

## Lignocellulosic waste valorization by hydrothermal carbonization and anaerobic digestion

R.P. Ipiiales, A.F. Mohedano, E. Diaz, M.A. de la Rubia  
Universidad Autónoma de Madrid  
[ricardo.ipiales@estudiante.uam.es](mailto:ricardo.ipiales@estudiante.uam.es)



BIO3



Universidad Autónoma  
de Madrid



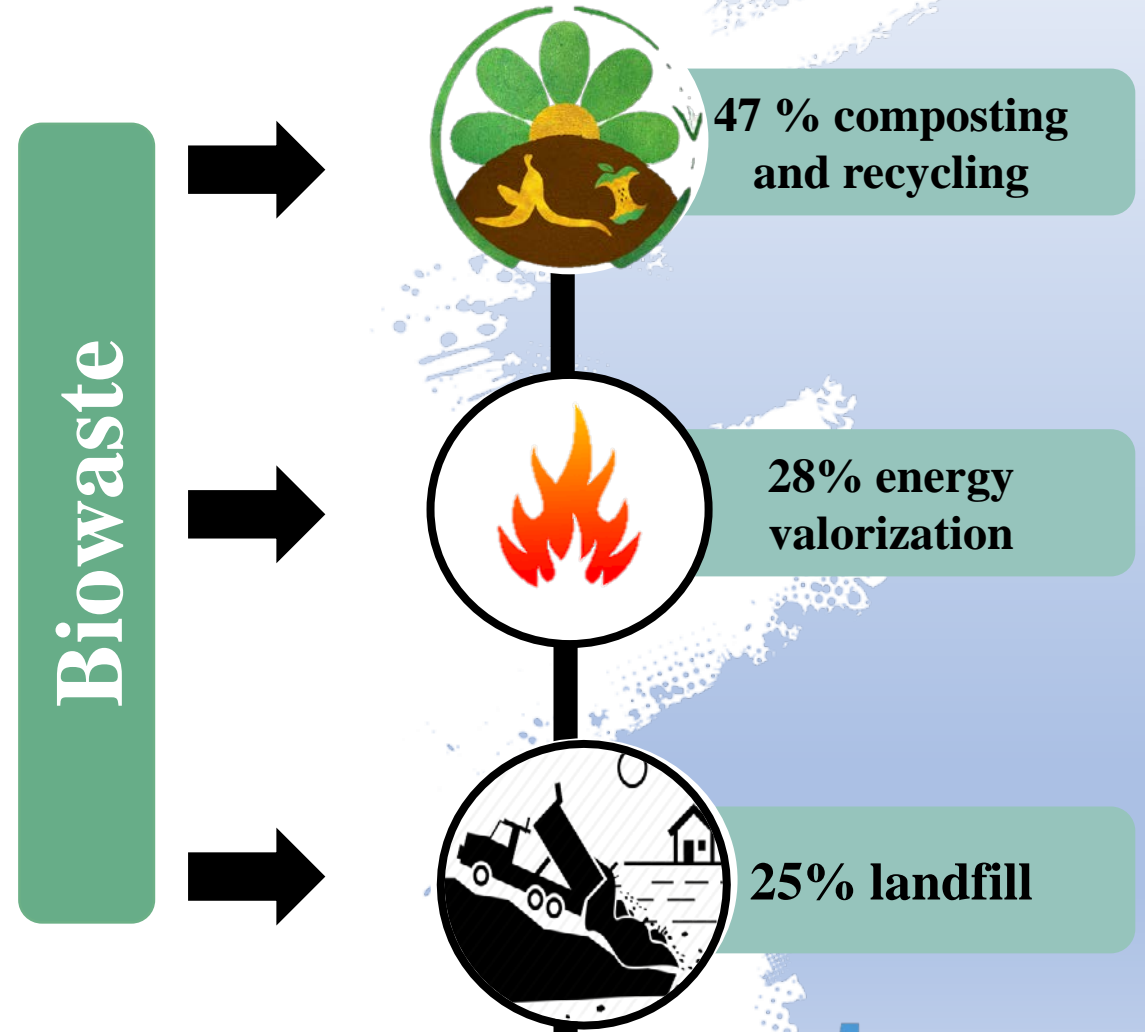
UNIÓN EUROPEA  
Fondo Social Europeo  
El FSE invierte en tu futuro

