

Pretreatment of Lignocellulosic Biomass using Tannery Wastewater for Solid State Anaerobic Digestion

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Background

Lignocellulosic
Biomass

Current
Disposal

Kano
Nigeria

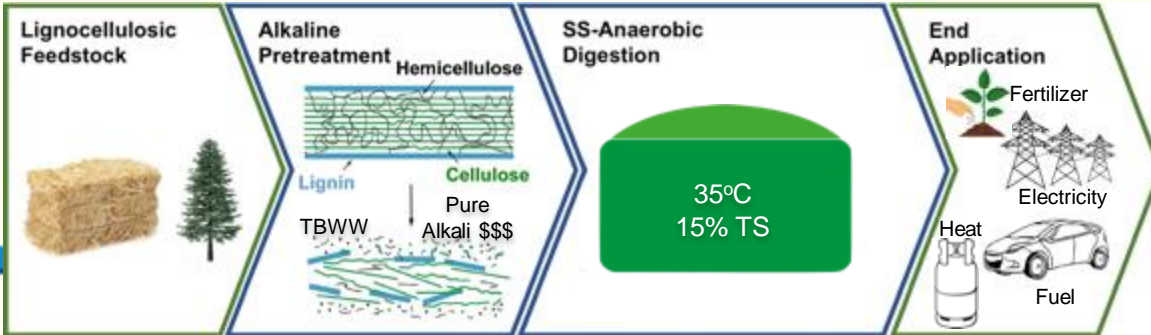
Beamhouse
Wastewater



- Agricultural wastes, crop residues.
- Most abundant material $180 \times 10^9 \text{ ty}^{-1}$
- Carbon source: 2nd Generation biofuel
- Disposed by burning locally
- $108 \times 10^6 \text{ t}$ rice paddy burnt in 2018
- India & China, South East Asia: 85%
- Nigeria: $1.8 \times 10^6 \text{ t}$

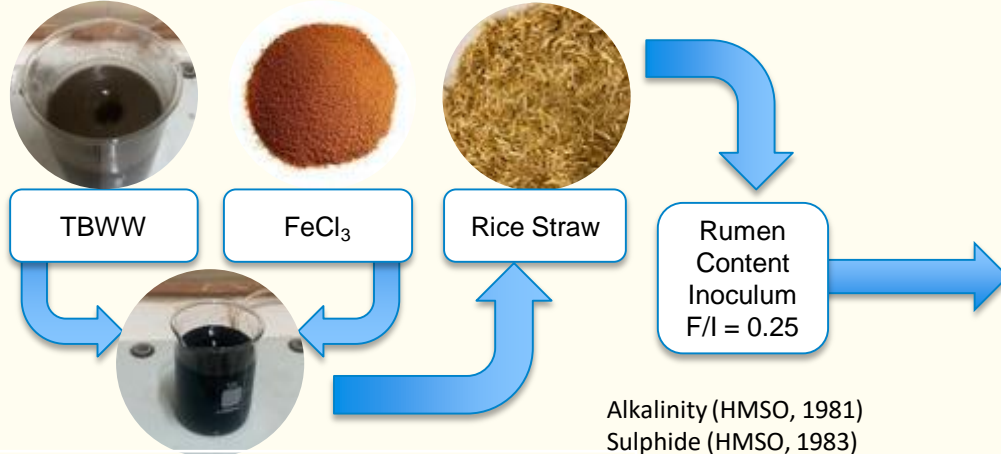
- 90% of Nigeria's tanning
- $1 \times 10^6 \text{ m}^3 \text{ y}^{-1}$ Tannery Wastewater
- Untreated, discharged, water pollution
- Soaking, **Beamhouse**, Tanning
- >50%, Lime ($\text{Ca}(\text{OH})_2$) source
- Alkalinity >12,000 mg l^{-1} , pH 12,
- **Low cost alkaline pretreatment**

Input Chemicals	Tanning Process	Wastewaters	TBWW Content	
H_2O	Soaking	Soaking (23%)	$\text{Ca}(\text{OH})_2$ Na_2CO_3 CaCO_3 NH_4OH NaOH NH_4	alkalinity source
$\text{Ca}(\text{OH})_2$ & Na_2S	Liming	Beamhouse (54%)		
Na_2CO_3 & NaOH	Re-liming			
NH_4Cl or $(\text{NH}_4)_2\text{SO}_4$	De-liming			
NH_4Cl or $(\text{NH}_4)_2\text{SO}_4$	Pickling		H_2S CaSO_4 Na_2SO_4 Na_2S	sulphide source
$\text{Cr}_2(\text{SO}_4)_3$, NaHCO_3 & HCOONa	Tanning	Tanning(23%)		



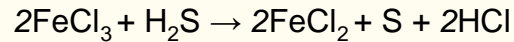
AIM: Determine how to optimise tannery beamhouse wastewater for pretreatment of lignocellulosic biomass for solid state mesophilic AD.

