



Innovative micronutrient fertilizers by biosorption for organic farming

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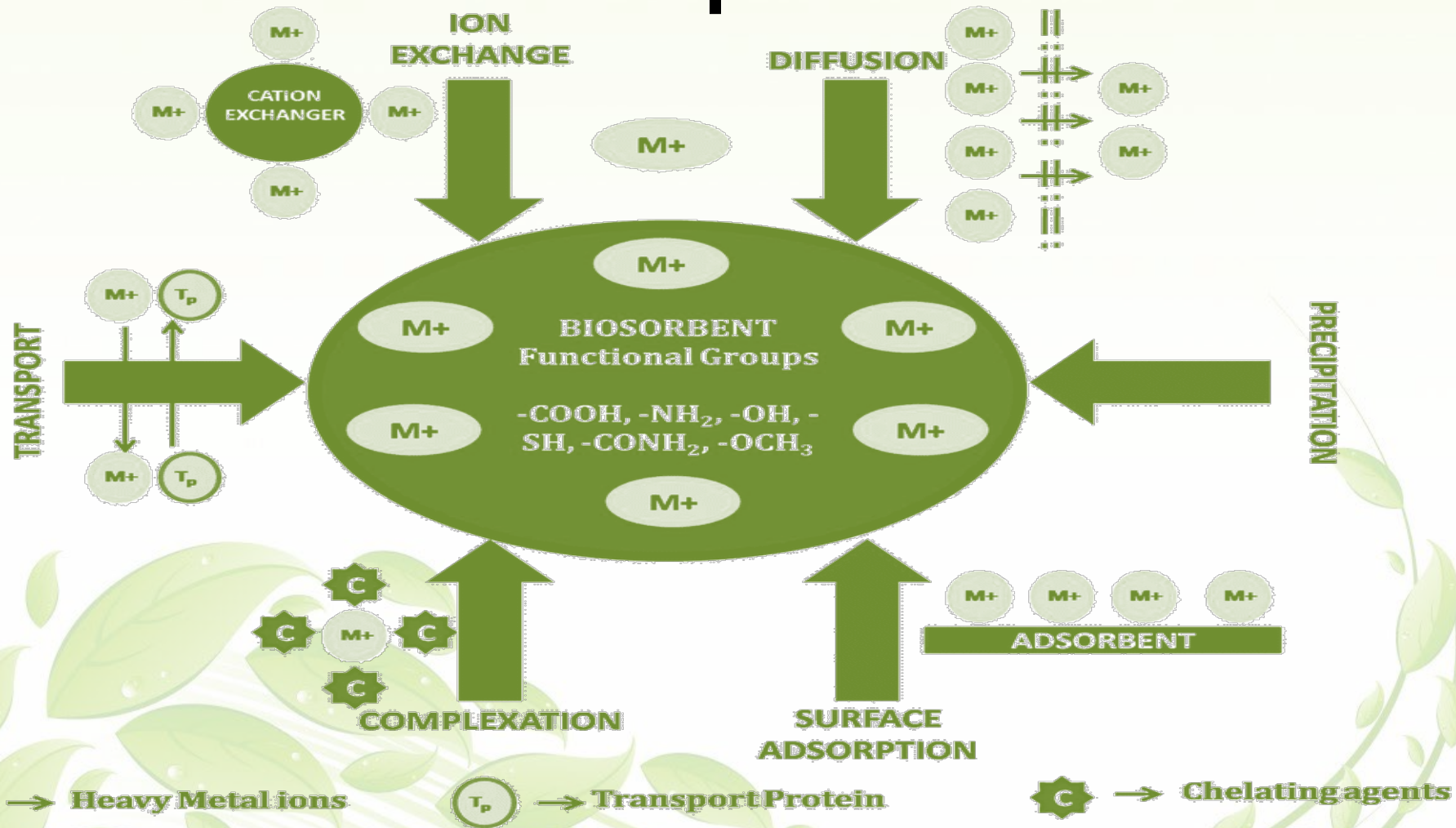




Introduction

- Population growth rate exceeds grain yield by three times, crop area remains the same. The global crisis has made the situation much worse, millions of people are at risk of starvation.
- More than two-thirds of European Union countries are severely deficient in at least one of the micronutrients.
- Today, the main goal is to improve the efficiency of fertilizer ingredients while reducing the environmental impact of their use. The European Green Deal calls for a 25% share of organic farming.
- Micronutrient fertilizers for organic farming will play an increasingly important role.

