

Integrated process for PHA production from lignocellulosic waste: A new anaerobic biorefinery

Luis D. Allegue, Maria Ventura, Daniel Puyol Santos, Juan A. Melero

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Context

Lignocellulosic waste



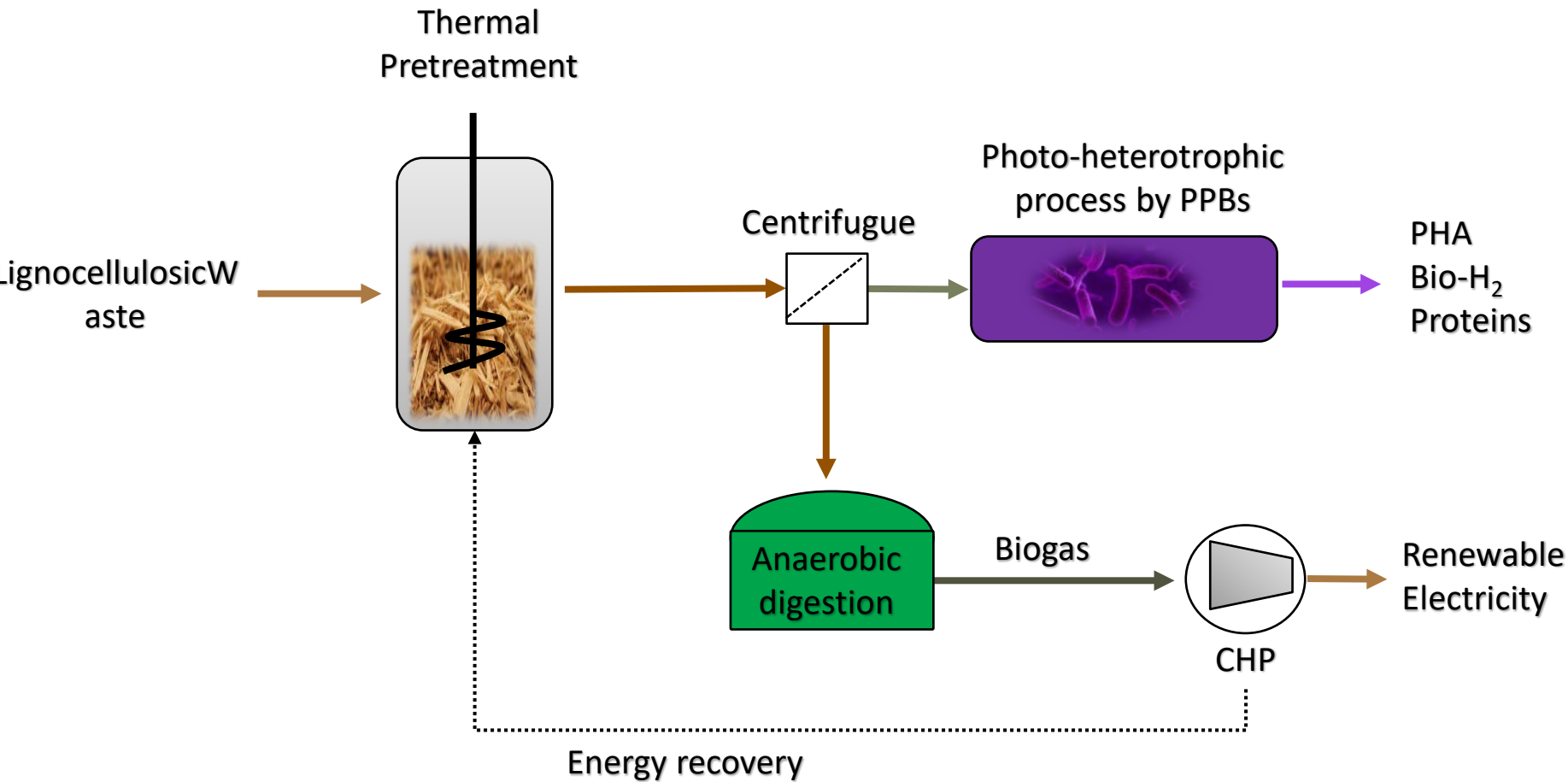
The upcycling of waste biomass into high-added value products can be an attractive route for attaining the circular bio-economy as well as environmental sustainability

1. Most abundant natural renewable resource
2. Agricultural, forest, and municipal waste
3. Does not compete with food production



