

Hyperthermophilic fermentation (HF) of Food Waste allows the reliable recovery of Volatile Fatty Acids (VFA) by means of stripping.

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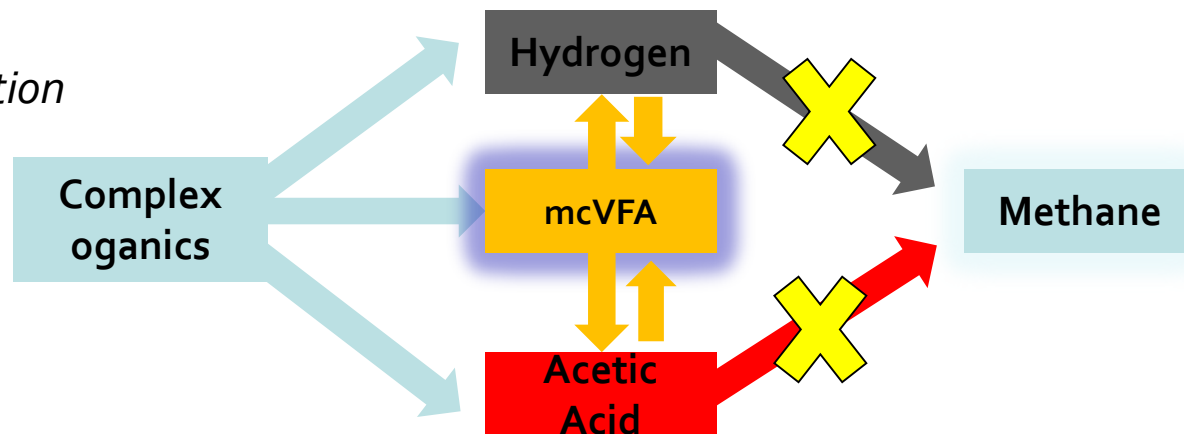
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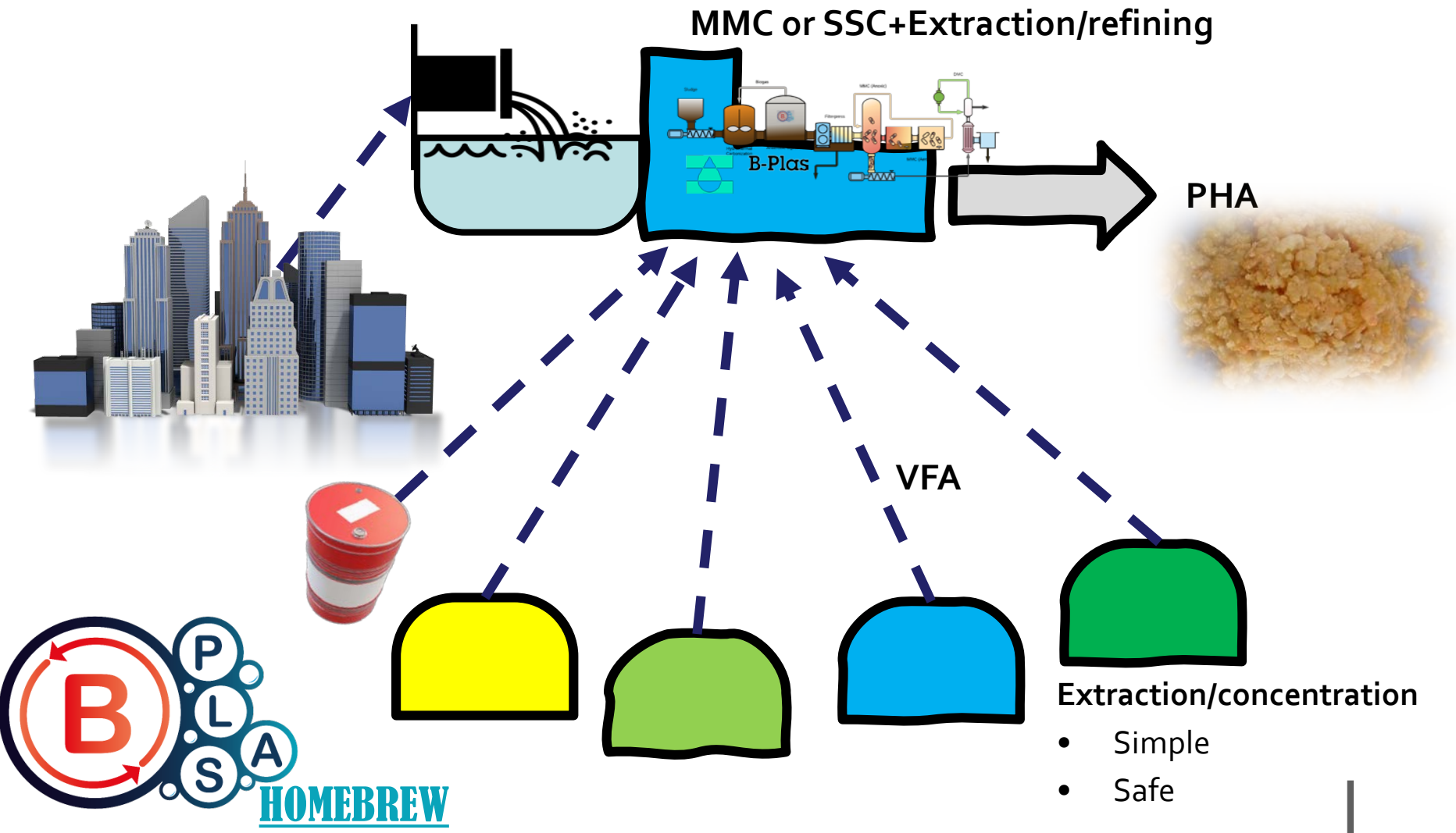
Food Waste to VFA