Biosorption





Biosorption – new trends

Biosorption process

Focus on:
sorbate removal

Focus on:
biosorbent enrichment

Wastewater
treatment
(90 600 papers)

Biological feed
supplements with
micronutrients
(7 040 papers)

Micronutrients
fertilizers
(1 640)

Potential biosorbents

BIOSORBENTS

Plants

- Leaves
- Seeds



Fungi

- Micromycetes
- Macromycetes



Algae

- Microalgae
- Macroalgae



Animal

- Bones
- Eggshells



Microbes

- Bacteria
- Archea

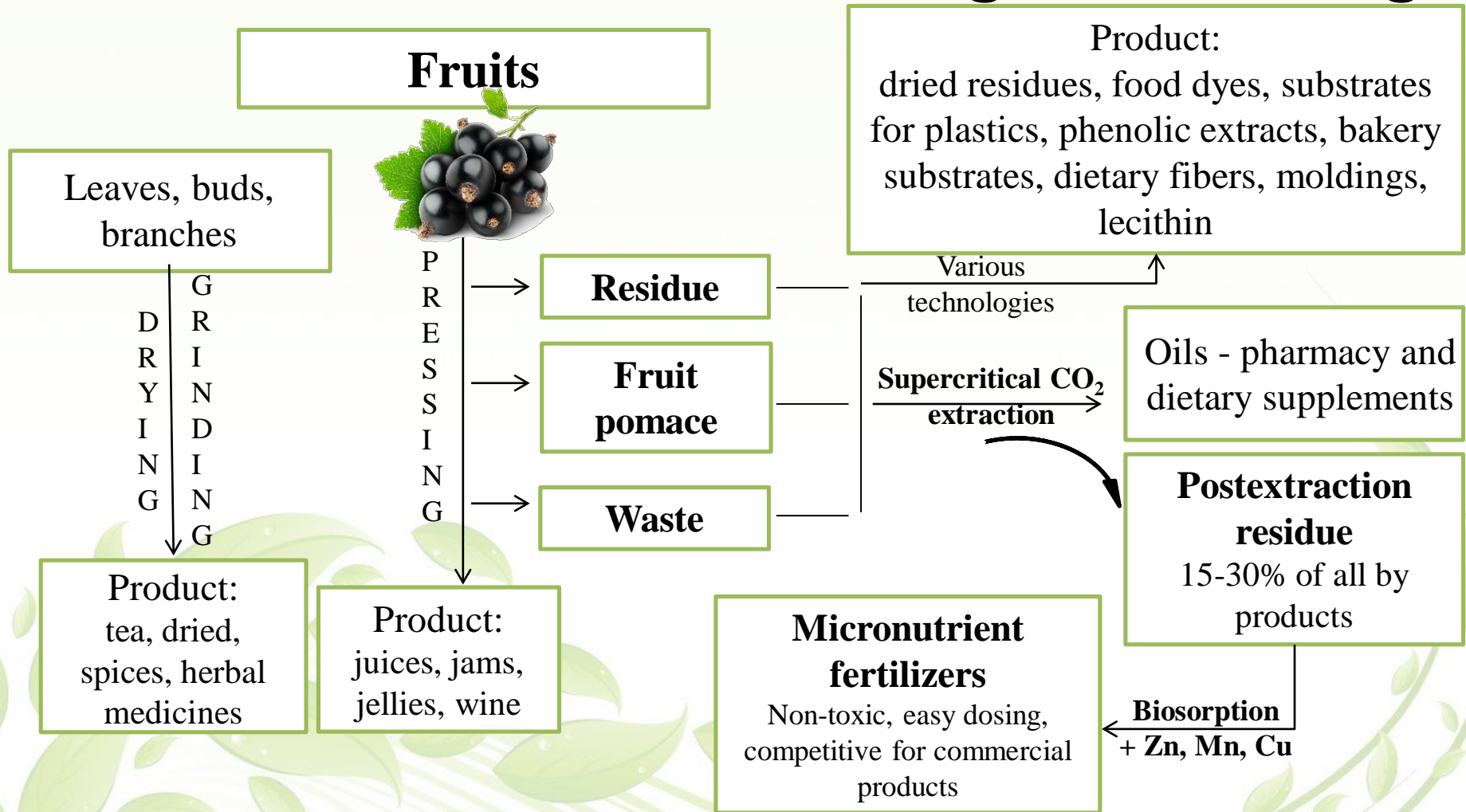


Waste

- Manure
- Agricultural waste



Micronutrient fertilizers for organic farming





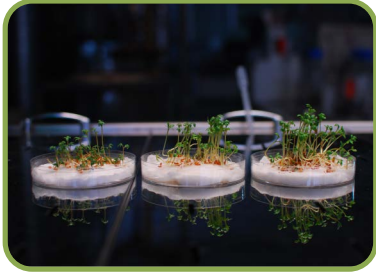
Previous studies

*Biosorption of metal ions to the biomass of
seeds of berries*

2012/05/E/ST8/03055

- Basic research.
- Biosorption in laboratory and bench scale.
- Selection of process parameters for single ions: Zn(II), Mn(II), Cu(II).
- Preliminary utility tests on plants.

Main results



Petri dish tests

- Tests on garden cress according to IRST standard
- Promising results - comparable to commercial chelates products



Pot trials

- Tests on white mustard – up to 2.5x higher dry mass, Zn, Mn and Cu content were higher by 25%, 18% i 38%, respectively



Field trials

- Two-season tests on maize - 10% biofortification
- Tests on raspberries – 12% biofortification



Current studies

- Implementation project: “Innovative micronutrient fertilizers by biosorption for organic farming” TANGO-V-C/0019/2021-00, WUST and EKOPLON consortium.
- Development of production technology for new biomass-based fertilizers.
- Biosorption carried out in a multi-ion system.
- Use of standardized waste streams as micronutrient solution.
- Scaling up the biosorption process to pilot conditions.



Expected results

- Organo-mineral fertilizers with micronutrients in organic form for food biofortification (Zn, Cu, Fe, Mn).
- Fertilizers dedicated to organic crops: cucumber and/or berries.
- Fertilizer formulation safe for plants and the environment.
- Waste-free technology (micronutrient recovery).

Determination of sorbate concentration and process duration time

- The experiment was conducted until the matrices were fully loaded - i.e. for 9h.
- The volume of the bed was 40 mL.
- Each matrix was prepared in 3 replicates.
- The experiments were conducted using Zn(II) at a concentration of 300 ppm.
- The sorption capacity of the matrices was determined by comparing ICP-OES results for biomass before and after the biosorption process.