Context

Photo-biorefinery



Material and methods

Lab-scale proof of concept



Pruning waste



120 – 150 – 180 °C
1:5 water to SV ratio

Severity factor:

$$R_o = \int_0^t \exp\left(\frac{T(t) - T_{Ref}}{14.75}\right) dt$$

R₀: 2.1 – 3.1 – 3.9



Specific Phototrophic Activity Test (SPA)



Conditions:
45 W m⁻² IR Light
1 g DQO L⁻¹
PPB inoculum



Standard BMP test

Results

Thermal hydrolysis

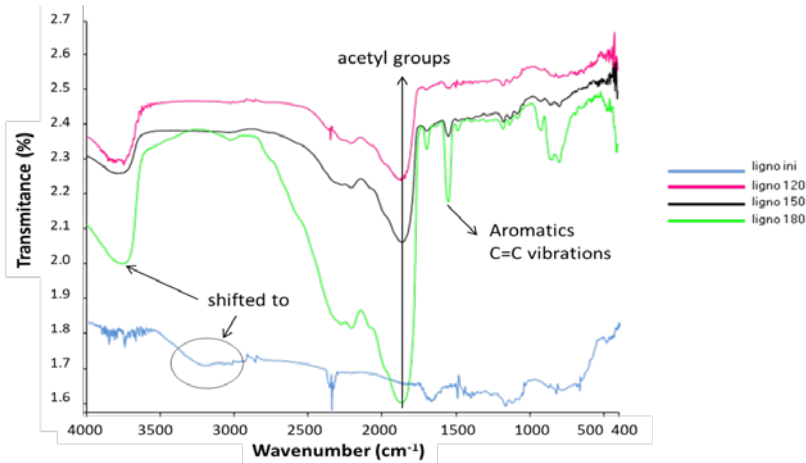


Figure 1: FTIR spectra of the three hydrothermal pretreatments, 120(pink), 150 (black) and 180 °C (green) and initial (blue) solid phases.

- Crystallinity increase(CR_I)

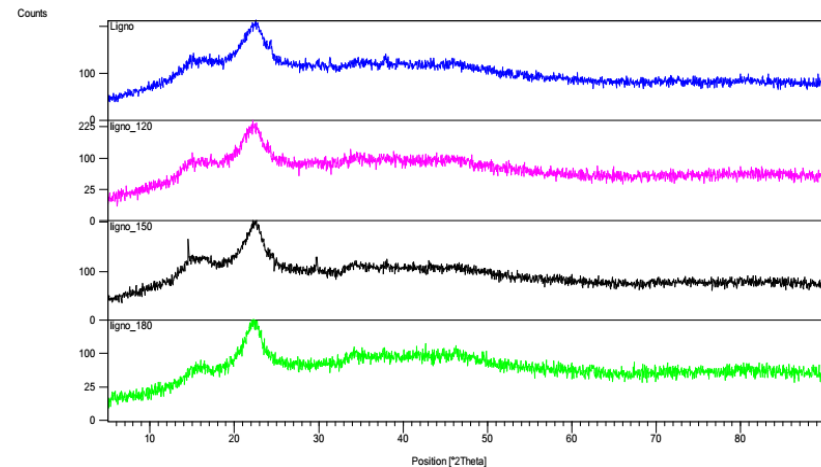


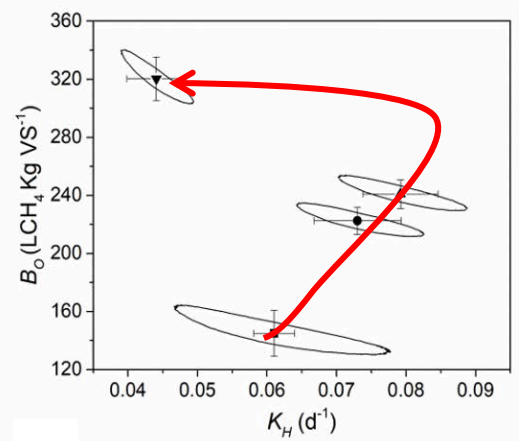
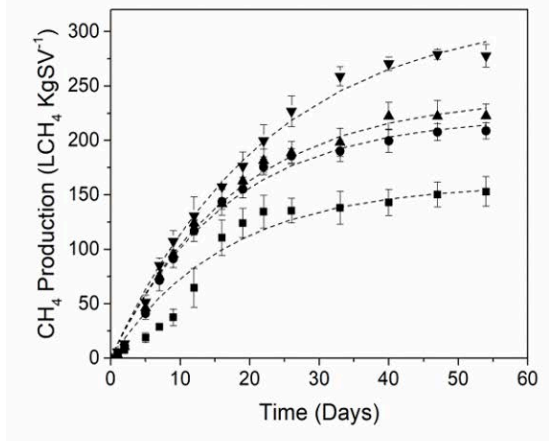
Figure 2: Comparison of DRX spectra of the raw waste (blue) and the hydrothermal pretreatments solid phases were 120 (pink), 150 (black) and 180 °C (green).