# Background



$2.2 \cdot 10^8$  t MSW year<sup>-1</sup>

≈ 10% lignocellulosic biomass

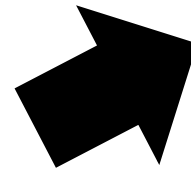


# Background

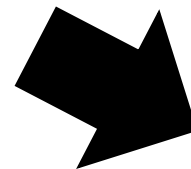
**Urban pruning  
waste**



**Energy  
resource**



**Industrial level**



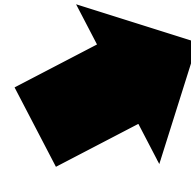
**Home level**

# Background

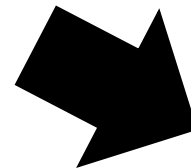
**Urban pruning  
waste**



**Energy  
resource**



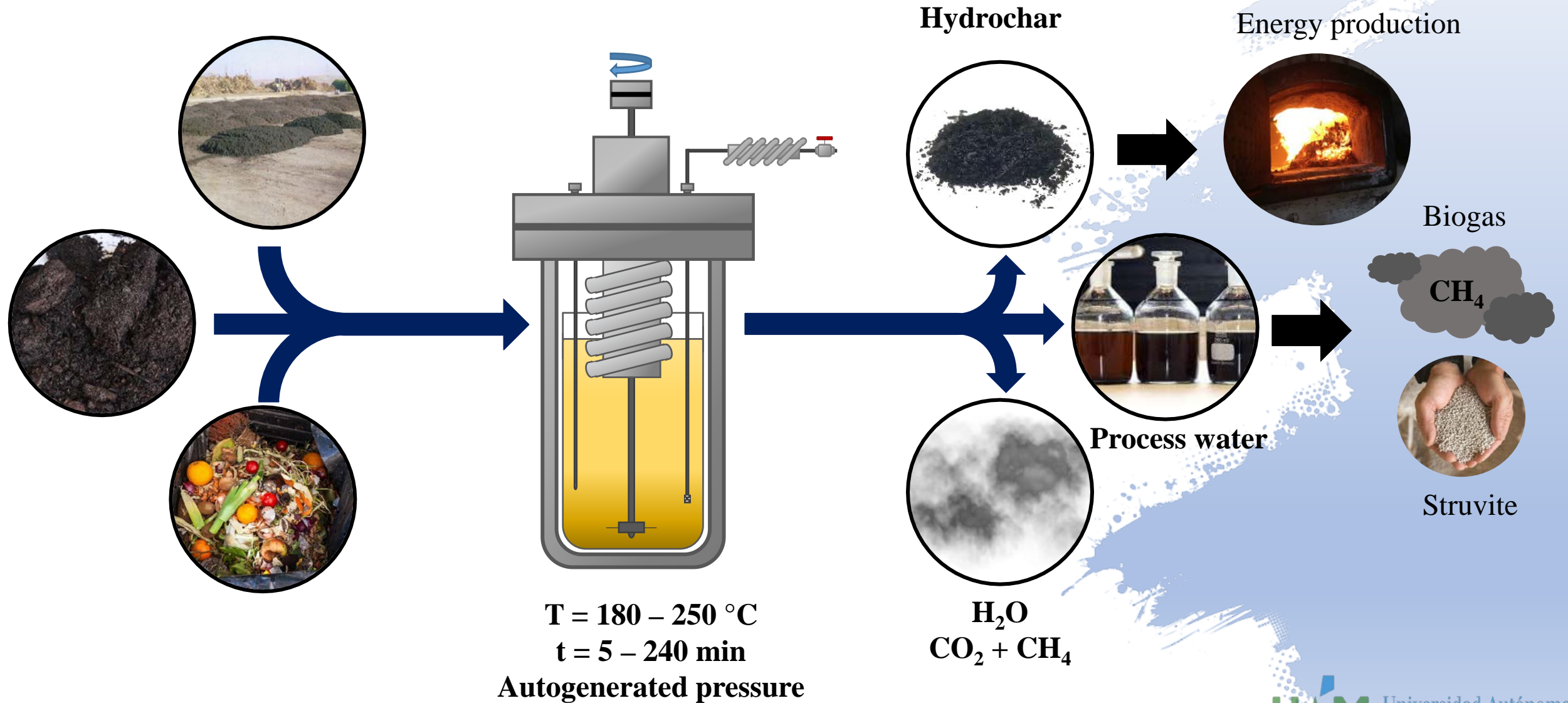
**Industrial level**



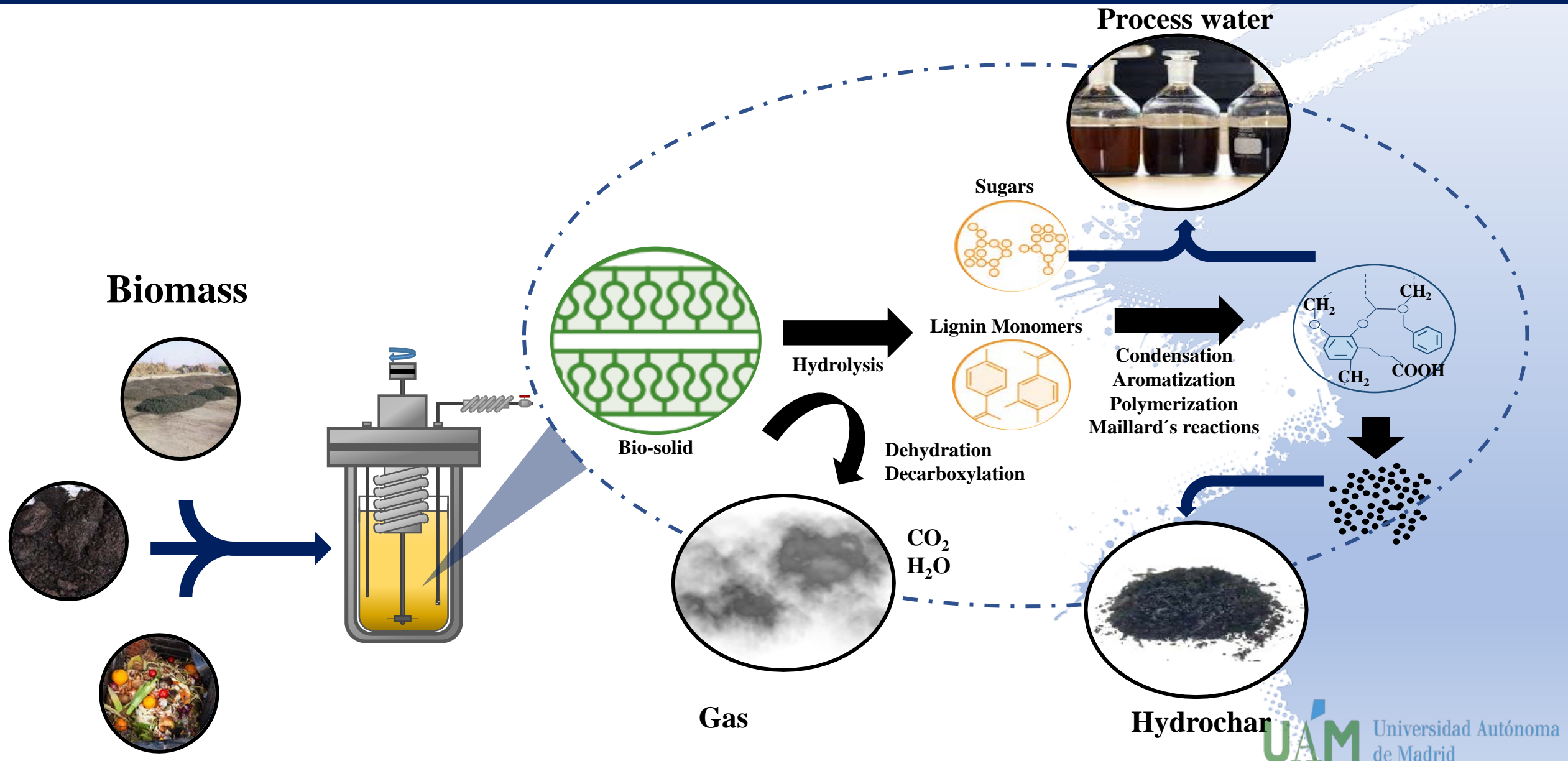
**Home level**



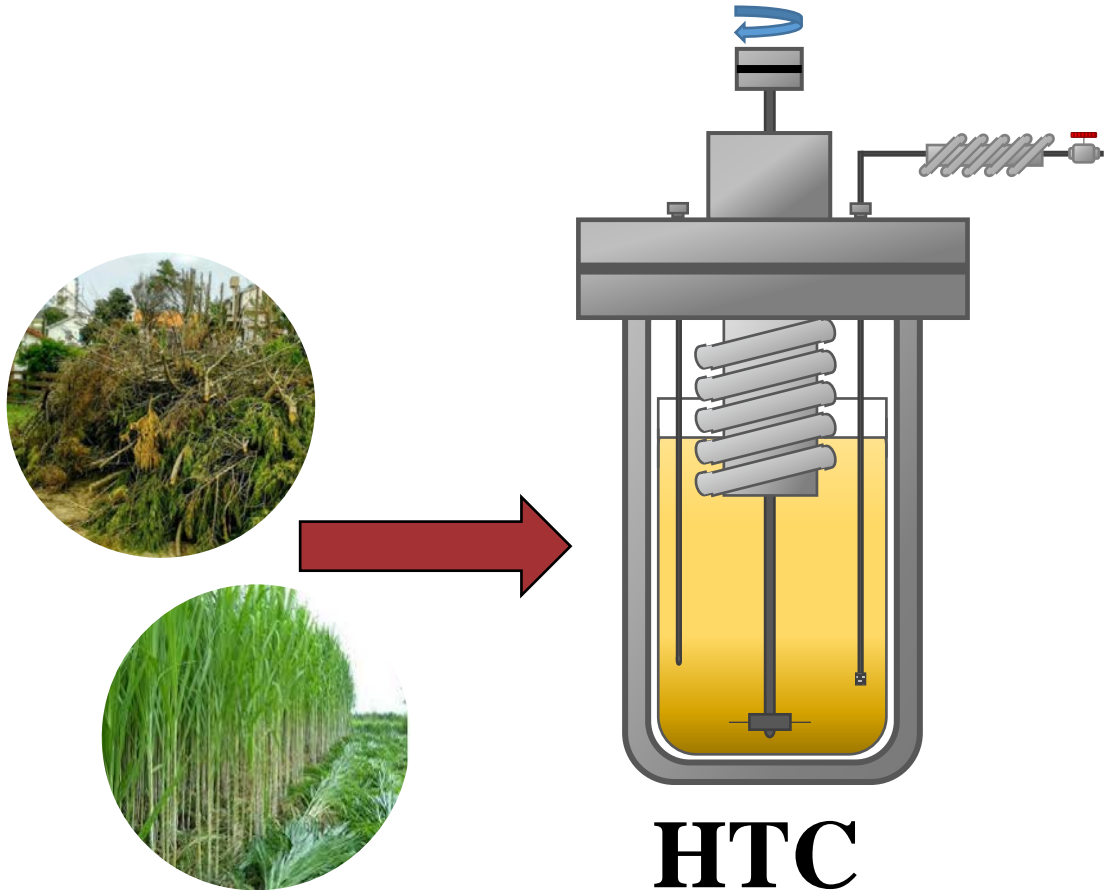
# Hydrothermal carbonization (HTC)



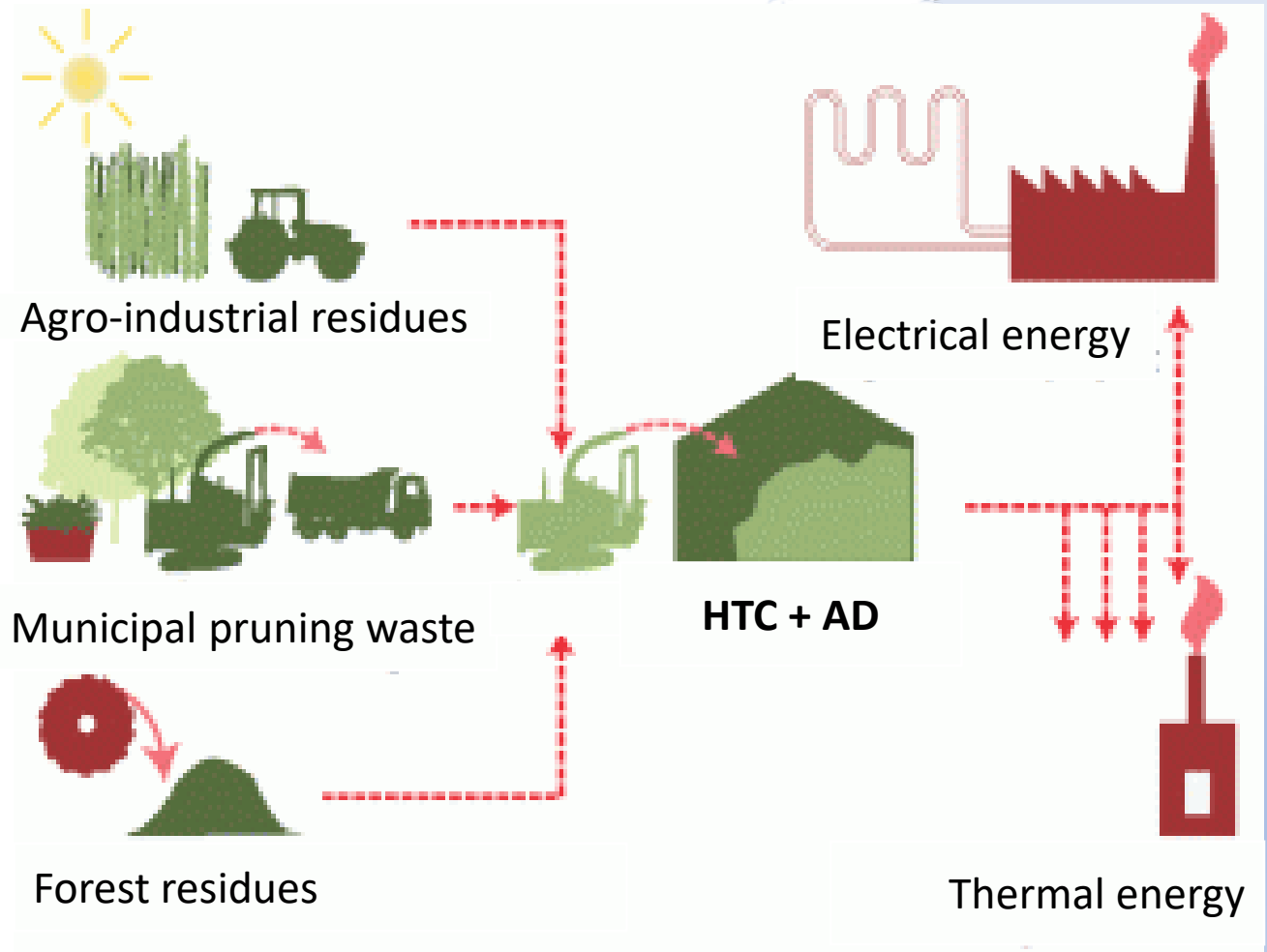
# Hydrothermal carbonization (HTC)



# Objective



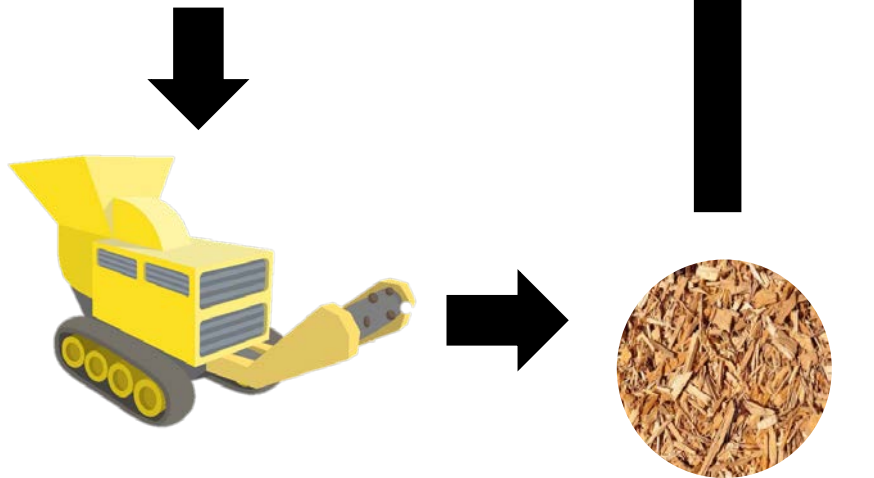
**T = 180 – 210 – 230 °C**  
**t = 60 min**



