Low energy treatment technology for leachate valorization - LIFE LEACHLESS











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Background

- In the EU, annually **16 tonnes** of materials are used by each person and **6 tonnes** of it are converted into waste.
- Solid waste can be disposed in various ways:
 - Incineration.
 - Landfilling.
 - Recycling.
 - Composting.









- Landfilling has been the most commonly used solid waste disposal, specially in the Mediterranean and Eastern Europe countries.
- Landfills present long-term threats to soil, air, groundwater and surface water due formation of greenhouse gases (methane gas and carbon dioxide from decomposing garbage) and leachate.



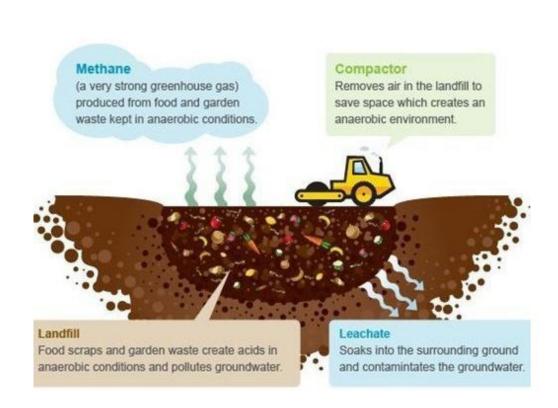






Leachate

- Leachate is the **liquid fraction** of the already existing moisture/liquid within the **solid waste** and the continuously formed liquid with dissolved and suspended solids extracted from the waste while rainfall percolates through it.
- Not only during their useful life, but also **fifty years after their closure**, landfills keep on producing leachate.
- Approximately, **10 m³** of leachate is generated per **115 tonnes** of solid waste.
- The **composition** of leachate **differs** from site to site and also within the landfill, the composition of the leachate alters with time (from weeks to years).





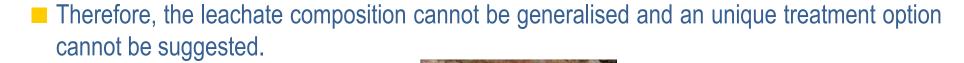






Leachate

- The composition of the leachate depends on factors such as:
 - characteristics of the waste.
 - moisture content.
 - climatic conditions.
 - degree of compaction.
 - age of the landfill.













Leachate

- In the absence of treatment, leachate is:
 - Recycled back to the waste to maintain the biological activity in the composting solid waste by keeping it moist.
 - Send it to sewer or to a wastewater treatment plant (WWTP) in case they do not treat it on site.

Leachate treatment processes comparative costs (Source: Adapted from Giraldo, 2001)

| Treatment technology | Cost (€/m³) | | |
|--|-------------|--|--|
| Aerobic process with nitrogen removing | 15.00 | | |
| Two steps reverse osmosis | 7.50 | | |
| Biologic process + carbon activated + precipitation | 18.75-26.25 | | |
| Biologic process + reverse osmosis + concentrate evaporation | 26.25-30.00 | | |
| LIFE LEACHLESS technology (solar evaporation/condensation + forward osmosis) | 4.75 | | |









LIFE LEACHLESS project

- LIFE LEACHLESS project demonstrates the **feasibility of an innovative in-situ treatment process** for leachates generated in landfills and waste treatment plants.
- The project LIFE LEACHLESS proposes a **sustainable management** composed of specially designed solar panels, which reach to very high temperatures to evaporate the leachate.
- Then the vapour is condensed to follow its path through **forward osmosis** (FO) step. FO requires less energy than the reverse osmosis (RO) and has less fouling problems.
- The project is easy to replicate and easy to operate and maintain.
- The proposed system is a universal solution independent of the leachate composition.









Main objectives

- The LIFE LEACHLESS project will promote water resources management actions in accordance with the Water Framework Directive 2000/60/EC by enabling managers of landfills and waste treatment centres to achieve good qualitative and quantitative status of their effluents.
- The LEACHLESS project proposes a **treatment model** that will be carried out **"in-situ"** using a **cost-effective** novel technology that combines **solar evaporation/condensation** plus **forward osmosis**. The prototype will be powered by **renewable energies** (solar energy, biomass and residual heat), which will minimise the **carbon footprint** of the process.
- The final effluent will be **reused** for **cleaning** and **gardening** purposes. A minority **semi-solid** residual **stream** will be also generated in the process. Due to its special composition (rich in metals and inorganic elements), this stream will be **valorised** in ceramic industries to improve the final products characteristics.









