

Effect of methanol-organosolv pretreatment on anaerobic digestion of lignocellulosic materials



Armando Oliva, Lea Chua Tan, Stefano Papirio, Giovanni Esposito, and Piet N. L. Lens

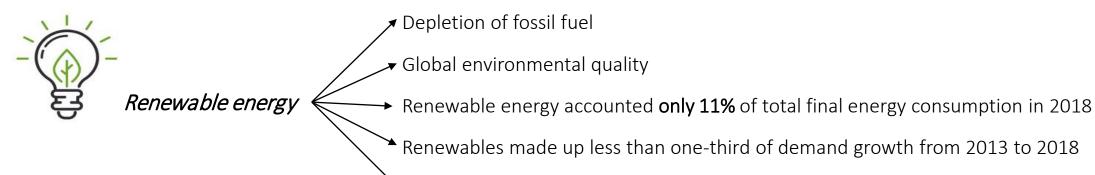


8TH INTERNATIONAL CONFERENCE ON SUSTAINABLE SOLID WASTE MANAGEMENT

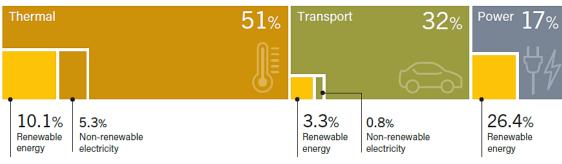
24 June 2021

Overview

Biogas



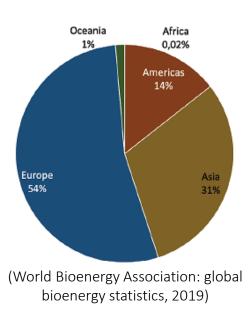
The world is not on track to limit global warming



(REN21: Renewable global status report, 2020 – Data from 2017)

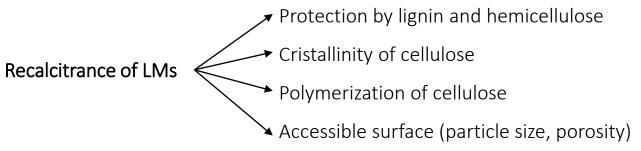
- ✓ Few atmospheric pollutants per unit
- Several applications
- Line distribution already in place
- ► Globally, domestic supply of biogas was 62 million Nm³ in 2017
- Global electricity generation from biogas increased of 90% (2010-2016)

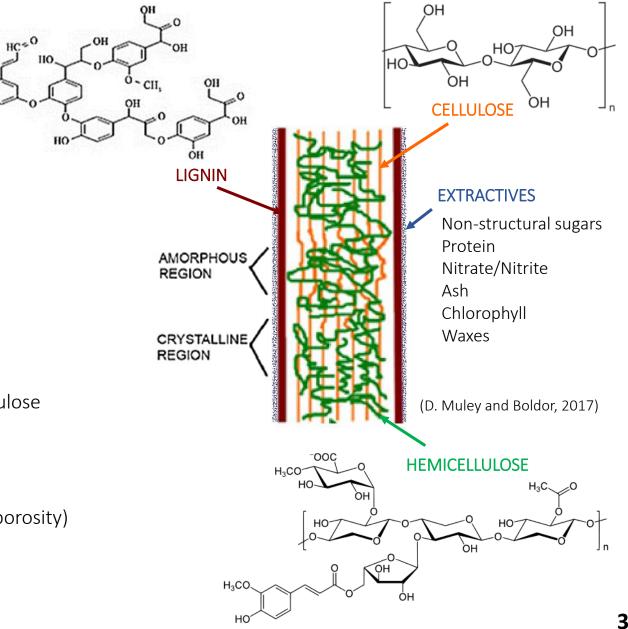
We are exploiting **only 1.6-2.2%** of the potential of anaerobic digestion



