

*8<sup>th</sup> International Conference on Sustainable Solid Waste Management*

*24 June 2021*

## Effect of char recirculation in fixed bed gasifiers: experimental and modelling analysis

*Francesco Patuzzi<sup>1</sup>, Daniele Antolini<sup>1</sup>, Stergios Vakalis<sup>2</sup>, Marco Baratieri<sup>1</sup>*

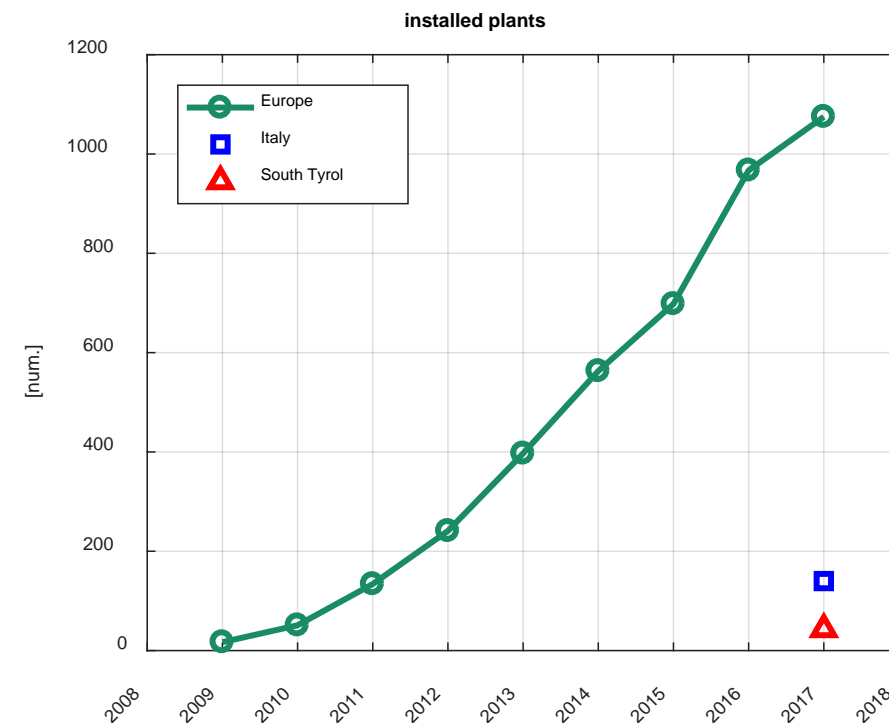
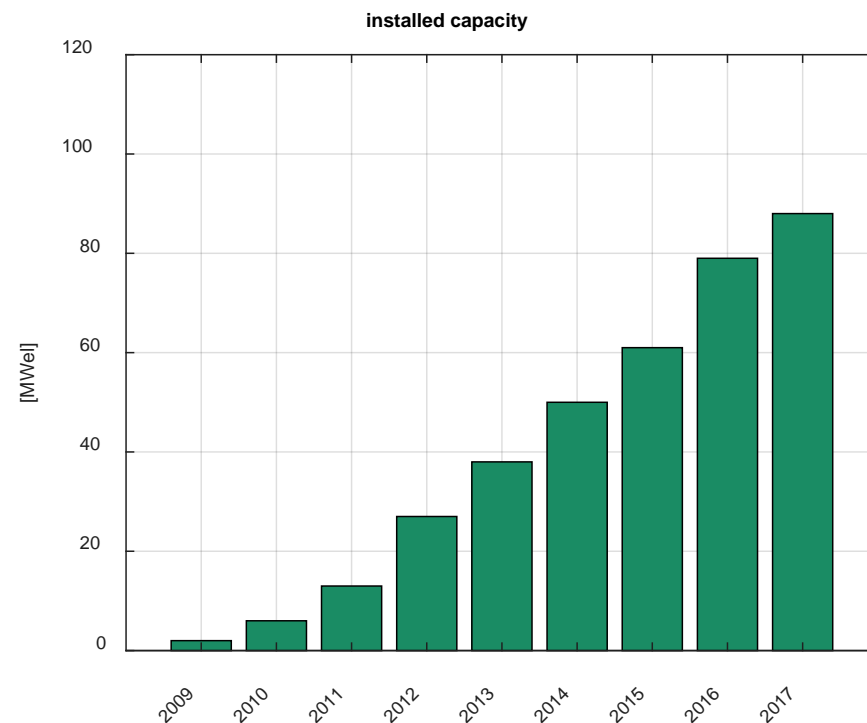
*<sup>1</sup> Faculty of Science and Technology, Free University of Bozen-Bolzano, Italy*

*<sup>2</sup> University of the Aegean, Mytilene, Greece*

## Small-scale biomass gasification in EU

Size of the plants < 0.5 MW<sub>el</sub>  
 Number of installed plants > 1000

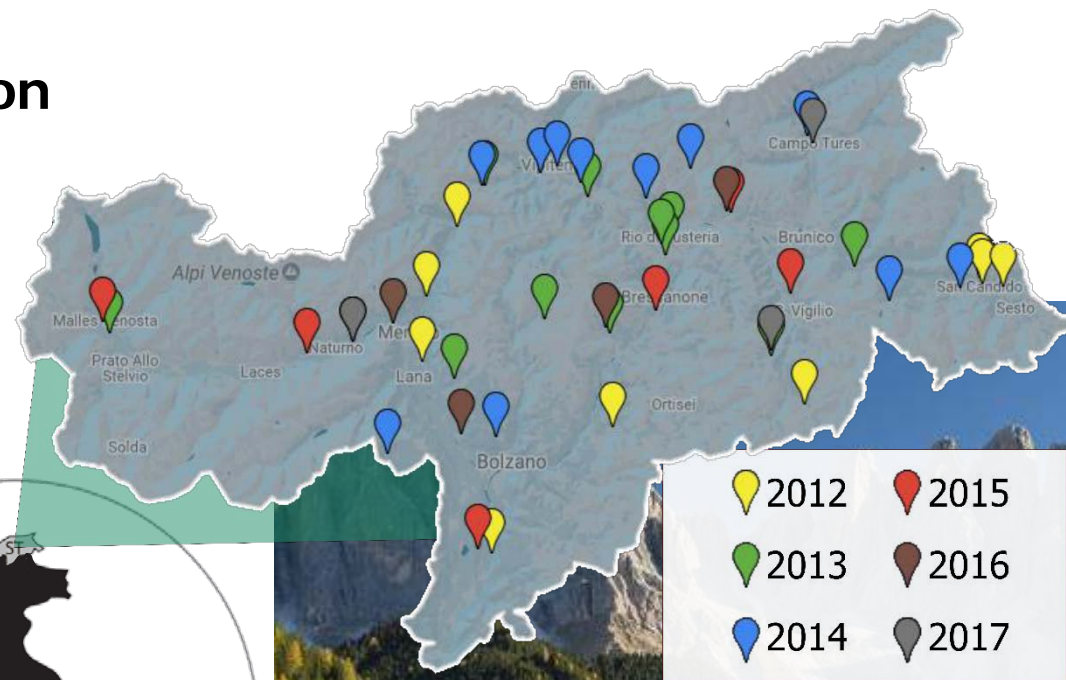
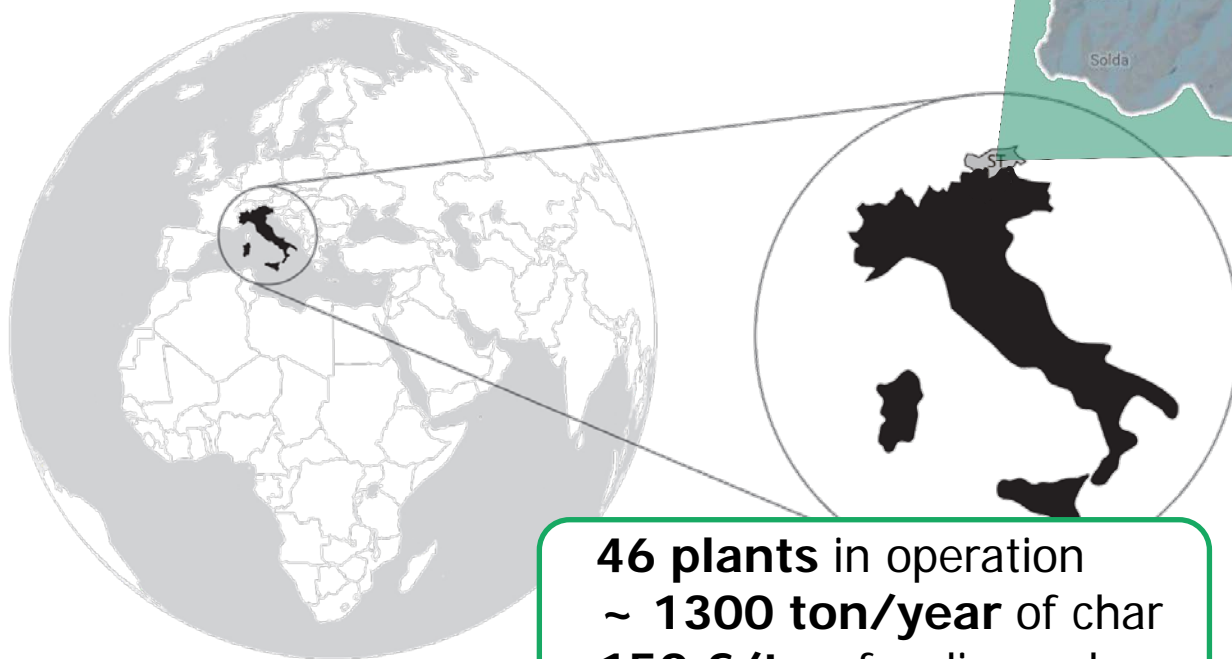
Application: CHP (feed in tariff)  
 Technology: fixed bed gasifiers



