



Optimal utilization of seafood side-streams through the design of new holistic process lines

# RECOVERY OF BIOMOLECULES FROM LIQUID SIDE-STREAMS FROM MUSSEL PROCESSING

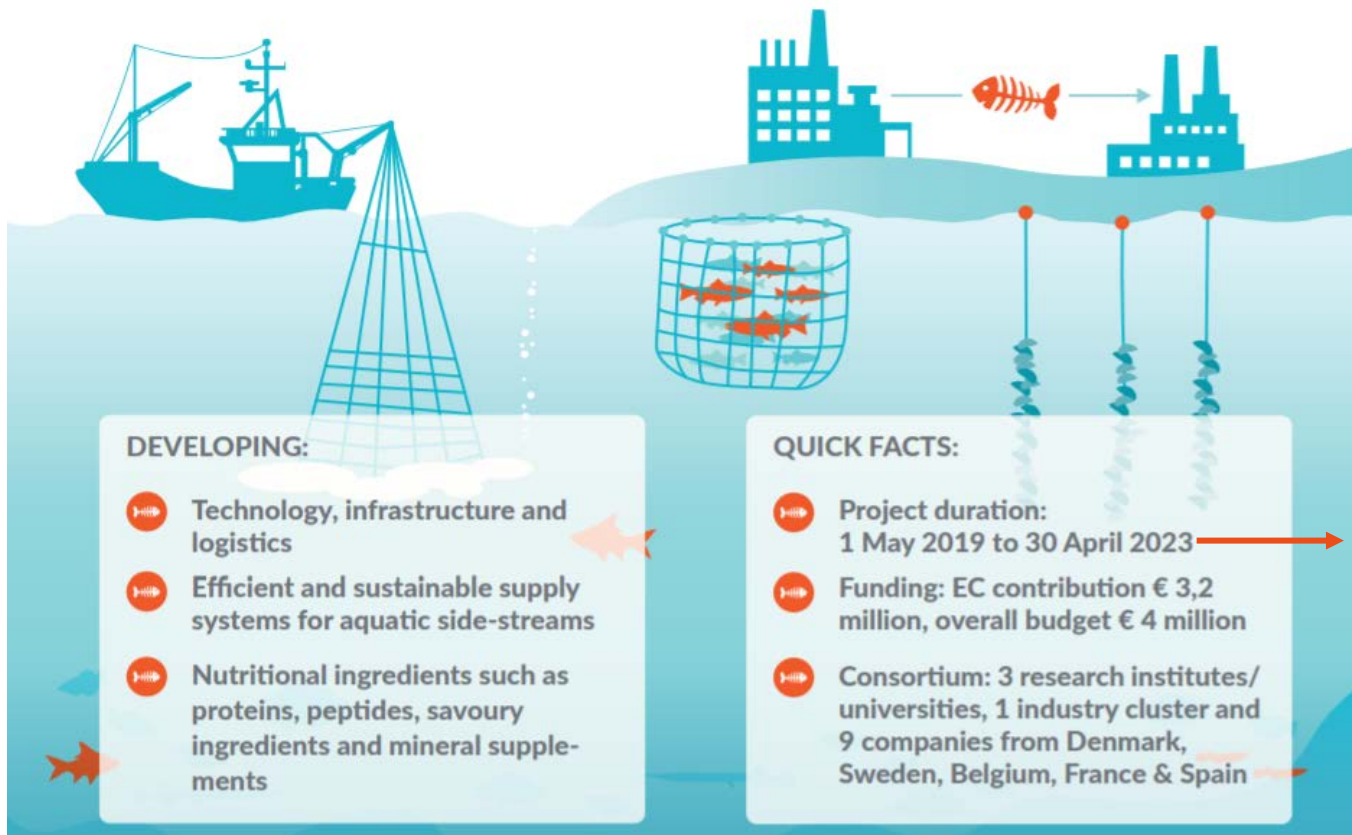
Mónica Gutiérrez, Bruno Iñarra, David San Martín & Carlos Bald