- Solid destruction: 13-29%
- COD solubilization: 9-24%
- DQO/N/P: 100/3/0.5

Results

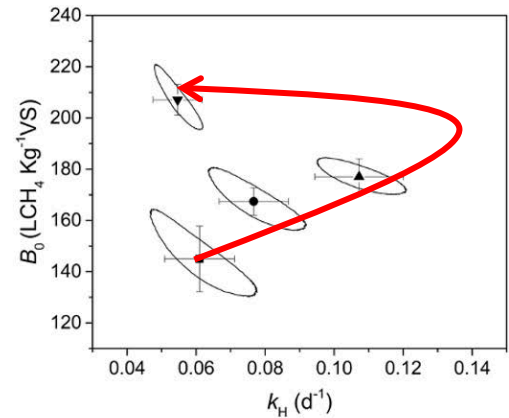
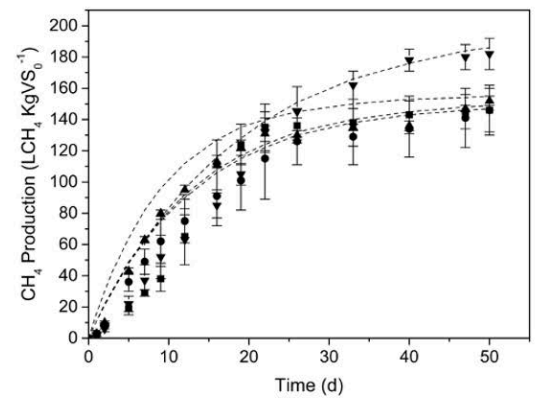
Anaerobic digestion

No elimination of liquid fraction



- Control
- 120°C
- ▼ 150°C
- ▲ 180°C

Elimination of liquid fraction



Potential presence of inhibitory compounds above 180 °C.

Figure 3: BMP results and 95% confidence regions for the first-order kinetic parameters.

Results

Energy integration balance

Table: Energy integration balance. Results were simulated for a combined heat and power (CHP) system for electricity and thermal energy production.

Substrate	Total Energy biogas kWh t ⁻¹	Thermal Output kWh t ⁻¹	Electrical Output kWh t ⁻¹	Thermal energy required kWh t ⁻¹	Electrical balance kWh t ⁻¹	Thermal energy balance kWh t ⁻¹	Electric output Euro t ⁻¹
Raw	1343	739	443		428	739	64
TH-120°C	1343	739	443	154	408	585	61
TH-150°C	1398	769	461	177	426	592	64
TH-180°C	1693	931	559	210	524	721	79