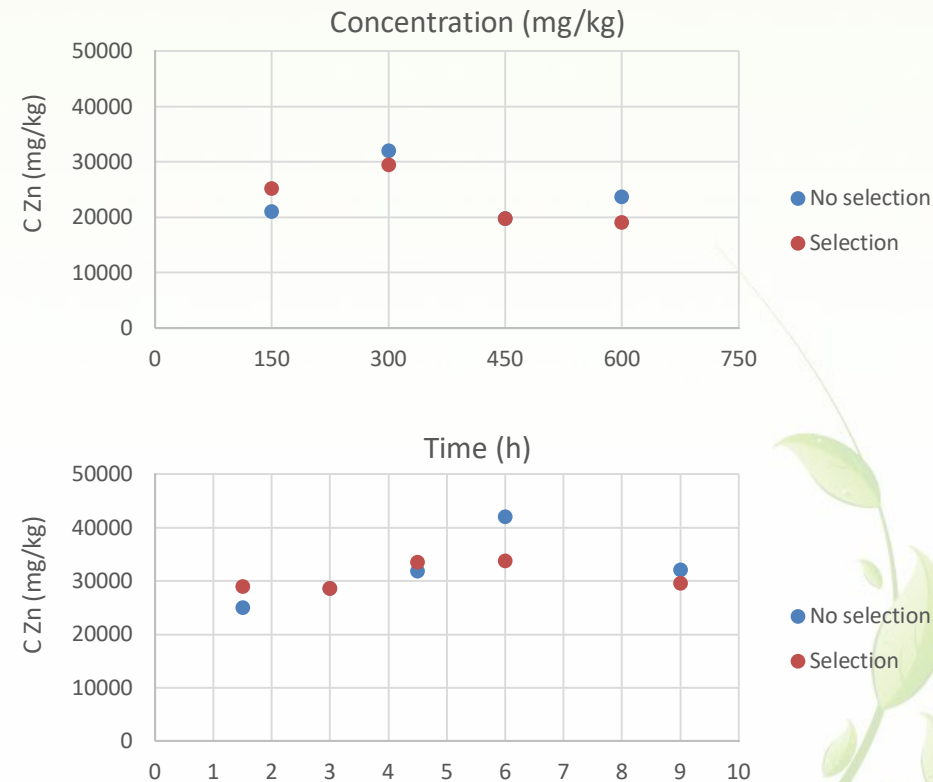


Fig. 1. Sorbate concentration and biosorption time determination.



Selection of sorbate concentration in a multielemental biosorption

	Content in enriched biomass (ppm)			
Concentration Cu:Mn:Zn (ppm)	Cu	Mn	Zn	Sum
38:300:65	28 635 ± 6 861	14 304 ± 1 474	2 257 ± 103	45 198
75:300:125	32 183 ± 2 253	9 973 ± 981	2 954 ± 295	45 111
150:600:250	34 082 ± 4 876	13 003 ± 3 007	3 763 ± 832	49 648
100:100:100	32 209 ± 6 049	5 355 ± 240	6 399 ± 355	43 965
200:200:200	33 294 ± 3 518	6 263 ± 98	6 526 ± 102	46 084
300:300:300	36 391 ± 6 840	6 562 ± 277	6 868 ± 325	49 822



Final process parameters

Sorbate	Cu(II), Zn(II), Mn(II)
Biosorbents	Blackcurrant seeds, Baltic algae (Fucus)
Sorbate concentration	300 mg/L
Reactor volume	70L
Micronutrient solution volume	200L
pH	5
Temperature	25°C
Material losses	10%
Volumetric flow rate	1L/min
Process time	6h
Drying	24 h, 50°C

Installation

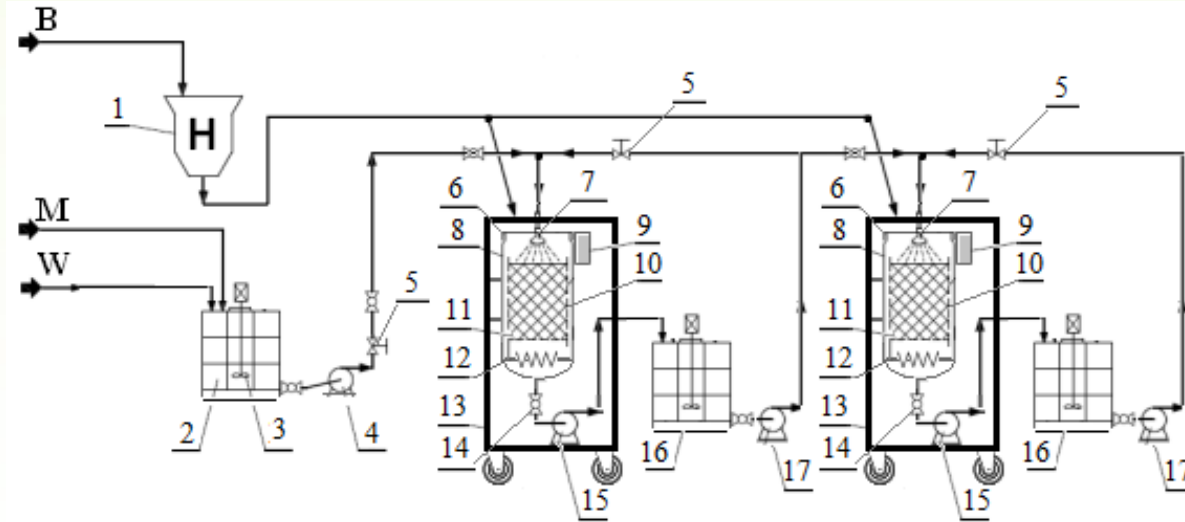


Fig. 4. Simplified scheme of the process in fixed bed mode – a system of two column reactors

Streams: B – Biomass, M – Micronutrients, W- Deionized water.

