

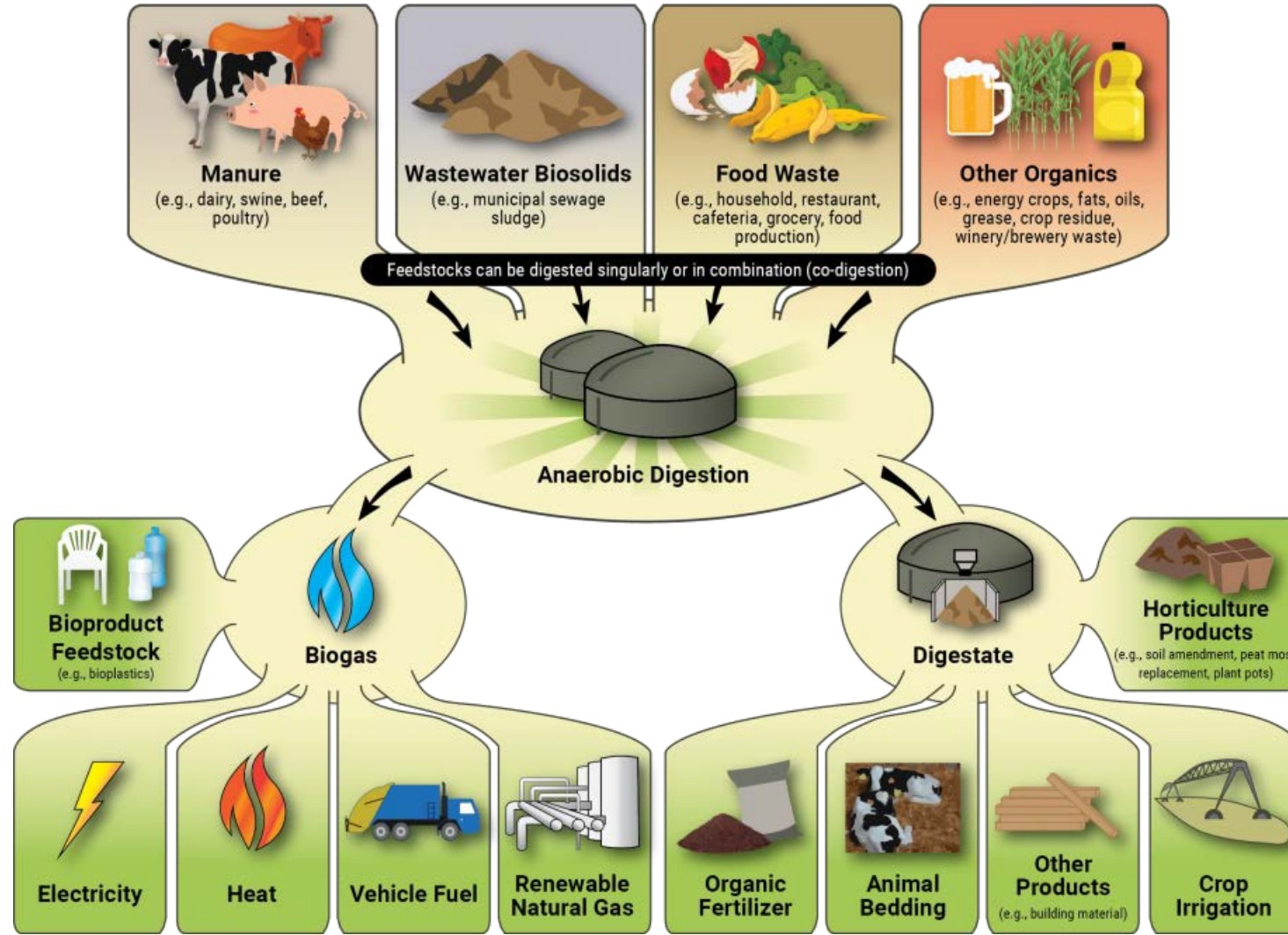


Implementation of Photocatalytic Membrane Reactor for Liquid Digestate Sanitation

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<https://www.epa.gov/agstar/how-does-anaerobic-digestion-work>

Digestate does not come without sanitation risks

$$S = S1 * S2 * S3$$

S1: Ineffective thermal inactivation

S2: Potential transmission pathways (air, water, food, animal contact)

