

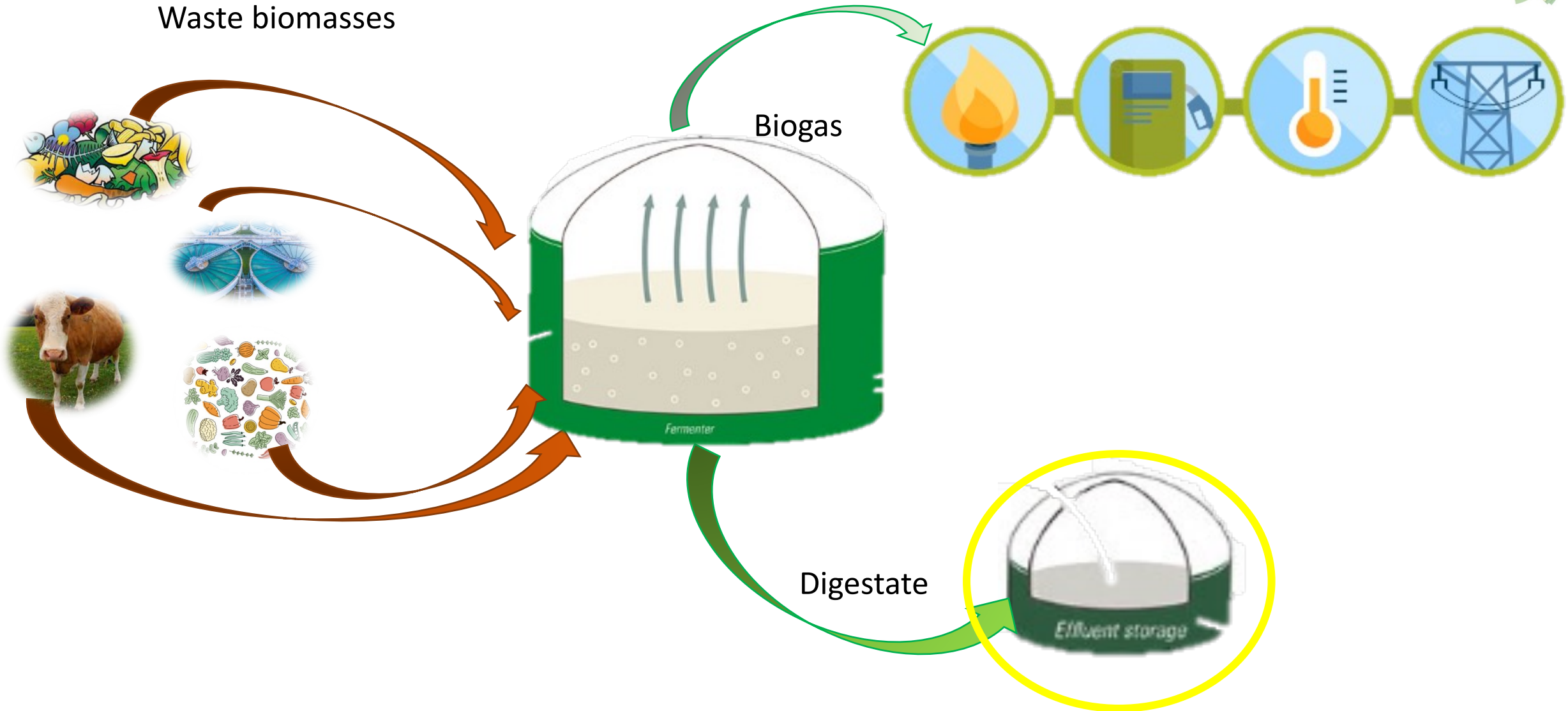
Close the loop: study of the effect of digestate derived biochar on anaerobic digestion of organic fraction municipal solid waste.