# WaSeaBi: Optimal utilization of seafood side-streams through the design of new holistic process lines



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## COORDINATOR



## PARTNERS



Bio-based Industries Consortium



Horizon 2020  
European Union Funding  
for Research & Innovation

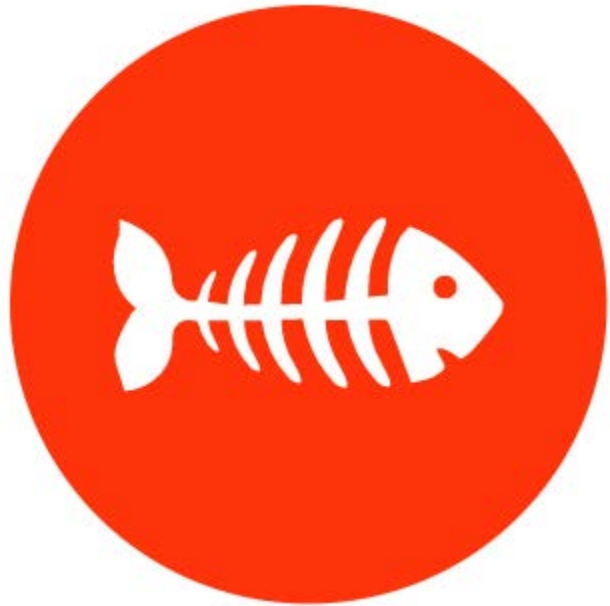
Grant agreement No 837726.



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## The context:

The current exploitation of the aquatic resources is hampered by inefficiency as up to 70 % end up as low-value products or waste, unsustainable considering the rising population.

## WaSeaBi Objective:

Ensure that side-streams from aquaculture, fisheries and aquatic processing industries can be exploited for production of new products and ingredients. By **developing storage solutions, sorting technologies and decision tools** that will secure an efficient, sustainable supply system for

Efficient and Sustainable Supply Systems for Aquatic Side-Streams

Nutritional ingredients

Proteins, peptides, savoury ingredients and mineral supplements

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## 6 different side-streams:

Representing typical **aquaculture, fisheries and aquatic processing industries** in Europe:

Side-stream	Potential use
Solid side-stream from Cod industry	Food ingredient
Brine from salted Cod	Protein for reinjection/in-house use
Solids & process water from herring	Food ingredients
Salmon solids, mackerel, by-catches	Food & Feed ingredients
Mussel cooking water	Food ingredients (Savoury compounds)
Mussel shells	Food & Feed ingredients (mineral supplements)

WaSeaBi will take a whole chain perspective to succeed with **high quality production of:**

- Bioactive peptides for nutraceutical, food and feed application
- Protein-based food ingredients
- Savory ingredients and mineral supplements for food and feed



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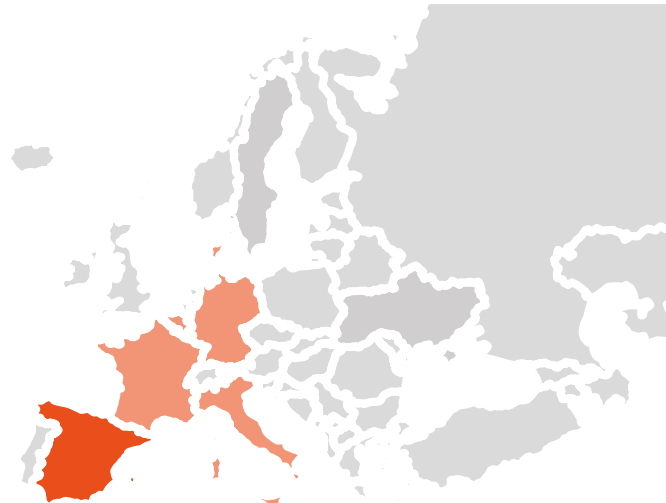


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## Some facts about mussel production:

- The European Union is the **second largest producer** after China (EUFOMA 2019)
- In the north-West of Spain, the **annual production** of mussels is 200 000 tonnes (35 % of the world) (Bello 2012)
- The industrial thermal treatment of mussels generates between **300 and 400 L/t wastewaters** that are continuously disposed into the sea without previous treatment (Prieto 2015)



## Objectives:

- 🐟 Optimization of direct concentration of high value molecules
- 🐟 Estabilization of high molecules extracts
- 🐟 Evaluate the use of this concentrates for savory compounds uses

- Bello P.M *et al.* Material Flow Analysis in a cooked mussel processing industry. Journal of Food Engineering 113 (2012) 100–117.
- EUMOFA. Case study: Fresh mussel in the EU (2019) Publications Office of the European Union, [www.eumofa.eu](http://www.eumofa.eu), doi:10.2771/862.
- Prieto M.A., *et al.* (2015) "An environmental management industrial solution for the treatment and reuse of mussel wastewaters. Sci. Tot. Environ. 538 117–128.