S3: Human health risk

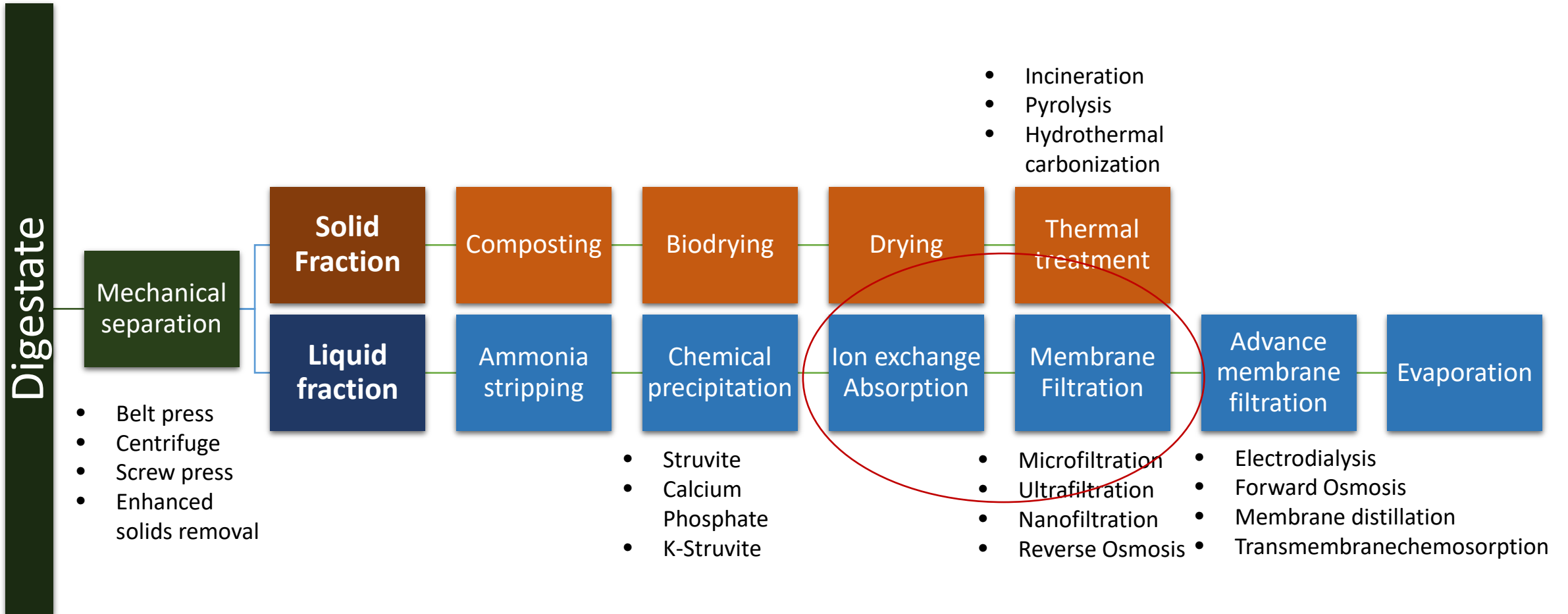
Must be:

- Treated on site
- Disposed in acceptable distances

Effective and low-cost new sanitation method

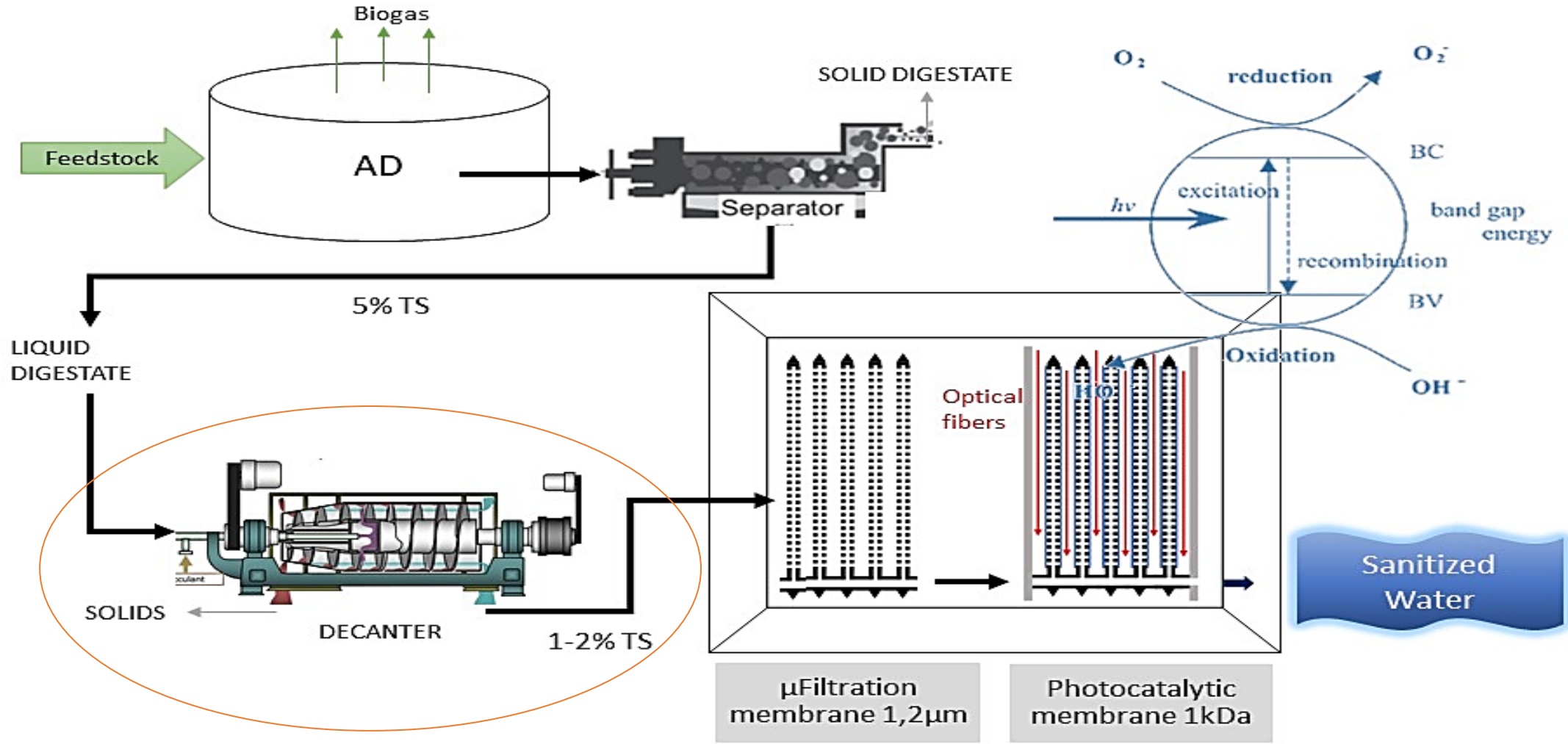
- ✓ Circular economy
- ✓ Environment protection
- ✓ Profitability