Main equipment: 1 – Biomass homogenizer; 2 – Micronutrient solution tank; 3 – Stirrer; 4, 15, 17– Peristaltic pumps; 8- Reactor tanks; 10 – Sieve; 16 – Recirculated solution tanks (equipped with pH regulator).





Multielemental biosorption results

	Baltic algae, raw (mg/kg)	Baltic algae, enriched (mg/kg)	Enrichment coefficient
Cu	17.2 ± 6.0	22 946 ± 1 848	1 302
Mn	417 ± 17	5 684 ± 565	13.6
Zn	71.1 ± 13.6	9 291 ± 1 112	130
	Blackcurrant seeds, raw (mg/kg)	Blackcurrant seeds, enriched (mg/kg)	Enrichment coefficient
Cu	12.8 ± 0.2	8 415 ± 3 296	6 584
Mn	26.1 ± 0.2	2 802 ± 1 029	107
Zn	25.6 ± 1.3	8 030 ± 220	312

Multielemental content of product

Macronutrient	Content (%)	Micronutrient	Content (g/kg)
C	45.1	Cu	8.42
N	4.13	Mn	2.80
P ₂ O ₅	1.36	Zn	8.30
K ₂ O	1.20	Fe	0.256
SO ₃	0.840	Toxic elements*	Content (mg/kg)
CaO	0.615	Cd	3.85·10 ⁻⁴
MgO	0.0965	Ni	4.63·10 ⁻³
Na ₂ O	0.0310	As	2.65·10 ⁻⁵
*Below the legal limit		Pb	2.42·10 ⁻³
		Cr	6.78·10 ⁻³
		Hg	1.16·10 ⁻⁵