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## Steps for biomolecules recovery:



Optimization of direct concentration of high value molecules



Estabilization of high molecules extracts



Evaluate the use of this concentrates for savoury compounds uses

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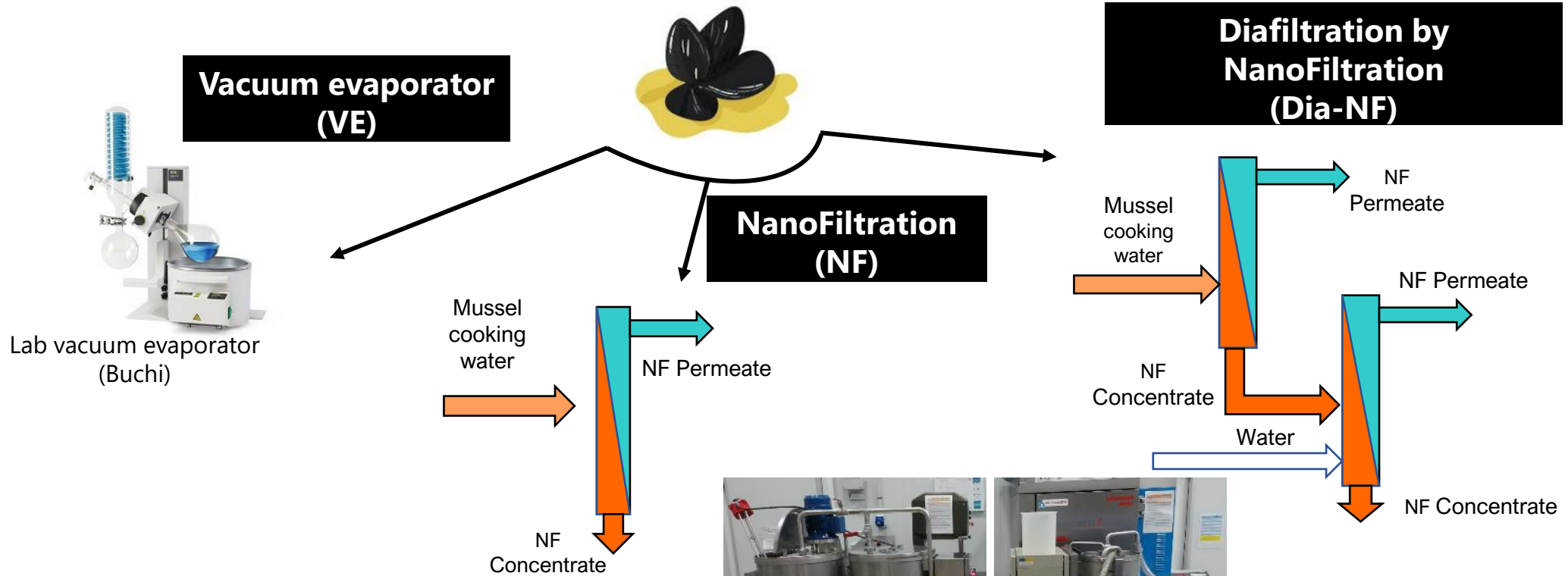
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## Concentration techniques:



Homogenization and heating reactor



Nanofiltration pilot plant



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## Analytical and microbiological control:

### Quantitative Composition

Protein
Ashes (%)
Humidity (%)
COD (mgO <sub>2</sub> /l)
Chloride (mg/l)

### Microbial composition

Salmonella spp (Inv/25 g)
Listeria monocytogenes (Inv/25 g)
Aerobios mesófilos (ufc/g)
Enterobacterias (ufc/g)
Escherichia coli (ufc/g)