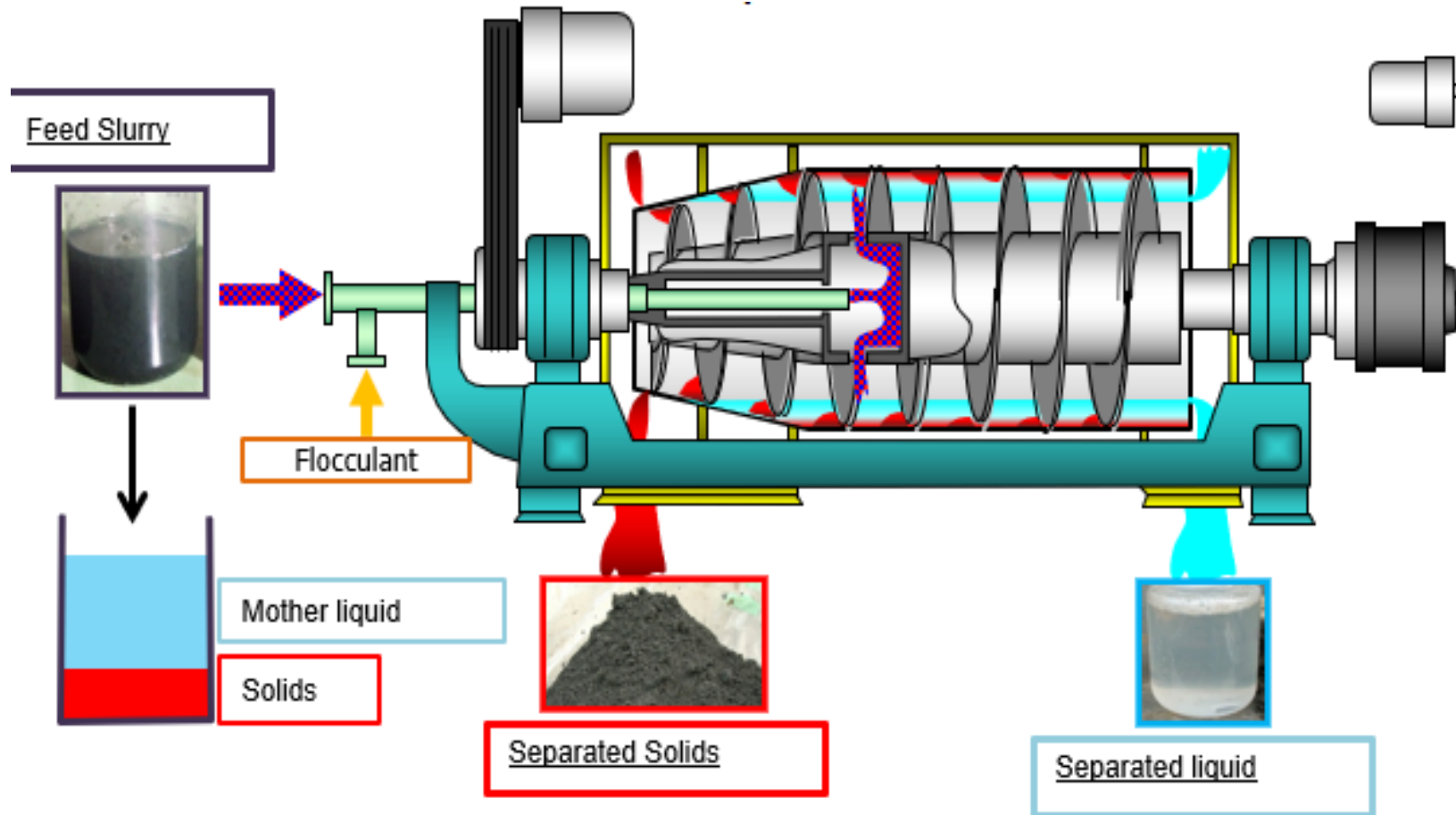


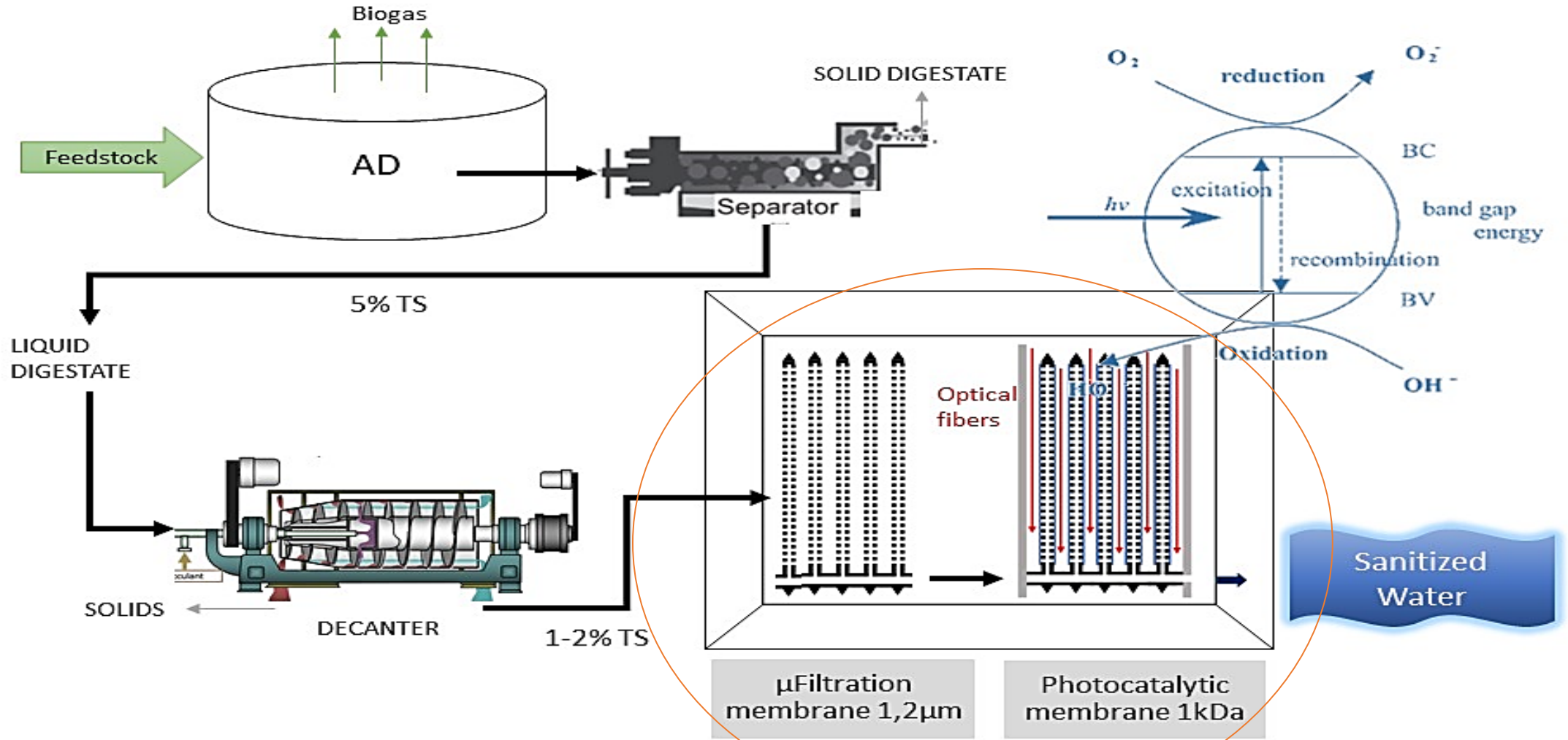


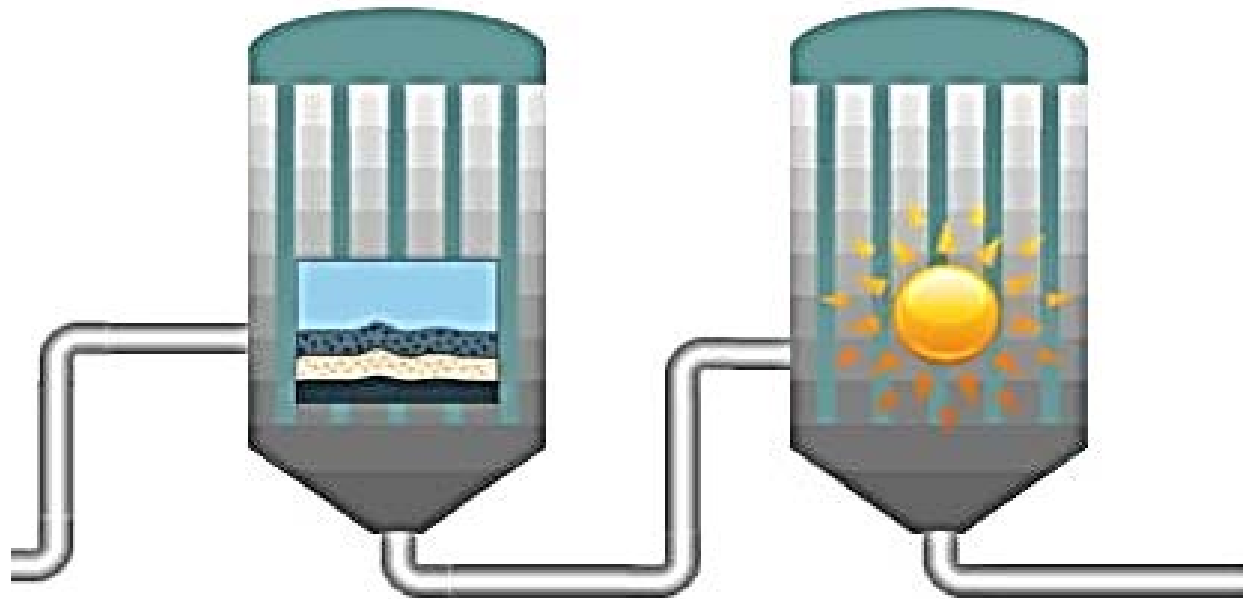
Parameter	Unit	Whole digestate	Liquid digestate	Solid digestate
		mean±sd (min-max)	mean±sd (min-max)	mean±sd (min-max)
Dry Matter	%	5.6±1 (3.9-8.2)	3.22±1.6 (1.3-5.8)	22.5±7 (11.2-35)
pH	-	8.1±0.17 (7.7-8.5)	8.2±0.2 (7.9-8.6)	8.3±0.3 (6.7-9.4)
Organic Matter	%	3.78±0.78 (2.2-5.4)	1.9±1.6 (0.7-5.7)	29±30.3 (11-87)
Total N	%	0.5±0.9 (0.4-7.8)	0.33±0.08 (0.2-0.4)	1.3±1 (0.5-2.8)
NH₄⁺	%	0.3±0.4 (0.02-3.6)	0.22±0.06 (0.1-0.4)	0.4±0.24 (0.2-0.8)
Total P	%	0.16±2.6 (0.06-21.1)	0.04±0.05 (0.01-0.1)	0.9±1.1 (0.2-3.3)
Total K	%	0.4±0.8 (0.03-6.6)	0.24±0.08 (0.1-0.4)	0.57±0.61 (0.1-1.7)
Ca	%	0.15±0.2 (0.06-1.7)	0.044±0.05 (0.01-0.1)	0.68±0.17 (0.5-0.9)
Mg	%	0.03±0.09 (0.003-0.6)	0.04±1.9 (0.007-5.1)	0.23±0.07 (0.1-0.3)
Na	%	0.13±0.05 (0.004-0.2)	0.09±0.03 (0.07-0.2)	0.06±0.03 (0.01-0.1)
Cl⁻	%	0.22±0.06 (0.1-0.3)	0.35±0.39 (0.1-1.2)	0.14±0.07 (0.03-0.2)
Zn	mg/kgDM	403±154 (155-1020)	504±374 (209-1220)	144±83 (50-318)
Cu	mg/kgDM	129±93 (24-343)	197±135 (59-449)	73.4±36 (28-139)
Salmonella	-	11.1% presence	6.7% presence	14.3% presence
E. coli	cfu/gr	295±6233 (<10-30000)	(<10-13000)	72±185 (30est-490)
E. faecalis	cfu/gr	(<40-1.2*10⁶)	(<10-250000)	565±3014 (120-7900)