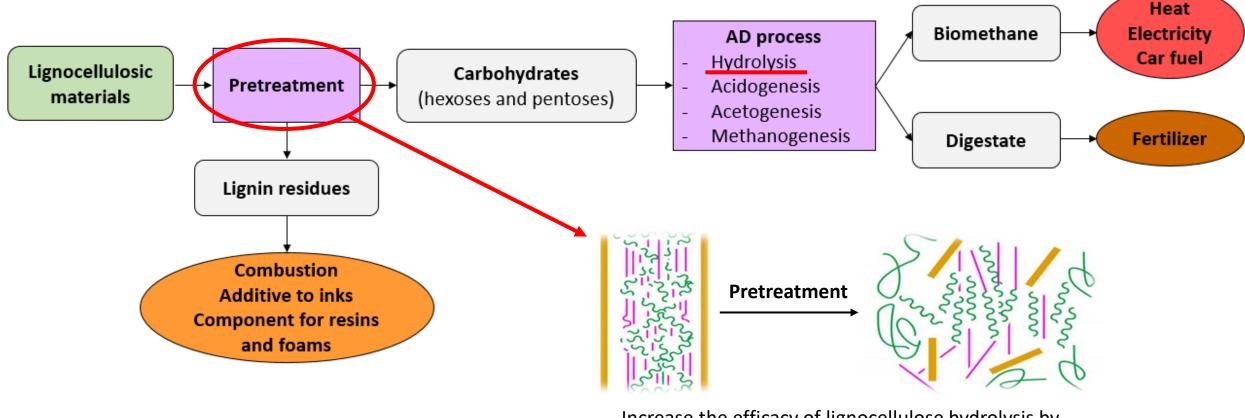
Lignocellulosic composition

- Most abundant bio-resource ٠
- 2×10^5 Mt of biomass are globally produced every year ٠
- 1000 Mt of dry matter are produced annually in the EU ٠
- Low-cost waste materials ۲
- No competition between food and energy production ٠





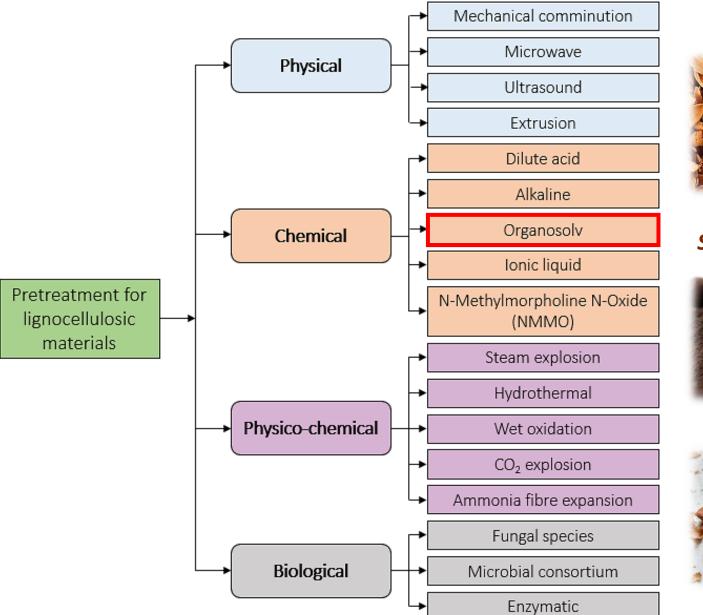
Anaerobic digestion process



Increase the efficacy of lignocellulose hydrolysis by improving the accessibility to cellulose

- Removing lignin and/or hemicellulose
- Decreasing the degree of polymerization and crystallinity of the cellulosic component of biomass

Pretreatment methods and raw substrates





Spent coffee grounds





1.2 million tons/year+ 24% over prior 10 year average≈ 70% of the total weight is shell

23% cellulose 22% hemicellulose 31% lignin

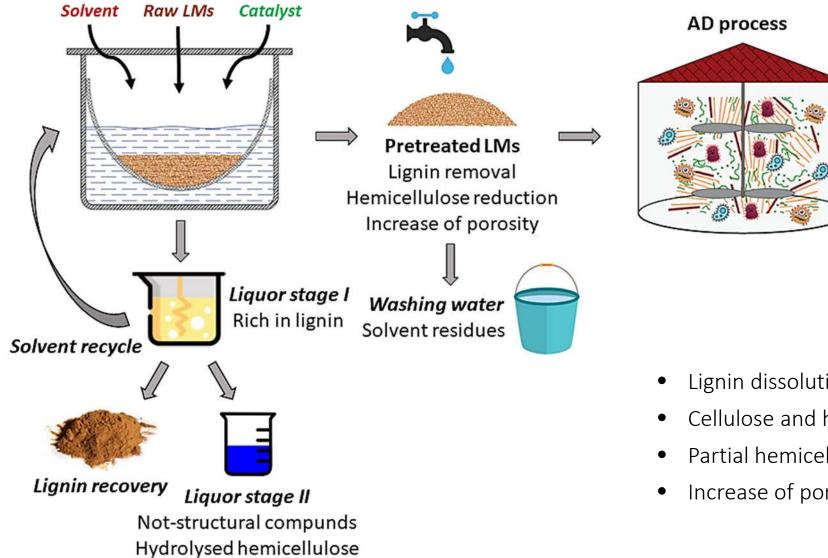
6 million tons/year + 1.3% per year in the last decades ≈ 50% of the fruit mass became a waste