# Characterization of urban pruning waste (UPW)



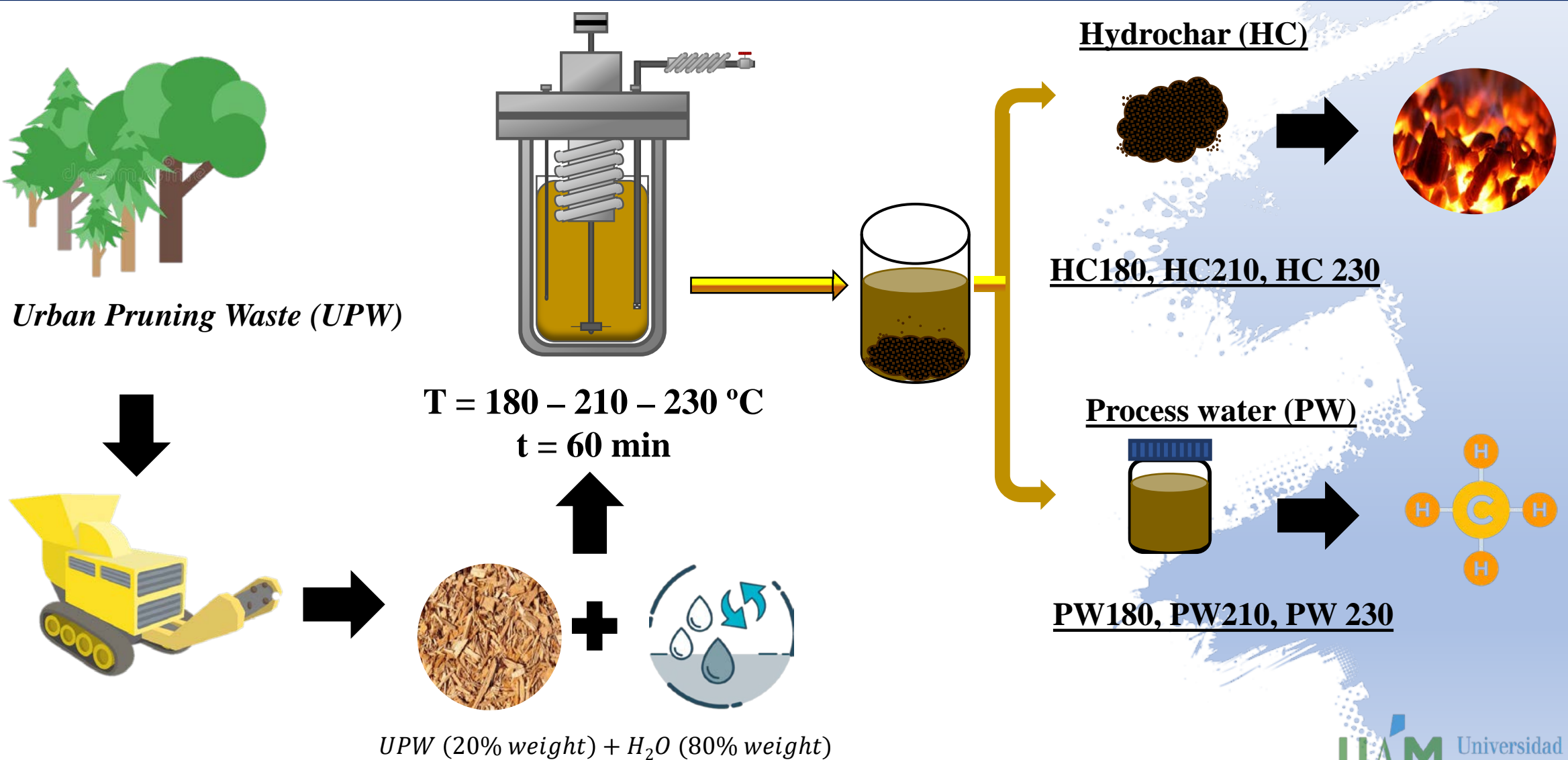
*Urban Pruning Waste (UPW)*



Characteristics	UPW
Moisture (%)	4.8 ± 0.2
C (%)	46.9 ± 1.1
H (%)	6.1 ± 0.4
N (%)	0.9 ± 0.1
S (%)	0.4 ± 0.2 X
O* (%)	40.6 ± 0.1
Volatile matter (d.b.%)	76.5 ± 0.1 X
Ash (d.b.%)	5.1 ± 0.1
Fixed carbon (d.b.%)	18.4 ± 0.1
HHV (MJ kg <sup>-1</sup> )	19.7 ± 0.1
H/C	1.55
O/C	0.65
NPK	0.9/0.1/0.5



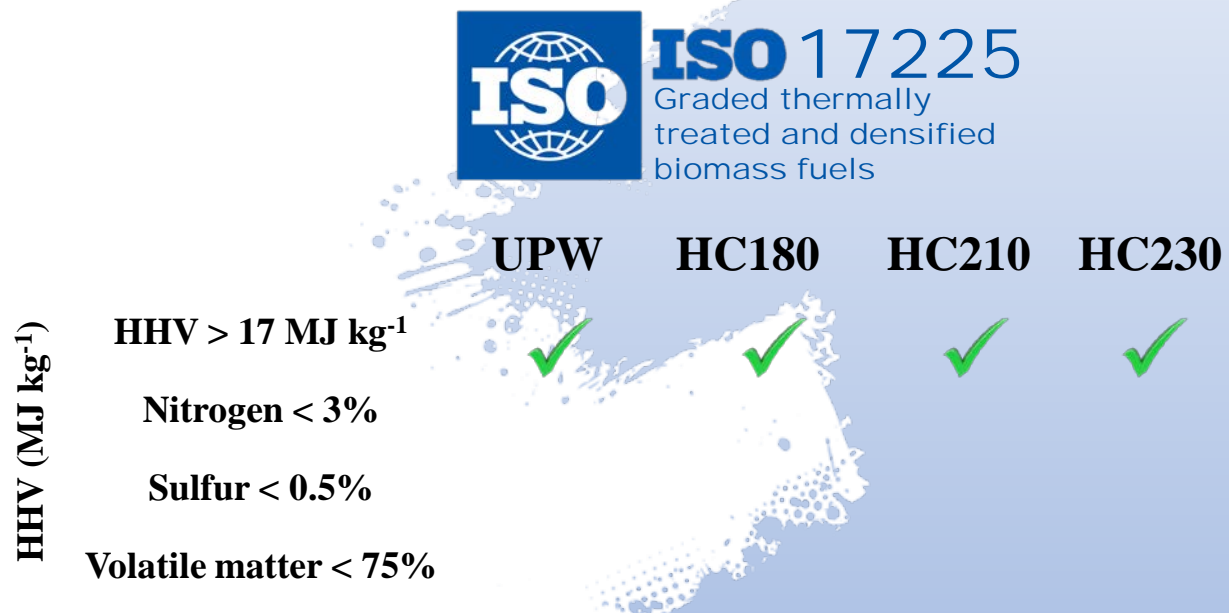
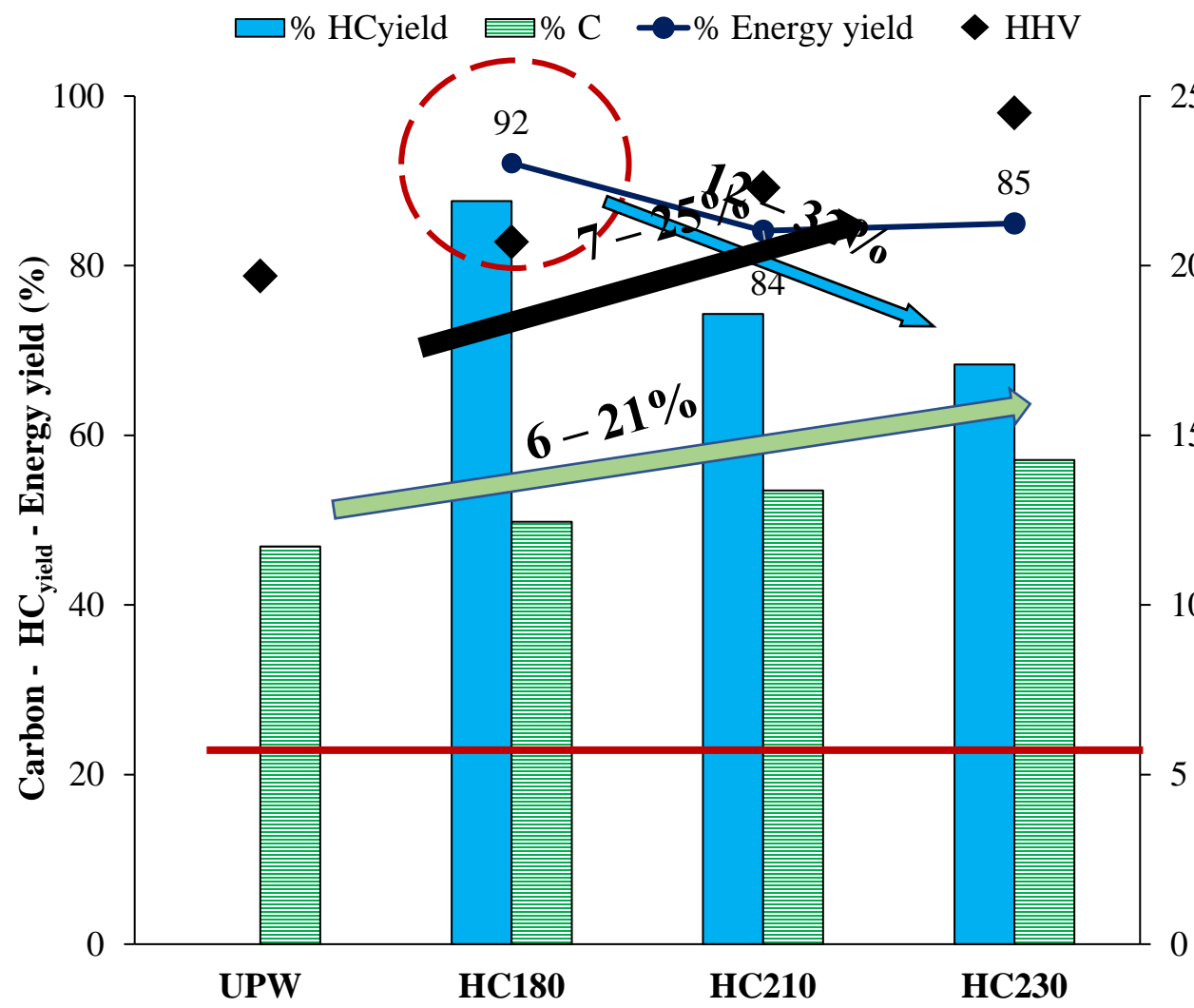
# Methods