- ❖ 3-year monthly data of digestate from two Greek biogas plants
- ❖ Unstable nature of digestate → wide ranges
- ❖ Presence of pathogens
- ❖ Presence of organic micropollutants → risk of leaching



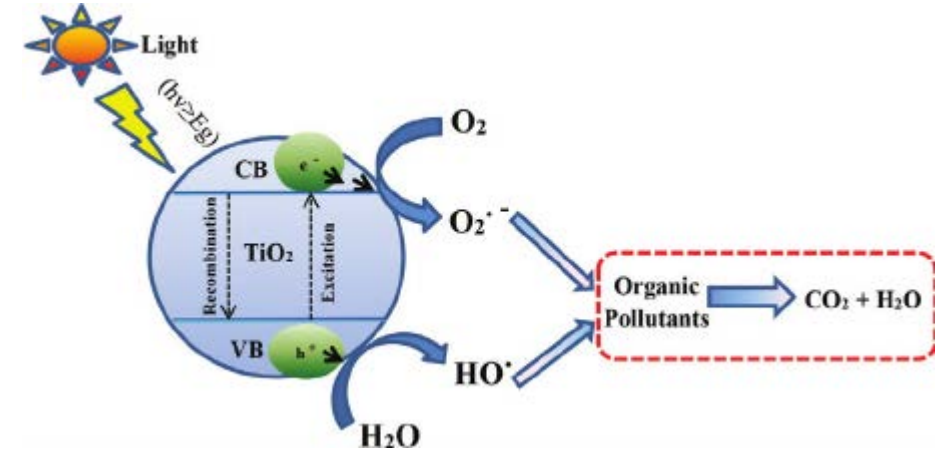






µFiltration
membrane 1.2µm

Photocatalytic
membrane 1kDa



PHOTOCATALYSIS

- ✓ cost effective
- ✓ less-energy spending
- ✓ Non-selective oxidation of contaminants
- ✓ simultaneous bactericidal impact
- ✓ chemical-free

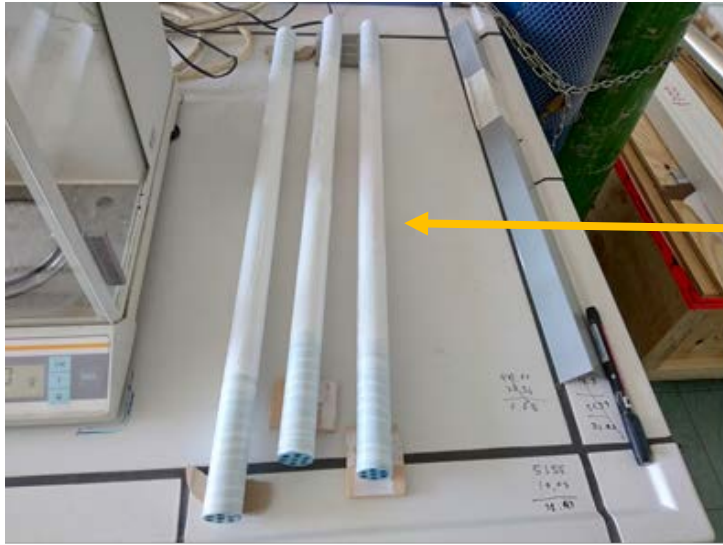
A Photocatalytic Nanofiltration Reactor (PNFR) where, nanofiltration and photocatalysis act simultaneously and in a synergetic way, overcomes individual drawbacks and cope with the complexity of the aqua matrices independently of their source.

Limitation of Nanofiltration as a stand-alone process:

- Conventional Nanofiltration processes generate a retentate effluent more concentrated than the feed
- Toxic micropollutant that must be managed and disposed with special and costly approaches
- Nanofiltration alone cannot reject the multitude of compounds classified as micropollutants

Limitation of Photocatalysis as a stand-alone process:

- Photocatalysis, usually applied in the form of ultra-thin photocatalytic coatings stabilised on light transparent substrates and get involved in continuous flow processes
→ Nanoparticles separation
- Mass transfer limitations, poor mixing and short contact times lead to moderate photocatalytic degradation performance
- Competitive action of organic matter that usually exists in industrial effluents



600 mm length monoliths (membranes) after dipping in the wash coating slurry of TiO₂.