Francesca Demichelis, Fabio Alessandro Deorsola, Tonia Tommasi, Debora Fino

Polytechnic of Turin



Introduction to anaerobic digestion



Our approach

The flowchart illustrates the process of converting OFMSW into various products. It starts with OFMSW (Organic Fraction of Municipal Solid Waste) entering a reactor. From the reactor, the process splits into two main paths. The top path involves a reactor with a stirrer and a gas outlet, leading to the production of Bio-oil and pyrogas. The bottom path involves a reactor with a stirrer and a gas outlet, leading to the production of biochar. The biochar is then further processed with KOH to produce KOH-biochar. The final products are Bio-oil and pyrogas, biochar, and KOH-biochar.

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graph LR; OFMSW[OFMSW] --> R1[Reactor]; R1 --> R2[Reactor]; R1 --> Digestate[Digestate]; R2 --> BioOilPyro[Bio-oil and pyrogas]; R2 --> Biochar[biochar]; Biochar --> KOHBiochar[KOH - biochar]; KOHBiochar --> R3[Reactor]; R3 --> BioOilPyro2[Bio-oil and pyrogas];
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OFMSW

Digestate

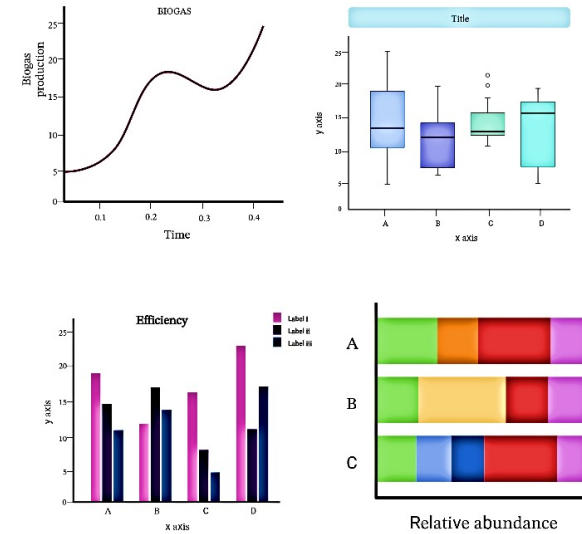
+ KOH

Bio-oil and pyrogas

biochar

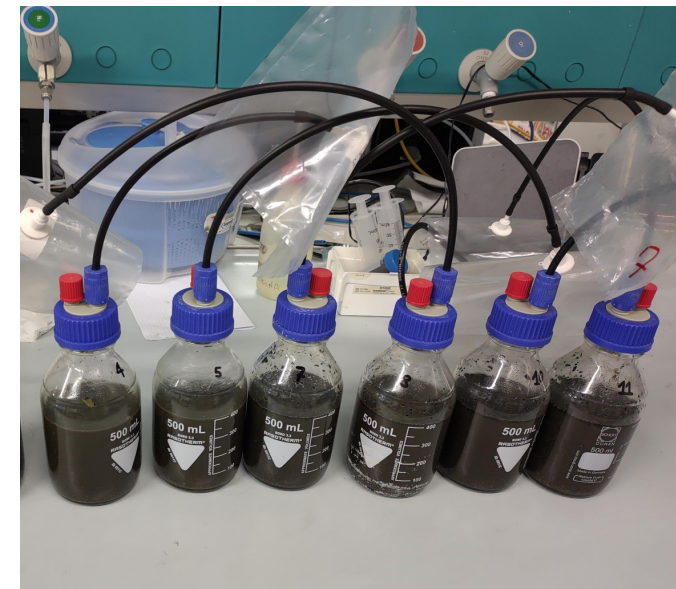
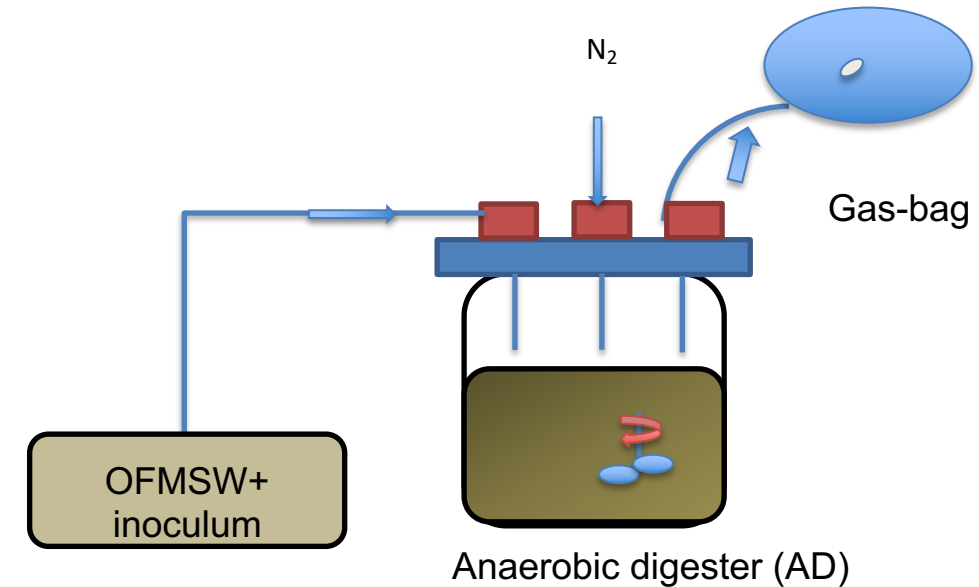
KOH - biochar