Final product

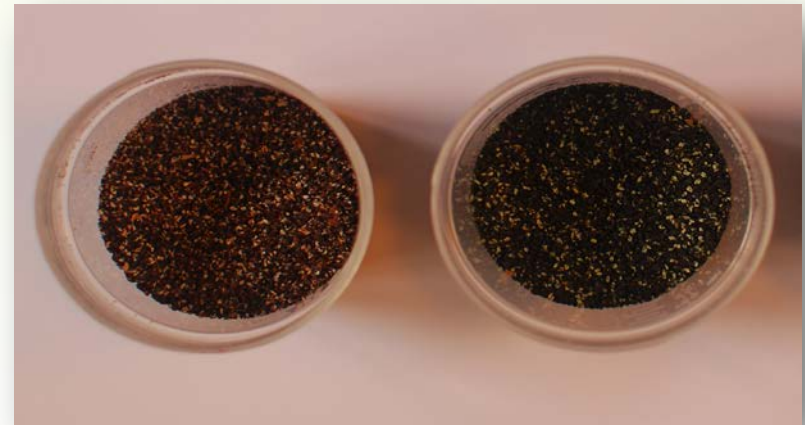


Fig. 9. Final product



Fixed bed modelling

Model	Equation	Linear form	Parameters	R ²
Thomas	$\frac{C_t}{C_0} = \frac{1}{1 + \exp\left[\left(\frac{k_{Th}q_e x}{Q}\right) - k_{Th}C_0 t\right]}$	$\ln\left(\frac{C_0}{C_t} - 1\right) = \frac{k_{Th}q_e x}{Q} - k_{Th}C_0 t$	Zn(II) $k_{Th} = 0.0209$ (mL/min mg) $q_e = 8.66$ (mg/g)	0.914
			Cu(II) $k_{Th} = 0.0353$ (mL/min mg) $q_e = 4.05$ (mg/g)	0.948
			Mn(II) $k_{Th} = 0.0523$ (mL/min mg) $q_e = 5.52$ (mg/g)	0.858
Nelson-Yoon	$\frac{C_t}{C_0 - C_t} = \exp(k_{YN}t - \tau k_{YN})$	$\ln\frac{C_t}{C_0 - C_t} = k_{YN}t - \tau k_{YN}$	Zn(II) $\tau = 14.8$ (min) $k_{YN} = 0.0053$ (1/min)	0.914
			Cu(II) $\tau = 12.6$ (min) $k_{YN} = 0.005$ (1/min)	0.948
			Mn(II) $\tau = 12.9$ (min) $k_{YN} = 0.097$ (1/min)	0.858
Wolborska	$\partial \frac{\partial c_b}{\partial t} + v \frac{\partial c_b}{\partial H} + \frac{\partial q}{\partial t} = D_{ax} \frac{\partial^2 c_b}{\partial H^2}$	$\ln\left(\frac{c}{c_0}\right) = \frac{\beta_a c_0 t}{q} - \frac{\beta_a H}{v}$	Zn(II) $\beta_a = 0.0240$ (1/min) $q = 8.46$ (mg/g)	0.833
			Cu(II) $\beta_a = 0.0253$ (1/min) $q = 4.72$ (mg/g)	0.941
			Mn(II) $\beta_a = 0.0251$ (1/min) $q = 6.19$ (mg/g)	0.523
Adams-Bohart	$\frac{C_t}{C_0} = \exp\left(k_{AB}C_0 t - k_{AB}N_0 \frac{z}{U_0}\right)$	$\ln\left(\frac{C_t}{C_0}\right) = k_{AB}C_0 t - k_{AB}N_0 \frac{z}{U_0}$	Zn(II) $N_0 = 3188$ (mg/L) $k_{AB} = 0.00751$ (mL/min mg)	0.833
			Cu(II) $N_0 = 1991$ (mg/L) $k_{AB} = 0.0127$ (mL/min mg)	0.941
			Mn(II) $N_0 = 1547$ (mg/L) $k_{AB} = 0.0162$ (mL/min mg)	0.523

Fixed bed modelling

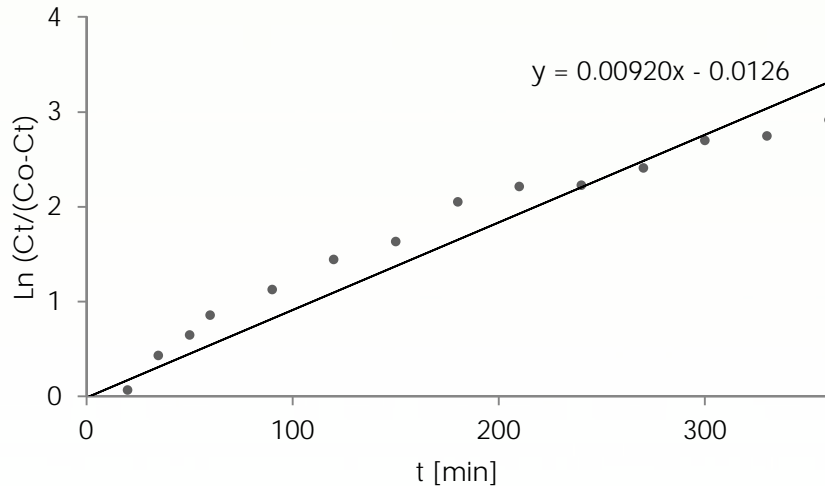


Fig. 5. Linearization of data for post-extraction residues with Zn(II), Nelson-Yoon model.

