

A Practical Operator Model of Biogas Yield from Full-scale Sewage Sludge Anaerobic Digestion

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Background

- Overall 80% of sewage sludge in the UK is treated using anaerobic digestion (AD)
- Anaerobic digestion is a practical and cost-effective method for the stabilisation and treatment of residual sewage sludge
- It is also a significant producer of renewable energy in the form of biogas
- There is still a lack of practical modelling tools available to guide operators and maximise the energy output



AD is a dynamic system affected by multiple factors:

Sludge composition

Sludge age

Primary SAS ratio

Volatile fatty acid
(VFA)

Iron dosing

Ammonia



Pretreatment



Asset age

Hydraulic retention time
(HRT)

Temperature

Dry solids (DS)

Volatile solids (VS)

Mixing efficiency

Organic loading rate

Data Summary

Routinely collected parameters:

- Temperature
- DS
- HRT

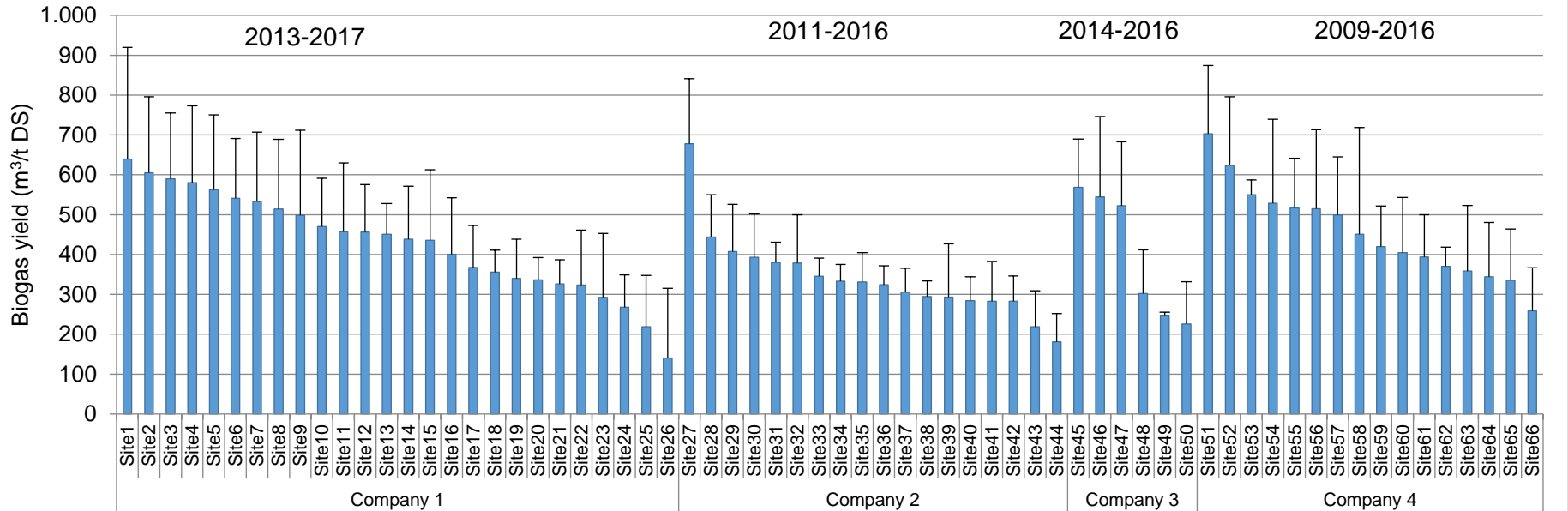
Additional parameters collected at specific sites:

- VS, sludge age, primary SAS ratio, VFA etc.