Source: 2018 - IEA bioenergy Task 33

## The South Tyrol (Südtirol) region

Area: 7400 km<sup>2</sup>  
Population: 511750 ab.  
42% forest



**46 plants in operation**  
**~ 1300 ton/year of char**  
**150 €/ton for disposal**



## Possible utilization pathways

Many possible application are reported in the literature

- for co-firing in power plants
- as soil improver
- as adsorbent
- as catalytic support



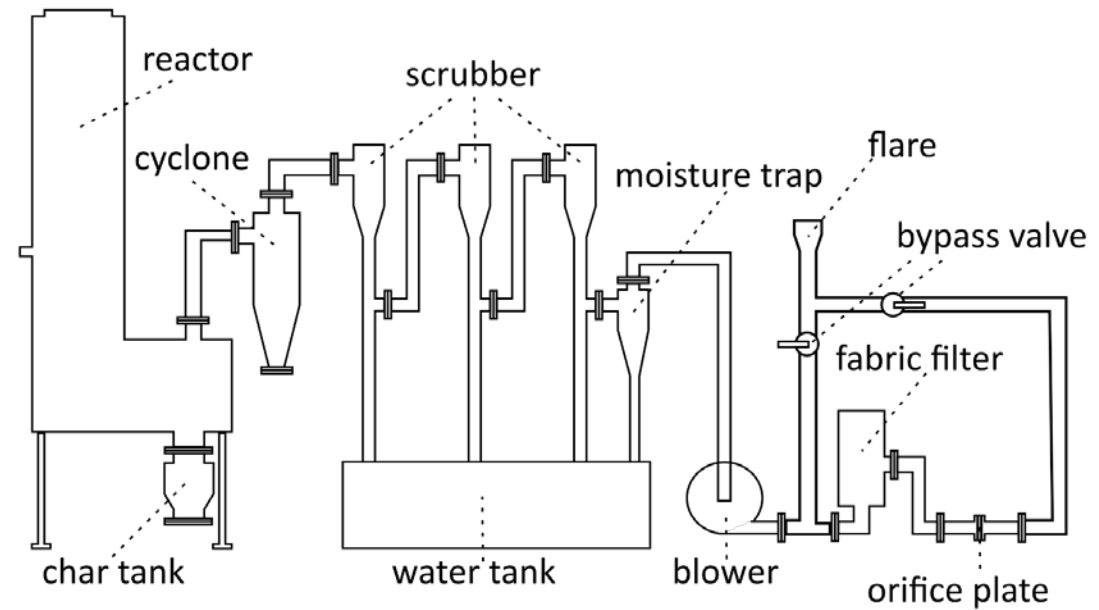
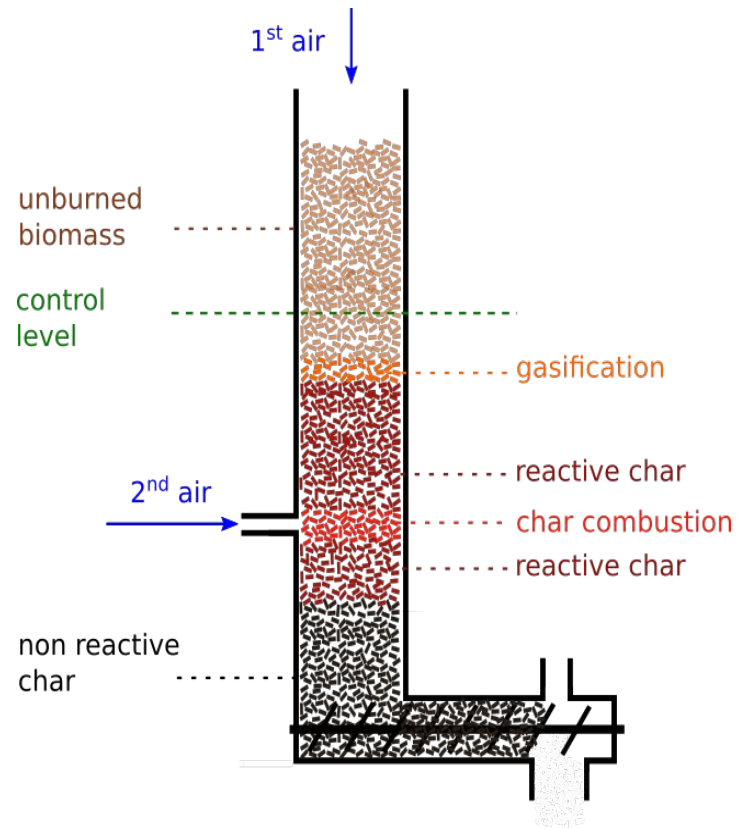
**THE AIM OF THIS WORK** is  
to investigate the effect of  
**recirculating char**  
in fixed bed gasification systems

## Open-top gasifier

Fixed bed reactor – Nominal size:  $4 \text{ kg}_{\text{biom}}/\text{h}$



## Open-top gasifier



## **Measured quantities and characterized properties**

- Mass IN
- Mass OUT
- Charge and discharge time
- Secondary air mass flow rate (mass flow controller)
- Producer gas flow rate (differential pressure over a calibrated orifice)
- Gas composition (microGC)

## **Derived quantities and process parameters**

- Biomass and char mass flow rates
- Total air IN (nitrogen balance)
- Equivalence Ratio
- Energy fluxes
- Cold Gas Efficiency

## Fuel characterization

Standard spruce pellet EN plus A1 – 6 mm diameter

- moisture content
- ash content
- elemental analysis C,H,N,S (Vario MACRO Cube, Elementar)
- HHV - LHV (C 200 - IKA)

Moisture	Ash	C	H	N	S	O	LHV
[%wt <sub>ar</sub> ]		[%wt <sub>dry</sub> ]					[MJ/kg <sub>dry</sub> ]
7.1	0.3	49.8	5.6	0.1	0.4	43.8	16.9





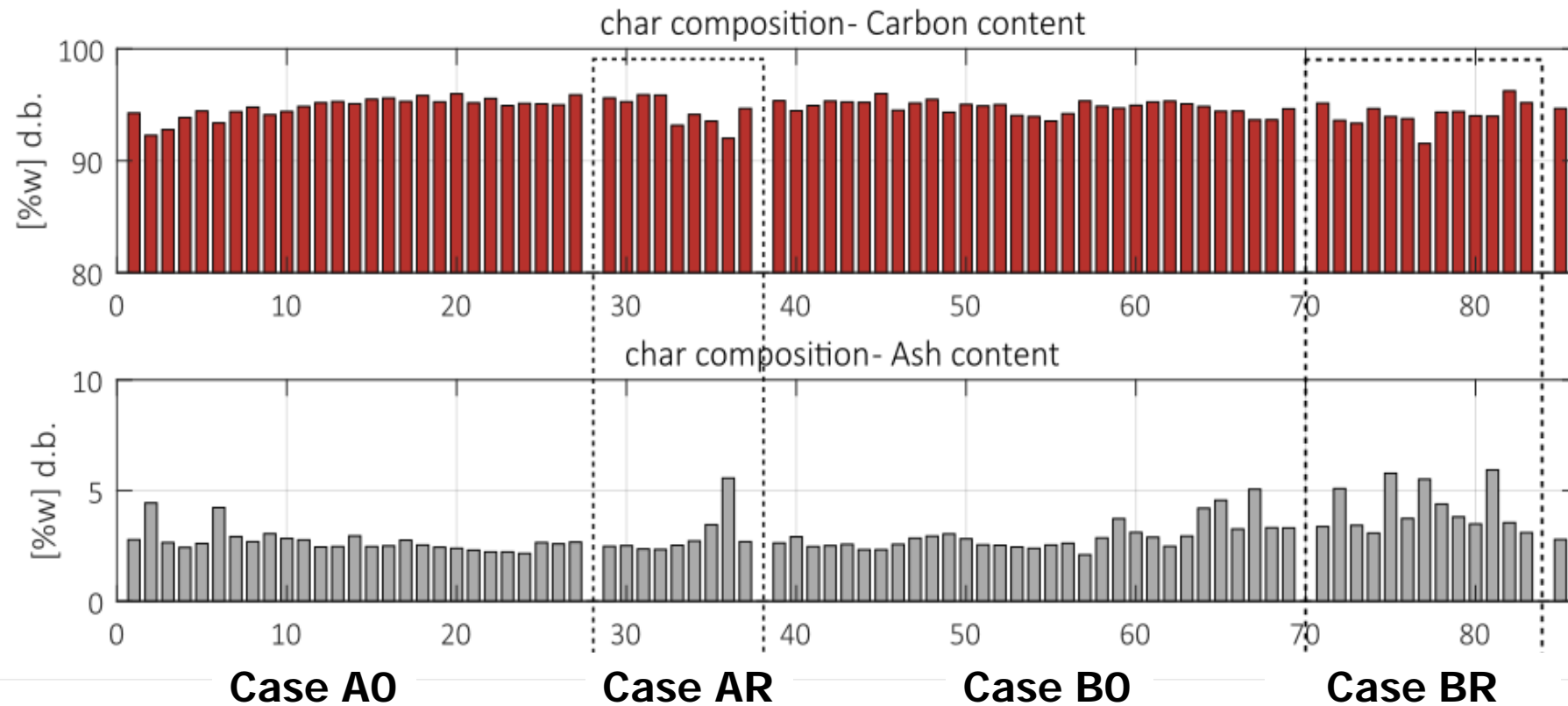
## Study cases

	char yield / recirc. share	2 <sup>nd</sup> air injected	Blower SP	ER (when the fuel is only biomass)
	[%]	[NLPM]	[Hz]	[-]
<b>Case A</b>	~ 10	10	40	< 0.25
<b>Case B</b>	~ 5	26	40	~ 0.25