Bio-oil and pyrogas



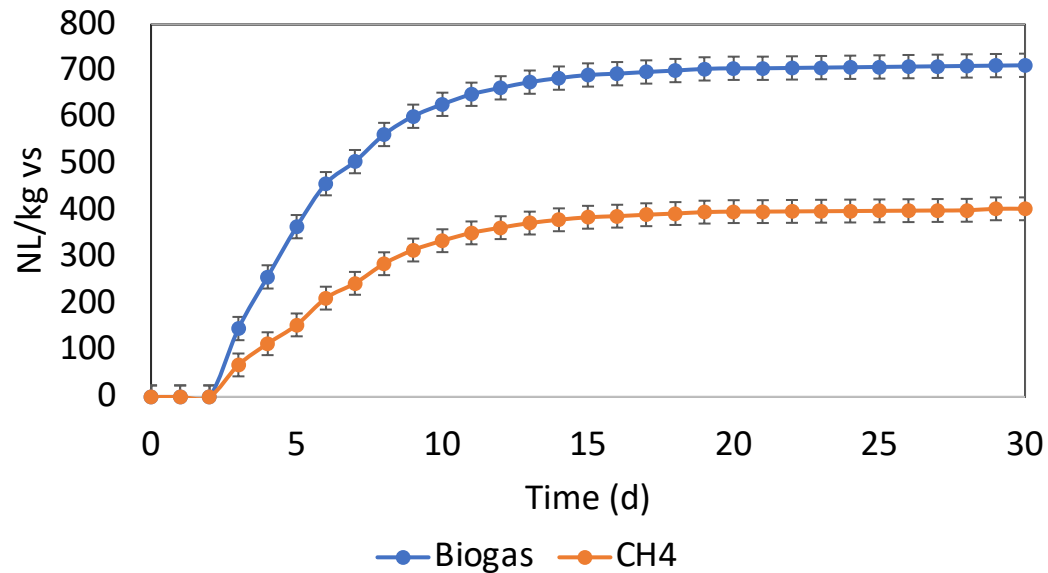
Anaerobic digestion conditions

- Batch mode feed
- Total solid (TS) (%) feed: 6 %
- Substrate (S): organic fraction municipal solid waste (OFMSW) from San Carlo S.p.A. (Fossano, Italy)
- Inoculum (I): digestate of cow-agricultural waste (Candiolo, Italy)
- S:I = 2:1
- T = 37 °C
- Volume = 500 mL
- Test in triplicate



