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"Engine fuels production via hydrotreatment of hydrothermal liquefaction bio-crude oil and pyrolysis bio-oil"

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YES or NO to Fuels?

- Fuels are interlinked with growth and development
 >Agriculture, industry, technology
- However, the increasing demand on fossil fuels has negative implications:
 - >Dependence from oil-producing countries
 - >Intense fluctuation of fuel prices
 - >Reduction of natural resources
 - >Green house effect & Climate change



Biofuels are Part of the Solution

Can boost national economy

- Create new employment opportunities
- >Reinforce other industries
 - >Sugar industry, Paper industry etc.

Can contribute to the reduction of atmospheric pollution

≻CO, SOx, HC, PM

Follows environmental EU commitment

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Paper, Kyoto Protocol (2012)
RedGreen, green house gas emissions
Reduction of total carbon footprint

Reduces dependence of oil imports

Countries can produce their own biofuels

Wheat Straw Waste

Wheat straw waste: Promising feedstock for 2nd generation biofuels production



Main Objective - Feedstocks

- Research target: " 2nd generation Engine fuel production"
- Two feedstocks were investigated

≻Pyrolysis bio-oil

≻HTL bio-crude

- Both oils produced from wheat straw wastes
- The Oils have different upgrading challenges

Ph	ner	lol	S

Carboxylic acids

Aldehydes

Ketones

Methoxyphenols

Pyrolysis bio-oil					Н
	Properties	Units	Pyrolysis bio-oil	HTL bio-crude	
	Density at 15°C	gr/ml	1.024	1.002	
	S on dry basis	wppm	596	175	
Al-	H on dry basis	wt%	6.50	8.38	
and a set of the loss	C on dry basis	wt%	42.13	55.87	
	O on dry basis	wt%	29.41	22.56	
	Viscosity at 40°C	cSts	156	NA	
	TAN	mgKOH/g	79.92	88.24	
	H2O dissolved	wt%	21.86	13.05	
	HHV	MJ/kg	20	27	
	Pour point	°C	-3	21	
	MCR	wt%	15.7	13	

HTL bio-crude



Experimental Procedure

- Hydrotreatment experiments were conducted in TRL 3
 HDT unit at CERTH
 - >Continuous flow
 - Capacity 60 ml/hr
- Commercial hydrotreating NiMo/γ-Al₂O₃ catalyst
- Effect of operating parameters
 - Reaction temperature
 - >H₂ supply



HDT Operating window tested

Parameters	Units	Cond. 1	Cond. 2	Cond. 3
Temperature	°C	330	360	330
Pressure	psi	1000	1000	1000
H ₂ /Oil ratio	scfb	5000	5000	3000
LHSV	hr⁻¹	1	1	1

TRL 3 Hydrotreating unit



Results – Elemental Composition

- Oxygenates were totally removed via aqueous phase
 >Organic phase have almost zero oxygen and water content
- Higher temperatures lead to higher aqueous phase yields
 More severe hydrodeoxygenation reactions
- HDT of bio-crude lead to higher organic yields compared to HDT of bio-oil





Properties	Units	Pyrolysis bio-oil	HTL bio-crude
Density at 15°C	gr/ml	0.91-0.94	0.84-0.87
S on dry basis	wppm	30-80	10-80
H on dry basis	wt%	11.3-11.7	12.5-13.4
C on dry basis	wt%	85.5-86.8	83.0-86.1
O on dry basis	wt%	1.70-2.99	0.00-3.34
Viscosity at 40°C	cSts	4.9-14.6	5.3-13.3
TAN	mgKOH/g	0.00-0.87	0.18-6.0
H2O dissolved	wt%	0.001-0.02	0.002-0.65
нну	MJ/kg	42.8-43.5	43.4-45.9
Organic phase	v/v %	65-70	59-70
Aqueous phase	v/v %	32-34	38-45

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Results – Elemental Composition

- HDT increase the hydrogen content resulting in high energy organic product
 - >60% higher H content in bio-crude products
 - >79% higher H content in pyrolysis bio-oil products
- HDT Bio-crude has higher H/C ratio compared to HDT bio-oil
 - >HDT bio-crude higher energy content



 HDT of bio-oil has higher H₂ consumption compared to HDT of HTL bio-crude





Results - Mass recovery curve - Product Yields

- Instability of HTL bio-crude and pyrolysis bio-oil, is a result of their heavy hydrocarbon molecules
- Hydrocracking and saturation of these heavy molecules improve stability
- Increase of T, raise the rate of hydrocracking and H₂ consumption
- Gasoline and diesel range hydrocarbons are produced



• HTL bio-crude optimum condition 1

>10 wt% gasoline, 62 wt% Diesel and 28 wt% heavy fuel

Pyrolysis bio-oil optimum condition 2
 >20 wt% gasoline, 43 wt% diesel and 37 wt% heavy fuel

GC-MS Chromatograph Results HDT Bio-Crude

- HDT reduced the oxygen- and nitrogen-containing compounds
- Organic liquid consists mainly from:

≻~50 wt% n-paraffins and high percent of saturated (Naphthene 7.88 -11.94 wt%) and unsaturated (Olefines 2.29 - 3.67 wt%) hydrocarbons

Palmitic acid (CH3(CH2)14C00H) → Heptadecane (C17H36) Oleic acid (CH18H340) → Octadecane (C18H38)





Catalyst Deactivation

- Catalyst deactivation is mostly caused by cocking, sintering, poisoning and metal deposition
- Fast catalyst deactivation, expressed via DP build-up, was observed
- For HTL bio-crude: the DP build up produced linearly with time on stream, starting from the 2nd DOS
- For pyrolysis bio-oil, the DP was steady for 4 DOS and increased rapidly at the end of DOS 4



Conclusions

- Hydrotreatment of pyrolysis bio-oil has led to an almost zero oxygen and water content product with high energy density
- The carboxylic acids of HTL bio-crude, especially the palmitic and oleic, were fully converted to the corresponding Heptadecane and Octadecane hydrocarbons leading to an almost zero oxygenate product
- Hydrotreatment of HTL bio-crude is characterized by lower hydrogen consumption and higher carbon yields, compared to hydrotreatment of pyrolysis bio-oil
- Refinery intermediate products were successfully produced from both routes
- Hybrid fuels can be produced via co-processing of HDT oil with petroleum fractions



Summarize







Thank you for your attention

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