- Beyond Methane, Volatile Fatty Acids (VFA) are the most thermodynamically stable organic compounds in anaerobic digestion → they can be produced with simple and non-sterile MMC
- Acidogenesis and spontaneous pH drop allow to convert food waste into VFA with high volumetric productivity with yield up to 70%
- The main issue is self-inhibition at 2-3% level that intrinsically limits the yield with high COD substrates (>50 gCOD/L)
- Extractive fermentation has been proposed as a method to overcome toxicity and within one-step refining of FW into chemicals.

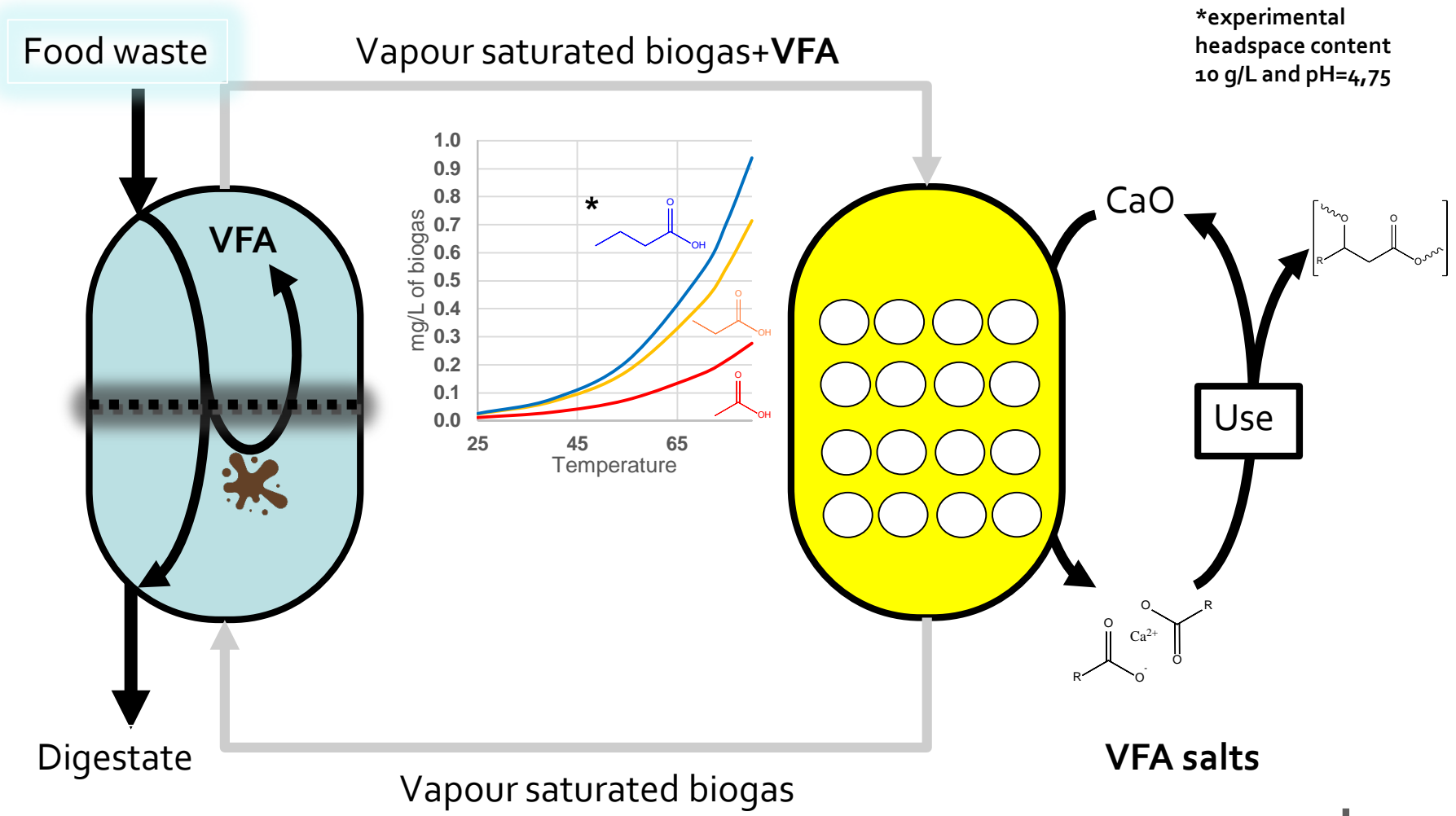