Glass sleeve of the UV lamps

SS-flanges (2 top and 5 bottom)



Side view

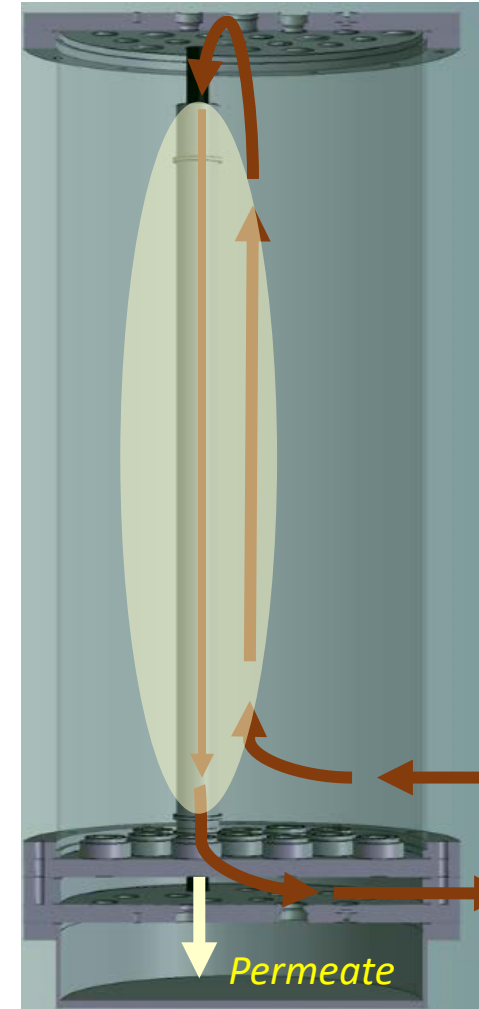
Glazed end of monolith

Perforated ring to hold the TiO₂ based mixed matrix fibers

Glass tube around the monolith introducing additional flow channel

Retentate

Permeate

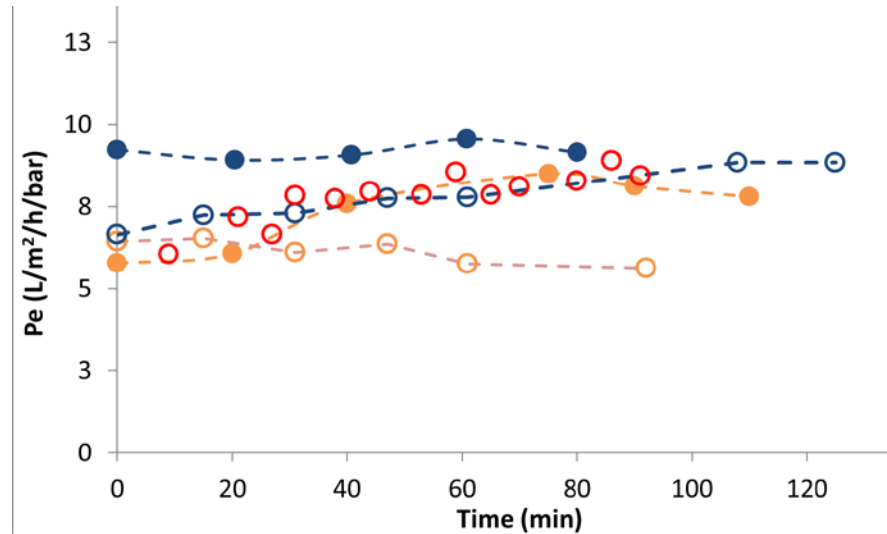


Cross section of side view

Liquid digestate

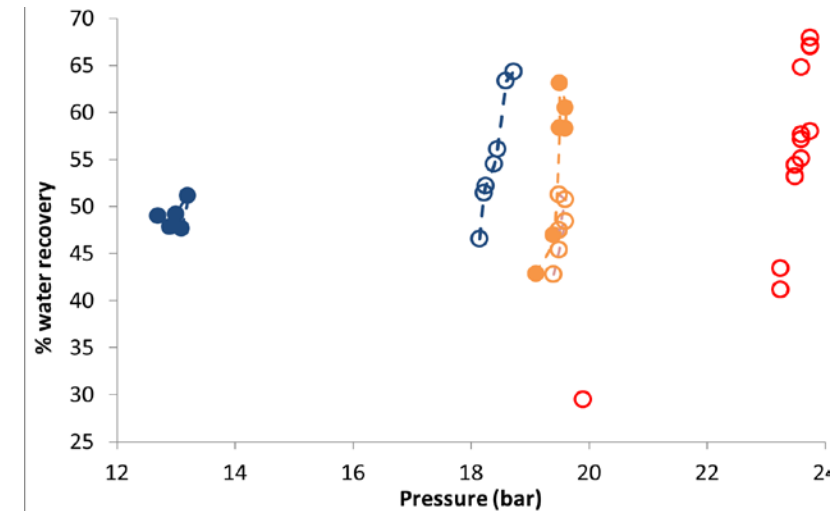
Retentate

Permeate



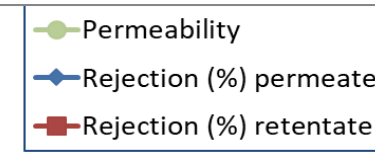
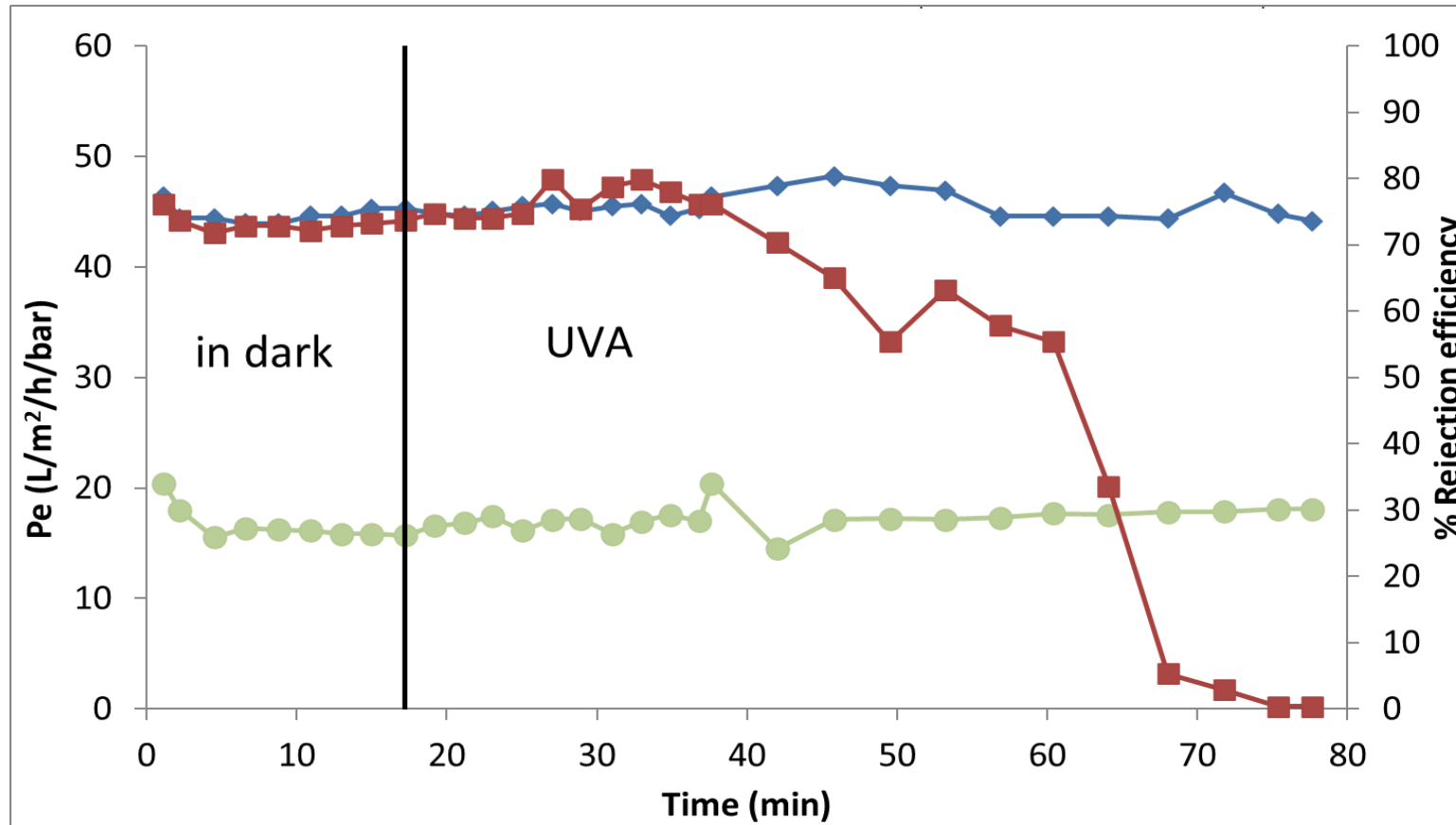
- Permeability_unmodified membrane with UV