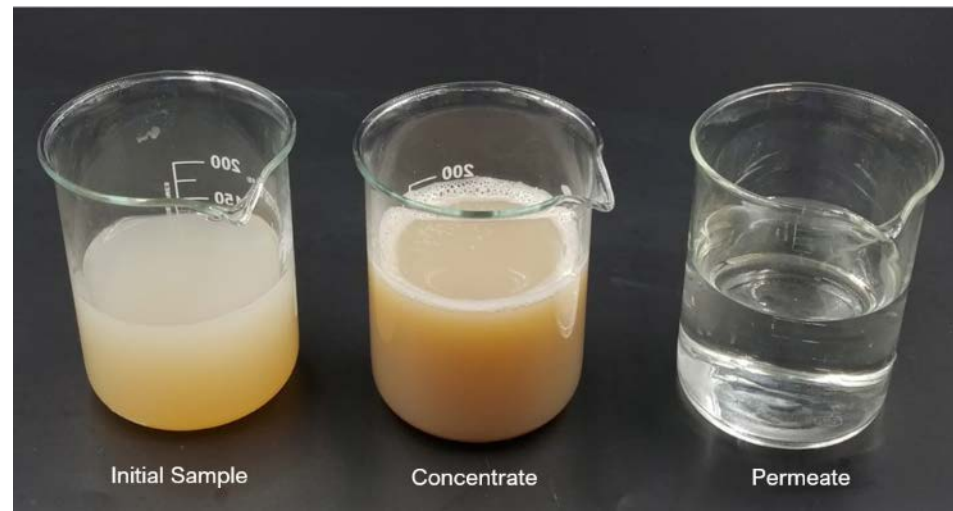
### Others

Protein content
Free Aa
Total Aa
Molecular weight distribution

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## RESULTS

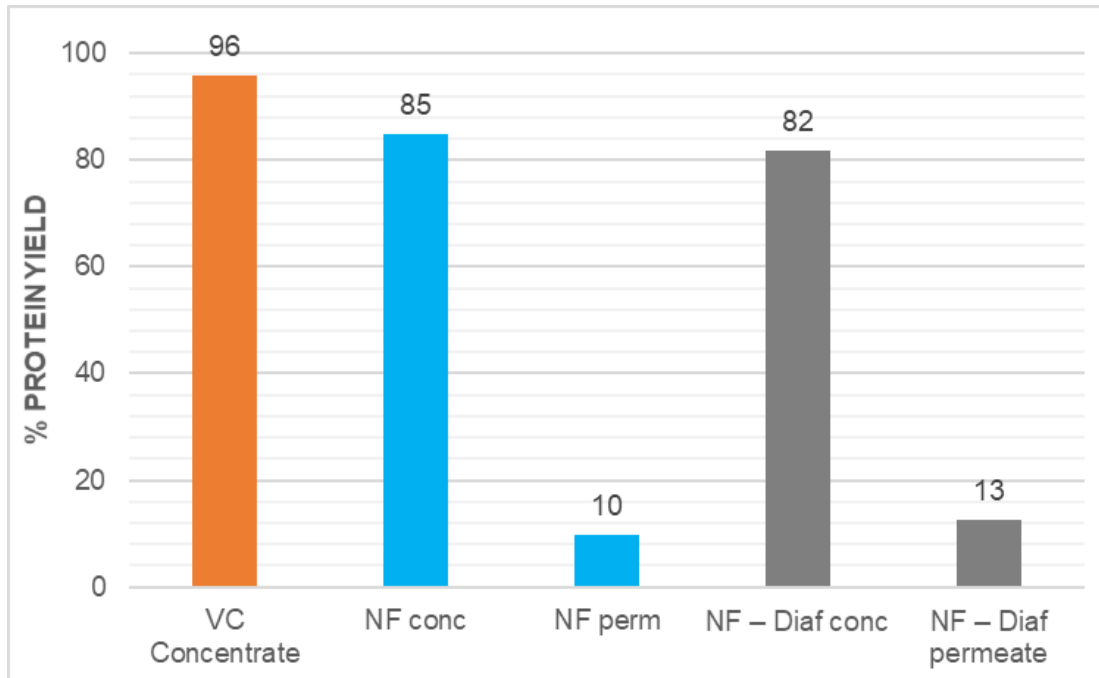
	Initial sample	VC Concentrate	NF concentrate	NF permeate	NF – Diaf concentrate	NF – Diaf permeate
Ashes (%)	2,38	<b>24,48</b>	2,40	2,42	1,20	2,20
Dry matter (%)	4,09	<b>39,66</b>	9,13	2,47	7,40	2,31
Protein (%)	1,14	<b>10,98</b>	4,85	0,14	4,68	0,12
Free Aa (%)	0,33	3,23	1,19	0,12	1,14	0,10
Chloride (g/l)	14,10	<b>138,18</b>	13,96	14,24	<b>7,12</b>	12,94
COD (mgO <sub>2</sub> /l)	22200	224000	104800	2260	111000	2040