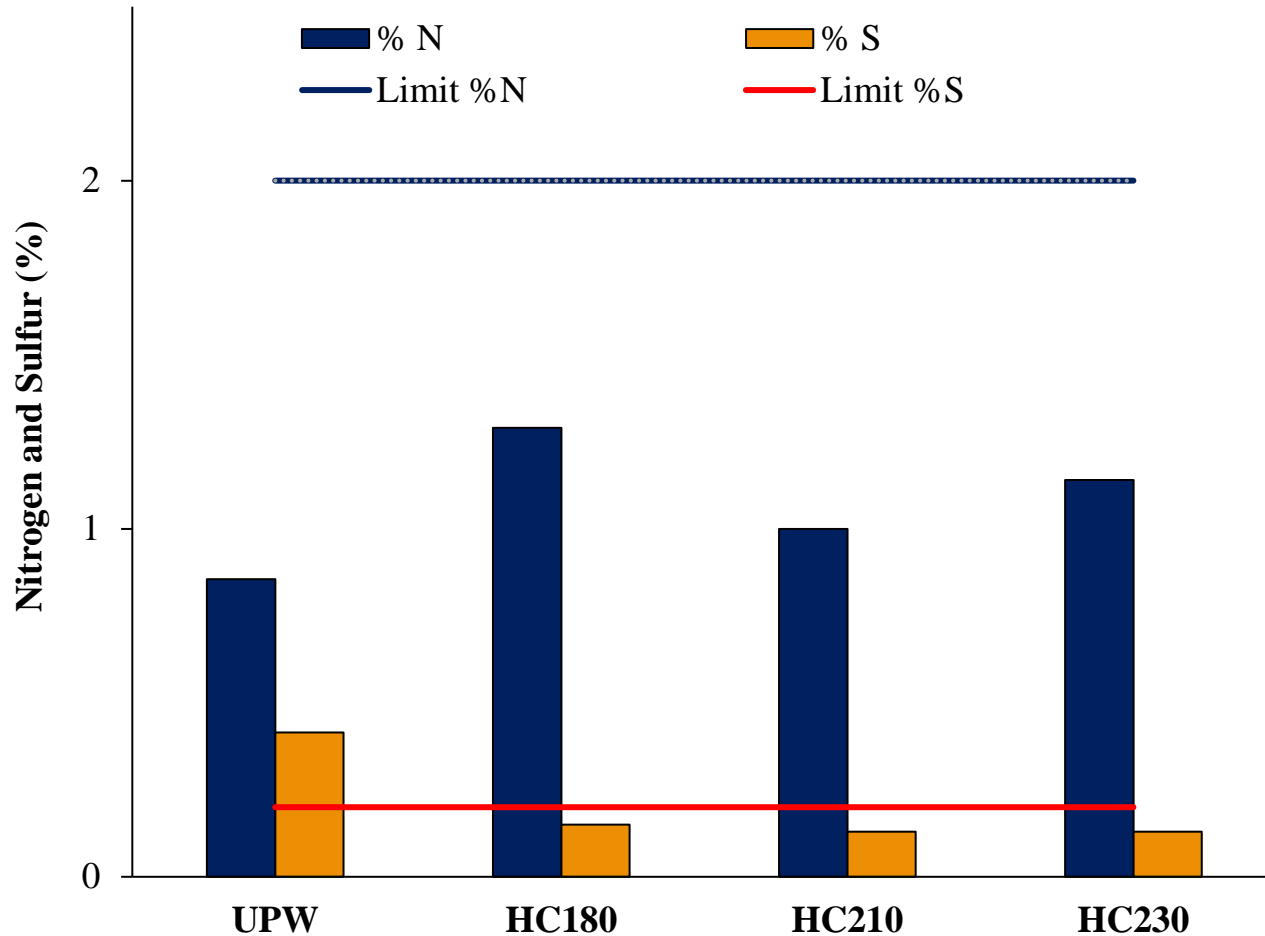
# Results



# 8th International Conference on Sustainable Solid Waste Management

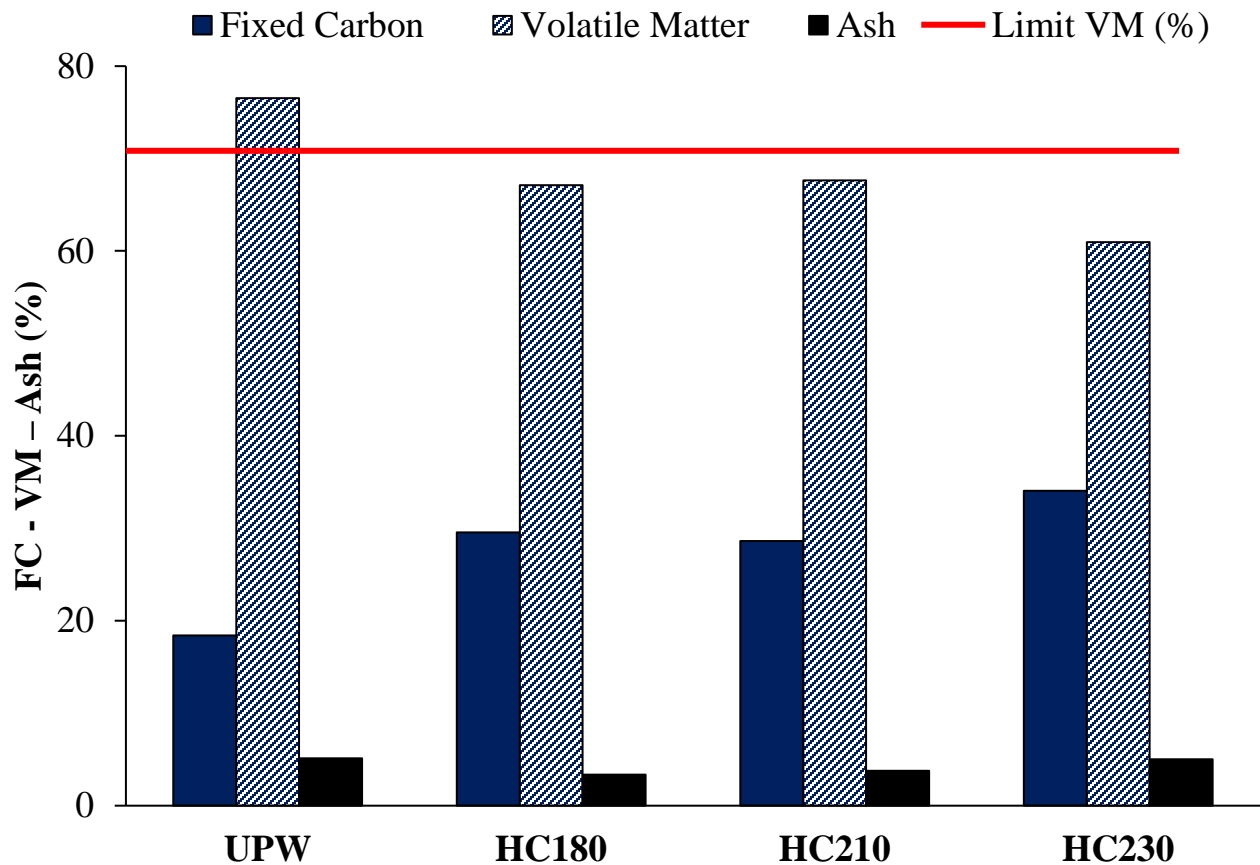


# Nitrogen and Sulfur content



	UPW	HC180	HC210	HC230
HHV > 17 MJ kg <sup>-1</sup>	✓	✓	✓	✓
Nitrogen < 2%	✓	✓	✓	✓
Sulfur < 0.3%	✗	✓	✓	✓
Volatile matter < 75%				

# Proximal analysis



	UPW	HC180	HC210	HC230
HHV > 17 MJ kg <sup>-1</sup>	✓	✓	✓	✓
Nitrogen < 2%	✓	✓	✓	✓
Sulfur < 0.3%	✗	✓	✓	✓
Volatile matter < 75%	✗	✓	✓	✓



# Proximal analysis

## Proximal analysis

Ash content

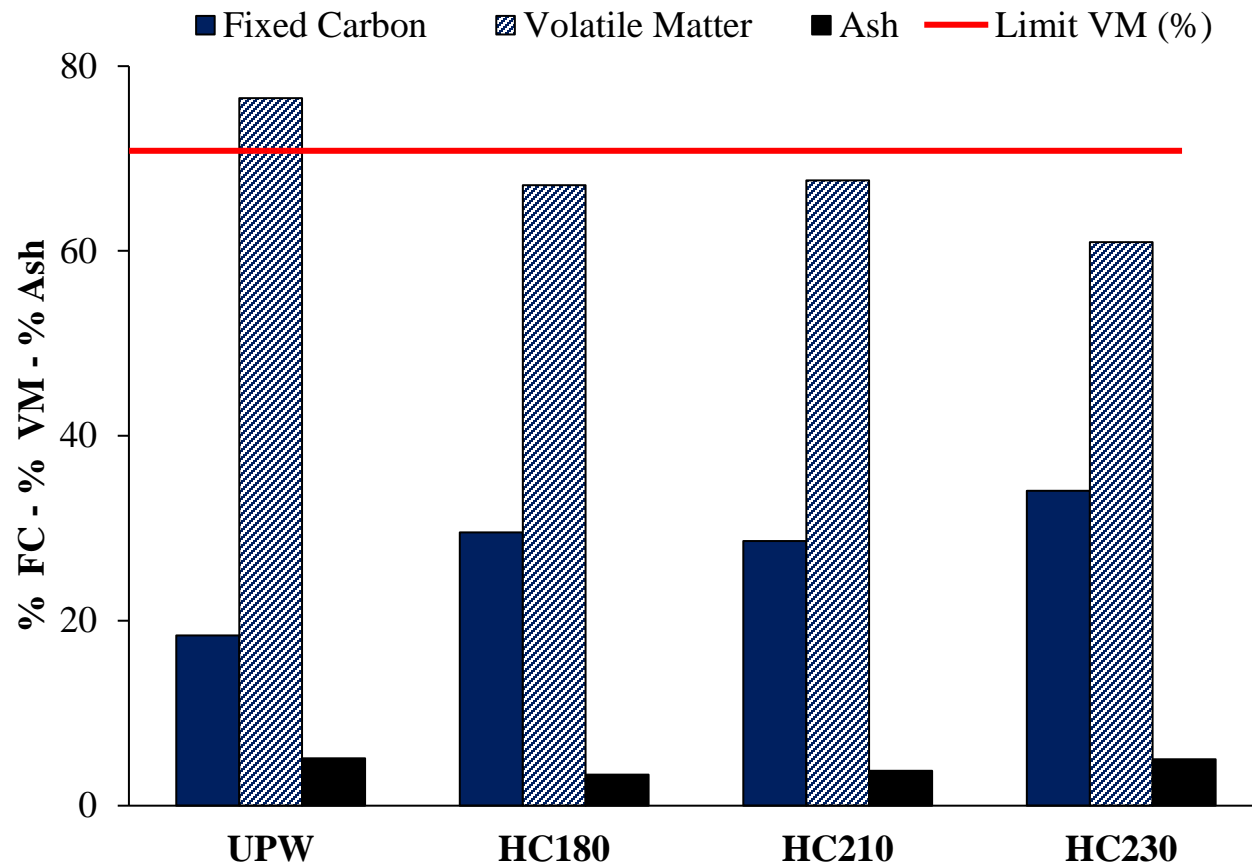


5 – 35%

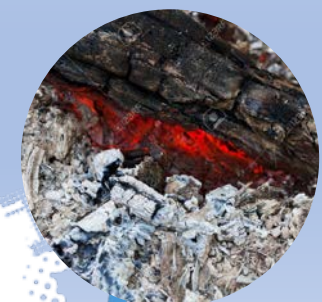
SI < 0.3 Low

FI < 4 Medium

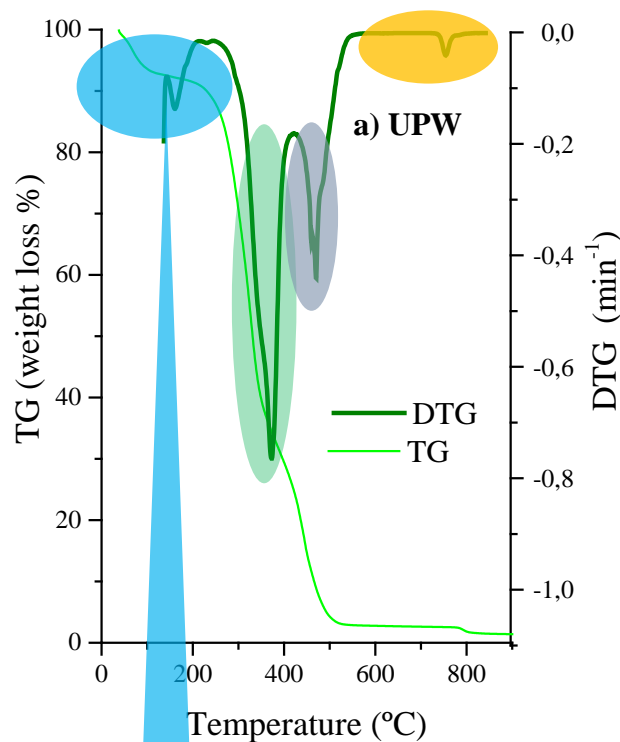
AI < 0.2 Low



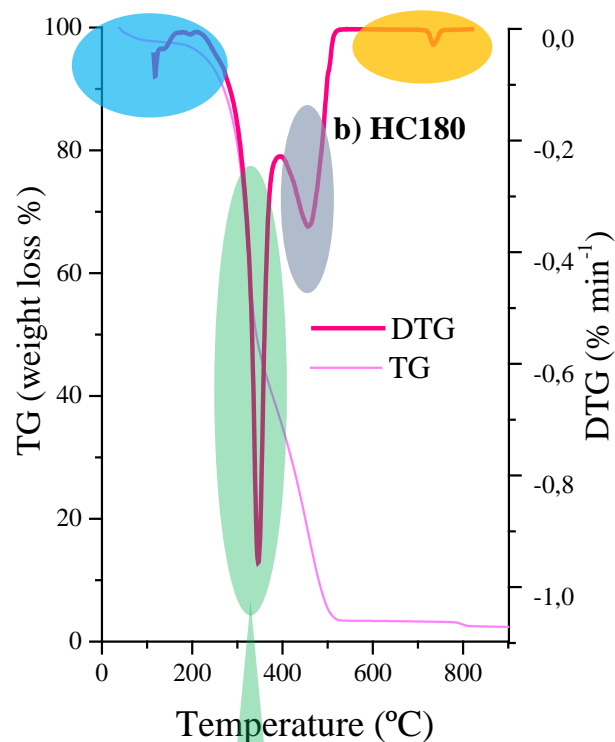
	UPW	HC180	HC210	HC230
$R_{b/a}$	1.3	1.0	1.2	1.2
SI	0.53	0.16	0.15	0.16
FI	7.47	3.08	2.56	2.08
AI (kg GJ <sup>-1</sup> )	0.30	0.09	0.07	0.07