### Sub-cases

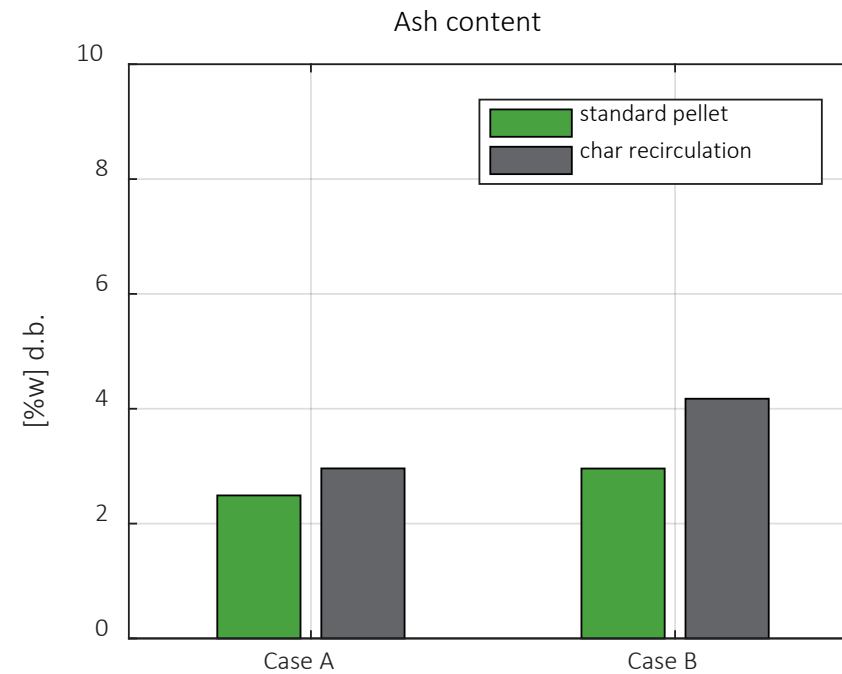
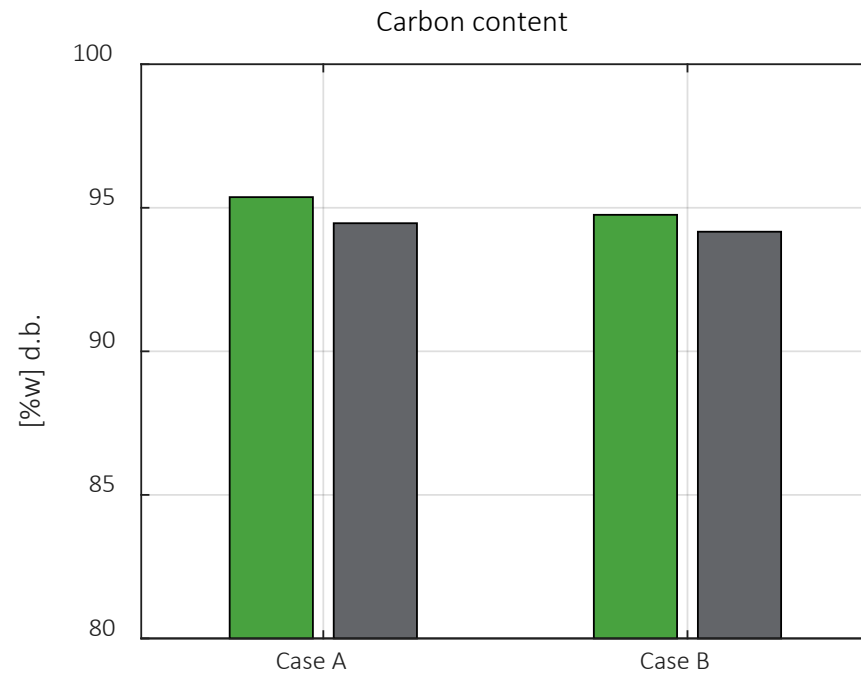
- **O:** fuel IN = standard pellet (biomass)
- **R:** fuel IN = standard pellet (biomass) + char (produced in the corresponding sub-case 0)

## Char characterization



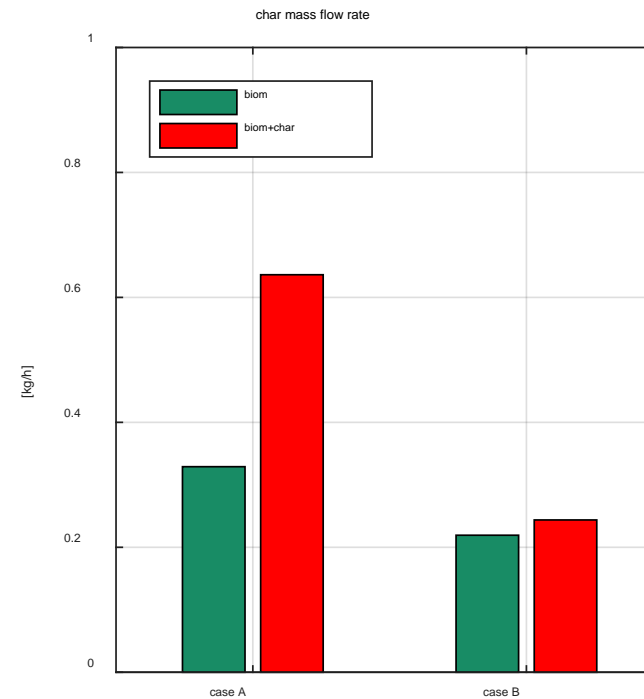
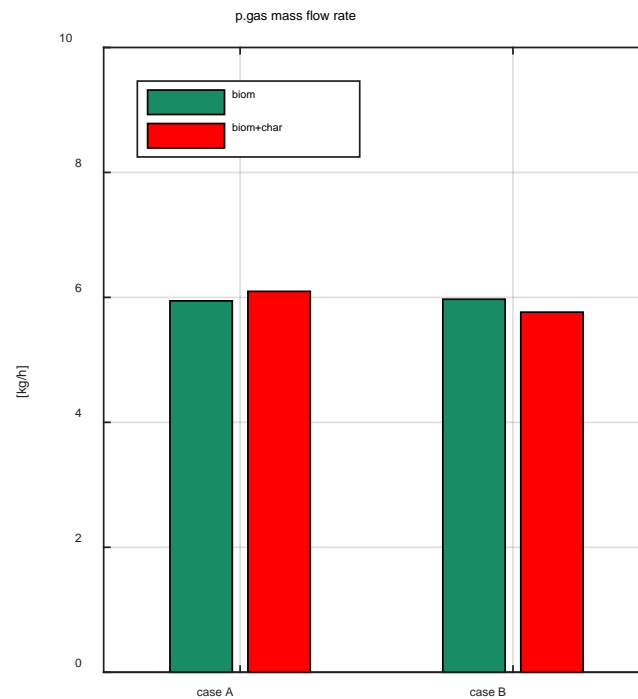
## Char characterization

- higher ash content → higher conversion

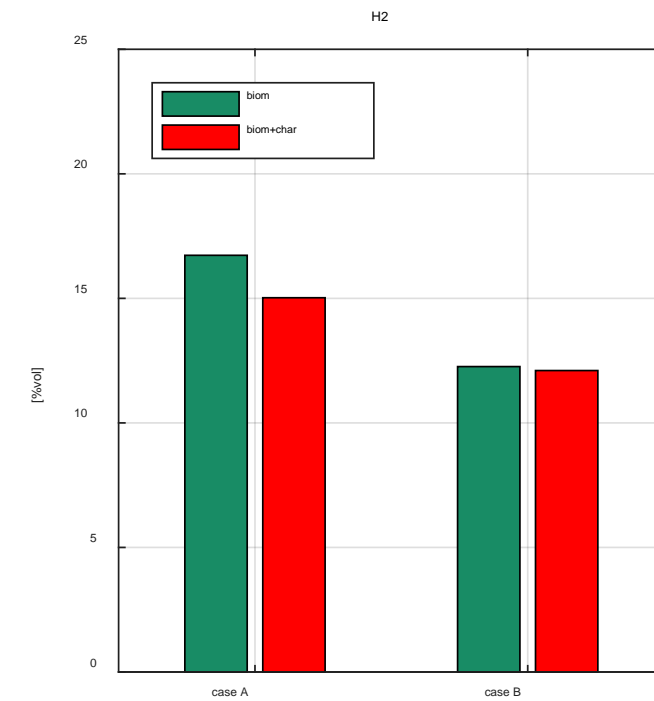
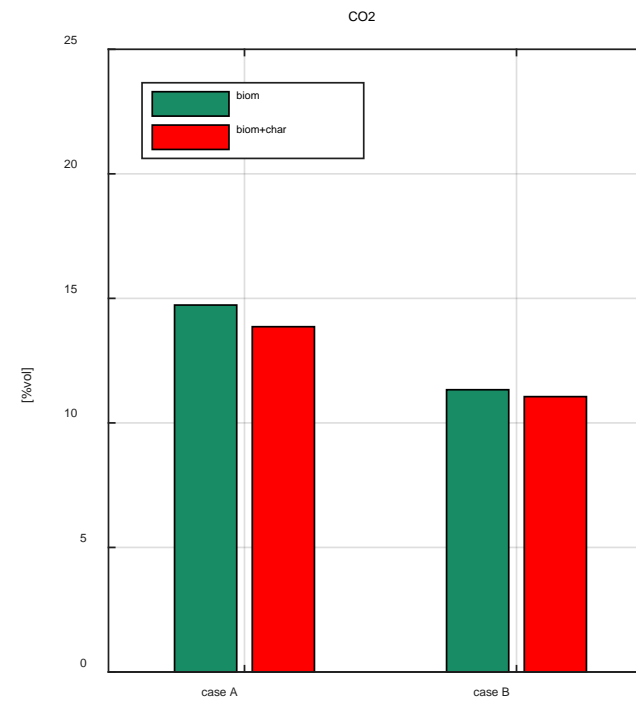
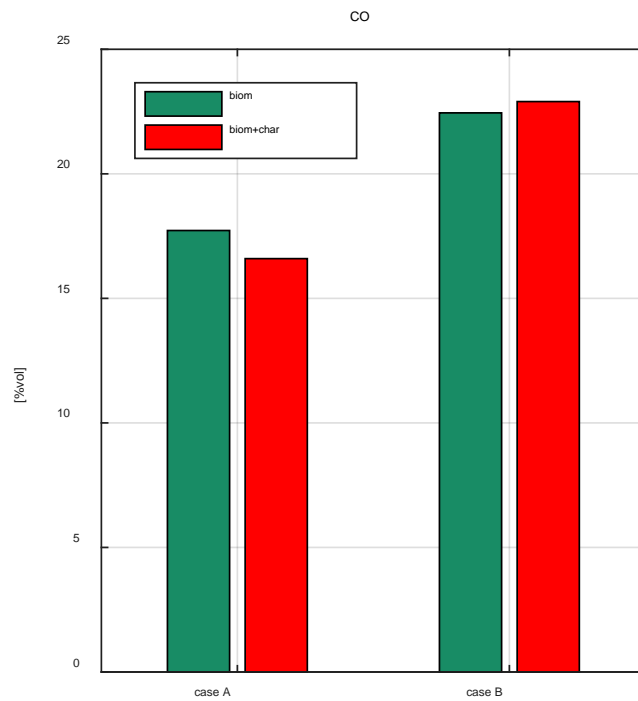


