





METHANE PRODUCTION AFTER FERMENTATION OF THE ORGANIC FRACTION OF MUNICIPAL SOLID WASTE FOR THE SELECTIVE PRODUCTION OF METABOLITES UNDER DIFFERENT pH AND REACTION TIMES

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Introduction





Pipyn and Verstraete (1981) - Thermodynamically, methane production is best from lactic acid and ethanol

OFMSW fermentation without pH control produces large amounts of ethanol and lactic acid (Jojoa-Unigarro and González-Martínez, 2021)

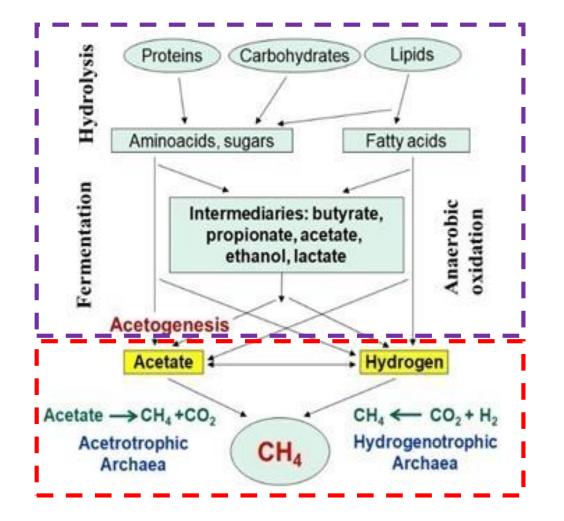
pH and reaction time are the most important variables during OFMSW fermentation

The objectives of this work:

- Evaluate the effects of pH and reaction time on the selectivity of products during OFMSW fermentation.
- Determine the effects of fermentation on the specific methane production methanization kinetics.

| 0, 0 | 41 | | | | | |
|----------------|--|--|--|--|--|--|
| Substrate | Free energy ∆G⁰ per mol CH₄ produced (kJ) | | | | | |
| Acetic acid | -31.0 | | | | | |
| Propionic acid | -32.3 | | | | | |
| Butyric acid | -32.7 | | | | | |
| Lactic acid | -68.8 | | | | | |
| Ethanol | -59.5 | | | | | |
| | | | | | | |

Free energy changes of CH₄ production from different substrates



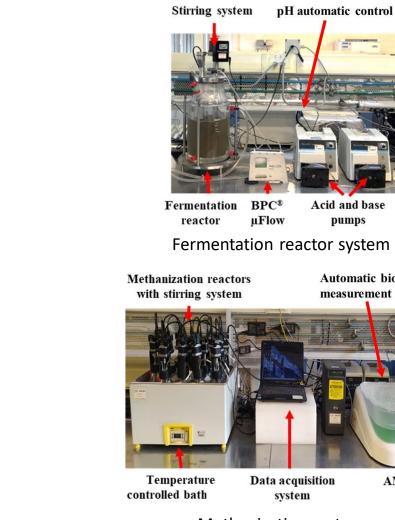
Main transformations during anaerobic digestion











Method.

Operation condition and assembly fermentation test:

- Temperature 35° C
- Reactor volume 3 L
- pH = 4, 5 and 6
- Fermentation time= 1, 3 and 6 days
- Solids concentration 4% VS
- The digestate was centrifuged to obtain a liquid and a solid.

Operation condition and assembly methanisation test:

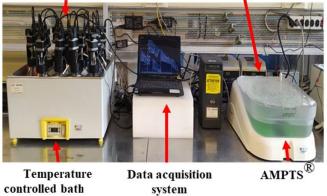
- Temperature 35° C
- 400 ml work volume
- 8 g_{VS} inoculum (UASB sludge)
- Phosphate buffer at pH 7
- Inorganic nutrients added
- Substrate Fermented OFMSW
- Liquid fraction: 25, 50, 100 and 150 mL ٠
- Solid fraction: 4, 8, 16 and 24 g