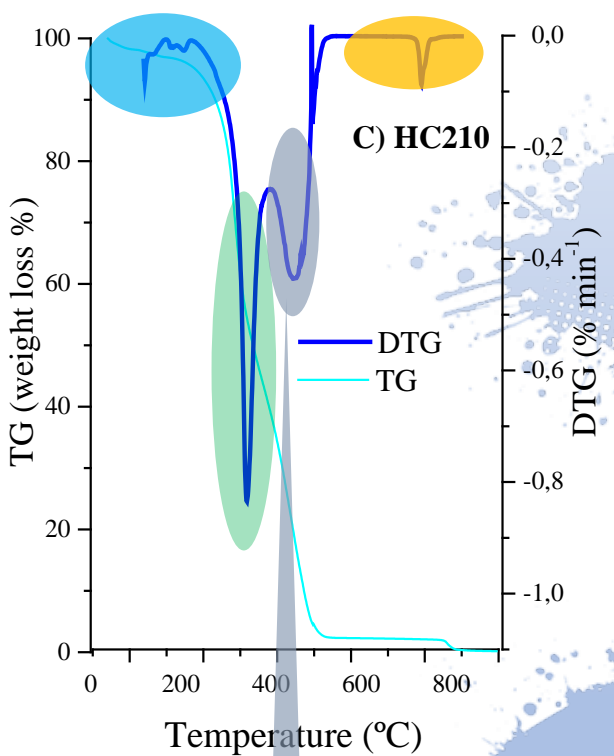
# Thermogravimetric and differential TG profiles



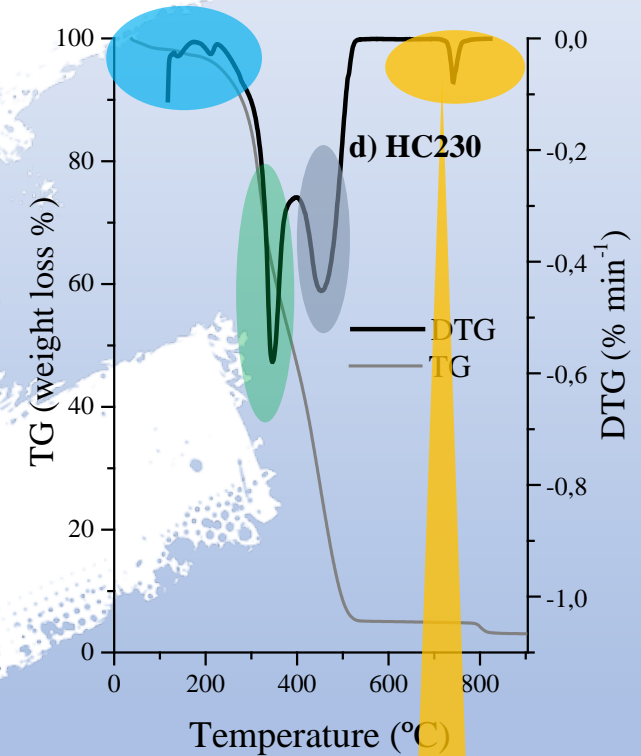
Loss of moisture and light volatile compounds < 100  $^{\circ}\text{C}$



Devolatilization of VM, cellulose and hemicellulose 240 – 320  $^{\circ}\text{C}$

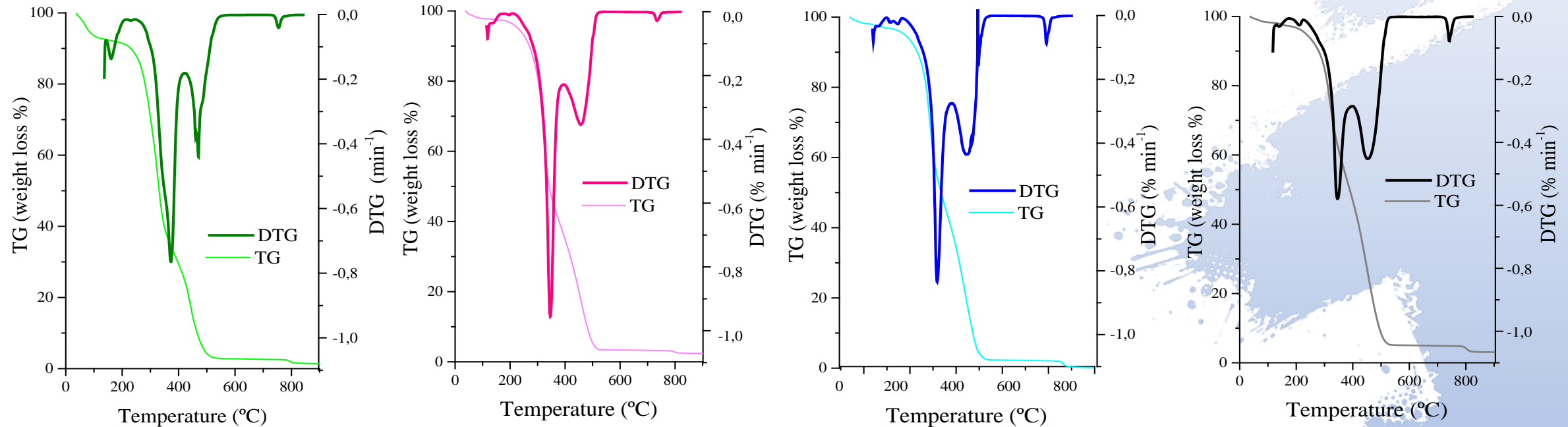


Combustion of high molecular weight compounds, lignin and FC 420 – 440  $^{\circ}\text{C}$



Inorganic matter decomposition like carbonates 760 – 780  $^{\circ}\text{C}$

# Thermogravimetric and differential TG profiles



	UPW	HC180	HC210	HC230
$T_i$ (°C)	239	242	251	254
$T_m$ (°C)	326	325	318	313
$T_b$ (°C)	533	528	528	536
$CCI \cdot 10^{-7}$ (min <sup>-2</sup> °C <sup>-3</sup> )	7.8	8.0	8.4	9.6
$Z_i$ (% min <sup>3</sup> )	8.6	10.6	11.4	11.6
$H_j$ (% min <sup>4</sup> )	0.2	0.3	0.4	0.4

HC combustion reactivity



# Process water characterization

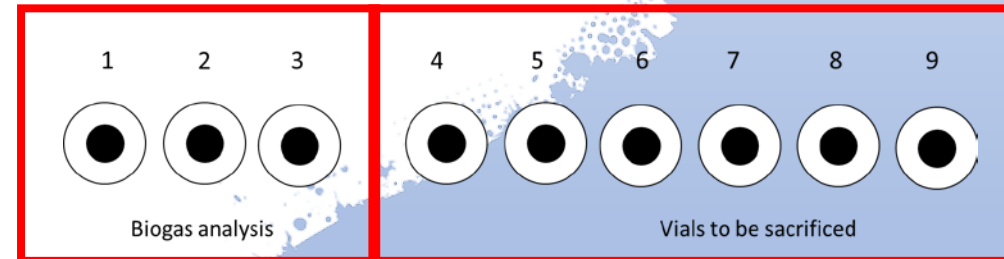
	PW180	PW210	PW230
<b>pH</b>	$3.5 \pm 0.1$	$3.4 \pm 0.1$	$3.5 \pm 0.1$
<b>COD (g L<sup>-1</sup>)</b>	$51.1 \pm 1.3$	$39.3 \pm 0.5$	$44.9 \pm 2.4$
<b>TOC (g L<sup>-1</sup>)</b>	$21.1 \pm 0.1$	$17.0 \pm 0.1$	$18.4 \pm 0.1$
<b>TVFA (g L<sup>-1</sup>)</b>	$1.5 \pm 0.0$	$0.9 \pm 0.0$	$0.2 \pm 0.0$
<b>TS (g L<sup>-1</sup>)</b>	$30.7 \pm 0.3$	$19.3 \pm 0.3$	$21.6 \pm 0.4$
<b>VS (g L<sup>-1</sup>)</b>	$27.0 \pm 0.4$	$16.1 \pm 0.2$	$18.5 \pm 0.3$



## Biochemical methane potential

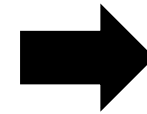
ISR = 2

- 15 g VS L<sup>-1</sup> granular anaerobic sludge
- 7.5 g VS L<sup>-1</sup> substrate



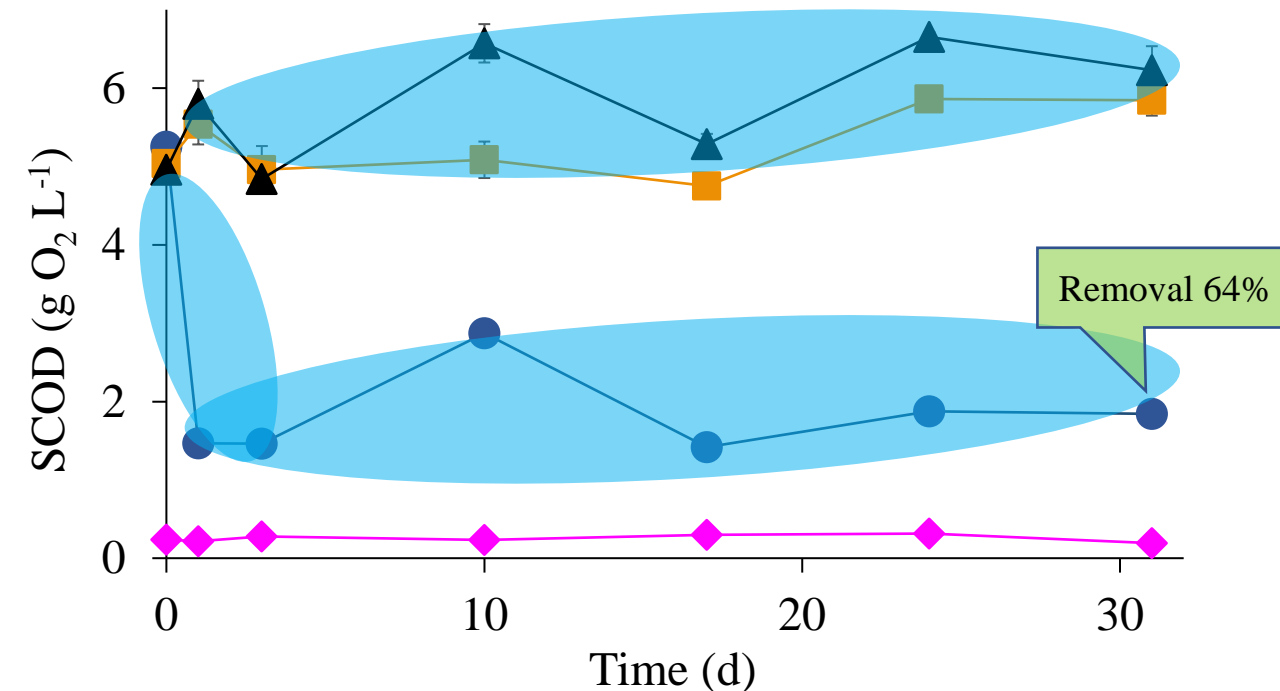
# Biochemical methane potential

- ✓ pH (7.5 – 7.8)
- ✓ Alkalinity ( $> 2.5 \text{ g CaCO}_3 \text{ L}^{-1}$ )
- ✓ Total ammonia nitrogen ( $1700 \text{ mg L}^{-1} < \text{inhibition values}$ )