## Mass flow rates

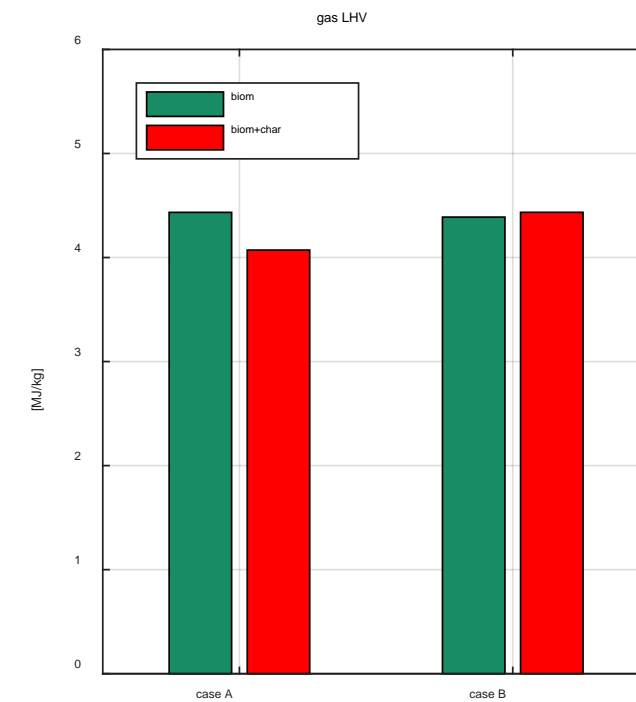
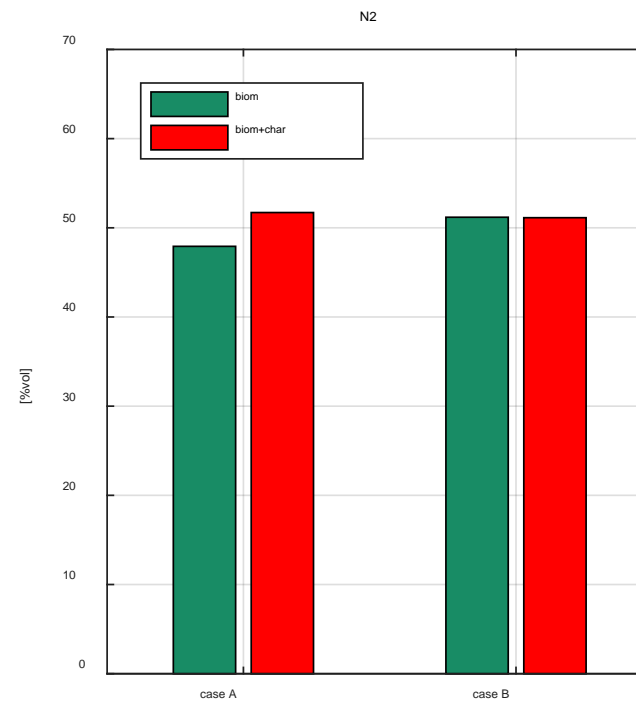
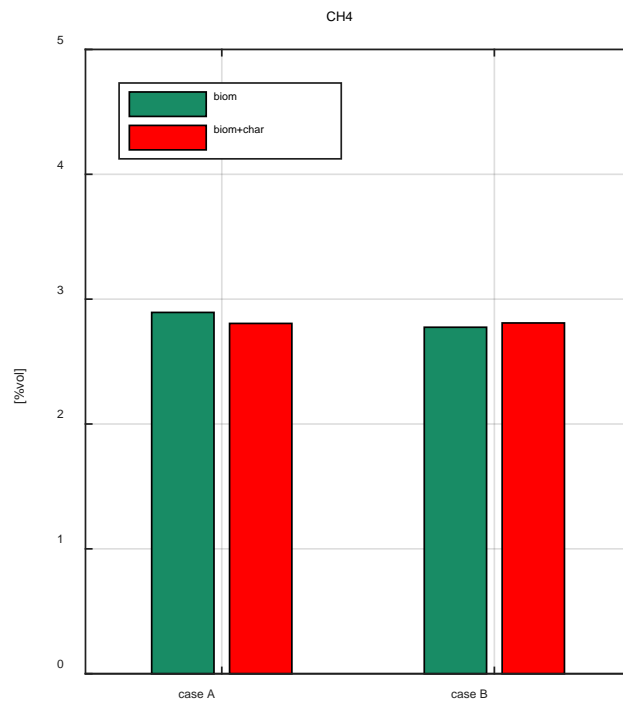
- producer gas: almost constant
- char: increases



## Gas composition

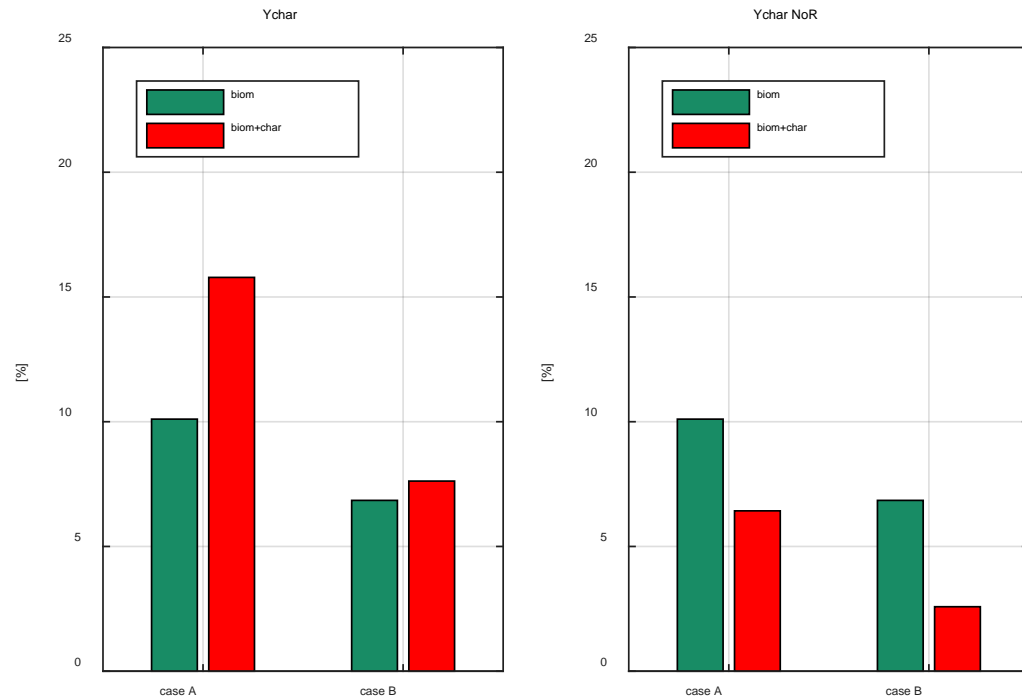


## Gas composition



## Overall effect of char recirculation

- Overall char yield: decreases

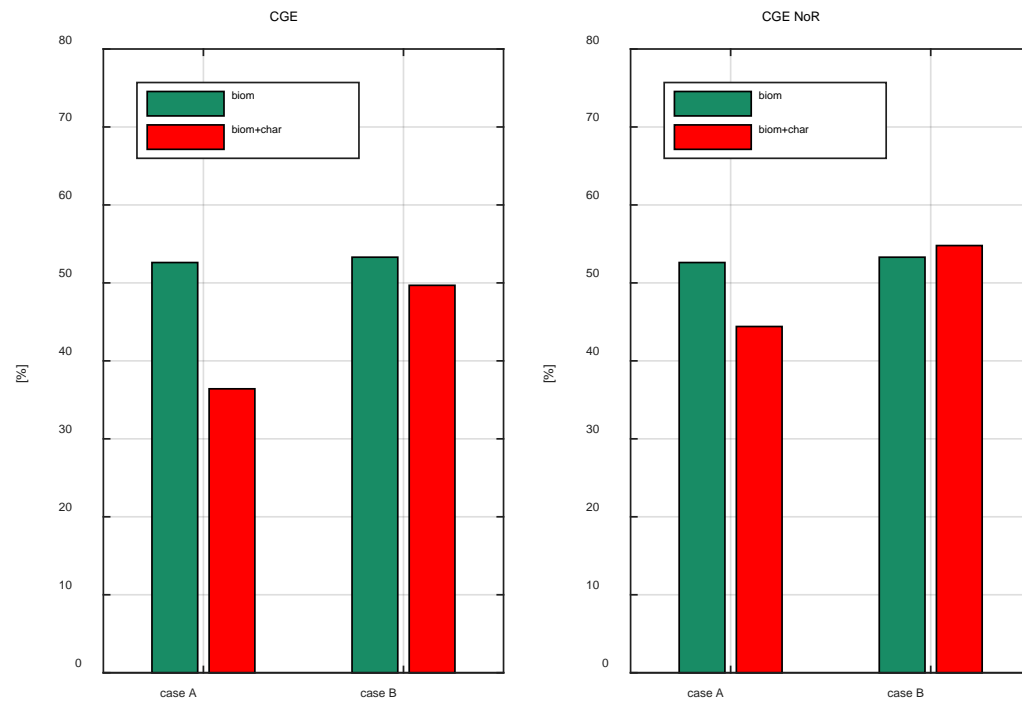


$$Y_{char} = \frac{\dot{m}_{char\ OUT}}{\dot{m}_{biom\ IN} + \dot{m}_{char\ IN}}$$

$$Y_{char\ NoR} = \frac{\dot{m}_{char\ OUT} - \dot{m}_{char\ IN}}{\dot{m}_{biom\ IN}}$$