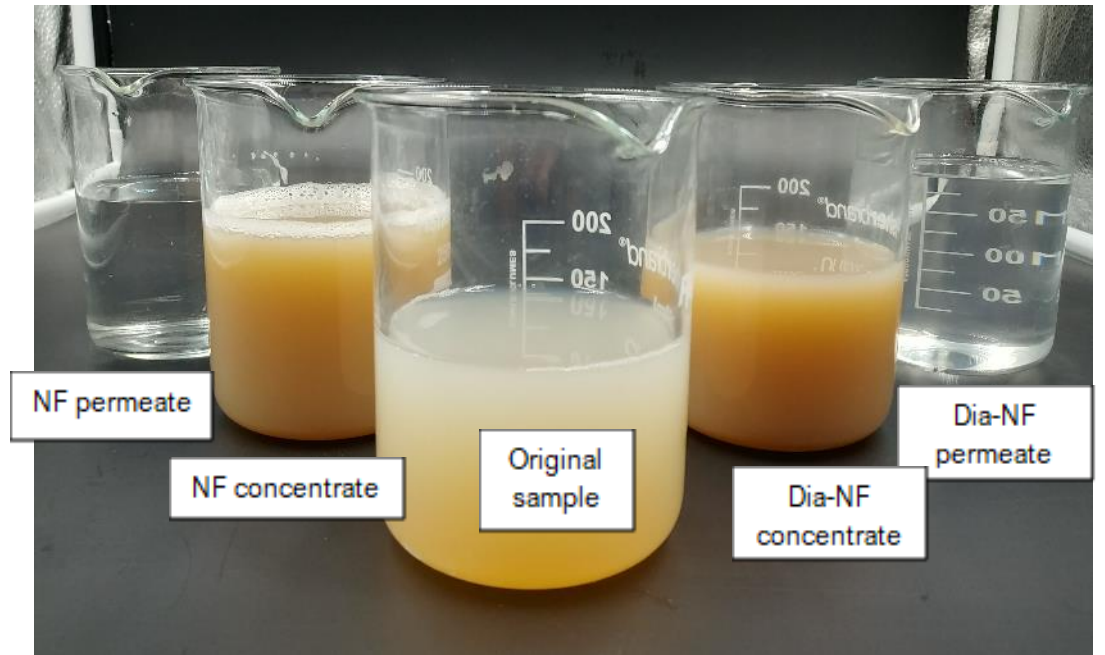
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Optimization of direct concentration of high value molecules



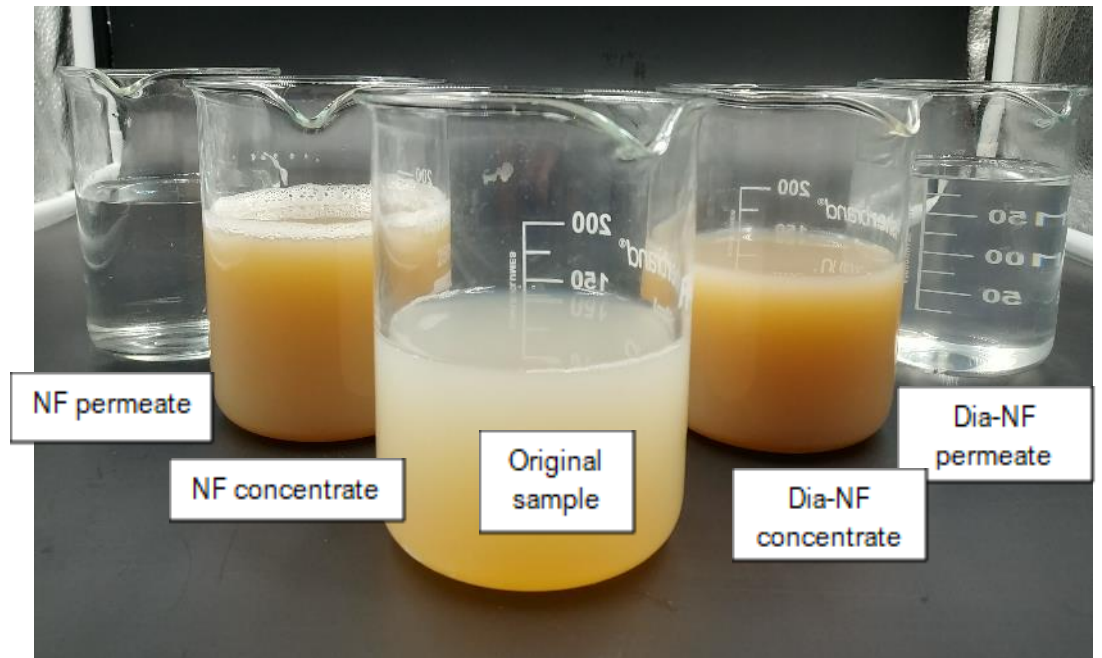
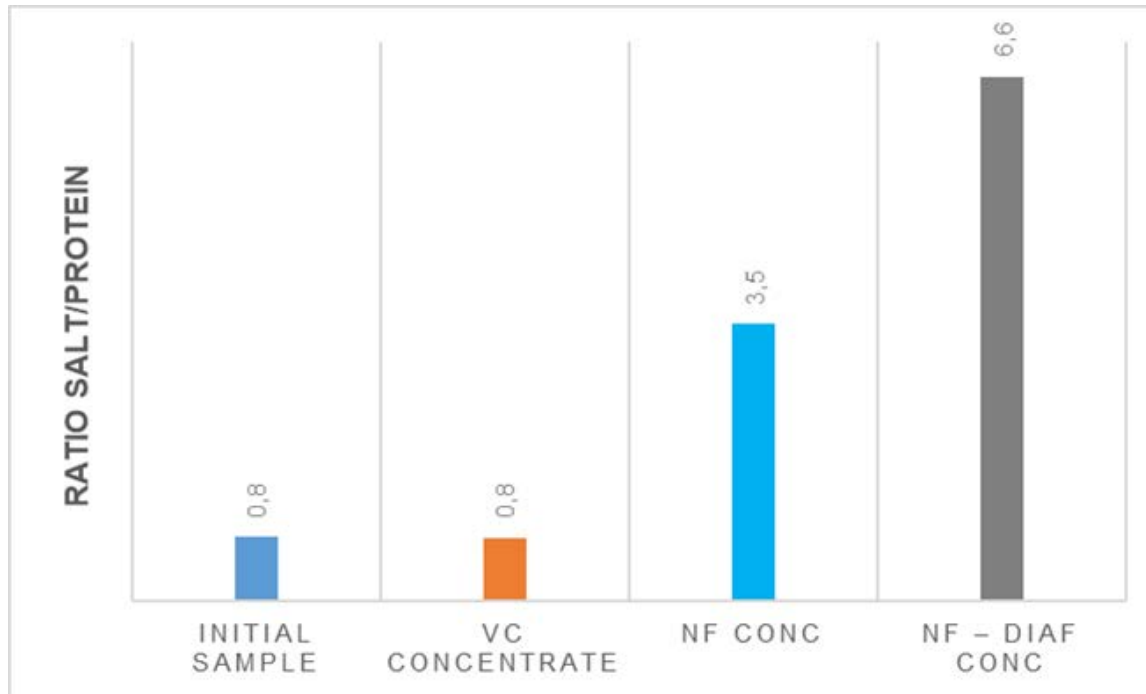
Protein yield for the different concentration techniques tested