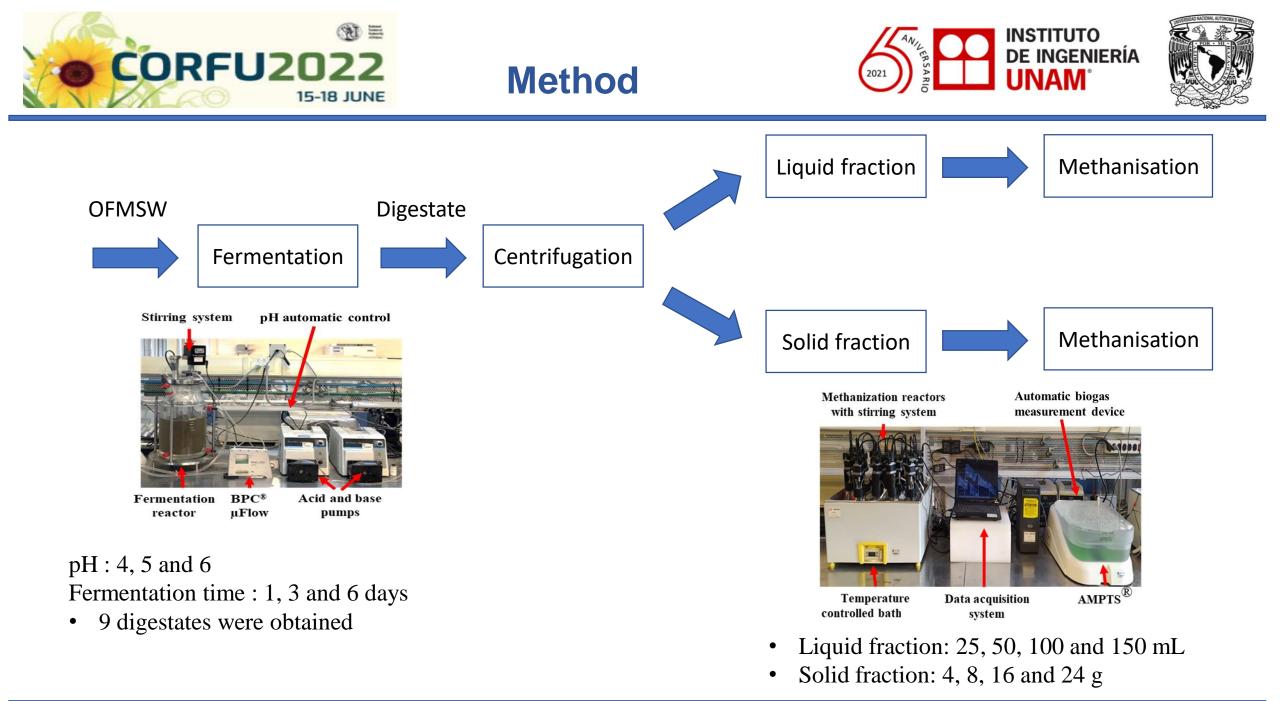
Methanisation system

Acid and base pumps

Fermentation reactor system

Automatic biogas measurement device











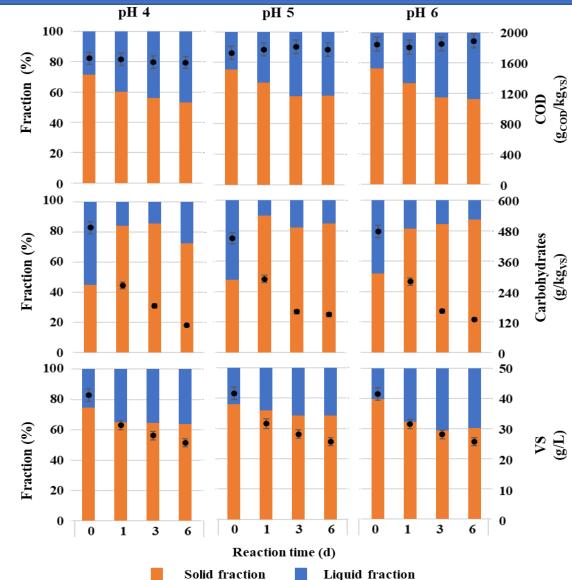


Figure. Distribution of COD, carbohydrates, and volatile solids among liquid and solid fractions over reaction time.