## Overall effect of char recirculation

- Overall char yield: decreases
- Overall CGE: increases in case B (process conditions better tuned up)



$$CGE = \frac{\dot{m}_{pgas} \cdot LHV_{pgas}}{\dot{m}_{biom\ IN} \cdot LHV_{biom\ IN} + \dot{m}_{char\ IN} \cdot LHV_{char\ IN}}$$

$$CGE_{NoR} = \frac{\dot{m}_{pgas} \cdot LHV_{pgas}}{\dot{m}_{biom\ IN} \cdot LHV_{biom\ IN}}$$



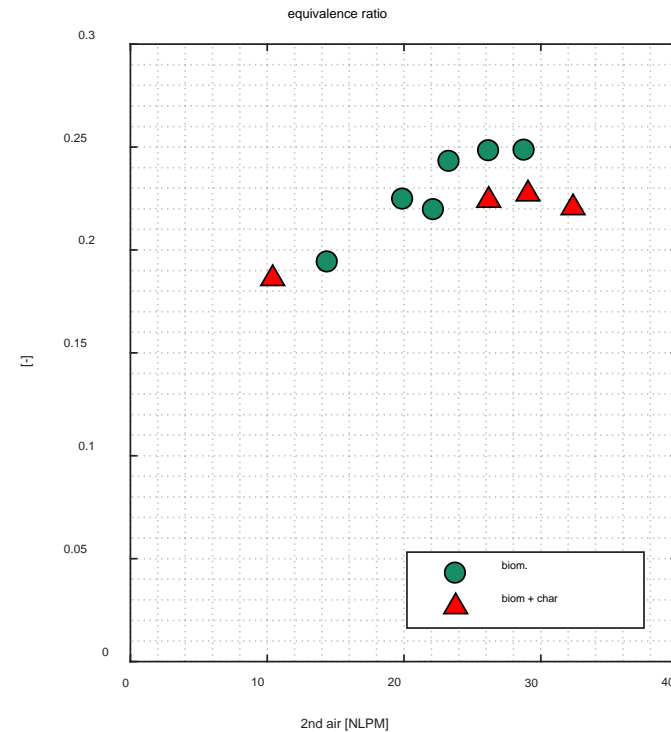
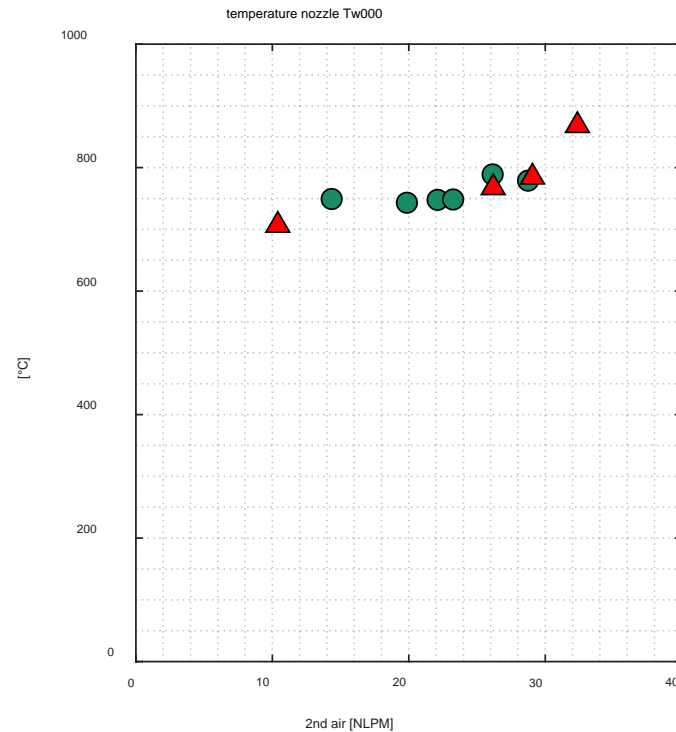
## 2<sup>nd</sup> air modulation

- Can the process conditions be further tuned up to optimize the process for char recirculation?

	<b>char yield / recirc. share</b> [%]	<b>2<sup>nd</sup> air injected</b> [NLPM]	<b>Blower SP</b> [Hz]	<b>ER</b> (when the fuel is only biomass) [-]
<b>Case C</b>	3 - 10	14 - 32	40	0.19 - 0.25

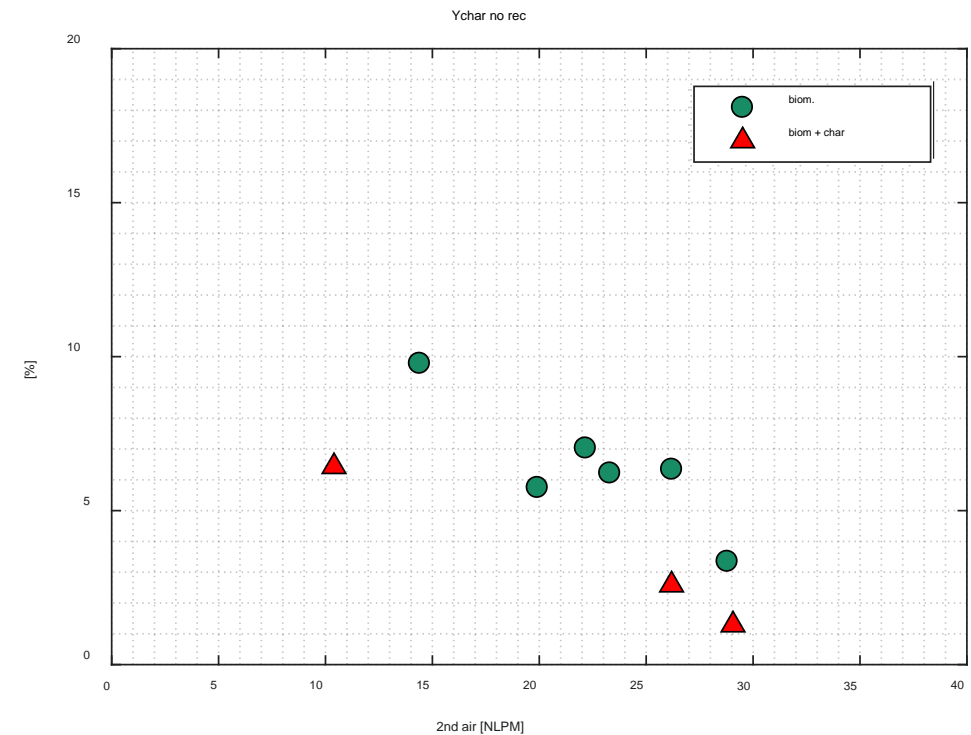
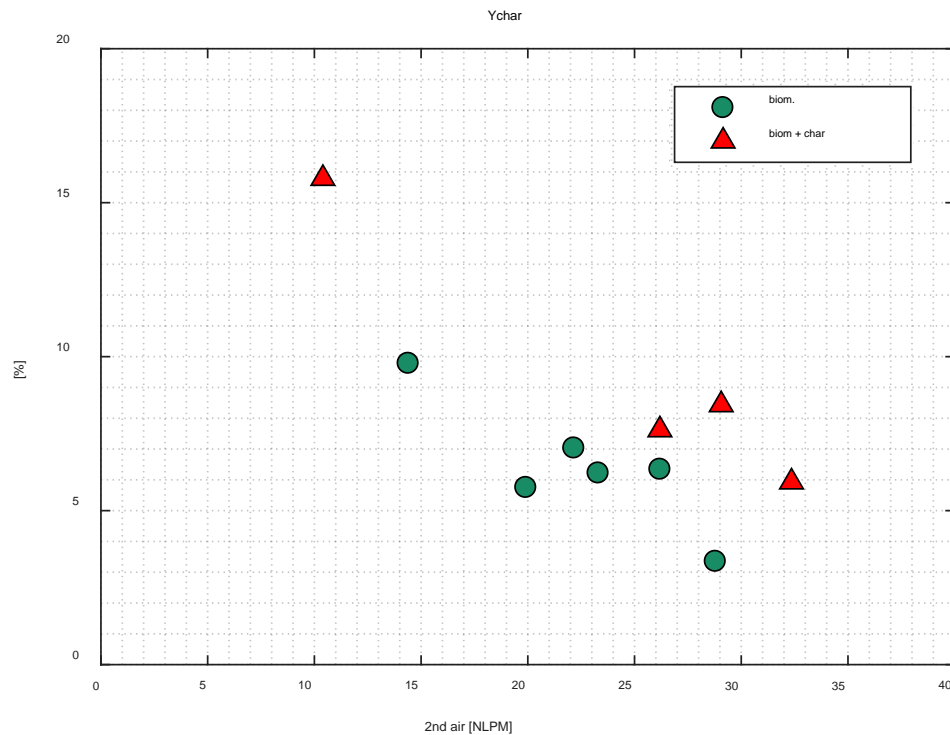
## 2<sup>nd</sup> air modulation