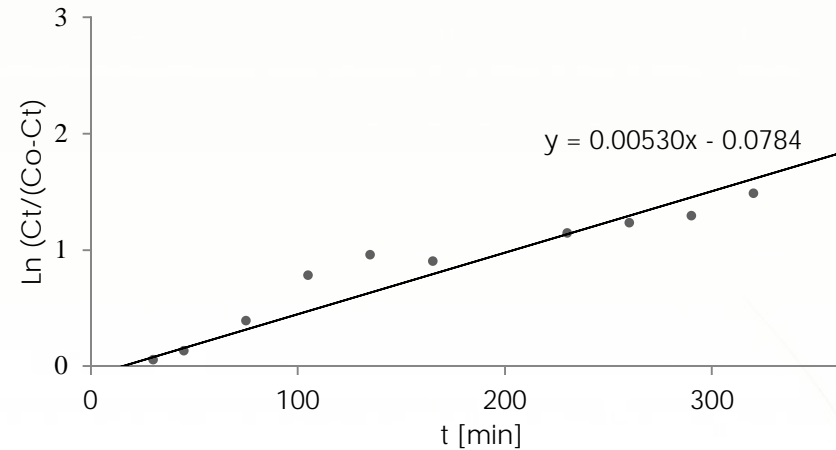


Fig. 6. Linearization of data for post-extraction residues with Mn(II), Nelson-Yoon model.

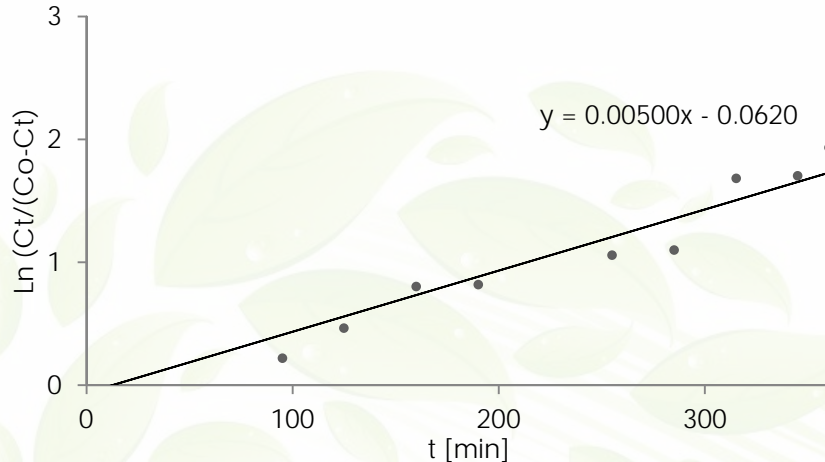


Fig. 7. Linearization of data for post-extraction residues with Cu(II), Nelson-Yoon model.

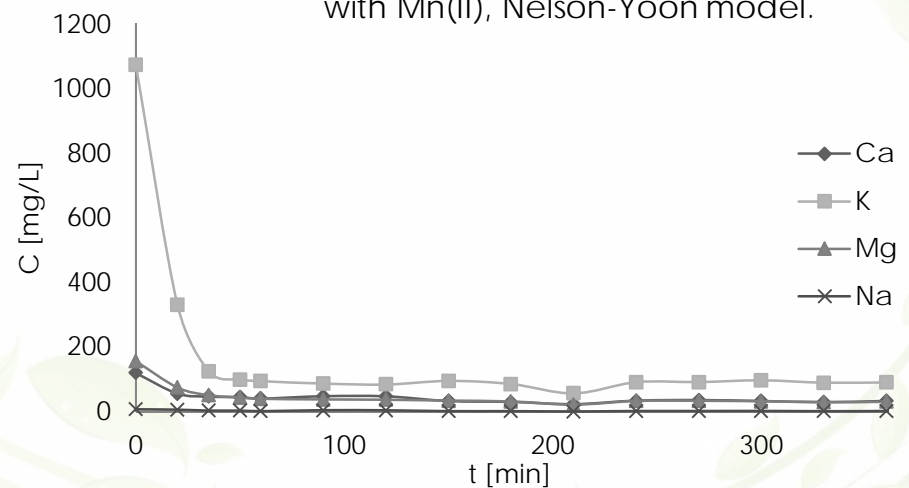


Fig 8. Release of Ca(II), K(I), Mg(II), Na(I) during the process.