- Permeability_unmodified membrane without UV
- Permeability_photocatalytic membrane with UV
- Permeability_photocatalytic membrane without UV
- Permeability_unmodified membrane without UV

- ❖ Permeability properties are not affected by photocatalytic coating of the nanofiltration membrane
- ❖ **Preservation of membrane productivity and extended life span**



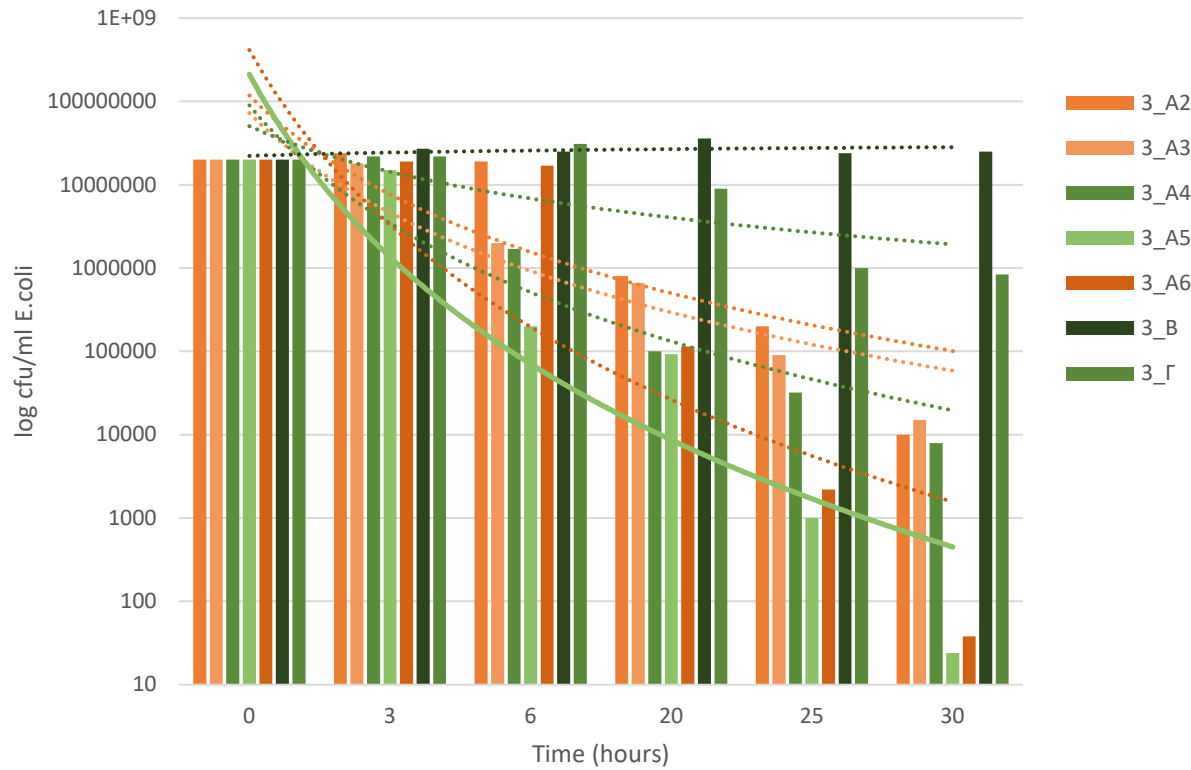
- unmod. Mem. With UV
- unmod. Mem. Without UV
- photocat. Mem. With UV
- photocat. Mem. Without UV
- unmod. Mem. Without UV