Materials & Methods



Alkalinity (HMSO, 1981)
 Sulphide (HMSO, 1983)
 TS and VS (APHA, 2005)
 NDF (BS, 2006)
 ADF and ADL (BS, 2008)

$$A = [\text{HCO}_3^-] + 2[\text{CO}_3^{2-}] + \sum [\text{X}^-] + ([\text{OH}^-] - [\text{H}^+])$$



100% 50% 25% FeCl₃ Concentrations

Volume of sample	100.0 ml
H ₂ S Concentration	2499.2 mg/l
H ₂ S mass	249.9 mg
H ₂ S molar mass	34.1 g/mol
H ₂ S mols	0.0073 mol
FeCl ₃ mols	0.0147 mol
FeCl ₃ molar mass	162.2 g/mol
FeCl ₃ mass	2377.5 mg

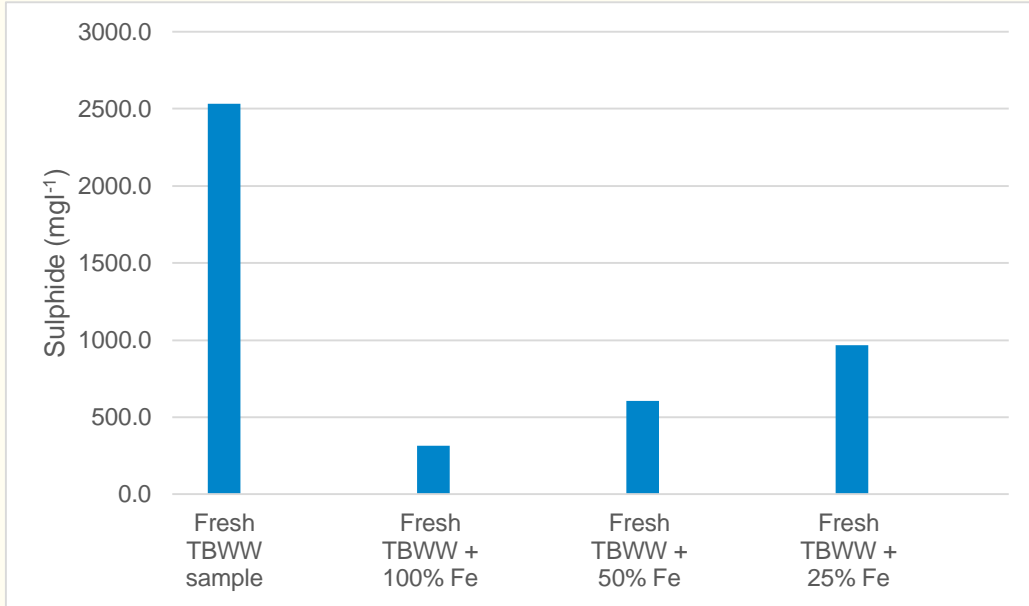


RS + S Free TBWW

RS Control

Inoculum Control

Results

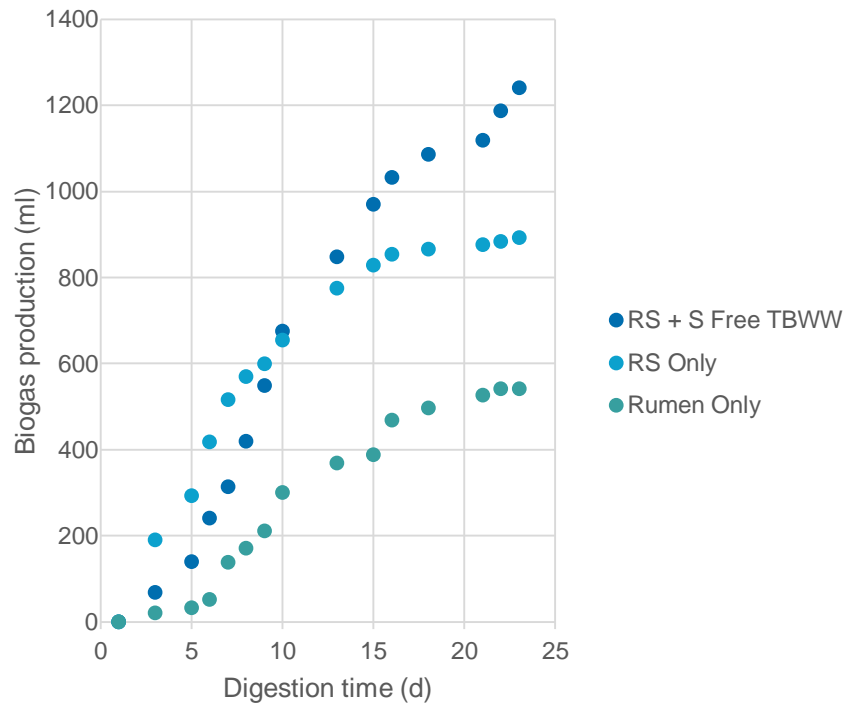


	CaCO ₃ Alkalinity (mg l ⁻¹)	Alkaline loading rate (g CaCO ₃ g RS ⁻¹)
Fresh TBWW	32,711.7	32.7%
S-Free TBWW	12,197.9	12.2%
10% Ca(OH) ₂	13,497.1	13.5%