Main effects of increasing 2<sup>nd</sup> air flow rate



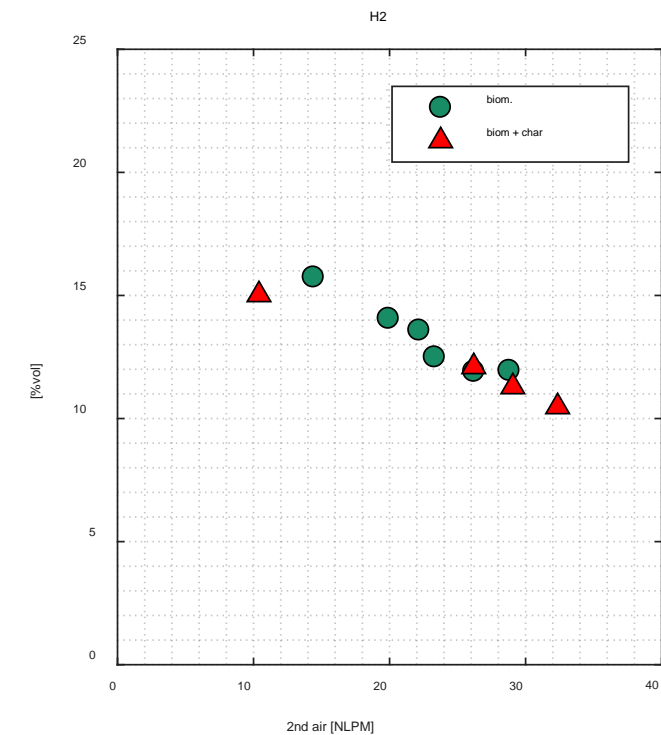
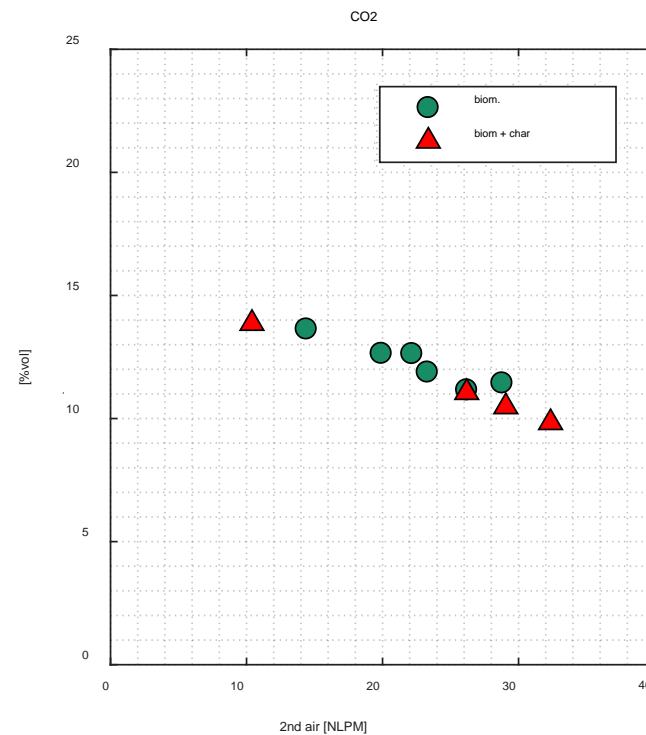
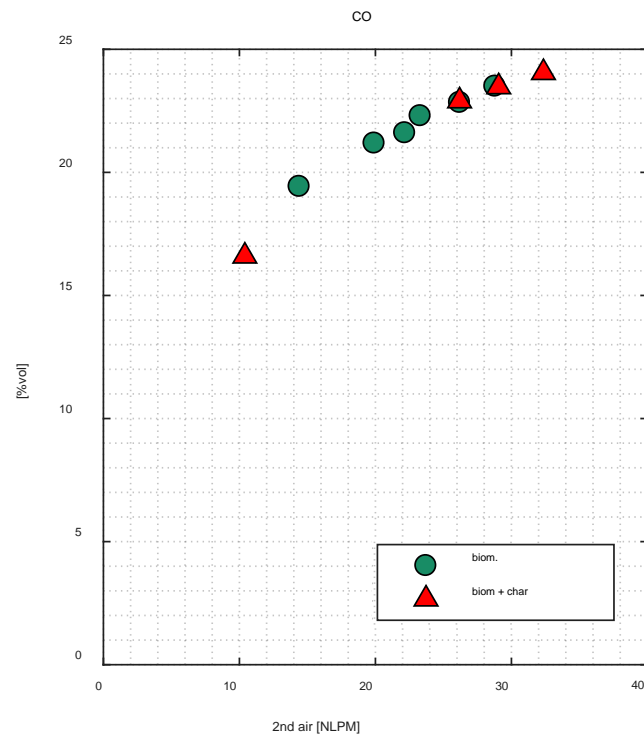
## 2<sup>nd</sup> air modulation

### Char yield



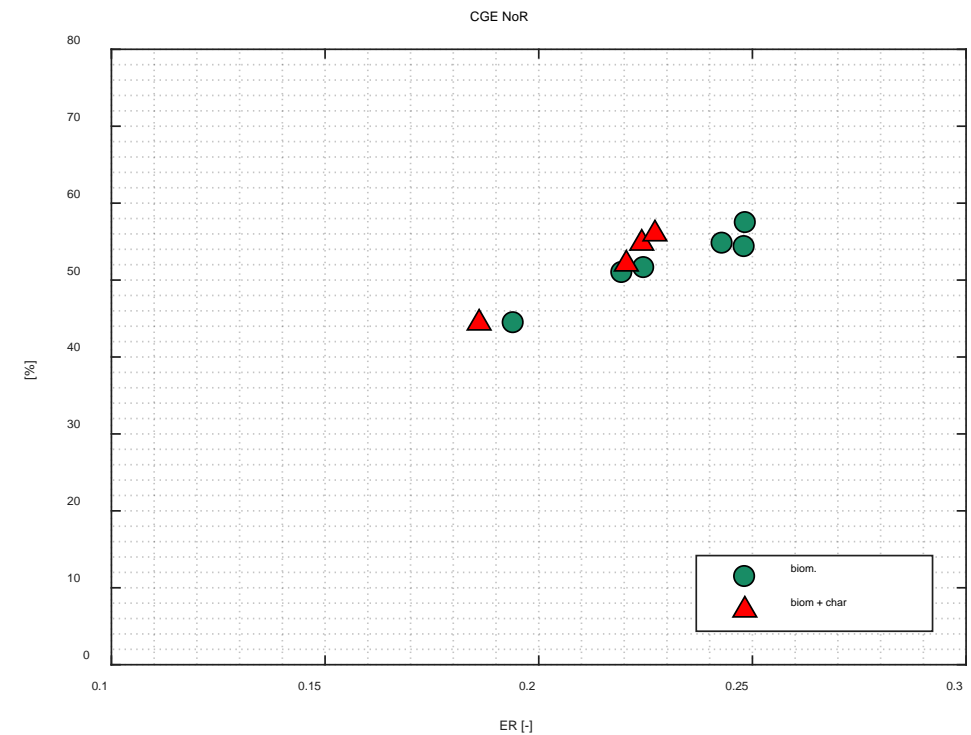
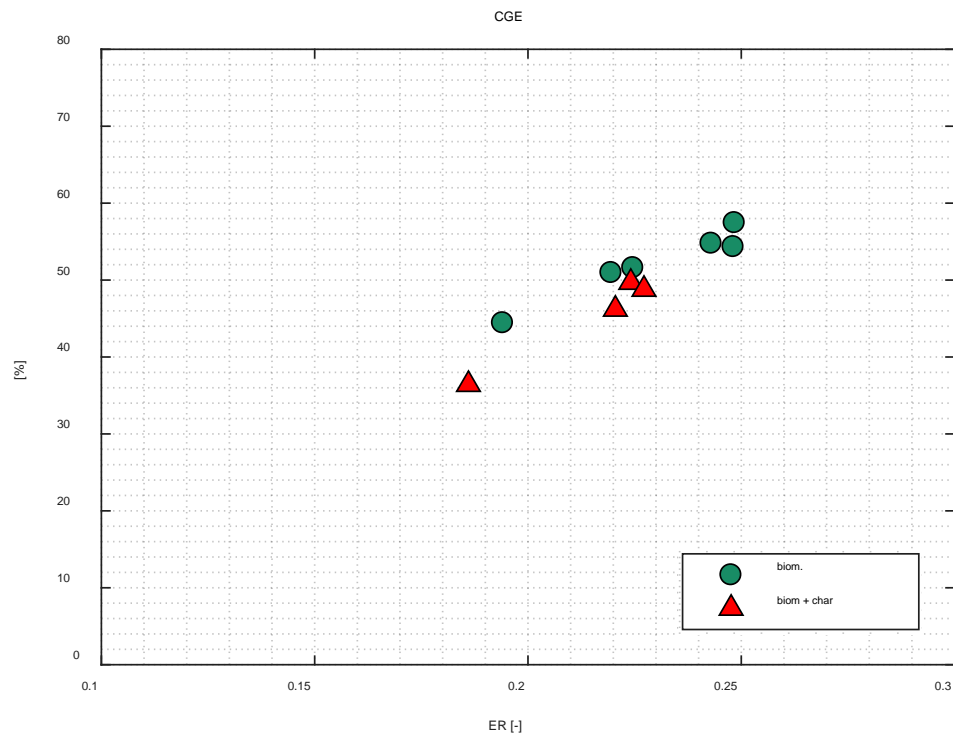
## 2<sup>nd</sup> air modulation