Data Summary

Conventional mesophilic anaerobic digestion (MAD) dataset



Multiple Regression Analysis

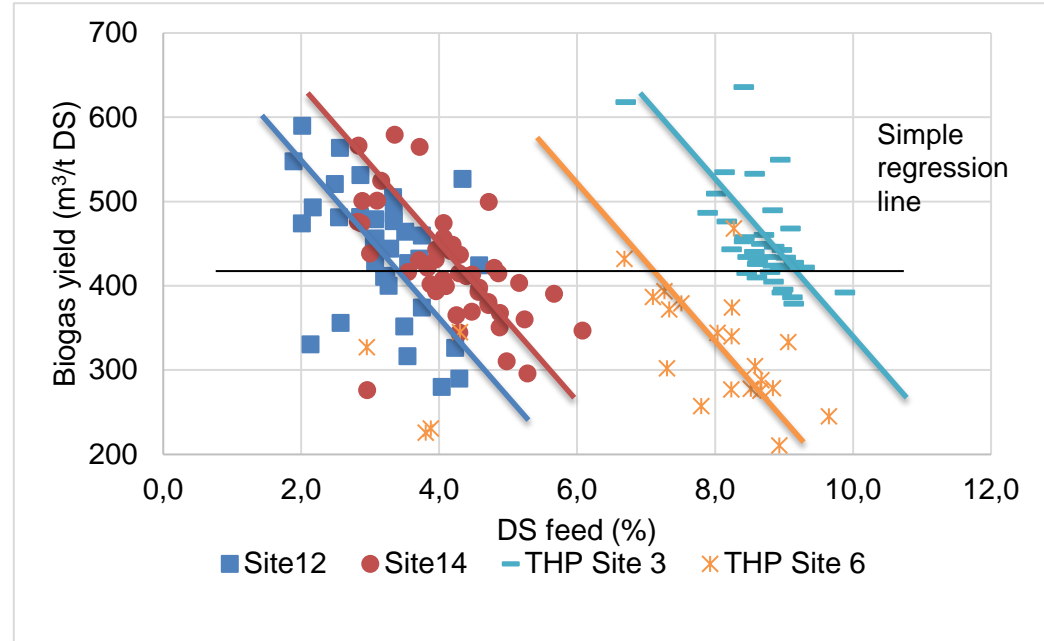
Simple linear multiple regression:

$$y = b_1x_1 + b_2x_2 + \dots + b_nx_n + C$$

- Significant predictors are selected based on $P < 0.05$

However, the full-scale AD data are clustered

- Categorical factor: multi-level regression
- Centering approach: evaluating the relative changes



Multiple Regression Analysis

Multi-level
factor



Conventional MAD model:

$$\text{Biogas yield} = \underline{230.9 * (\text{Ln}(\text{Temperature}) - 3.6)} + \underline{136.2 * (\text{Ln}(\text{HRT}) - 3.0)} - \underline{224.8 * (\text{Ln}(\text{DS}) - 1.5)} + \underline{75.5 * ((\text{Ln}(\text{HRT}) - 3.0) * (\text{Ln}(\text{DS}) - 1.5))} + \underline{\text{site factor}}$$