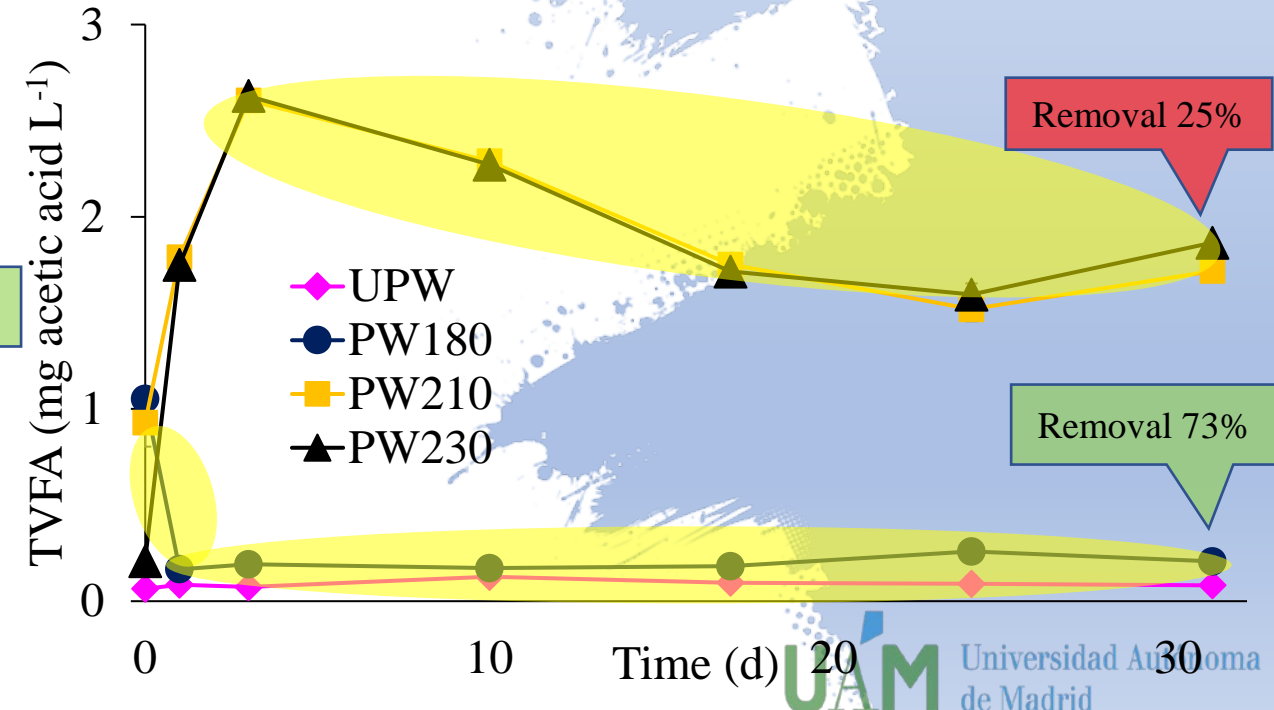


**Adequate for the AD process**

### Soluble chemical oxygen demand (SCOD)

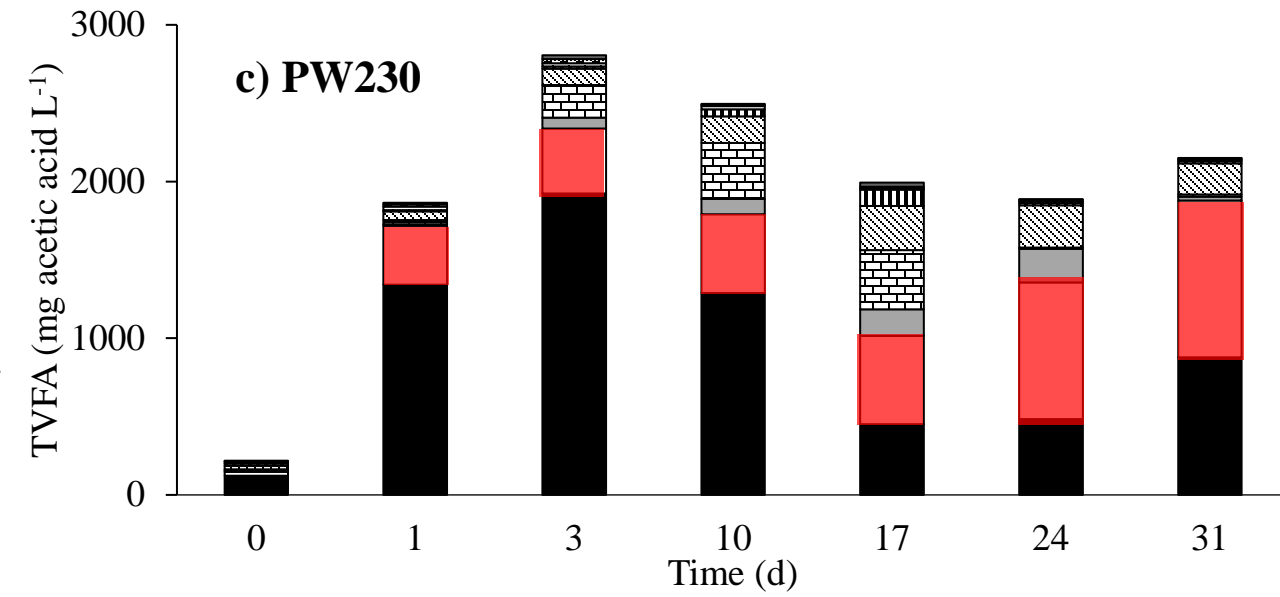
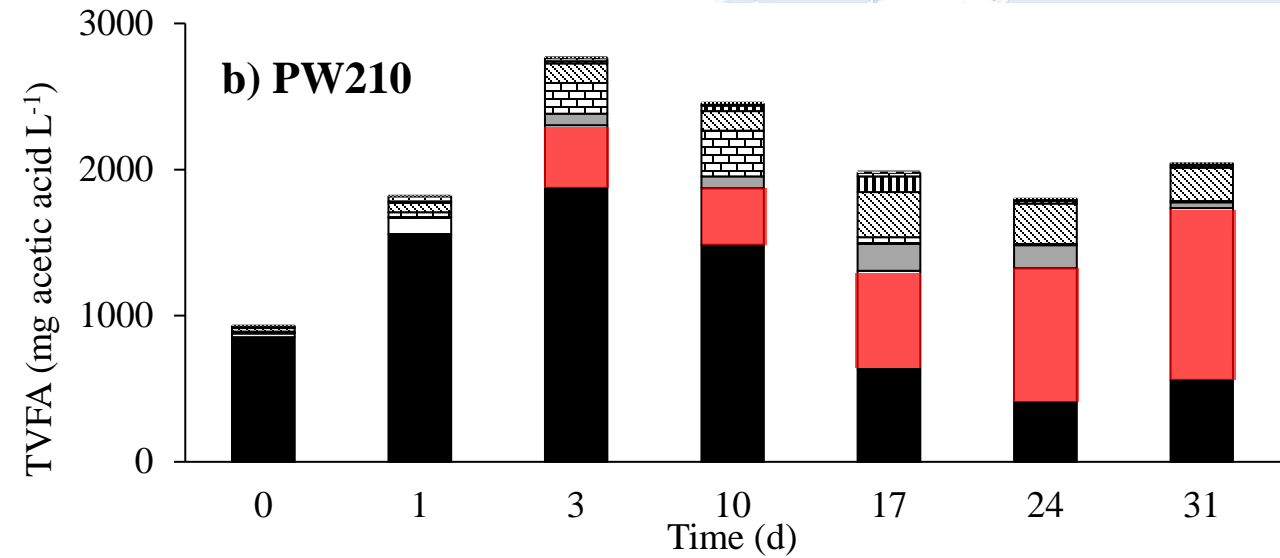
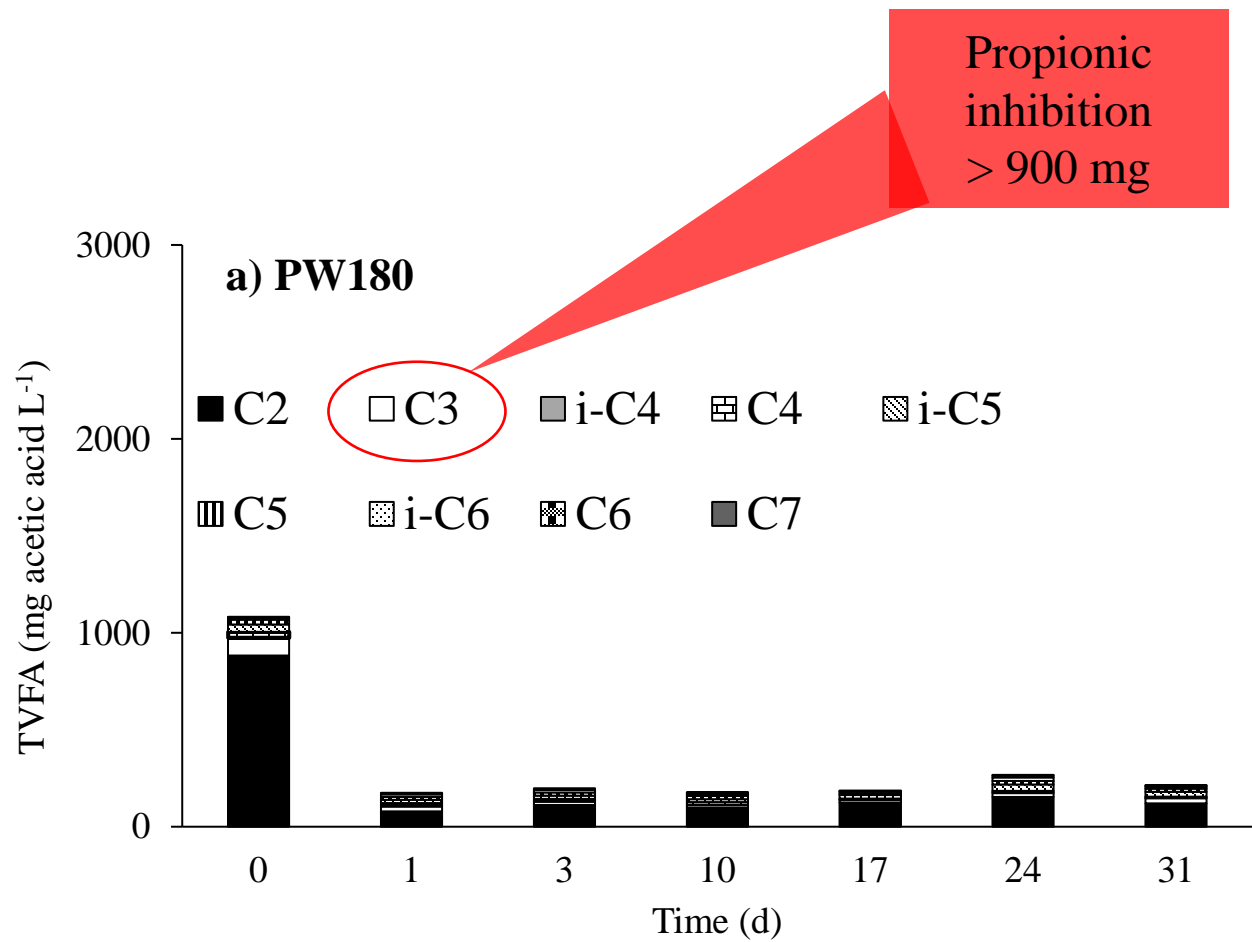