Waste streams as micronutrients source - standarization

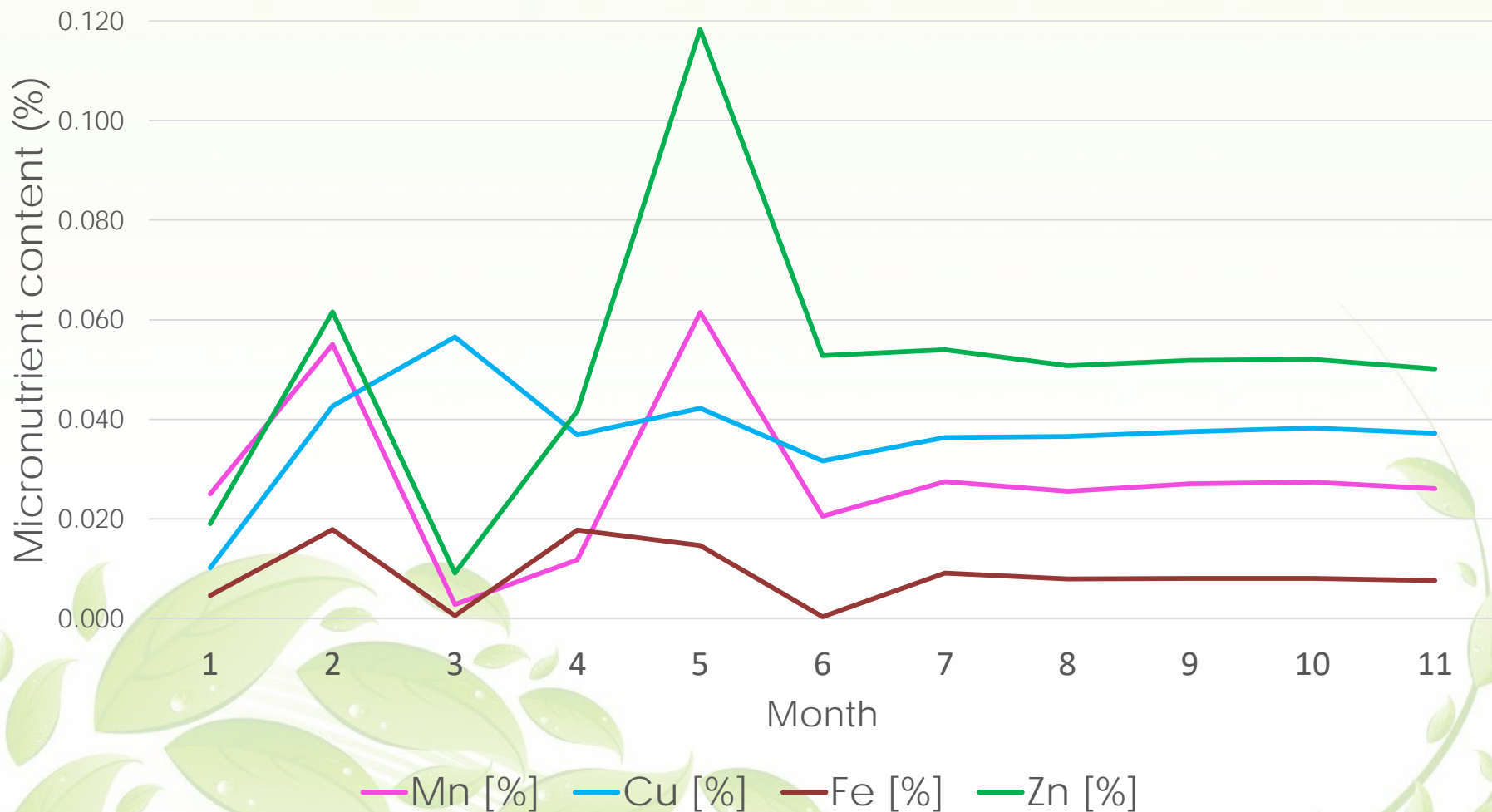


Fig. 2. Sidestream – micronutrients concentration vs. month

Perspectives and next steps



Scale up to pilot plant scale

transfer of verified bench-scale solutions



Selection of the process parameters

minor modifications of installation



Registration of the new product

pot and field trials of the final formulation on selected plant





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Thank you for your attention!

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