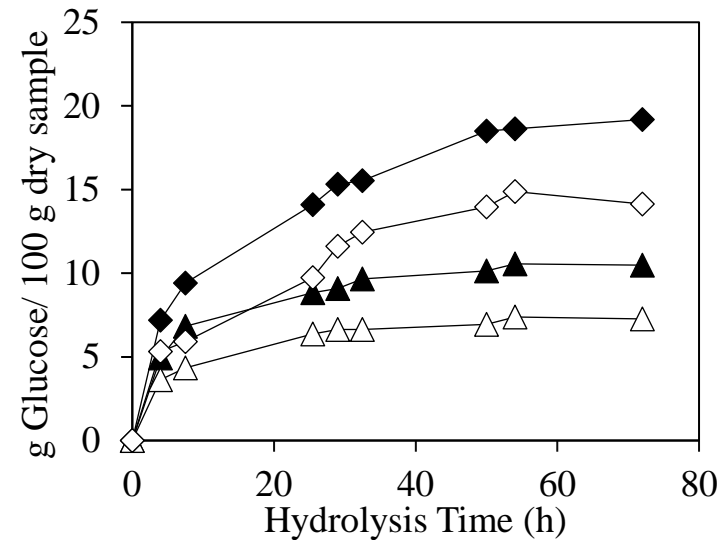
Cellulose-to-glucose conversion yield:

- 0.48 g/g
- 0.35 g/g
- 0.24 g/g
- 0.19 g/g

10 FPU/g sub. Celluclast & 10 FPU/ g sub. Viscozyme

and

- ◆ 80 U β -glucosidase /g substrate & BSA
- ◇ 80 U β -glucosidase /g substrate
- ▲ 40 U β -glucosidase /g substrate & BSA
- △ 40 U β -glucosidase /g substrate



Cellulose-to-glucose conversion yield:

- ◆ 0.41 g/g
- ◇ 0.30 g/g
- ▲ 0.22 g/g
- △ 0.15 g/g

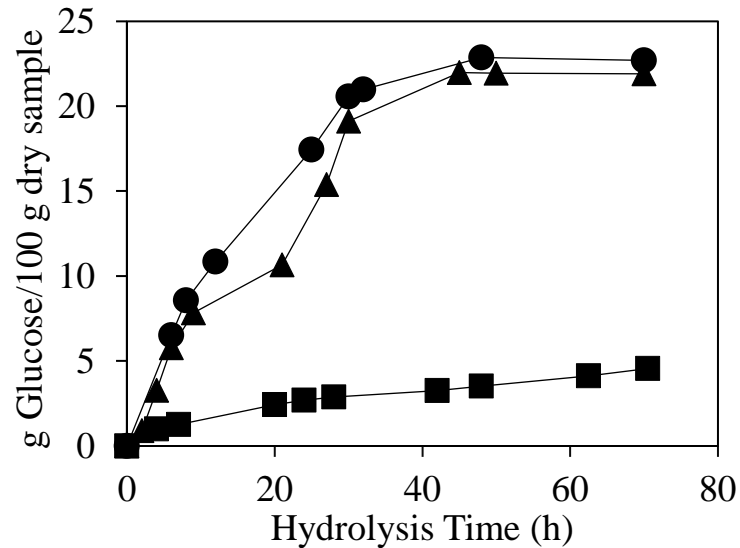
The best enzyme combination considering glucose release from cellulose was evaluated using:

- ❖ either deionized water or
- ❖ the direct addition of the enzymes to the acid hydrolysate

20 FPU/g substrate Celluclast, 80 U β -glucosidase /g substrate & BSA

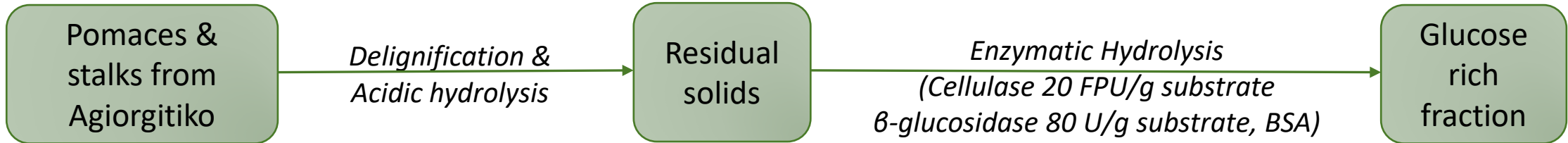
Enzymatic hydrolysate solution:

- Citrate buffer
- ▲ Deionized water
- Acid hydrolysate



Cellulose-to-glucose conversion yield:

- 0.48 g/g
- ▲ 0.44 g/g
- 0.10 g/g



- ✓ Strain: *Actinobacillus succinogenes*
- ✓ Carbon Source: Enzymatic hydrolysate (22.7 g/L glucose)
- ✓ Feeding: Concentrated free sugars from Agiorgitiko pomaces (consisting mainly of glucose and fructose)
- ✓ Nitrogen source: 5 g/L Yeast Extract
- ✓ MgCO_3 : 5 g/L
- ✓ Working volume: 500 mL
- ✓ Temperature: 37 °C
- ✓ pH: 6.7
- ✓ Aeration: CO_2 0.1vvm
- ✓ Agitation: 180 rpm