Positive electrical and thermal balances

Results

Photoheterotrophic process

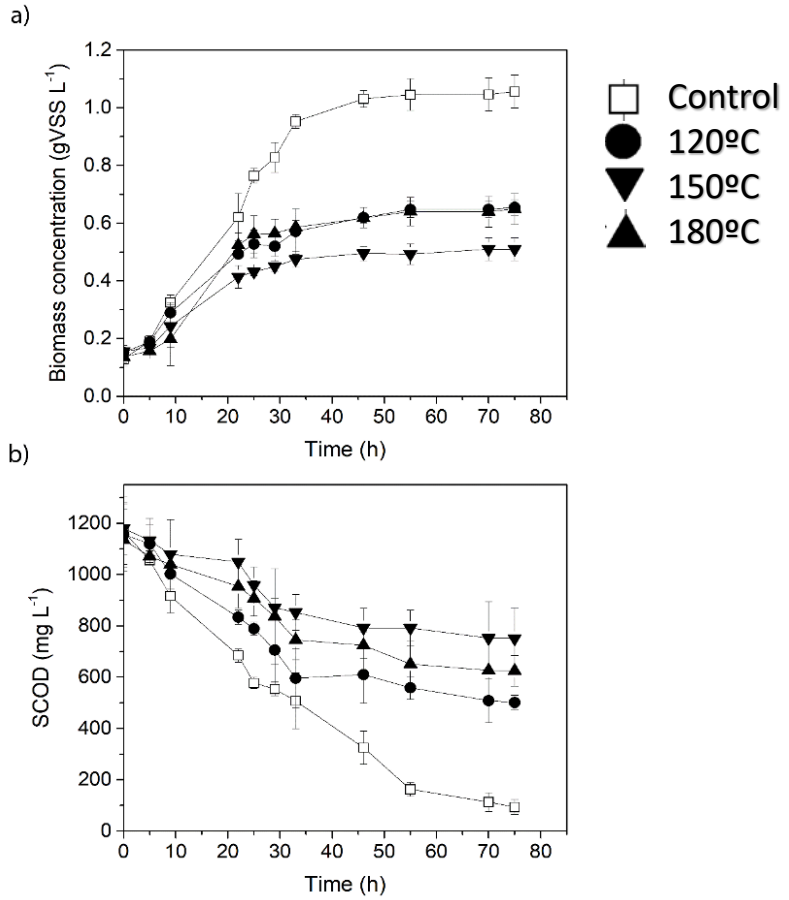


Figure 4: Comparison of biomass growth (a) and SCOD consumption (b) in the SPA tests using the liquid fraction

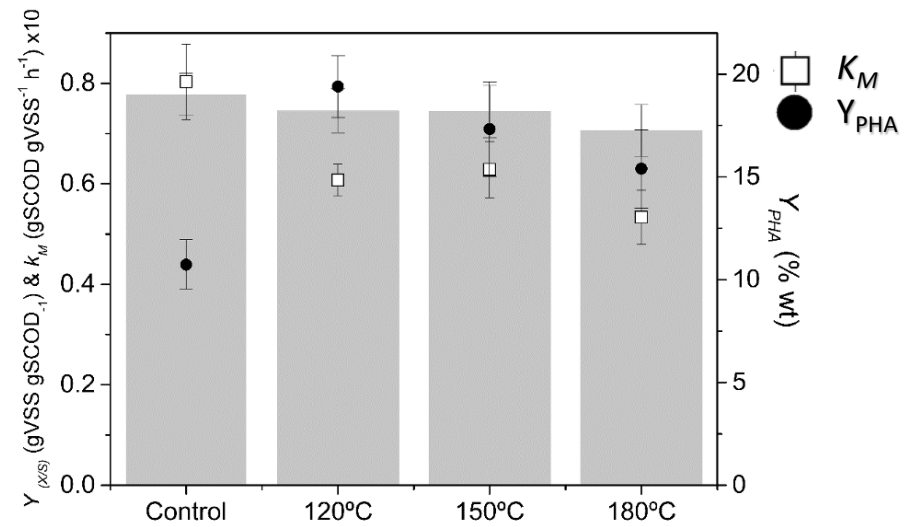


Figure 5: Comparison of biomass yield (Y_{X/S}) (columns) with specific phototrophic activity (k_M × 10) (open squares) and PHA production yield (Y_{PHA}) (black circles) in SPA tests

- 37-60% COD consumption
- Nitrogen limitation
- 15-20% PHA in dry mass

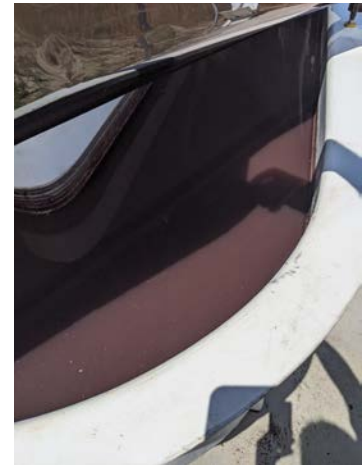
Discussion

Prospects and industrial implications

- Current industrial PHA cost: $\approx 4\text{-}8 \text{ € t}^{-1}$
- The theoretical maximum PHA production yield reported by PPBs is $0.9 \text{ mol}_{\text{PHA}}$
 $\text{mol}_{\text{Acetate}}^{-1}$ *. This is vastly higher than any aerobic processes

**DEEP
PURPLE**

**BIO-BASED
INDUSTRIES**
Public-Private Partnership



Conclusions

Key findings

- High temperatures in the thermal pre-treatment lead to better solubilisations, but may produce inhibitory products.
- Up to 180 LCH₄ Kg VS⁻¹ produce in BMP test after removal of liquid fraction
- An energetically sustainable process is achieved.
- Up to 20% PHA in dry mass is accumulated by PPB
- The PPB integrated biorefinery concept offers potential for the reduction of PHA production costs, inviting for future research

Thank you!

Luis.diaz.allegue@urjc.es

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