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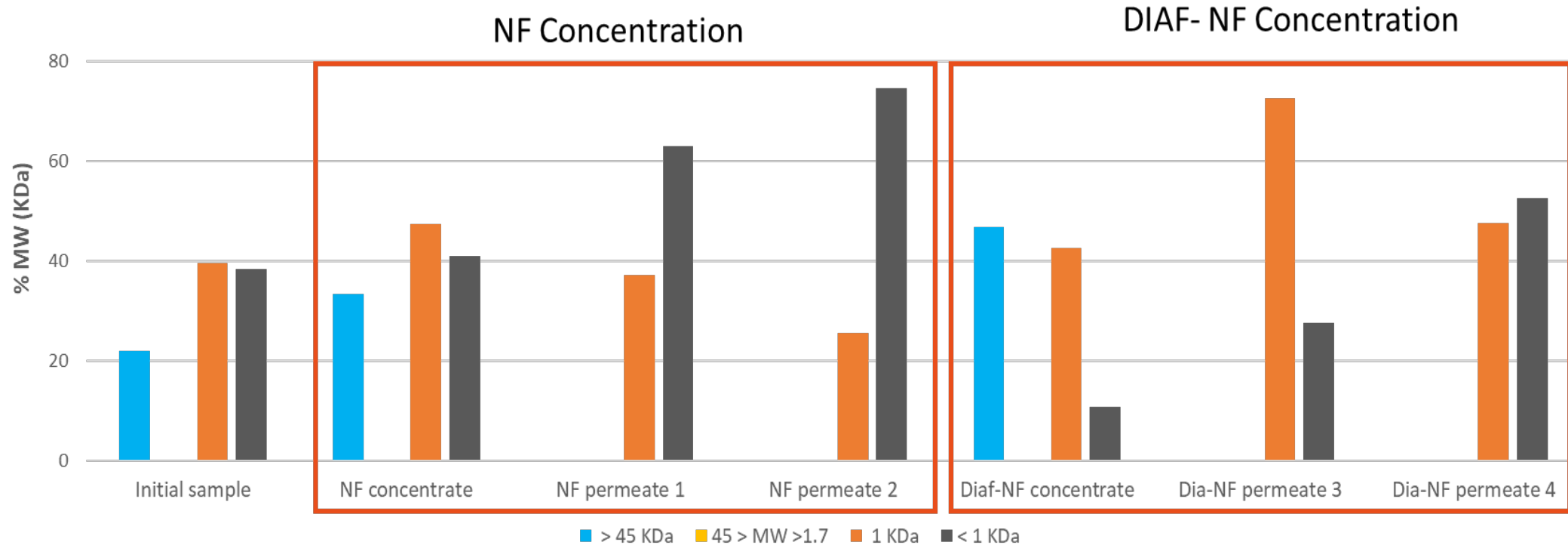