The figures of the project





| | Start: 01/10/2016 | Total budget: 1,775,805 € | | |
|-------|-----------------------|---------------------------|---|--|
| Dates | End: 31/12/2020 | Figures | EU contribution: 1,041,237 € (60% of eligible budget) | |
| | Extension: 30/06/2023 | | 3 partners | |

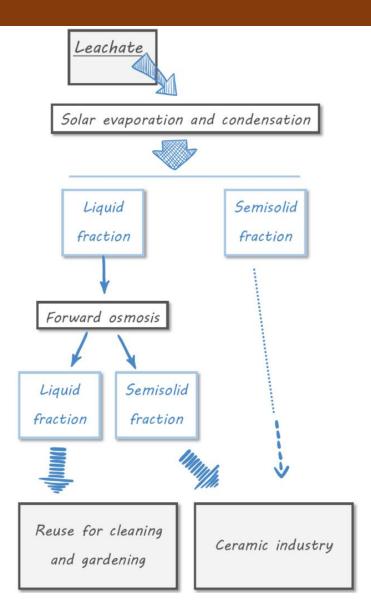








Process diagram





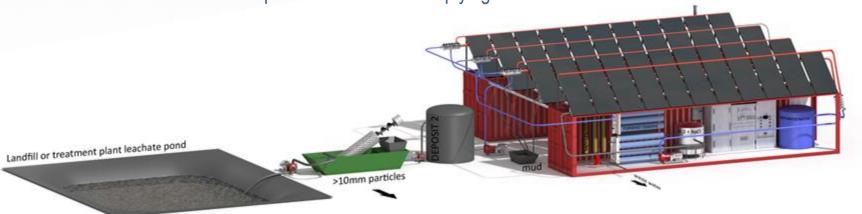






LIFE LEACHLESS prototype

- The proposed treatment system is composed of two main separation processes:
 - a **novel solar panel**, which evaporates and condenses the leachate in the first step.
 - **forward osmosis** step to obtain effluent complying with the reuse standards.



- This system will be placed in three containers (12mx2,4mx2,9m), for the easy portability between the demonstrations sites:
 - a waste treatment centre in Spain.
 - a landfill in Greece.
- The maximum **capacity** of the plant is **12-8 m³/day**.

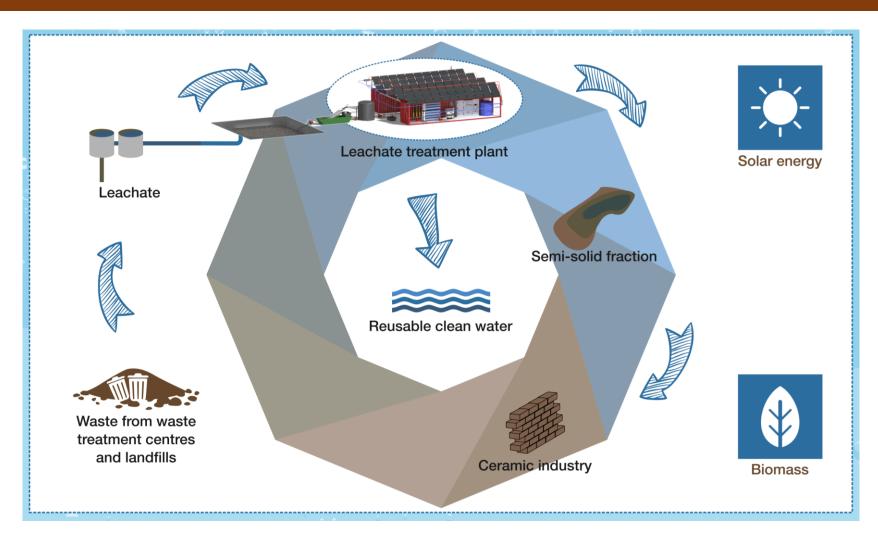








LIFE LEACHLESS project and circular economy philosophy











- Prior to the construction of the demonstration plant, **laboratory-scale tests** were carried out with the two technologies.
 - Solar evaporation/condensation.
 - Forward-osmosis
- The aim was to optimise the **operating conditions** of the individual treatment processes.
- The results served as the basis for the **design** of the demonstration plant.













- After the lab-scale tests, the **construction of the demonstration plant** was carried out.
- The plant has been operated at **two demo sites.**















First demo site: Waste Treatment Centre in Lanzarote (Spain)





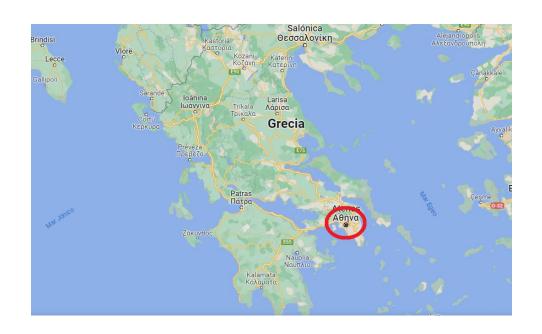








Second demo site: Ano Liosia landfill in Athens (Greece)