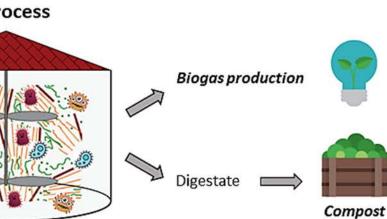
> 9% cellulose 34% hemicellulose 20% lignin

0.5 million tons/year + 16% over prior 10 year average High bulk density

10% cellulose4% hemicellulose40% lignin

Organosolv pretreatment



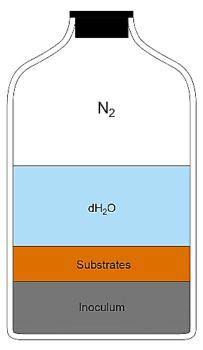


- Lignin dissolution
- Cellulose and hemicellulose in the solid phase
- Partial hemicellulose hydrolysis
- Increase of porosity

Experimental set-up: pretreatment and anaerobic digestion



Salvant	Catalyst	Temperature	Time	Substrate/Solvent
Solvent		(°C)	(min)	(w/v)
50% Methanol	/	130	60	20/200
50% Methanol	/	160	60	20/200
50% Methanol	/	200	60	20/200
50% Methanol	$0.01 \mathrm{M} \mathrm{H}_2 \mathrm{SO}_4$	130	60	20/200
50% Methanol	$0.01 \mathrm{M} \mathrm{H}_2 \mathrm{SO}_4$	160	60	20/200
50% Methanol	$0.01 \mathrm{M} \mathrm{H}_2 \mathrm{SO}_4$	200	60	20/200
	50% Methanol 50% Methanol 50% Methanol 50% Methanol	50% Methanol / 50% Methanol 0.01M H ₂ SO ₄ 50% Methanol 0.01M H ₂ SO ₄	Solvent Catalyst (°C) 50% Methanol / 130 50% Methanol / 160 50% Methanol / 200 50% Methanol 0.01M H ₂ SO ₄ 130 50% Methanol 0.01M H ₂ SO ₄ 160	Solvent Catalyst (°C) (min) 50% Methanol / 130 60 50% Methanol / 160 60 50% Methanol / 200 60 50% Methanol / 200 60 50% Methanol 0.01M H ₂ SO ₄ 130 60 50% Methanol 0.01M H ₂ SO ₄ 160 60



Mesophilic AD \rightarrow 37 °C Wet AD \rightarrow 2% TS Inoculum/Substrate \rightarrow 1.5 g VS/g VS