Protein/salt ratio of the different concentration techniques tested

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Optimization of direct concentration of high value molecules



Molecular weight profile of NF and Diafiltration fractions

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## Steps for biomolecules recovery:



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Estabilization of high molecules extracts



Evaluate the use of this concentrates for savory compounds uses

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Estabilization of high molecules extracts



Optimal Dryer parameters	Value
T inlet	165 °C
T outlet	68 °C
Pump rate	10 %
Aspirator rate	100 %
Spray air flow	25 mm

**Humedad** 6,4 % ± 0,3 %

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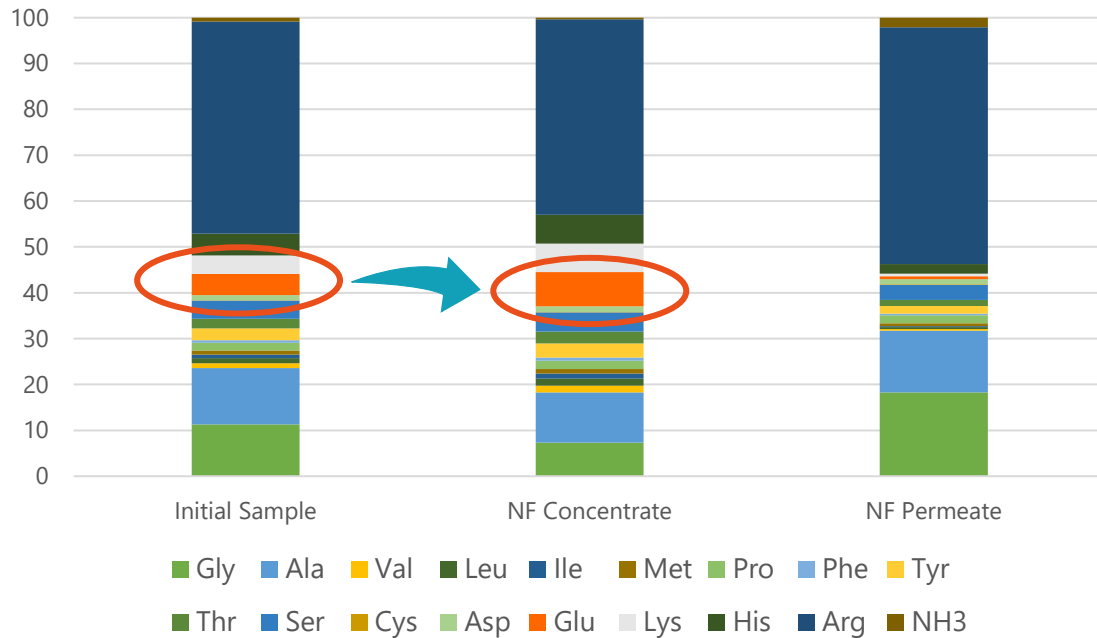


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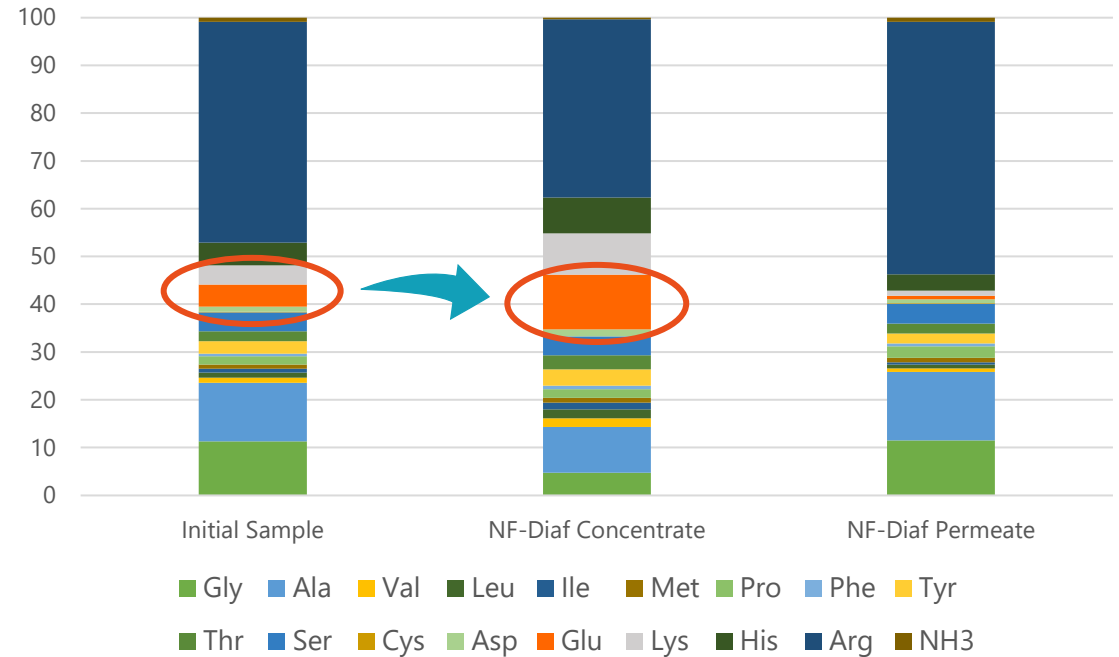