### Volatile fatty acids (VFA)

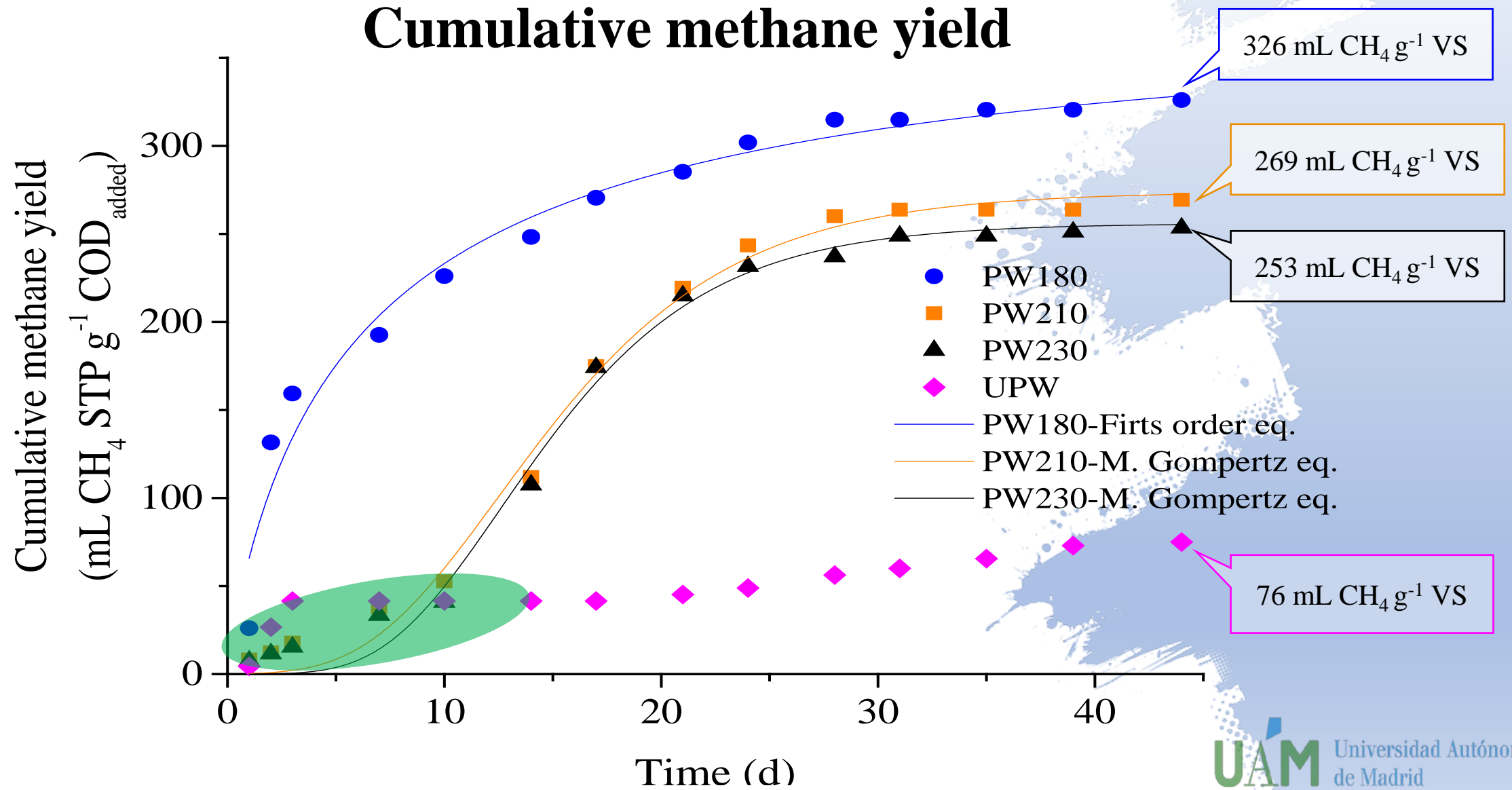




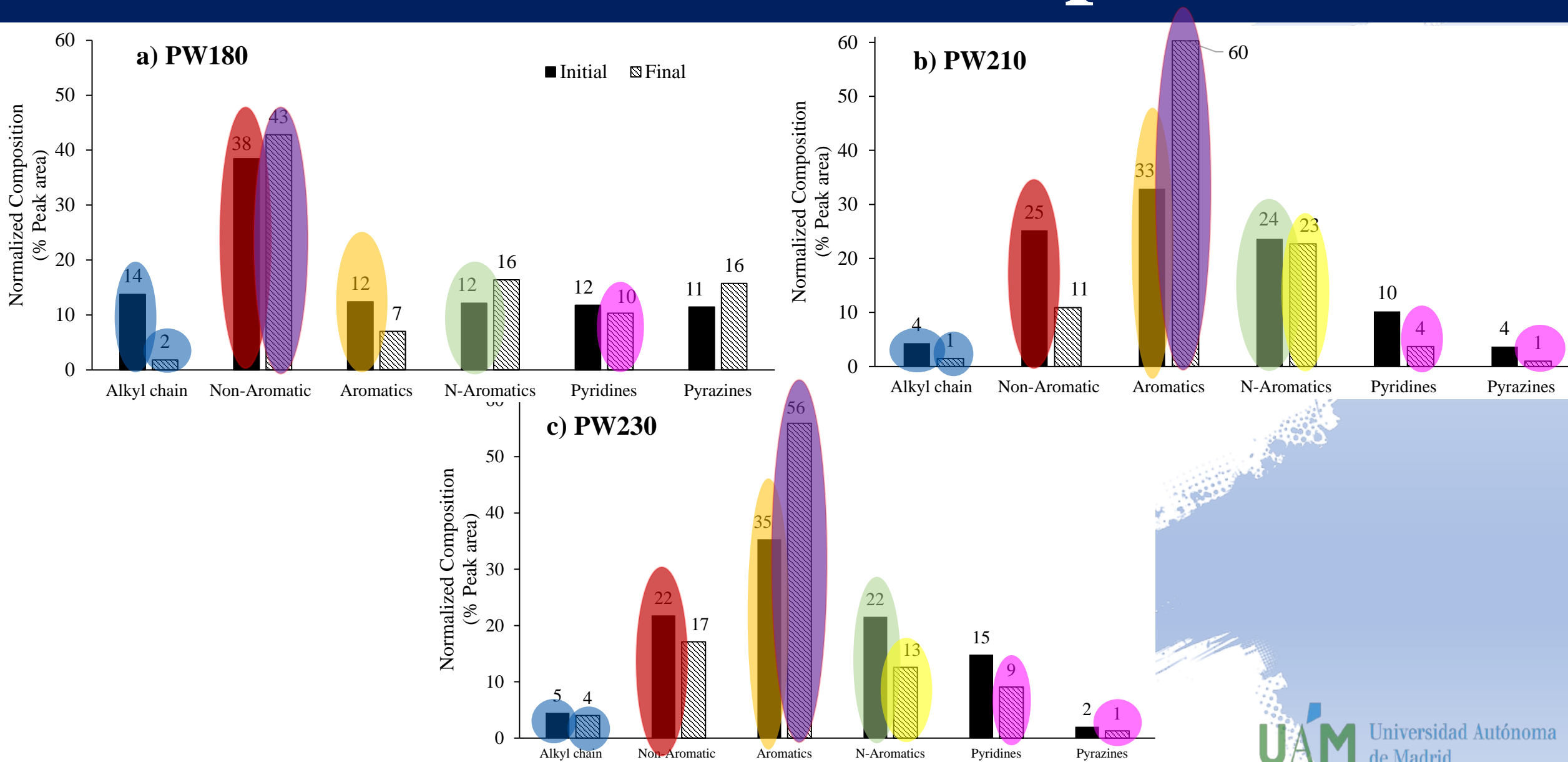
# Biochemical methane potential



# Biochemical methane potential



# Biochemical methane potential



# Energy synergy

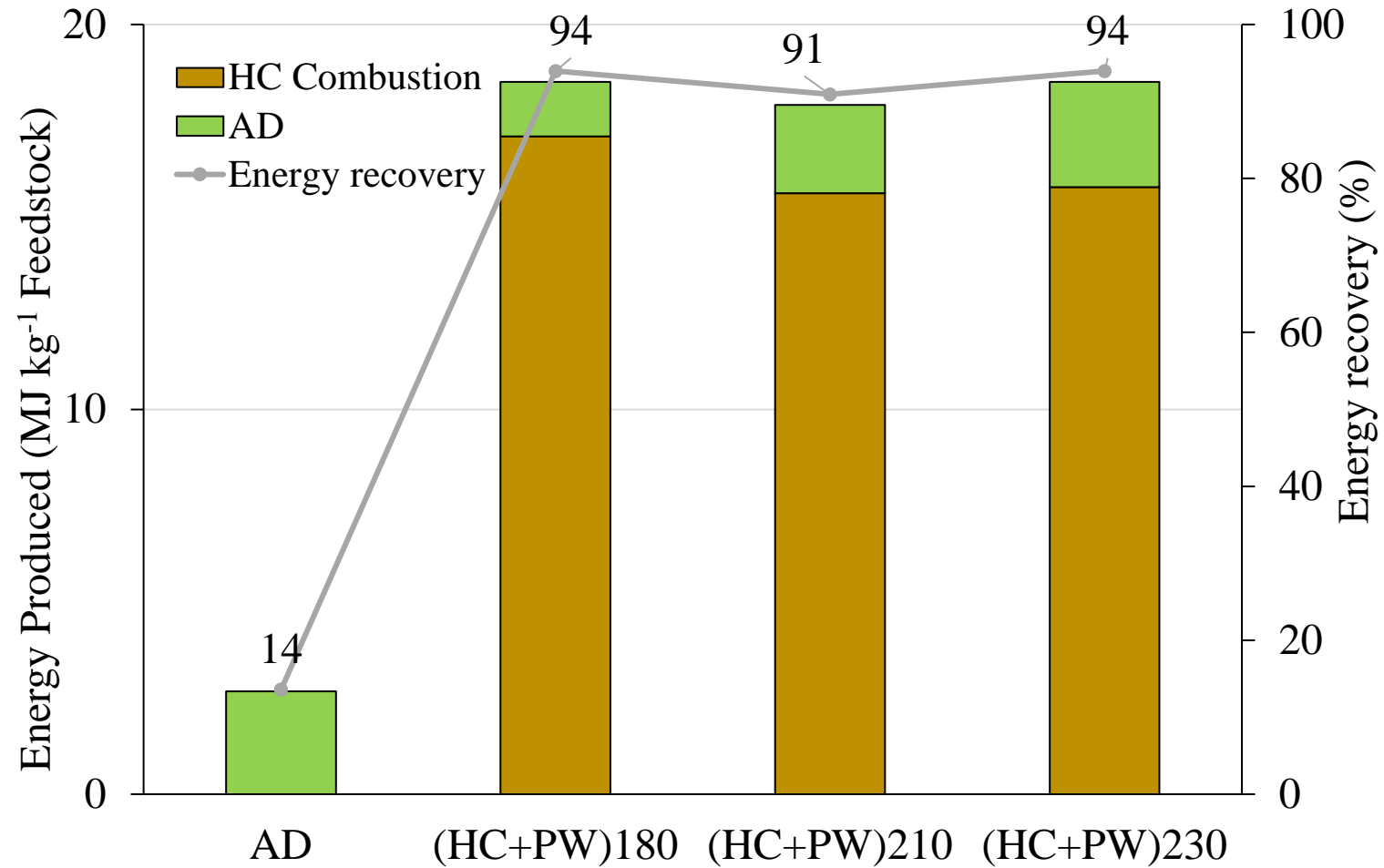
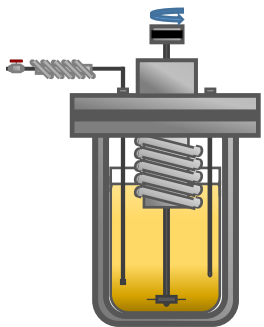
## Energy recovery