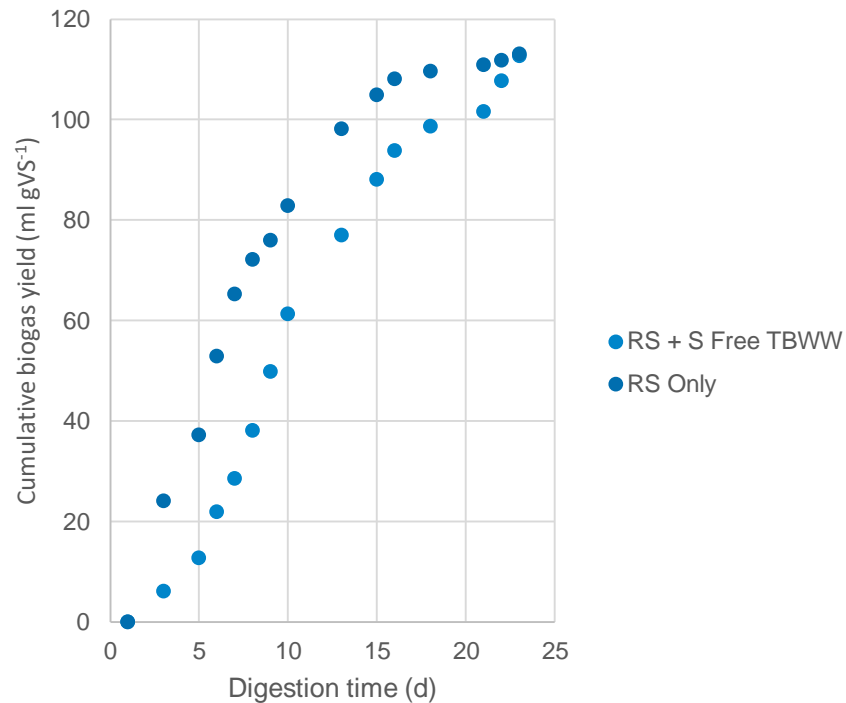
FeCl ₃ addition rate (%theoretical)	TS	VS
100	5.3%	58.9%
50	5.2%	66.6%
25	4.6%	64.8%

Results

Cumulative Biogas Production

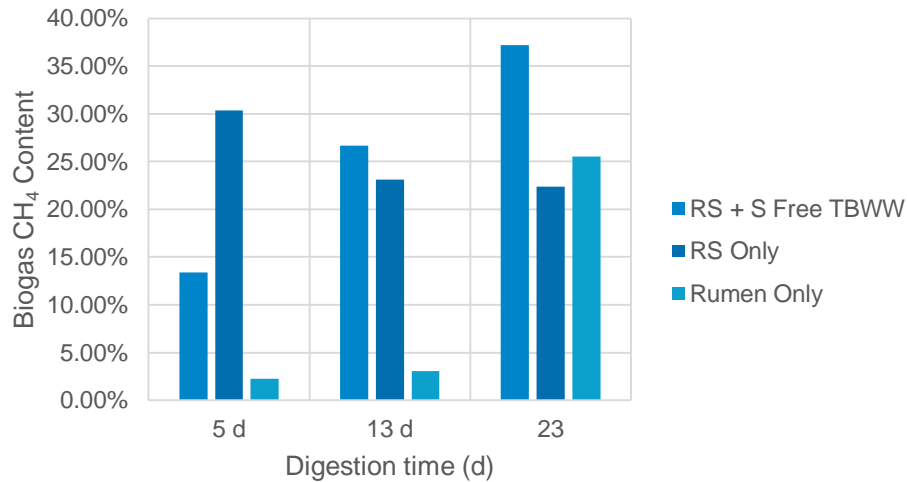


Cumulative Biogas Yield



Results

Average Biogas Methane Content



Average Biogas Sulphide Content (ppm)	5 d	13 d	23 d
RS + S Free TBWW	12.00	5.67	593.00
RS Only	5.00	4.50	61.00
Rumen Only	5.00	4.50	46.00

Conclusions

- FeCl_3 reduces sulphide in TBWW by up to 90%.
- Biogas production RS is increased by up to 10% through TBWW pretreatment.
- RS is digestible using rumen as inoculum.
- Sulphide even in low concentrations in TBWW reduces the rate of methanogenesis but does not cause complete inhibition
- Tannery beamhouse wastewater is a potential alkaline resource for increasing biogas yield of lignocellulosic biomass.
- *Next steps: Rerun experiments using TBWW with sulphide removed by drying.*

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Thank you for listening

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