COD

• The COD/SV ratio remains constant as the fermentation time increases

Carbohydrates

• Increasing the fermentation time decreases the concentration of carbohydrates in the fermentation reactor.

Volatile solids

• Increasing the fermentation time decreases the concentration of VS in the fermentation reactor.









pH 4 pH 5 pH 6 30 100 rate (%) 25 80 (g/L) **T**.... 60 15 COD 40 10 Fermen 20 5 0 0 3 3 3 6 6 Time (d) Time (d) Time (d) Methanol — Ethanol — Acetic ac. — Propionic ac. — Butyric ac. — Lactic ac. ••••• Soluble COD ••••• Fermentation rate

Figure . Metabolites produced during fermentation under different pH values. Comparison of soluble COD with the fermentation rate

- pH 4:
 - High ethanol production, which decreases over time

pH 5

• High production of lactic acid, which decreases with time and the concentration of ethanol remains constant with time.

pH 6

• High production of acetic acid at one day of fermentation and high production of butyric acid at 3 days of fermentation







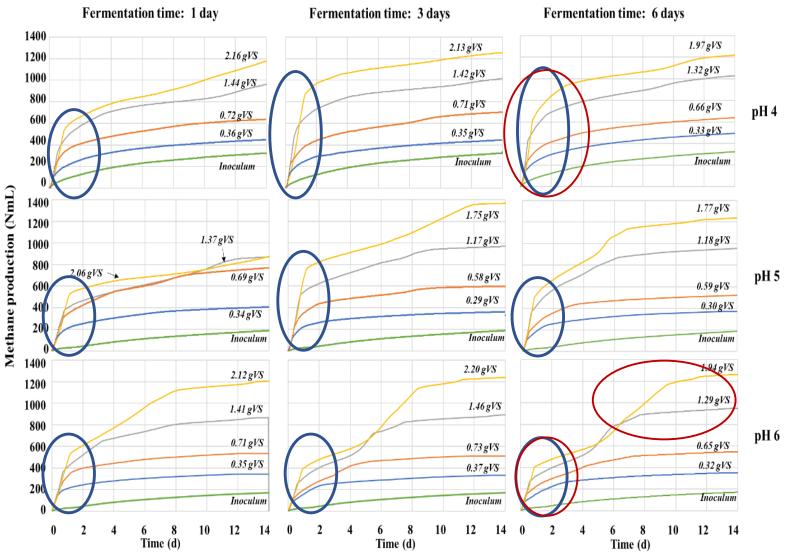


Figure. Methane production from the liquid fractions of fermented digestates at different pH values and fermentation times

- In all the curves, as the initial mass of VS increases, the generated volume of methane increases proportionally.
- When the pH of the fermentation decreases, it is observed that the curves present a single methanization stage.
 - In the first stage of methanization between 55-75% of the total methane is produced







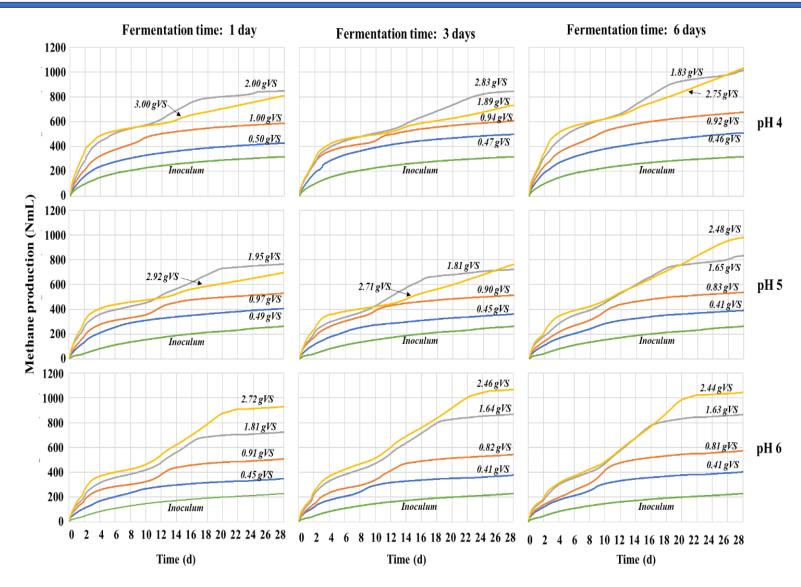


Figure. Methane production from the solid fractions of fermented digestates at different pH values and fermentation times