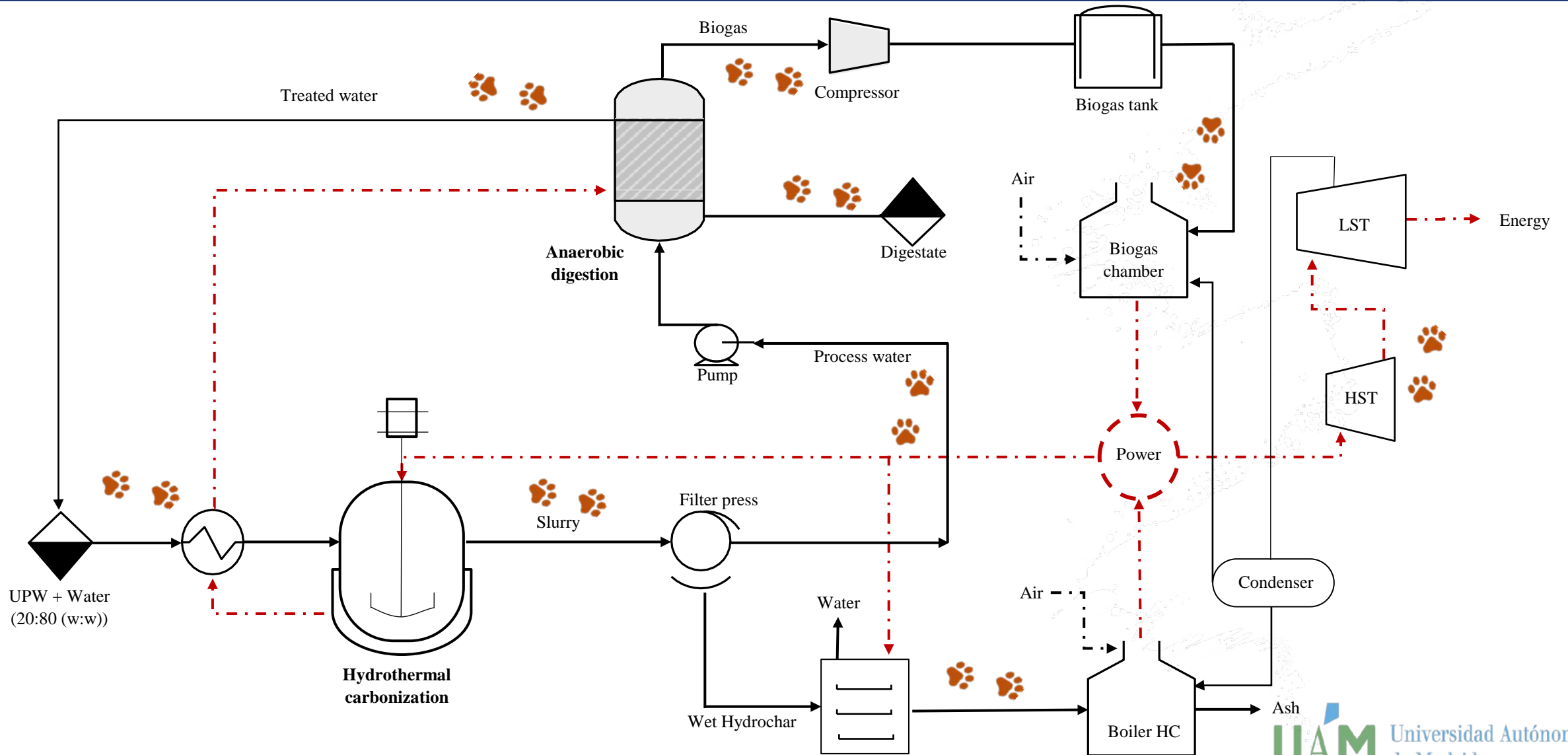
HC



CH<sub>4</sub>



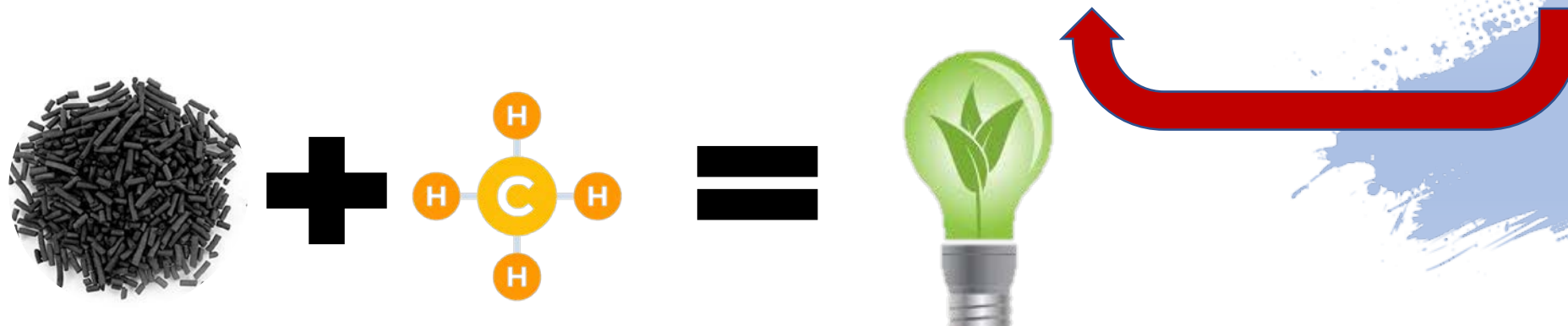
# HTC + AD process





# Energy balance

	Energy Input (kWh t <sup>-1</sup> <sub>feedstock</sub> )					Energy Output (kWh t <sup>-1</sup> <sub>feedstock</sub> )			η (%)	
	HTC reactor	Dewatering	Thermal dry	Pelletizer	Pump	Total input	Energy HC	Energy CH <sub>4</sub>		Total output
<b>HTC180</b>	364	8	82	9	7	<b>469</b>	1008	79	<b>1086</b>	<b>56</b>
<b>HTC210</b>	505	9	65	7	13	<b>599</b>	921	128	<b>1048</b>	<b>41</b>
<b>HTC230</b>	462	9	63	7	14	<b>555</b>	930	152	<b>1082</b>	<b>48</b>



# Conclusions

## Hydrochar



- Higher energy densification**
- Better physical and chemical properties**
- Higher combustion reactivity and behavior**
- Fulfill the requirements for energy production at industrial level**

## Process water



**Higher organic carbon content**

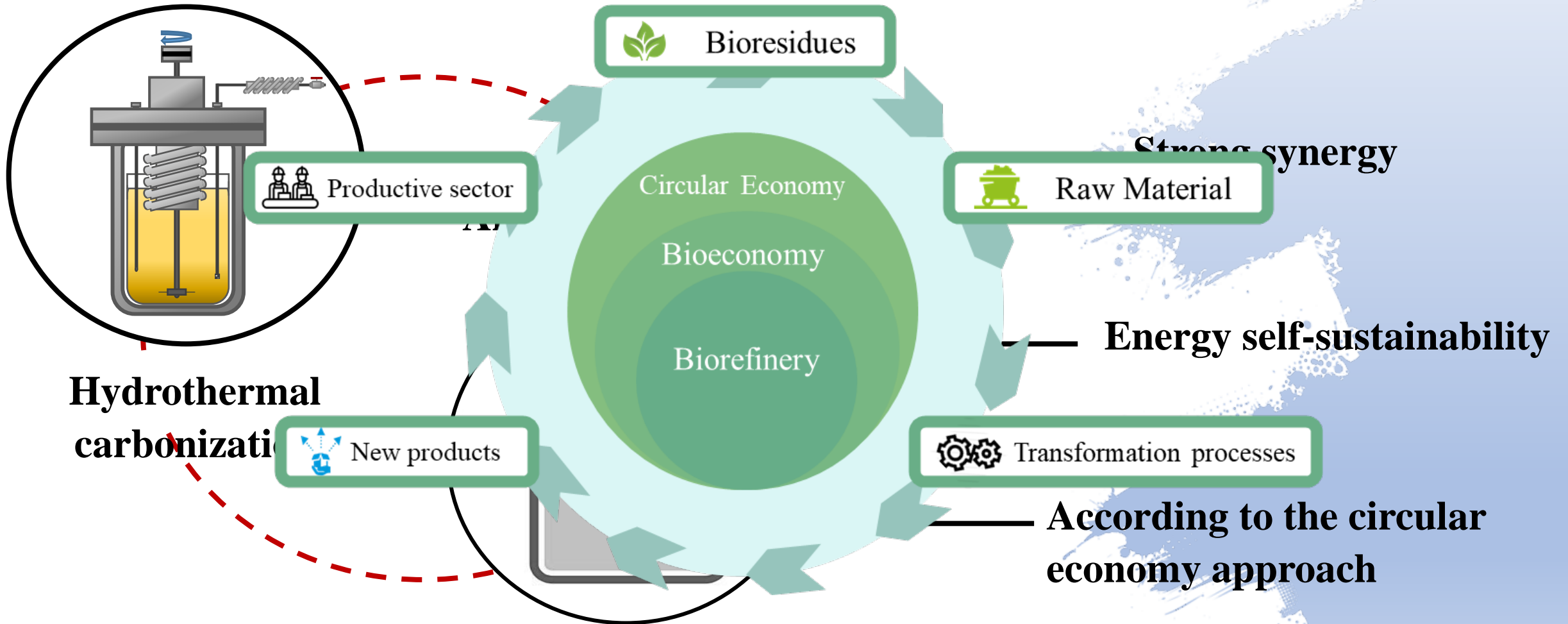
## Anaerobic digestion



**Higher methane potential yield**

**Higher organic removal in PW at lower temperatures**

# Conclusions



# 8th International Conference on Sustainable Solid Waste Management

## Acknowledgements

Authors greatly appreciate funding from Spain's MINECO (PID2019-108445RB-I00) and Madrid Regional Government (Project P2018/EMT-4344). R.P. Ipiates acknowledges financial support from Community of Madrid (IND2019/AMB-17092) and Arquimea-Agrotech Company.



# 8th International Conference on Sustainable Solid Waste Management



**“Nothing is  
impossible for the  
person who fights”**

**R. P. Ipiales**