### Gas composition



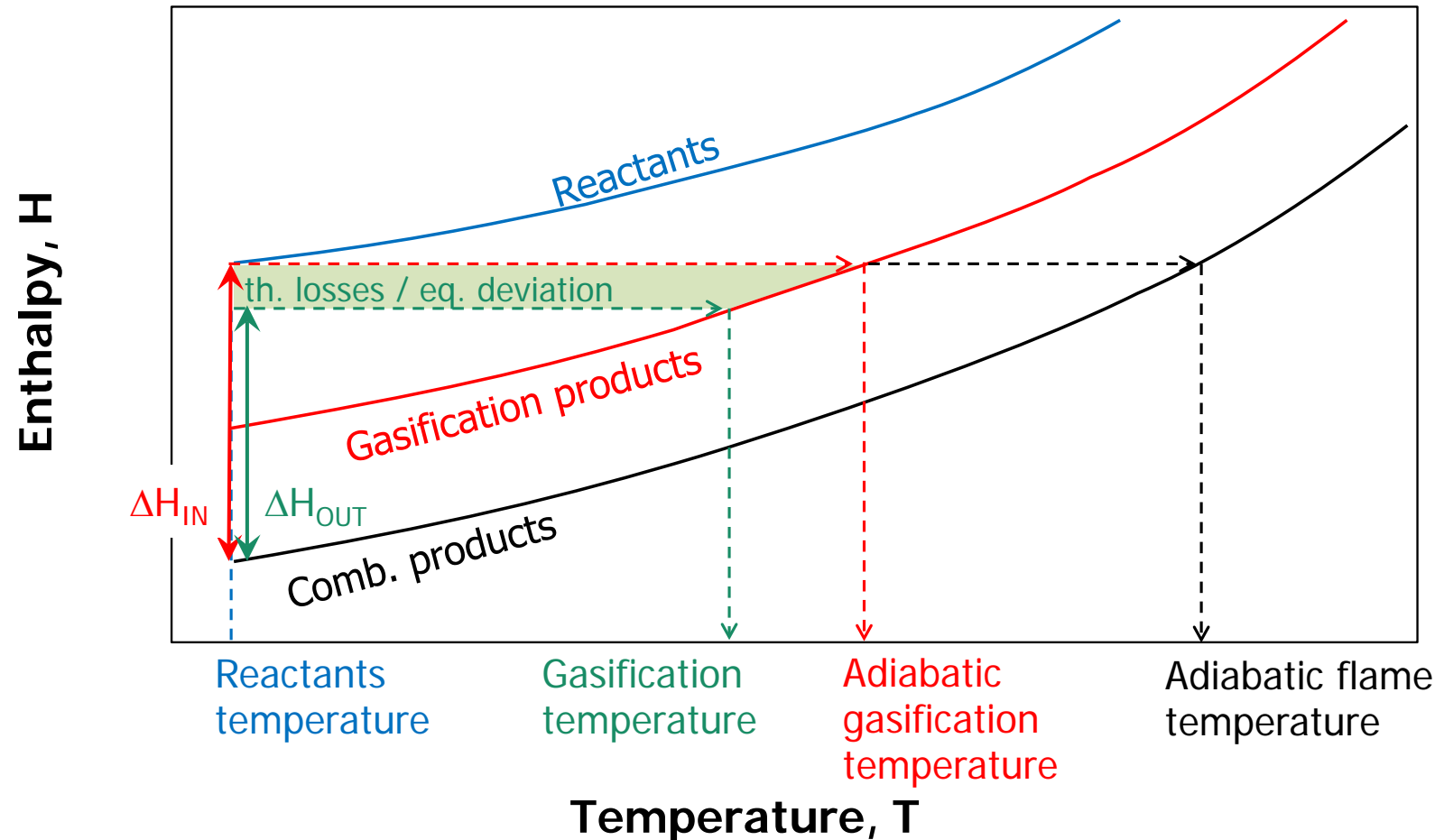
## 2<sup>nd</sup> air modulation

### Cold gas efficiency



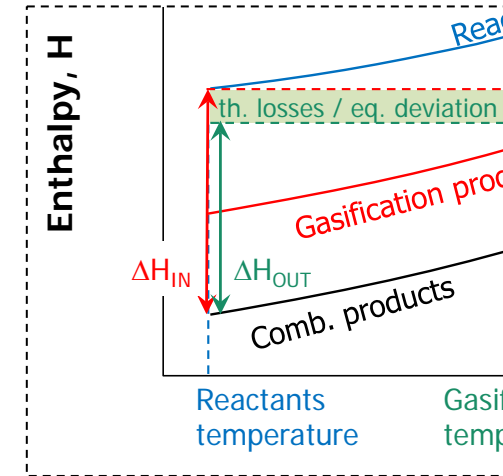
## Modelling approach

- based on a **thermodynamic solid-gas equilibrium** approach (Gibbs energy minimization method)
- overcomes the issues of the classical equilibrium strategy (fixed temperature and pressure)
- introduction of an **adiabatic gasification temperature**, defined in analogy to the concept of **adiabatic flame temperature** for the combustion process.



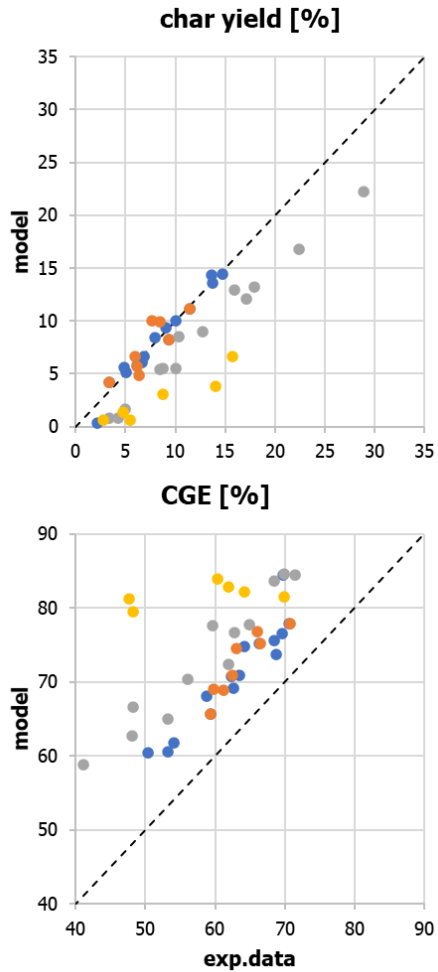
## Model calibration

$$\text{correction} = \frac{\Delta H_{\text{OUT}}}{\Delta H_{\text{IN}}}$$



## Model calibration

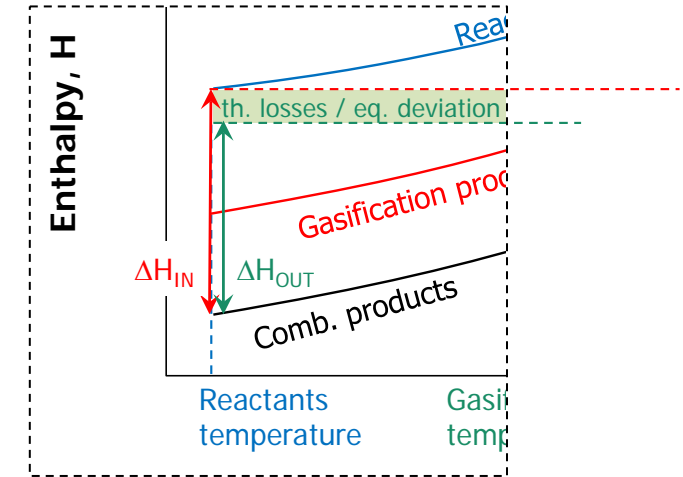
Adiabatic formulation



Four different exp. campaigns

- LOAD MODULATION (LM)
- CHAR RECIRCULATION (CR)
- TORREFIED PELLETS (TP)
- BARK AND CHIPS (BC)

$$\text{correction} = \frac{\Delta H_{\text{OUT}}}{\Delta H_{\text{IN}}}$$



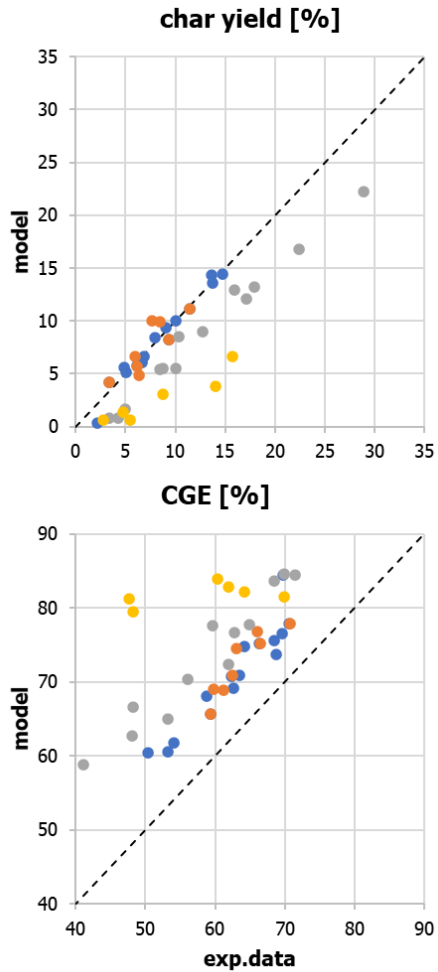


Four different exp. campaigns

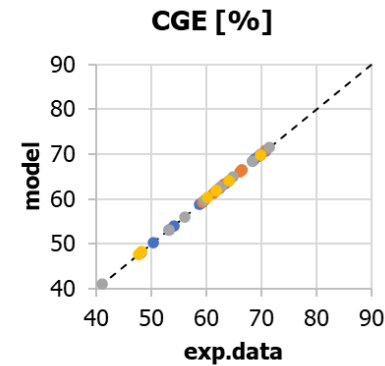
- LOAD MODULATION (LM)
- CHAR RECIRCULATION (CR)
- TORREFIED PELLETS (TP)
- BARK AND CHIPS (BC)

## Model calibration

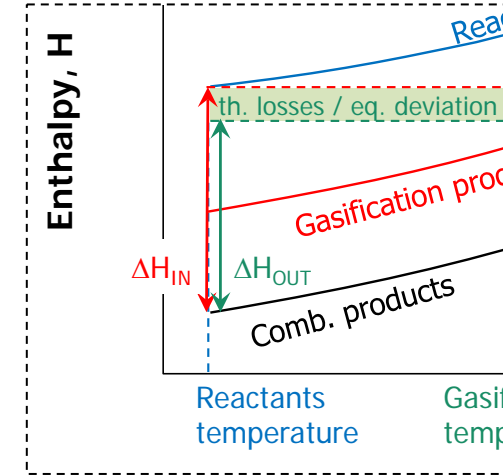
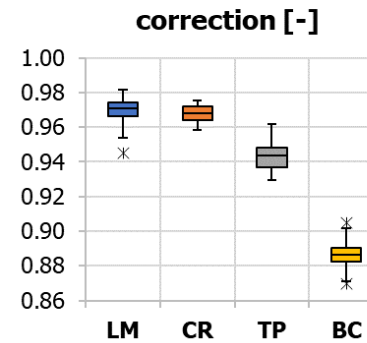
Adiabatic formulation