- ❖ *Clean water recovery of 50% can be reached at about 13.5 bar of transmembrane pressure*
- ❖ *>30% reduction in energy consumption of the photocatalytic nanofiltration process*



- ❖ Thiamethoxam: highly water-soluble molecule
- ❖ 73% rejection under dark due to absorption from permeate and retentate on the surface of membrane
- ❖ Decay of retentate rejection efficiency after 45 minutes due to ~20 mass ratio TiO₂/ Thiamethoxam

Conventional nanofiltration and photocatalytic nanofiltration experiment with a Thiamethoxam feed solution of 28 ppm. The vertical line corresponds to the initiation of the photocatalytic nanofiltration experiment

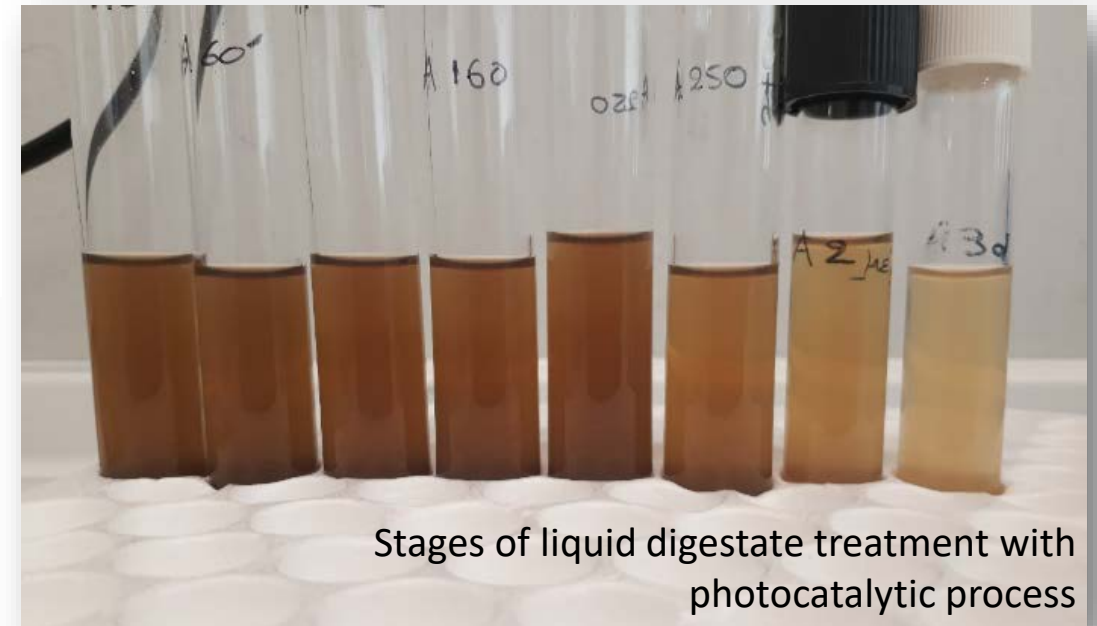


3_A: Different concentration of P25 under UVA

3_B: Maximum concentration 0,6 g/L P25 under dark conditions

3_Γ: Without P25 under UVA

- ❖ Synthetic waste inoculated with 10^7 cfu/ml E. coli.
- ❖ Photocatalysis dilution with 0,2- 0,6 g/L P25 under UVA.
- ❖ Disinfection 3 log observed after 25 hours of photocatalysis on sample 3_A5 0,5 g/L P25





- ❖ The implementation of the complete treatment process led to absence of pathogens and pollutants, reduction of COD by 86% , and increase of purity and transparency
- ❖ Photocatalysis as final sanitation stage in AD is efficient with economical and environmental advantages
- ❖ Industrial application of photocatalytic nanofiltration reactor on liquid digestate seems to overcome the drawbacks of digestate application on field
- ❖ Testing the photocatalytic nanofiltration reactor on real samples of liquid fraction of digestate from different AD plants
- ❖ Testing sanitation efficiency on different pathogens (E.faecalis, C. perfringens, Thermotolerant viruses)
- ❖ Scale up

Partners



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