COD Flow
In Anaerobic Digestion



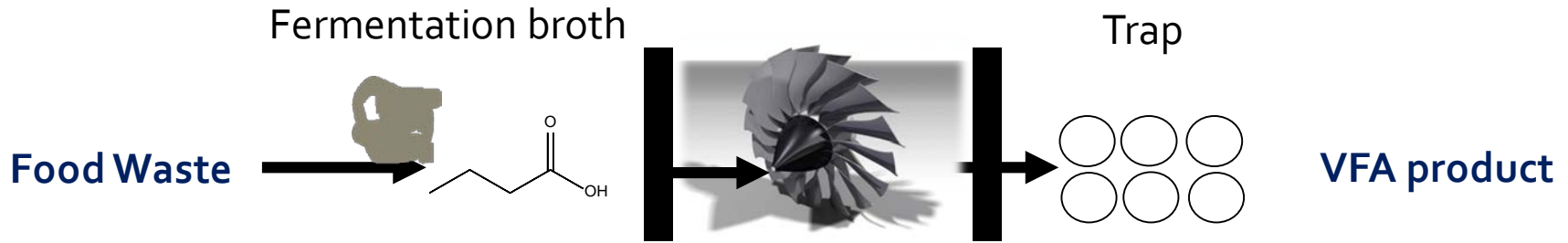
VFA polygeneration



VFA stripping



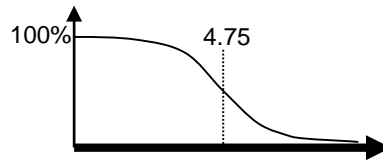
Biogas as solvent



$$\text{Mass transfer} = K_L a_1 (C_{\text{sat}} - C) = Q \cdot C = K_L a_2 C$$

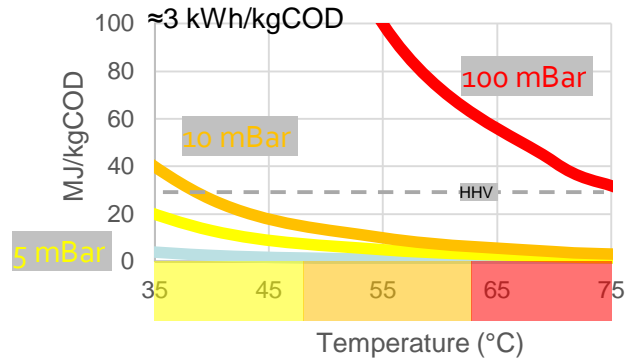
- Low cost, losses are not a problem
- Not toxic, no toxic residues in the VFAs.
- Extremely good phase separation due to different density.

- Stripping on Free VFA (pH < 5)
- High Henry constant (Low P_v) of VFA at low temperature
- Low mass transfer coefficient unless high power consumption



Ideal