Calibration to match the experimental CGE



$$\text{correction} = \frac{\Delta H_{OUT}}{\Delta H_{IN}}$$

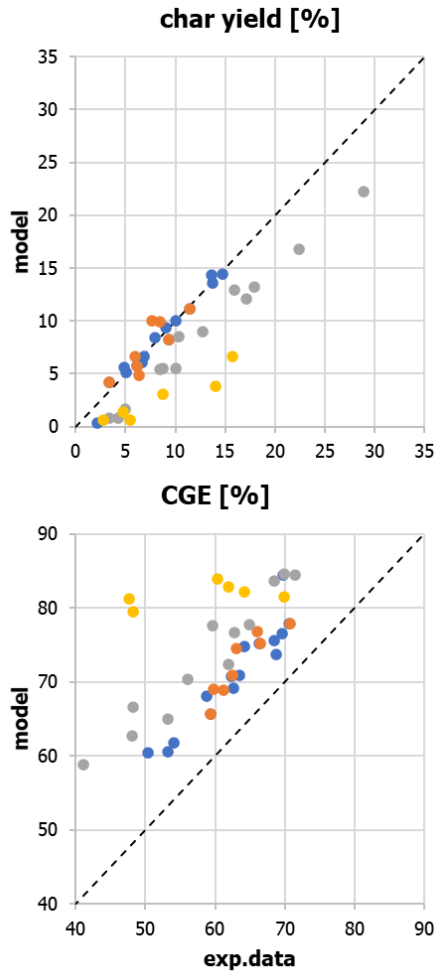


Four different exp. campaigns

- LOAD MODULATION (LM)
- CHAR RECIRCULATION (CR)
- TORREFIED PELLETS (TP)
- BARK AND CHIPS (BC)

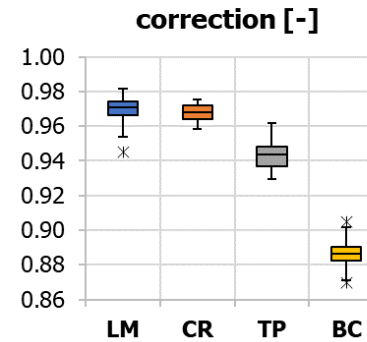
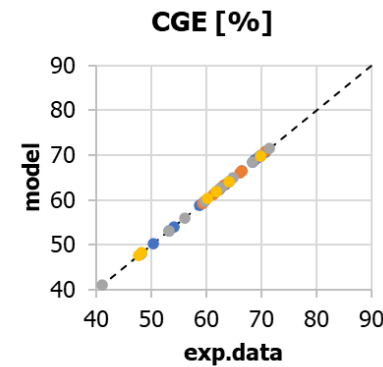
## Model calibration

Adiabatic formulation

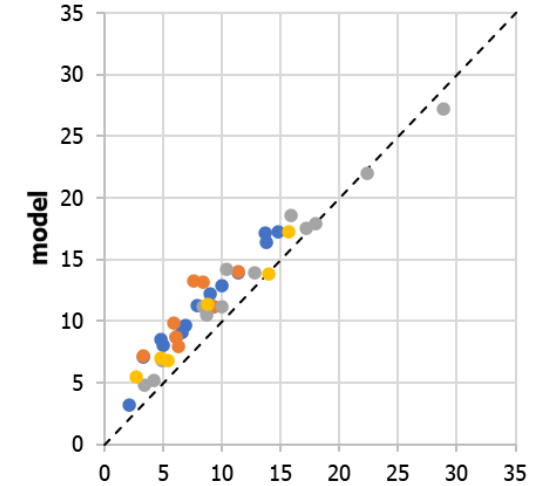


Calibration to match the experimental CGE

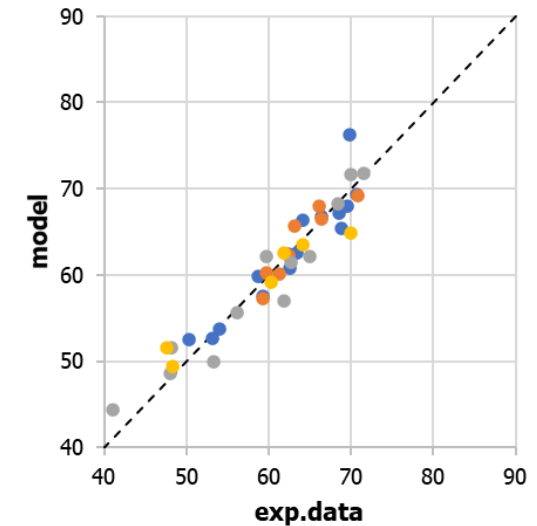
$$\text{correction} = \frac{\Delta H_{\text{OUT}}}{\Delta H_{\text{IN}}}$$



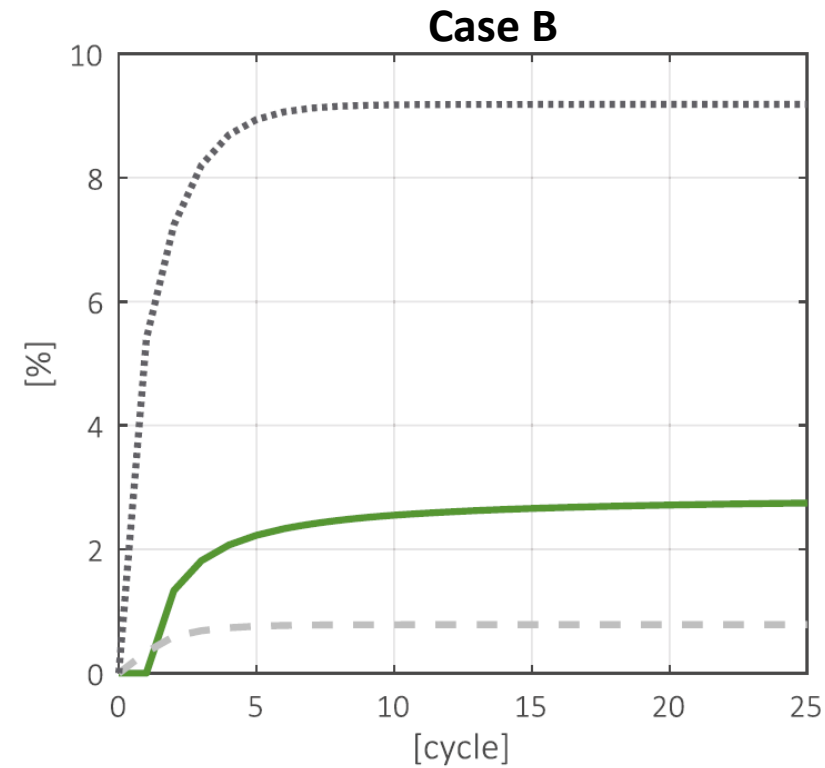
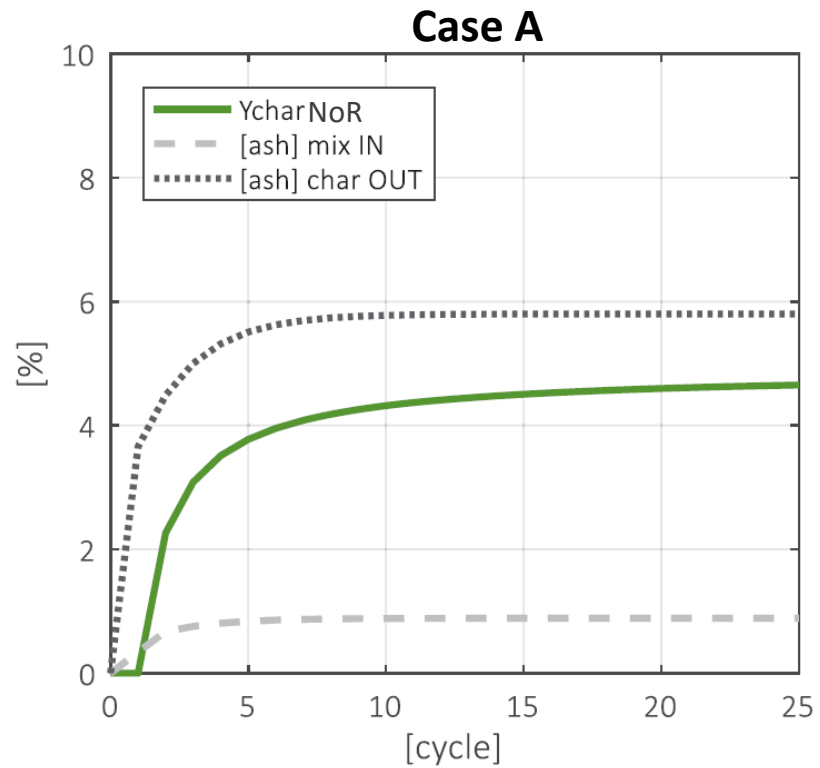
char yield [%]



CGE [%]



## Long term effect of char recirculation



## Conclusions

Char recirculation:

- Allows a significant reduction of the overall char yield (in the order of 40 - 60 %)
- Do not significantly impact the process if this is well tuned up
  - Gas composition and LHV remain almost constant
  - CGE slightly decreases (as per the producer gas flow rate)
  - Considering the overall effect, CGE slightly increases
- Secondary air modulation can make even more feasible char recirculation
- An asymptotic condition is reached after a certain number of recirculation cycles, as confirmed by both modelling and experimental results

## Open question

- What is the effect of granulometry?  
(this worked well, but the char particles were still maintaining the original pellet shape)



## Acknowledgments

This work was funded by



in the frame of the project **CHAR-RCC**:

**“CHAR Re-Circulation for improving the Conversion yields  
in fixed-bed biomass gasification systems”**



*24 June 2021*

Thank you very much for your kind attention!

francesco.patuzzi@unibz.it

visit us @  
bnb.groups.unibz.it