- In general, increasing the initial mass of VS increases the volume of methane.
- At a pH of 4 and 5 with the highest VS mass, 28 days of methanation were not enough.
- At the first stage of methanation, between 45-60% of total methane is generated, this increases when the pH decreases









| | | | | Methane production in first stage | | | | | |
|----|----|---|---------------------|-----------------------------------|--|---|--|--|--|
| pН | FT | | Fraction (as VS) | % of first stage over final | CH ₄ production (NL/kg _{VS}) | CH ₄ production (combined) (NL/kg _{VS}) | | | |
| 4 | 1 | Liq | 0,35 | 59±4 | 83 | 207 | | | |
| | | Sol | 0,65 | 69±3 | 124 | 207 | | | |
| | 3 | Liq | 0,35 | 75±6 | 132 | 237 | | | |
| | | Sol | 0,65 | 66±7 | 106 | 237 | | | |
| | 6 | Liq | 0,36 | 65±4 | 108 | 257 | | | |
| | | Sol | 0,64 | 64±7 | 149 | 237 | | | |
| 5 | 1 | Liq | 0,28 | 59±6 | 68 | 181 | | | |
| | | Sol | 0,72 | 64±7 | 113 | 101 | | | |
| | 3 | Liq | 0,31 | 69±8 | 151 | 272 | | | |
| | | Sol | 0,69 | 60±9 | 121 | | | | |
| | 6 | Liq | 0,32 | 53±17 | 101 | 206 | | | |
| | | Sol | 0,68 | 53±9 | 105 | 200 | | | |
| 6 | 1 | Liq | 0,35 | 64±11 | 109 | 201 | | | |
| | | Sol | 0,65 | 56±9 | 91 | 201 | | | |
| | 3 | Liq | 0,41 | 52±14 | 107 | 212 | | | |
| | | Sol | 0,59 | 53±9 | 105 | | | | |
| | 6 | Liq | 0,40 | 49±12 | 112 | 209 | | | |
| | | S_0^{FT} : Fermentation $time$ | | | 97 | 207 | | | |
| | | | | | | | | | |

 $M_{TVS} \cdot SMP_T = m_{LVS} \cdot SMP_L + m_{SVS} \cdot SMP_S$

 M_{TVS} : Total volatile solids SMP_T : Total specific methane production m_{LVS} and m_{SVS} : Mass of volatile solids in the liquid and solid fractions SMP_L and SMP_S : Specific methane production in the liquid and solid fractions

 $SMP_T = f_L \cdot SMP_L + f_S \cdot SMP_S$

 $fL \ \mbox{and} \ fS$: fraction as VS for liquid and solid fraction

Table. Specific methane production from the liquid and solid fermenteddigestates from OFMSW at first methanization stage

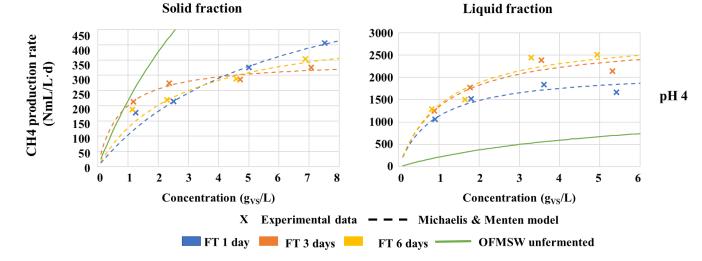
- The highest methane production was achieved at pH 5 and a fermentation time of 3 days
- Solid fraction contributes between 40 to 49% of the specific production