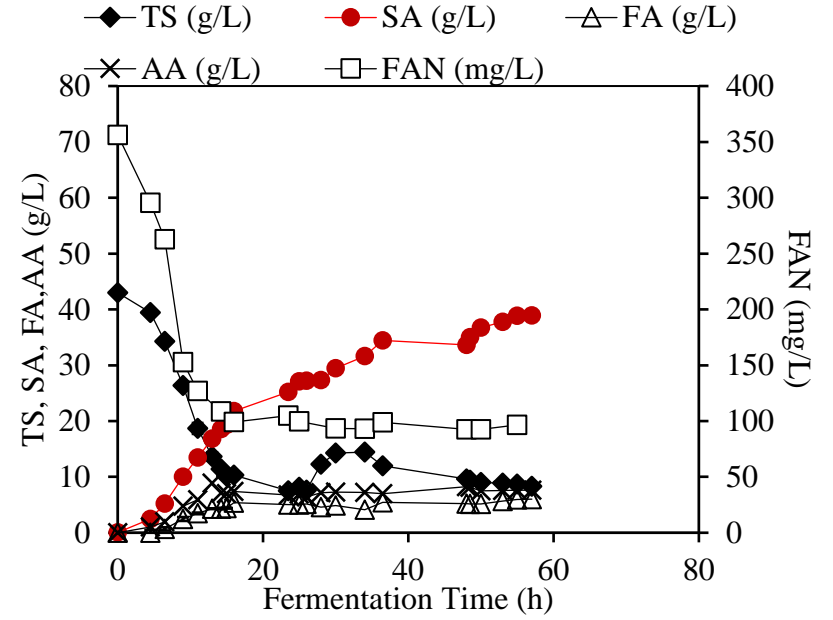
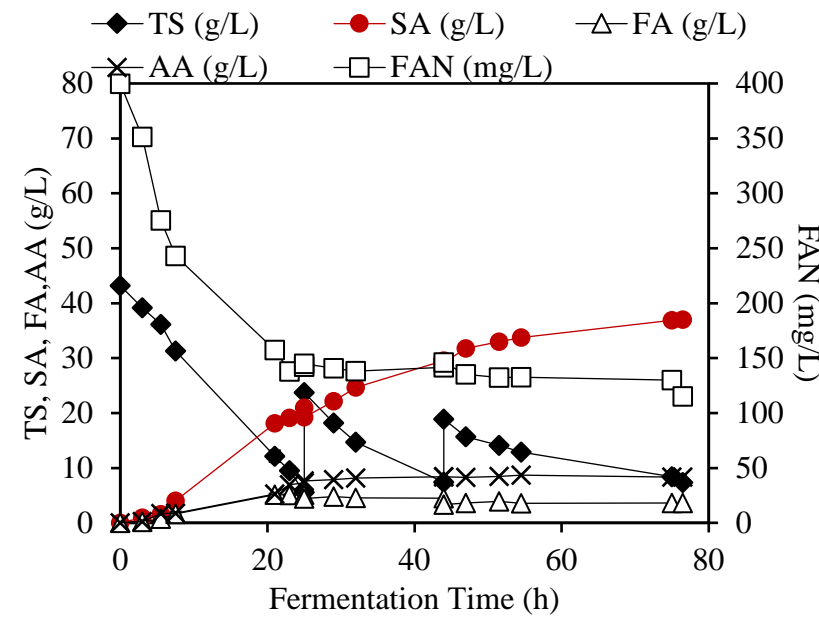
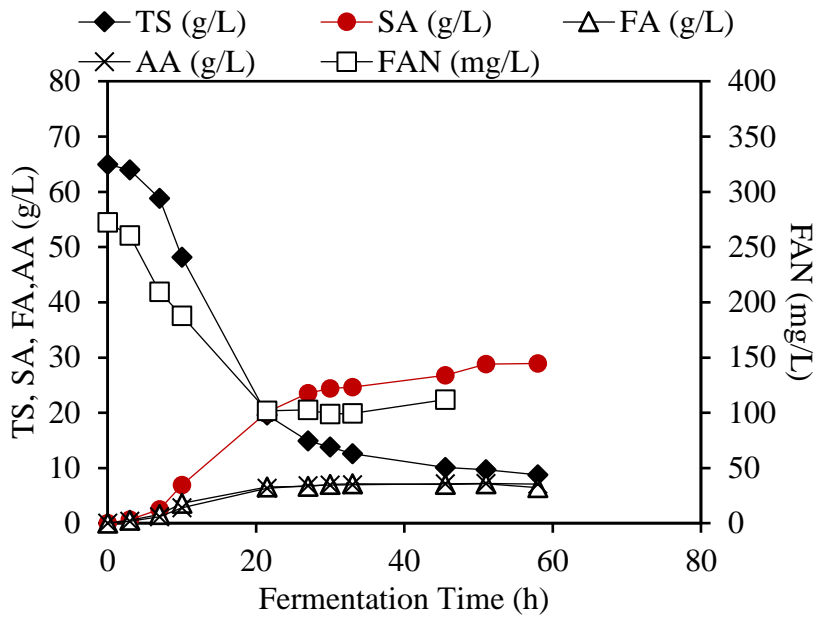