Anaerobic digestion performance

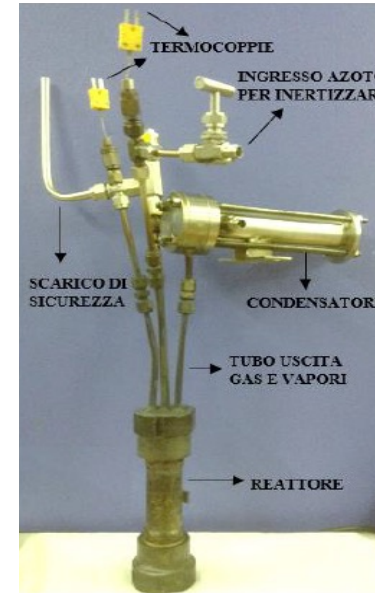
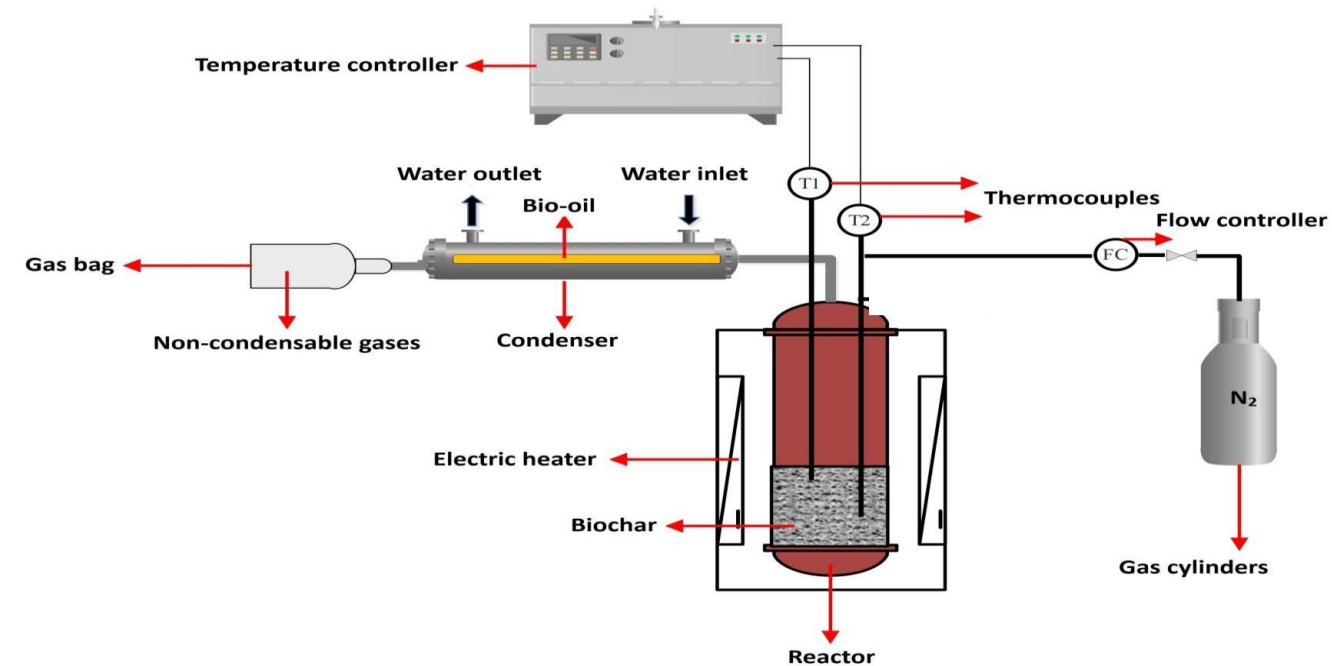
Anerobic digetion of OFMSW



	OFMSW		Inoculum CAS		Digestate	
	mean	dev.st	mean	dev.st	mean	dev.st
TS (%)	19	2.3	6	0.1	5.7	0.99
VS/TS (%)	97	1.8	67.9	1	52	2.76
C (%)	45.7	2.7	40.6	0.6	35.34	1.34
H (%)	6.1	0.3	3	0	6.08	2.1
N (%)	2.4	0.2	7.9	0.1	3.4	0.45
S (%)	0.2	0.1	0	0	1.45	0.01
O /%	45.4	3.1	48,5	2.1	49.73	0.23
pH	5.3	0.2	7.7	0.1	6.9	0.15