Variation explained: 0.46%

2.55%

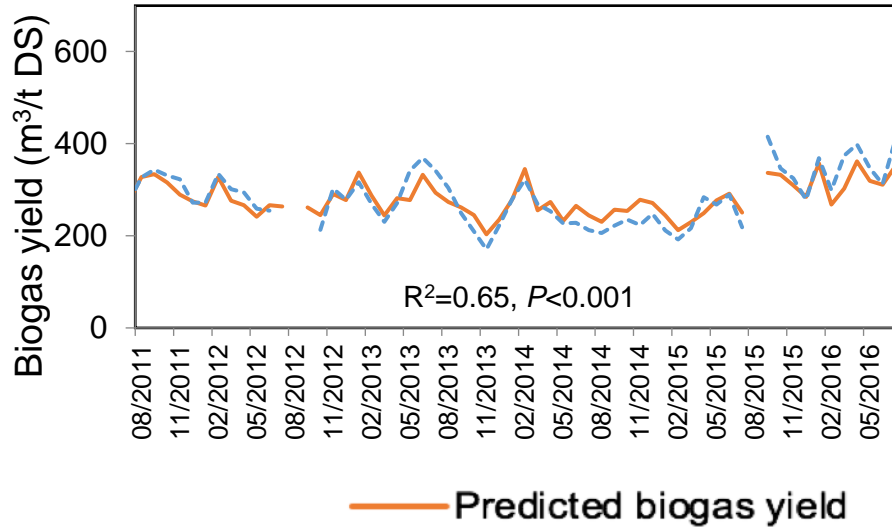
5.31%

0.11%

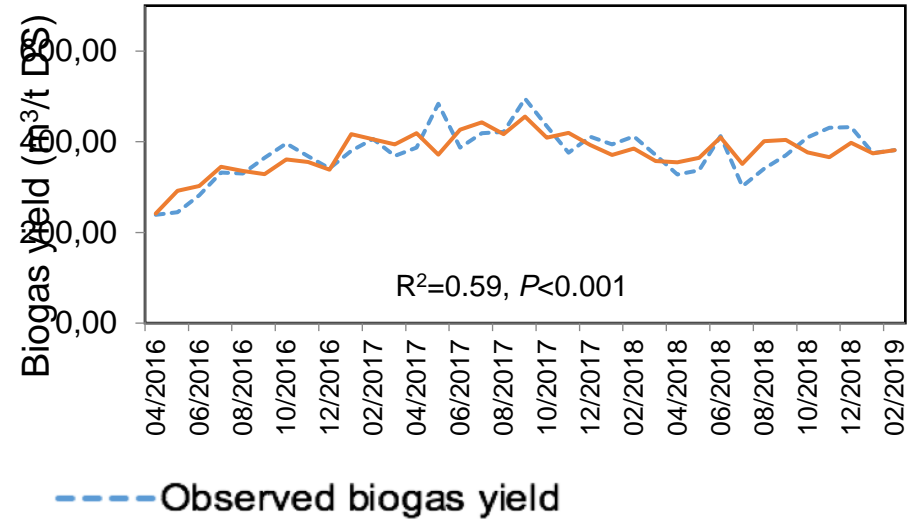
42.42%

Model Validation – Conventional MAD

Data involved in model generation
(2011 - 2016)
Site 42



Independent datasets
(2016 - 2019)
Site 38

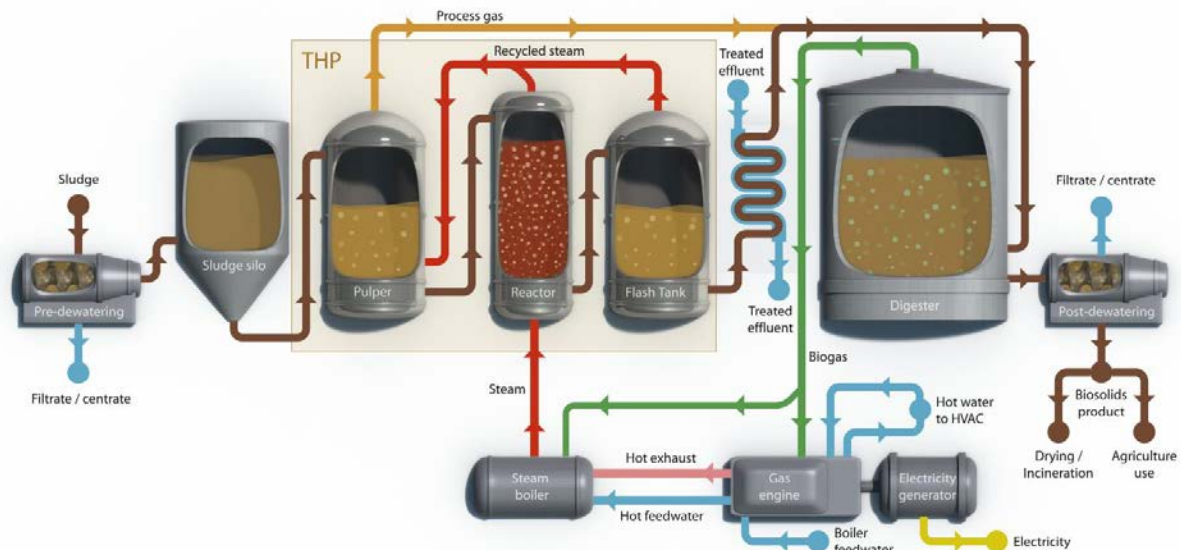


Expansion of Advanced AD

Thermal hydrolysis process (THP)