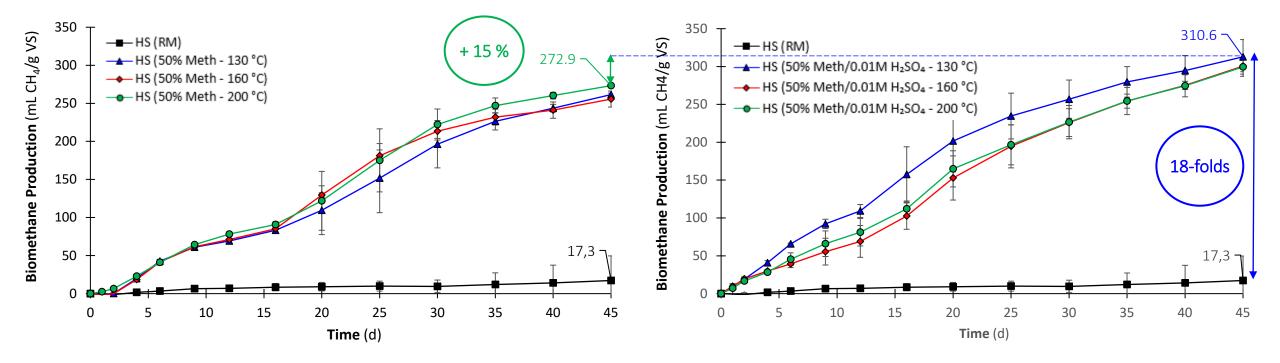
Inoculum \rightarrow Granular Sludge

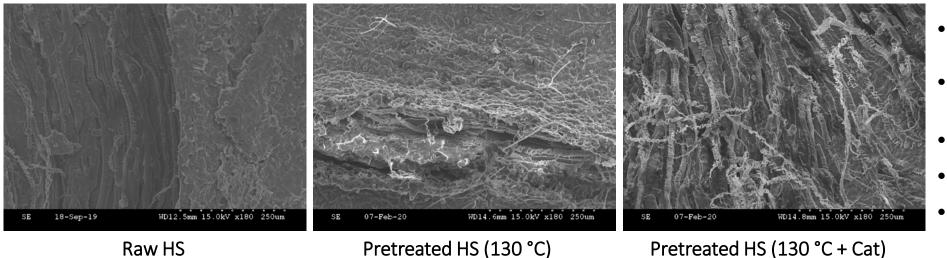
Substrates → Hazelnut skin Spent coffee grounds Almond shell