Ideal Energy for gas pumping = 100 (J/m³) / mBar

Ideal energy to displace 1 kg of COD (g)

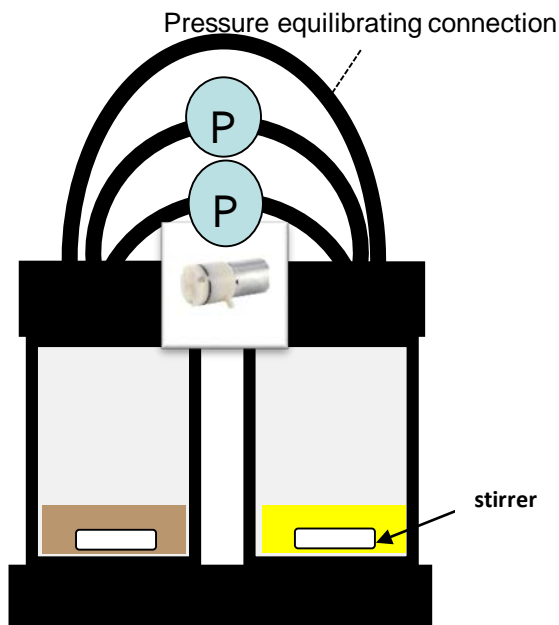


Hyperthermophilic digestion (HT) required for enough VFA in gas without huge gas pumping
High surface area to obtain enough volumetric productivity

Methods setup

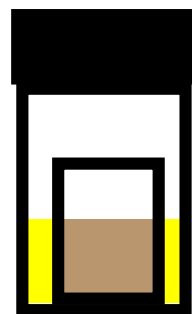
Pump&Mix

- Mechanical pumps
- Mechanical stirring
- 10 g sample
- 5 L/min gas flow
- pH,VFA, COD, reactor-trap



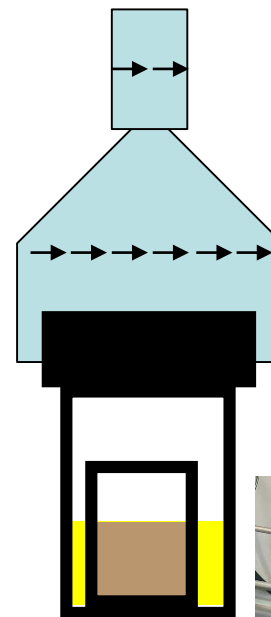
Static

- No mixing
- Gas diffusion
- Diffusion path ≤ 5 cm
- 10 g sample
- pH,VFA, COD, reactor-trap