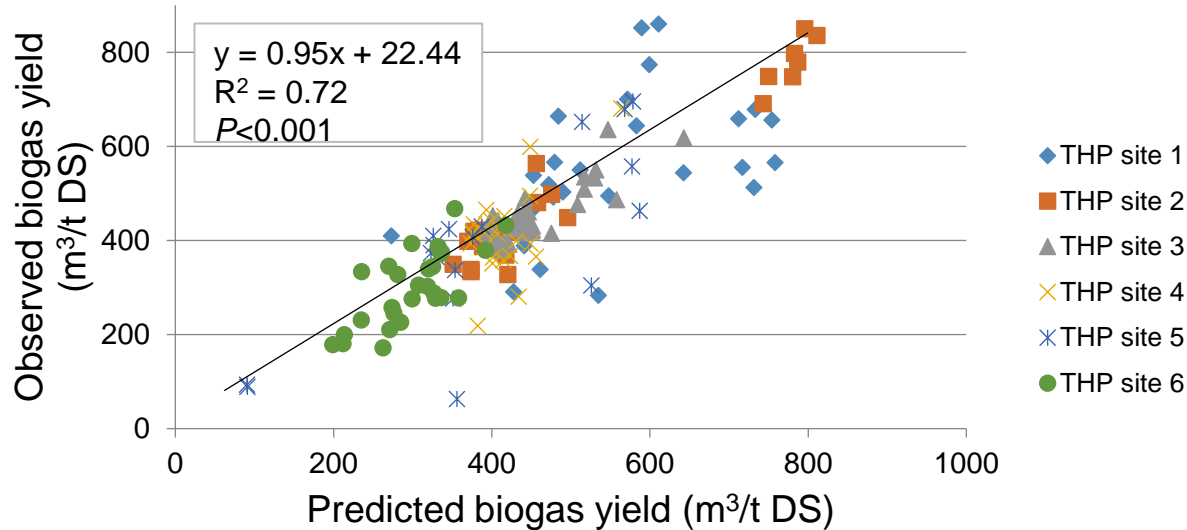
Increases:

- Loading rate
- Biogas yield
- VS reduction
- Pathogen kill
- Dewaterability



Combined Conventional-THP MAD Model Development

Apply conventional MAD model into THP datasets



Combined Conventional-THP MAD Model Development

Conventional MAD model :

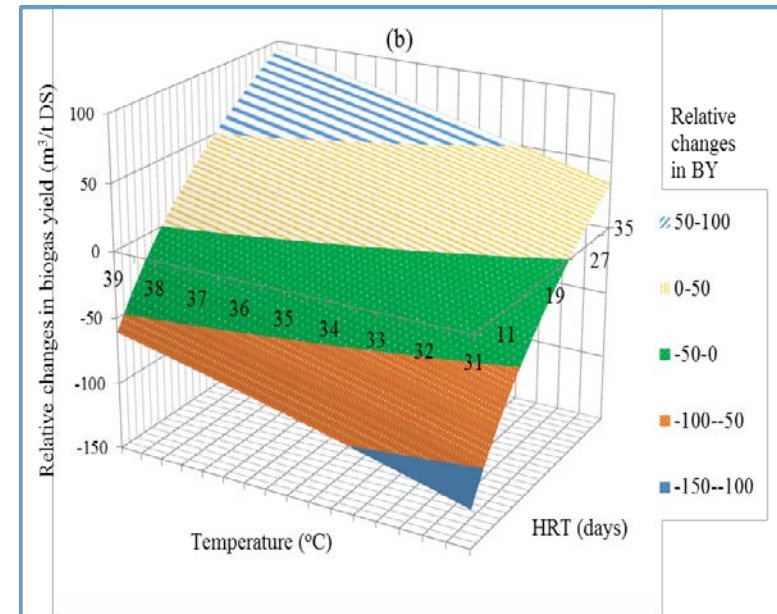
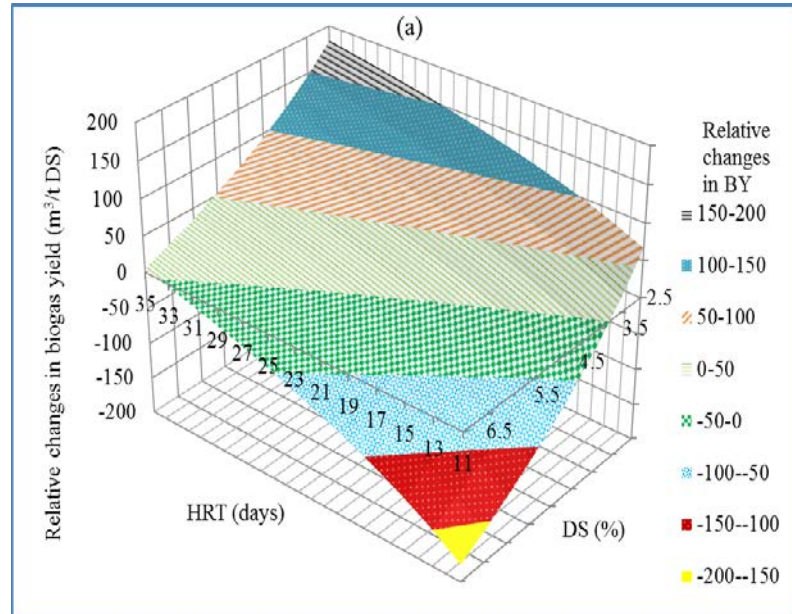
$$\text{Biogas yield} = 230.9 * (\text{Ln}(\text{Temperature}) - 3.6) + 136.2 * (\text{Ln}(\text{HRT}) - 3.0) - 224.8 * (\text{Ln}(\text{DS}) - 1.5) + 75.5 * ((\text{Ln}(\text{HRT}) - 3.0) * (\text{Ln}(\text{DS}) - 1.5)) + \text{site factor}$$