Working Volume \rightarrow 150 mL Head Space Volume \rightarrow 100 mL



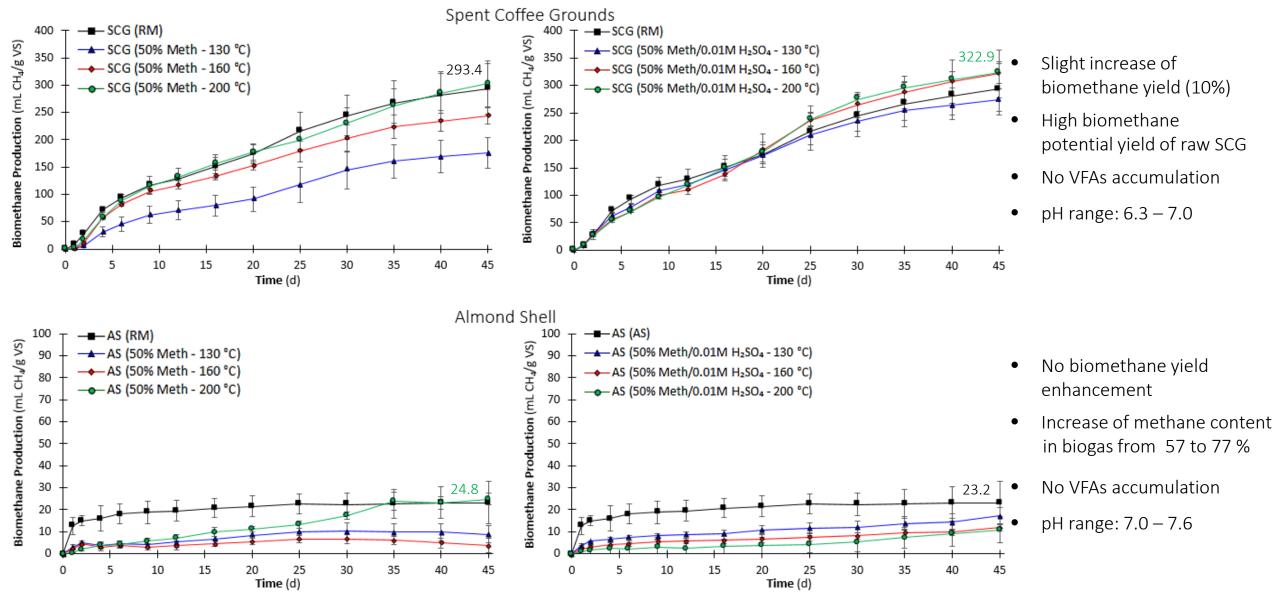
Methane production: Hazelnut skin



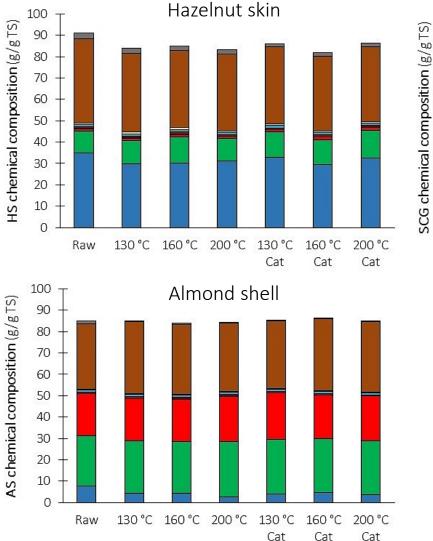


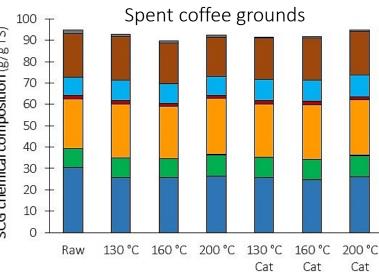
- Significant biomethane production enhancement
- Increase of methane production with catalyst addition
- Amorphous aspect of treated HS
- No VFAs accumulation
- pH range: 6.3 7.0

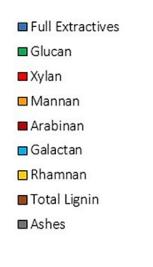
Methane production: Spent coffee grounds and almond shell



Effect on chemical composition







Recalcitrant nature of the three raw substrates: Hazelnut skin: 40% lignin, 14% sugars Spent coffee grounds: 20% lignin, 42% sugars Almond shell: 31% lignin, 45% sugars

Pretreated hazelnut skin

- 7-12% lignin removal from hazelnut skin
- Sugar content increased from 13.7 to **17.3%**
- Strong inverse correlation between lignin content and cumulative methane production

Pretreated spent coffee grounds

- Slight increase of sugars content
- The maximum lignin removal was **10%**

Pretreated almond shell

• No significant effect



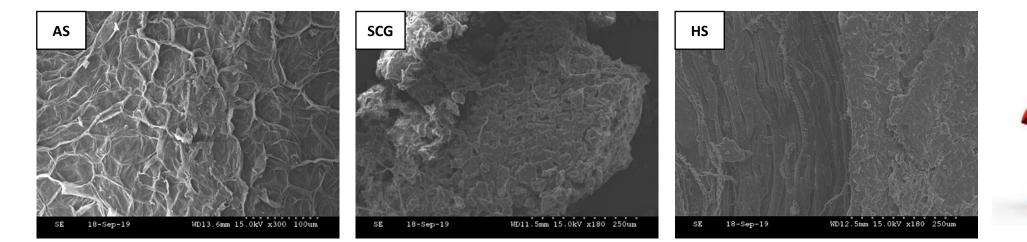
Why is the organosolv pretreatment failing for AS and SCG?

Lignin Content Almond Shell: 30.58 (± 0.13) g/g TS Spent Coffee Grounds: 20.31 (± 0.29) g/g TS

Chemical composition

Loss of non-structural compounds during the pretreatment (sucrose, glucose, fructose)

 $AS = 1.40 (\pm 0.10) g/g$ Water swelling capacity $SCG = 2.76 (\pm 0.06) g/g$ HS = 5.53 (± 0.49) g/g *Physical characteristics* → Porosity < Surface morphology (SEM)



Conclusions and future prospective

- OMethanol-organosolv pretreatment was **particularly effective** to enhance biogas production for hazelnut skin
- Methanol-organosolv pretreatment was slightly effective for spent coffee grounds and ineffective for almond shell
- Catalyst addition enabled to gain a higher methane production from hazelnut skin with the lowest pretreatment temperature
- ✓ The economic viability of the pretreatment for hazelnut skin is confirmed by the energy assessment, with a net positive energy recovery of 1.35 kWh/kg VS deriving from the extra biomethane produced under the optimal pretreatment condition
- 4
- Maximize and optimize lignin recovery from pretreatment liquor
- Verify the economic viability of the recovery of valuable compounds before undergoing pretreatment and anaerobic digestion (proteins, phenolic compounds, lipids, non-structural sugars)
- Further studies are required to explore **different pretreatments** able to raise the biomethane potential of spent coffee grounds and almond shell (ionic liquid, milling)

THANK YOU