JB reactor

- Pulsed react. rotation
- Gas diffusion (high)
- Diffusion path ≤ 5 cm
- 10 g sample
- pH,VFA, COD, reactor-trap



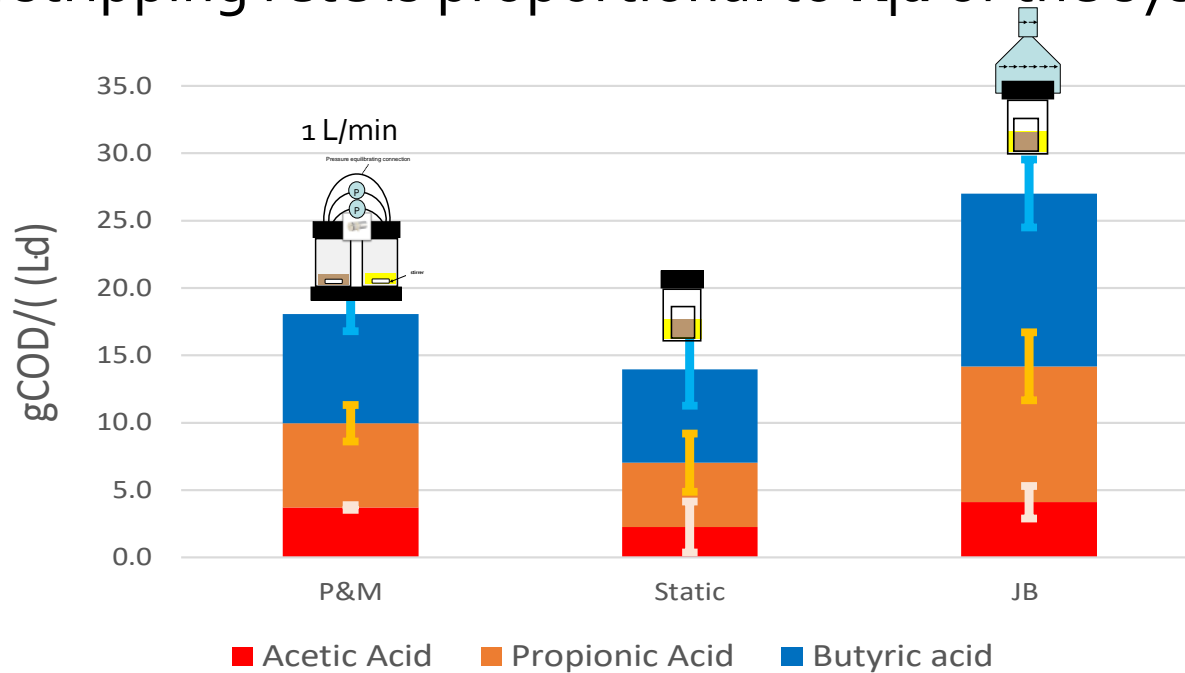
10 g/L VFA
pH=5

1 M NaOH,
CaO or CaCO₃

Methods setup: results

Model system, 4 h test

- VFA stripping rate (gCOD/L d)
- **Alkaline Trap** $\text{NaOH}=\text{CaO}=\text{CaCO}_3$
- The **limiting step** is $\text{VFA}(\text{aq}) \rightarrow \text{VFA}(\text{g})$
- VFA stripping rate is proportional to K_1a of the system.