Combined conventional-THP MAD model :

$$\text{Biogas yield} = 265.3 * (\text{Ln}(\text{Temperature}) - 3.6) + 133.7 * (\text{Ln}(\text{HRT}) - 3.0) - 216.4 * (\text{Ln}(\text{DS}) - 1.5) + 61.7 * ((\text{Ln}(\text{HRT}) - 3.0) * (\text{Ln}(\text{DS}) - 1.5)) + \text{site factor}$$

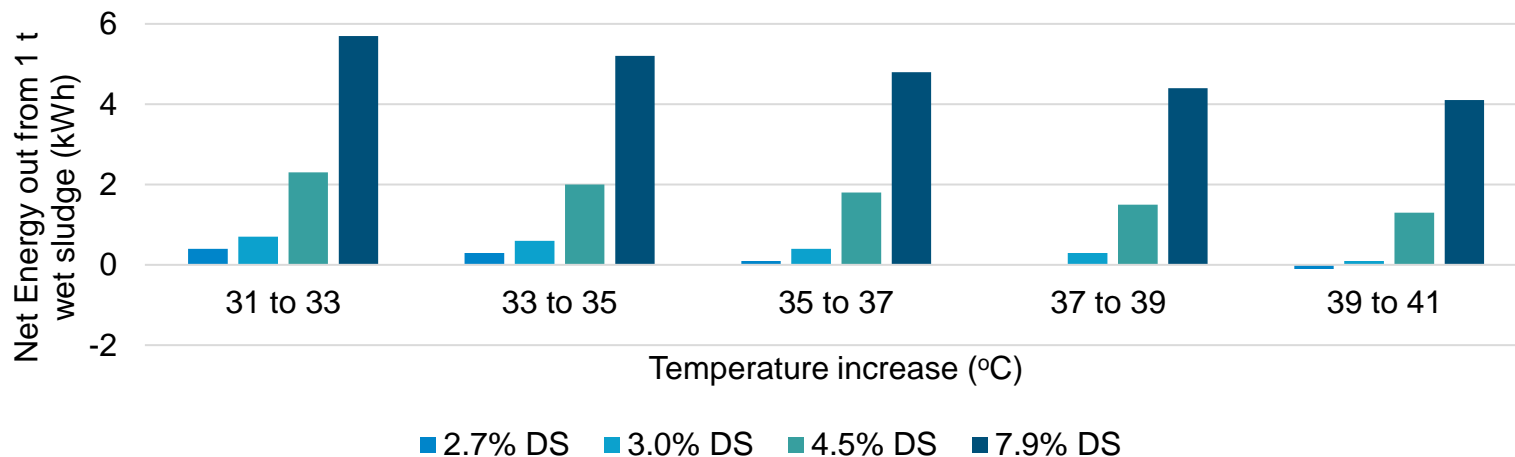
Combined Conventional-THP MAD Model

Impact of HRT, DS and temperature on performance



Optimisation Strategies

Net energy balance - changing temperature and DS



Energy required to heat 1 t wet sludge is 2.3 kWh. 2.7% DS is the lower 5% percentile range value of monthly average operational data for conventional MAD sites; 3.0% is the break point sludge feed DS for a positive net energy balance for MAD; 4.5% and 7.9% DS are the mean values of monthly average operational data for conventional and THP MAD sites, respectively.

Conclusions

- The first time that simple operational models of the AD process have been developed based on full-scale operational data
- Important to balance the three key operational parameters (temperature, HRT, and DS) to optimise the energy balance of the process
- Increasing sludge solids content improves overall AD energy balance
- **Liu, J. and Smith, S.R. (2020) A multi-level biogas model to optimise the energy balance of full-scale sewage sludge conventional and THP anaerobic digestion. *Renewable Energy* 159, 756-766**

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