Batch & Fed-Batch Fermentations

Batch Fermentation

Fed batch fermentation, Feeding with pulses

Fed-batch fermentation, Continuous feeding



Succinic Acid (SA): 24.6 g/L
 Formic Acid (FA): 7.1 g/L
 Acetic Acid (AA): 6.9 g/L
 Yield*: 0.47 g/g
 Productivity: 0.75 g/(L·h)

Succinic Acid (SA): 37.0 g/L
 Formic Acid (FA): 3.6 g/L
 Acetic Acid (AA): 8.3 g/L
 Yield*: 0.68 g/g
 Productivity: 0.48 g/(L·h)

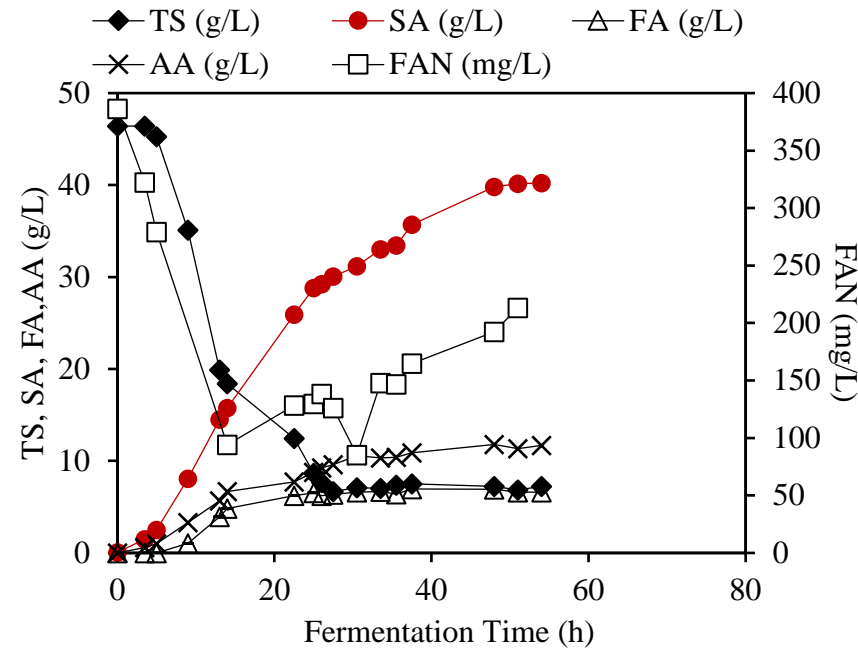
Succinic Acid (SA): 37.8 g/L
 Formic Acid (FA): 5.7 g/L
 Acetic Acid (AA): 7.6 g/L
 Yield*: 0.67 g/g
 Productivity: 0.71 g/(L·h)

*yield was calculated as the grams of sugars consumed divided by the total grams of succinic acid produced during fermentation



Fed-batch fermentation, with YE in feeding solution **INVALOR**

Continuous Feeding supplemented with yeast extract (10%)



Succinic Acid (SA): 40.2 g/L
 Formic Acid (FA): 6.6 g/L
 Acetic Acid (AA): 11.7 g/L
 Yield*: 0.67 g/g
 Productivity: 0.79 g/(L·h)

Fermentation type	Fermentation time (h)	SA (g/L)	Yield (g/g)	Productivity (g/(L·h))	FA:SA	AA:SA	Total by-products: SA
Batch	33	24.6	0.47	0.75	0.29	0.28	0.57
Fed-batch with pulses	76.5	37.0	0.68	0.48	0.10	0.23	0.32
Fed-batch with continuous feeding	53	37.8	0.67	0.71	0.15	0.20	0.35
Fed-batch with continuous feeding & YE	51	40.2	0.67	0.79	0.16	0.29	0.46

*yield was calculated as the grams of sugars consumed divided by the total grams of succinic acid produced during fermentation

A novel process was developed utilising waste streams produced after the winemaking process

- Value-added components (lipids, antioxidants) were isolated from the by-product streams
- The hydrolysis of the pretreated material was successfully performed without the addition of buffer solution
- The addition of BSA in enzymatic hydrolysis acts positively
- Fed-batch fermentations with continuous feeding improved succinic acid production
- The addition of yeast extract in feeding solution increases the concentration of succinic acid, productivity and by-product formation

The valorisation of winery wastes from Agiorgitiko variety leads to the development of sustainable wineries



*THANK YOU FOR YOUR
ATTENTION!*

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