Extractive fermentation test

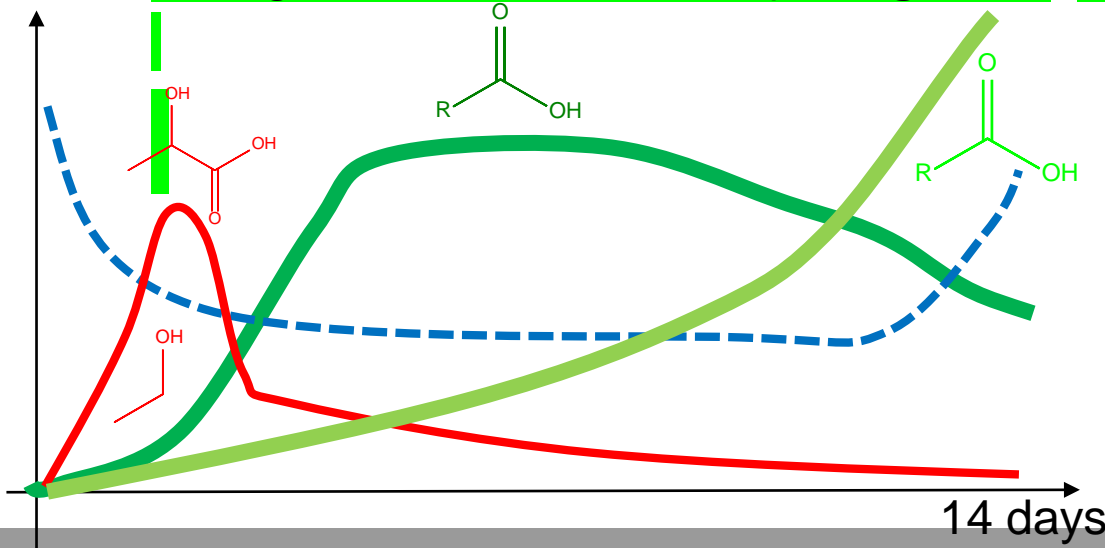
- Acclimatization/bioagumentation of HT inoculum at 55-65°C from commercial thermophilic digesters (corn silage+sewage sludge mixed inocula+ 5% Glucose 2 week)→Methane producing HT inoculum
- Homogeneous FW sample with composition in line with that of literature (Strazzera *et al.* 2018)
- Test performed at 65°C with 9 g FW+ 1 g inoculum (high substrate/Inoculum ratio)

	Avg	St. Dev (n=5)
COD (gO/gWet)	224	±3,00
sCOD (gO/gWet)	115	±2,00
N	1,2	±0,05
C	41	±1,21
H	6,5	±0,18
S	-	-
O	48	±1,32
ash	3,8	±0,10
C/N	38	±1,20
Lipids	32,9	±0,02
Carbohydrates	53,7	±0,01
Proteins	7,6	±0,36



Extractive fermentation test

- **Initial phase** → production of lactic acid, ethanol and VFA and pH drop to <math><5.2</math>
- After 3 days, dynamic equilibrium is reached with 10-20 **10-20 g/L of VFA**.
- >3 days, constant broth composition with progressive VFA stripping.
- <math><5\%</math> (COD/COD_{in}) methane and hydrogen generation.
- Stripping is the rate limiting step until the exhaustion of the process.
- **Extraction overcome the 3% barrier (145 gCOD_{VFA}/kg)**
- **65% VFA yield higher than non-extractive HT fermentation**
- **Average Volumetric Productivity $\approx 10 \text{ gCOD L}^{-1} \text{ d}^{-1}$**



Conclusions

Qualitative facts

- Hyperthermophilic fermentation with mixed sludge inoculum easily achieved in one week (ubiquitous microorganisms?)
- First Analytical system to evaluate acidogenesis yield beyond product inhibition (e.g. bio-acidification test)
- With selective removal of Volatile Fatty Acids → butyric acid is the main fermentation products

Quantitative Performances

- Even at acidic pH ($\text{pH} < 5$) $> 80\%$ FW solubilization, **65% VFA** yield in 14 days .
- Achieved maximum **$> 10 \text{ gCOD/L}$** d Volumetric productivity ($K_L a \approx 30 \text{ h}^{-1}$) mainly related to gas-liquid exchange between fermentation broth and biogas.
- Average concentration in biogas at **60% of saturation** ($\approx 1 \text{ gCOD/m}^3$)
- Estimated Gas pumping Energy → **1-3 MJ/kgCOD** at 10 mBar Pr. Drop.



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Thank you for your attention