Food Residues Biorefineries: Design strategy based on multifeedstocks analysis

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1. Introduction



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1. Introduction

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Figure 1. Residues classification generated in the stages of the supply chain

1. Introduction

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2. Research objective

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This work focuses on proposing a new strategy for defining the best technological configurations using concepts of composition of the feedstocks (including the multifeedstocks), platforms and products for Food Residues Biorefineries

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Biorefinery design strategy for biomass valorization

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Bioprocesses portfolio

Figure 2. Bioprocesses addressed to upgrade each fraction of biomass

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Figure 3. Bioprocess and TRL relation (a) cellulose; (b); hemicellulose and lignin (c); extractives and fats (d); pectin and starch (e) all fractions raw material

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Cellulose fraction

Table 1. Mass, energy, economic and environmental indicators

									Environmental	
			Mass indicators		Energy indicators		Economic indicators			indicator
			Yield (ton of	Carbon	Power requirement	Thermal energy			Production	
			product/Ton raw	conversion	(kWh/Ton raw material	consumption (MJth/kg raw	CapEx*	OpEx*	cost/Selling	Climate change (kg
BioProcess	Platform	BioProcess	material fraction	efficiency (%)	fraction)	material fraction)	(MUSD)	(MUSD)	price ratio	CO2 eq/Product)
Catalytic glucose production from	Glucose platform -						a: 0.23	a: 0.17		
CELLULOSE	Catalytic	BioP-Pt1	0.41	37.05	0.72	2.40 (H:80.5%, C: 19.5%)	b: 0.09	b: 0.39	30,5	0.48
	Glucose platform -						a: 1.42	a: 0.46		
Enzymatic hydrolysis from CELLULOSE	Enzymes	BioP-Pt2	0.80	92.60	1.80	0.73 (L:100%)	b: 0.53	b: 1.05	0,21	0.28
Fermentation - Saccharomyces						61.90 (M: 1%, L: 76%, C:	a: 1.82	a: 0.46		
cerevisiae, Distillation	Ethanol	BioP-C1	0.30	46.20	4.00	23%)	b: 0.67	b: 1.05	1.00	1,38
Fermentation - Clostridium							a: 0.26	a: 0.15		
acetobutylicum, Distillation	ABE	BioP-C2	0.25	40.51	1.50	0.07 (M: 98.2, C:1.8)	b: 0.59	b: 0.34	2.41	2,41
Fermentation - Lactobacillus casei,						44.30 (M: 1.3%, L: 9%, C:	a: 1.44	a: 18.36		
Distillation	Lactic acid	BioP-C3	0.66	65.75	3.10	89.7%)	b: 0.53	b: 41.55	3,11	3.16
						31.00 (H: 63%, M: 24%, C:	a: 1.53	a: 0.35		
Catalytic upgrading - Distillation	Levunilic acid	BioP-C4	0.56	72.75	8.8	13%)	b: 0.57	b: 0.80	0,20	2.89
							a: 3.69	a: 0.99		
Fermentation - Bacillus megaterium	PHB	BioP-C5	0.23	32.11	8.86	24.87 (L: 95%, C: 5%)	b: 1.36	b: 2.23	0,79	1.45
							a: 2.19	a: 4.73		
Fermentation - Aspergillus Terreus	Itaconic acid	BioP-C6	0.52	60.30	11.83	75.38 (L: 96%, C: 4%)	b: 0.81	b: 10.71	1,96	1.12
							a: 0.16	a: 0.25		
Catalytic upgrading - Distillation	Polylactic acid	BioP-C7	1.95	N.A.	17.17	0.1 (L:100%)	b: 0.36	b: 0.57	35.5	1.96

BioProcess

Figure 4. Mass, energy, economic and envornmental indicators of cellulose bioprocesses

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Strategy based on portfolio of BioProcesses according to Food residues valorization:

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Example: Orange Peel Wastes (Food Loss)

The bioprocesses were filtered from the Technological Readiness Level (TRL implemented) and the lowest values of operating costs (OpEx) and capital cost (CapEx).

Figure 2. Characterization of zones production

- ✓ OPW generated in a small-scale industry with a flow of 140 kg/h was considered.
- ✓ The value chain identification includes the stages of producers (crop) and processors (agribusiness).
- Agricultural residues such as leaves, branches, and flowers are generated in the producer stage (2 and 2.8 tons per hectare per year).
- ✓ These residues are disposed of in the field.

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Application of the strategy:

Define the sustainable objective according the factors that impact the valorization of biomass

The objective of valorization was to increment the economic impact of the use of FL

Step 3

Step 1

Choose the range of BioProcesses considering the objective of the analysis

Extractives: Bioactive compounds by agitated solvent extraction **All residual fraction:** Biogas production

Step 2

Select the BioProcesses according to the type of Biomass fractions using TRL

Extractives: Bioactive compounds by agitated solvent extraction and supercritical fluid extraction.

Cellulose: Glucose by catalytic process and enzymatic hydrolysis, Ethanol, ABE; Lactic acid, Levunilic acid; Polylactic acid Hemicellulose: Xylose production by acid hydrolysis, Furfural, Xylitol and Pentane Pectin: Pectin extraction Starch: Glucose production by enzymatic hydrolysis. All residual fraction: Biogas production

Step 4

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Define the scenarios or superstructure considering the process conceptual design

Scenario 1

valorizing the leaves, stems, and flowers in the producer stage to obtain biogas

Scenario 2

The OPW valorization for the production of bioactive compounds and biogas

Scenario 3

The integration of the residues from the producer stage and the transformation stage to obtain polyphenolic compounds (from OPW) and biogas (from the mixture of exhausted OPW and leaves, stems, and flowers).

Step 5

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Sustainability evaluate the scenarios or superstructure defined

The first analysis involved the evaluation and comparison of the three scenarios in terms of the economic metrics considering a fixed flow rate.

Figure 6. Costs distribution of the proposed biorefineries at a processing scale of raw material of 140 kg/h.

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Figure 7. Economic performance of the OPW biorefineries at different scales over the project lifetime for each scenario. a) Scenario 1, b) Scenario 2, c) Scenario 3.

The application of the Food Residues valorization strategy determined the best scenario considering the stated objective. In this sense, scenario 2 has a Minimum Processing Scale for Economic Feasibility (MYSELF) with a lower raw material flow than scenarios 1 and 3 (it is necessary to increase the processing scale from 3.36 tons/day to 11.5 tons/day)

5. Conclusion

- Food Residues integration as an alternative for the generation of added-value products can improve the value chain sustainability since emissions of polluting agents are reduced.
- Indeed, the analyzed case study allowed to elucidate how the generation of addedvalue products such as polyphenolic compounds increases the viability of the orange value chain through the implementation of biorefinery with good economic performance.
- Finally, an analysis related to the possible scale and technologies to be introduced are a fundamental input to propose valorization alternatives. Finally, the proposed methodology can be applied to any food waste since the value chains are already previously defined and the disposal problems are current problems that require a contextualized solution.

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6. Acknowledgments

The call PROGRAMA NACIONAL PARA LAS MUJERES EN LA CIENCIA UNESCOL'ORÉAL-MINCIENCIAS-ICETEX

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"Business and innovation competencies for economic development and productive inclusion of the regions affected by the Colombian conflict" SIGP code 58907. Contract number: FP44842-213-2018

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Thank you for your attention

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