Evaluate the use of this concentrates for savoury compounds uses

Free Aa Distribution in NF filtration



Free Aa Distribution in NF-Diaf Filtration



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## Conclusions

- 🐟 Different separation techniques had been tested: NF and Diafiltration-NF membrane filtration and vacuum evaporation
- 🐟 The best concentration system for protein concentration was the vacuum technology, that concentrate proteins almost 10 times
- 🐟 The problem of vacuum concentration is the high value of salt in the solution, so that, it is necessary to find a technique to remove NaCl
- 🐟 Both NF techniques yielded lower result in protein recovery, due to the permeation of small molecular weight proteins ( $\leq 0.1$  KDa)
- 🐟 The resulting NF permeate still had an organic load in the final effluent, but reduced enough to be discharged within the regulatory frame

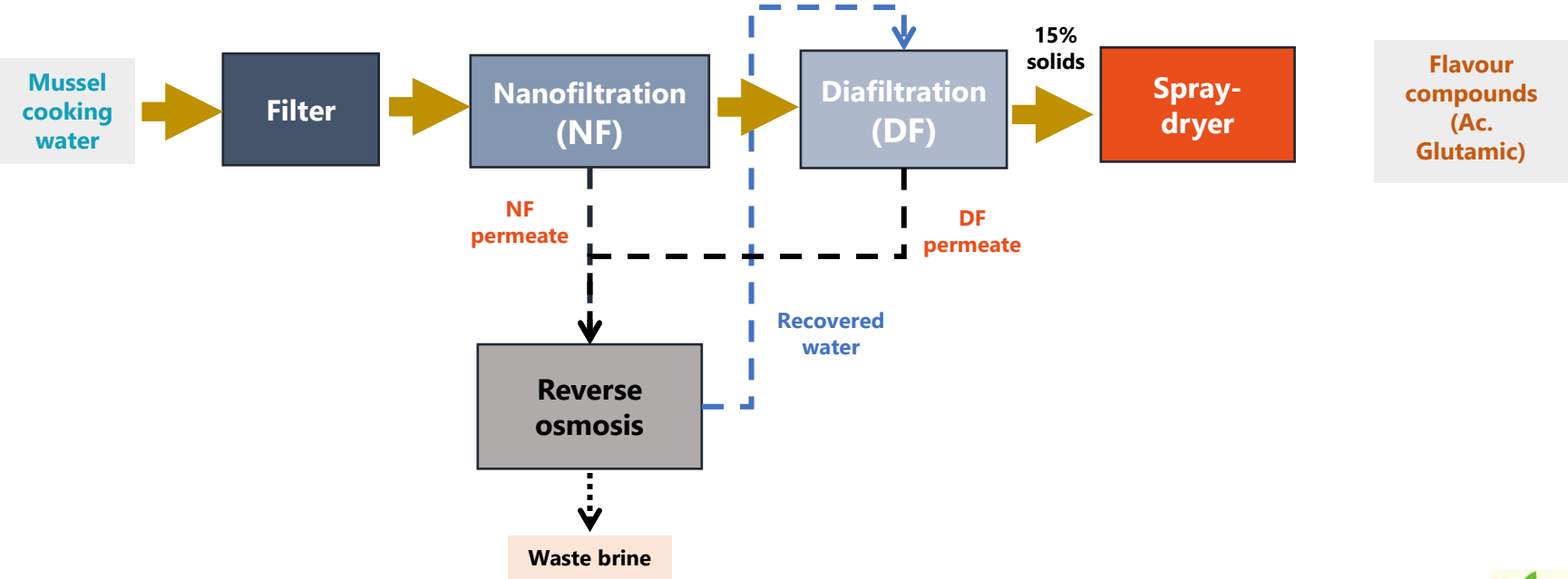
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## Conclusions

🐟 The best option for biomolecule recovery from mussel cooking waters was the next:





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# THANK YOU

# ANY QUESTION?

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Consortium



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