Results of the leachate treatment system from the demonstration plant:

| Physicochemical parameters | Unit | Initial leachate | Final effluent | Limit value |
|----------------------------|---------------------|---------------------|-------------------|----------------|
| BOD ₅ | mg/L O ₂ | 7,160 | 17 | < 25 |
| COD | mg/L O ₂ | 13,850 | 51 | < 125 |
| Suspended solids | mg/L | 1,820 | 1 | < 2 |
| Conductivity (20°C) | μS/cm | 31,100 | 787 | 700-1,000 |
| Total phosphorus | mg/L | 182 | 2.63 | < 10 |
| Intestinal nematodes | eggs/L | <1 | <1 | < 1 |
| Escherichia coli | cfu/100 mL | 3,158 | 1 | ≤ 50 |
| Volatile suspended solids | mg/L | 1,440 | 5 | < 20 |
| Copper | mg/L | 0.2 | < 0.01 | < 0.1 |
| Iron | mg/L | 153.76 | < 0.01 | < 2 |
| Sodium | mg/L | 2770.1 | 18.7 | < 70 |
| Aluminium | mg/L | 531.74 | < 0.01 | < 1 |
| Arsenic | mg/L | 0.5 | 0.05 | < 0.05 |
| Barium | mg/L | 0.2 | 0.02 | < 20 |
| Cadmium | mg/L | 0.2 | 0.002 | < 0.005 |
| Chromium | mg/L | 0.29 | 0.07 | < 0.1 |
| Tin | mg/L | 0.3 | 0.03 | < 10 |
| Manganese | mg/L | 0.2 | 0.02 | 0.5 |
| Nickel | mg/L | 0.31 | 0.03 | < 0.05 |
| Lead | mg/L | 0.2 | 0.04 | < 0.05 |
| Zinc | mg/L | 0.74 | 0.05 | < 0.5 |
| a-HCH | μg/L | 0.01 | 0.01 | < 0.05 |
| Endrin cetona | μg/L | 0.01 | 0.01 | < 0.05 |
| Heptaclor | μg/L | 0.01 | 0.01 | < 0.05 |
| Heptaclor epóxido | μg/L | 0.01 | 0.01 | < 0.05 |
| Lindano | μg/L | 0.01 | 0.01 | < 0.05 |
| p,p'-DDD | μg/L | 0.01 | 0.01 | < 0.05 |
| p,p'-DDE | μg/L | 0.01 | 0.01 | < 0.05 |
| p,p'-DDY | μg/L | 0.01 | 0.01 | < 0.05 |
| Aldrín | μg/L | 0.01 | 0.01 | < 0.05 |
| b-HCH | μg/L | 0.01 | 0.01 | < 0.05 |
| d-HCH | μg/L | 0.01 | 0.01 | < 0.05 |
| Dieldrín | μg/L | 0.01 | 0.01 | < 0.05 |
| Endosulfan I | μg/L | 0.01 | 0.01 | < 0.05 |
| Endosulfan II | μg/L | 0.01 | 0.01 | < 0.05 |
| Endosulfan sulfato | μg/L | 0.01 | 0.01 | < 0.05 |
| Endrin | μg/L | 0.01 | 0.01 | < 0.05 |
| | | | | |







Samples from the demonstration plant operation in Lanzarote:





Initial leachate

Final effluent

Effluent after evaporation/condensation

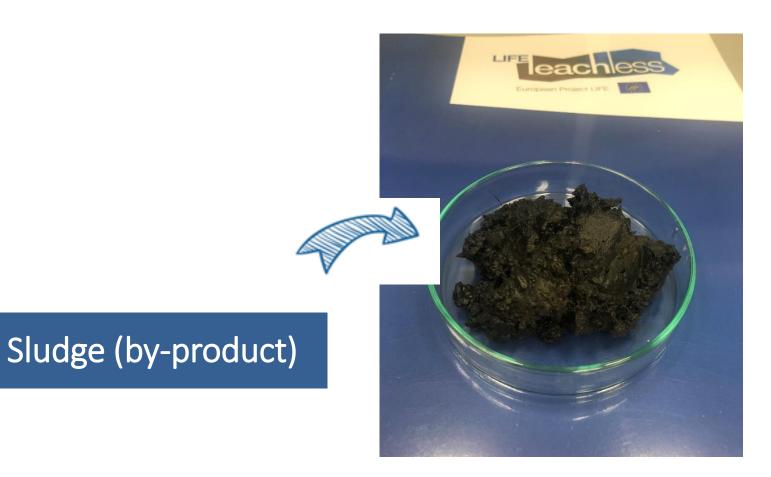








Samples from the demonstration plant operation in Lanzarote:











- All parameter **concentrations** have been considerably **reduced**.
 - COD reduction of 99%.
 - Very low metal concentrations.
 - Reduction of sodium concentration of 98%











Conclusions

- Optimisation of operating and process conditions for solar evaporation/condensation and forward osmosis.
- Aquaporin™ hollow fiber membrane selected for forward osmosis process.
- Recovery of up to **80-70%** of the leachate (the remainder is recovered as sludge or reused in the drawn solution).
- Quality of the final effluent according to the limits established by legislation.
- **Sludge** obtained as a by-product with an interesting metallic composition to be used in the formulation of **ceramic components**.



Thank you for your attention



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