Michaelis and Menten modeling of liquid and solid fractions fermented at pH 4



Kinetic parameters of the liquid and solid fractions

| - | Vmax (NmL/L·d) | | | $\mathrm{Km}\left(\mathrm{g}_{\mathrm{VS}}/\mathrm{L}\right)$ | | | Regression coefficients | | |
|-----------------------|--------------------------------------|--|--|---|---|---|---|---|---|
| Fermentation time (d) | | 3 | б | 1 | 3 | 6 | 1 | 3 | 6 |
| pH 4 🖌 | 2146 | 2846 | 2974 | 0.9 | 1.1 | 1.2 | 0.933 | 0.957 | 0.887 |
| pH 5 | 1366 | 2306 | 2248 | 0.3 | 0.8 | 1.0 | 0.913 | 0.972 | 0.914 |
| pH 6 | 1512 | 1232 | 1454 | 0.8 | 0.5 | 0.5 | 0.879 | 0.985 | 0.902 |
| pH 4 | 717 | 349 | 479 | 5.9 | 0.7 | 2.8 | 0.999 | 0.958 | 0.901 |
| pH 5 | 414 | 326 | 222 | 2.6 | 2.2 | 1.5 | 0.985 | 0.989 | 0.916 |
| рН б | 479 | 317 | 222 | 5.0 | 2.5 | 1.4 | 0.964 | 0.982 | 0.816 |
| | pH 4 pH 5 pH 6 pH 4 pH 5 | Den time 1 pH 4 2146 pH 5 1366 pH 6 1512 pH 4 717 pH 5 414 | on time 1 3 pH 4 2146 2846 pH 5 1366 2306 pH 6 1512 1232 pH 4 717 349 pH 5 414 326 | DD time 1 3 6 pH 4 2146 2846 2974 pH 5 1366 2306 2248 pH 6 1512 1232 1454 pH 4 717 349 479 pH 5 414 326 222 | on time 1 3 6 1 pH 4 2146 2846 2974 0.9 pH 5 1366 2306 2248 0.3 pH 6 1512 1232 1454 0.8 pH 4 717 349 479 5.9 pH 5 414 326 222 2.6 | on time 1 3 6 1 3 pH 4 2146 2846 2974 0.9 1.1 pH 5 1366 2306 2248 0.3 0.8 pH 6 1512 1232 1454 0.8 0.5 pH 4 717 349 479 5.9 0.7 pH 5 414 326 222 2.6 2.2 | on time 1 3 6 1 3 6 pH 4 2146 2846 2974 0.9 1.1 1.2 pH 5 1366 2306 2248 0.3 0.8 1.0 pH 6 1512 1232 1454 0.8 0.5 0.5 pH 4 717 349 479 5.9 0.7 2.8 pH 5 414 326 222 2.6 2.2 1.5 | on time 1 3 6 1 3 6 1 pH 4 2146 2846 2974 0.9 1.1 1.2 0.933 pH 5 1366 2306 2248 0.3 0.8 1.0 0.913 pH 6 1512 1232 1454 0.8 0.5 0.5 0.879 pH 4 717 349 479 5.9 0.7 2.8 0.999 pH 5 414 326 222 2.6 2.2 1.5 0.985 | on time 1 3 6 1 3 6 1 3 pH 4 2146 2846 2974 0.9 1.1 1.2 0.933 0.957 pH 5 1366 2306 2248 0.3 0.8 1.0 0.913 0.972 pH 6 1512 1232 1454 0.8 0.5 0.5 0.879 0.985 pH 4 717 349 479 5.9 0.7 2.8 0.999 0.958 pH 5 414 326 222 2.6 2.2 1.5 0.985 0.989 |

The figure. shows the methanation modeling for digestates fermented at pH 4 and in the table 3 the kinetic parameters of the liquid and solid fractions for each digestate.

- Decreasing the fermentation pH increases Vmax of the liquid fraction of the digestate.
- A shorter fermentation time increases Vmax of the solid fraction of the digestate.
- High Km values, lower affinity of the substrate to methanization









- Lower pH values and shorter fermentation allow better ethanol and lactic acid production.
- Higher pH values and longer fermentation times promote acetic and butyric acid formation
- During fermentation, hydrolysis mainly occurs during the first day causing total carbohydrates and COD to decrease with time.
- Hydrolysis rates decrease with fermentation time at all different pH values.
- The first methanization stage of the liquid fractions requires 1 to 2 days, and the solid fractions from 4 to 8 days.
- Liquid and solid fractions together represent 49 to 69% of total methane production
- Independently of pH and duration, OFMSW fermentation allows better and faster methanization







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Thank you for your attention!!!