Slow pyrolysis conditions

- Fixed bed reactor
- Feedstock:
 - KOH pre-treated digestate at KOH/digestate ratios = 1:4 ; 1:2 ; 1:1
 - Digestate as well
- $T = 400, 500, 600\text{ }^{\circ}\text{C}$
- Heating rate = $10\text{ }^{\circ}\text{C}/\text{min}$
- Residence time = 1h
- Volume = 100 mL



Biochar from KOH-pre-treated digestate

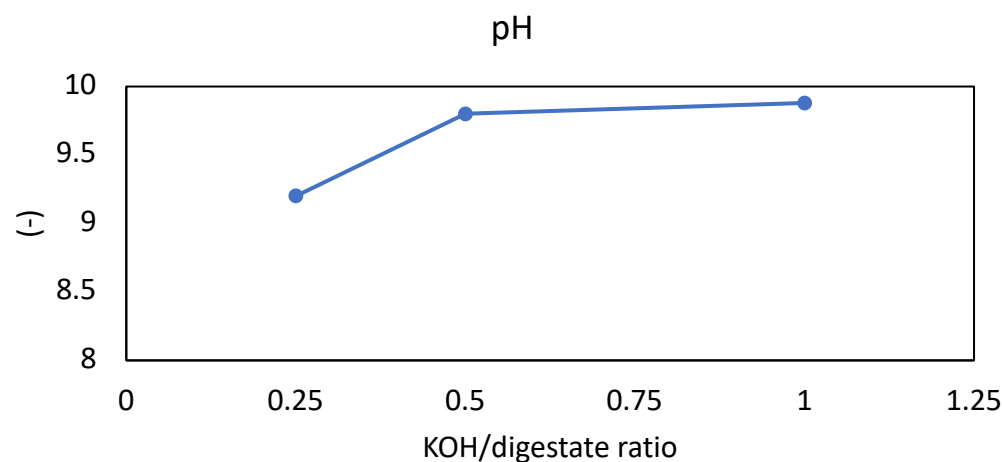
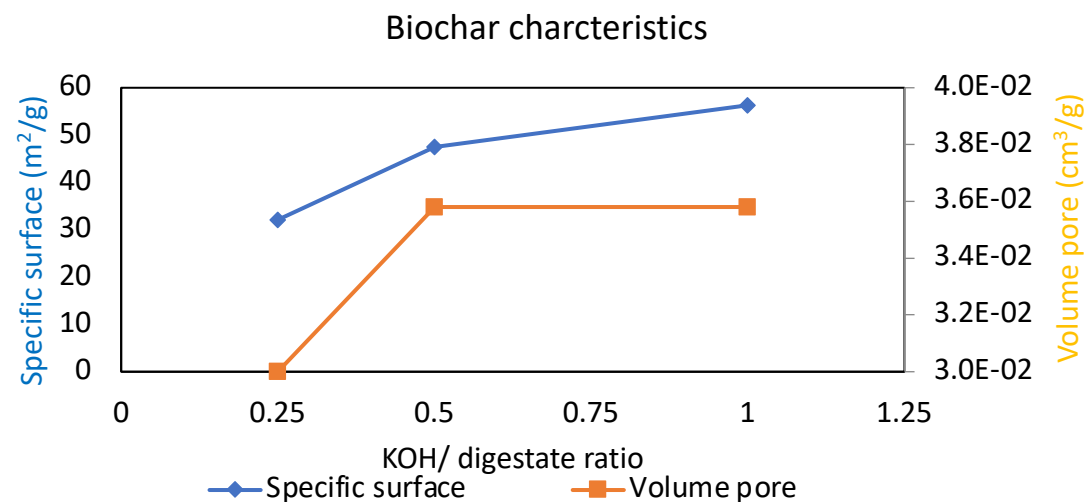
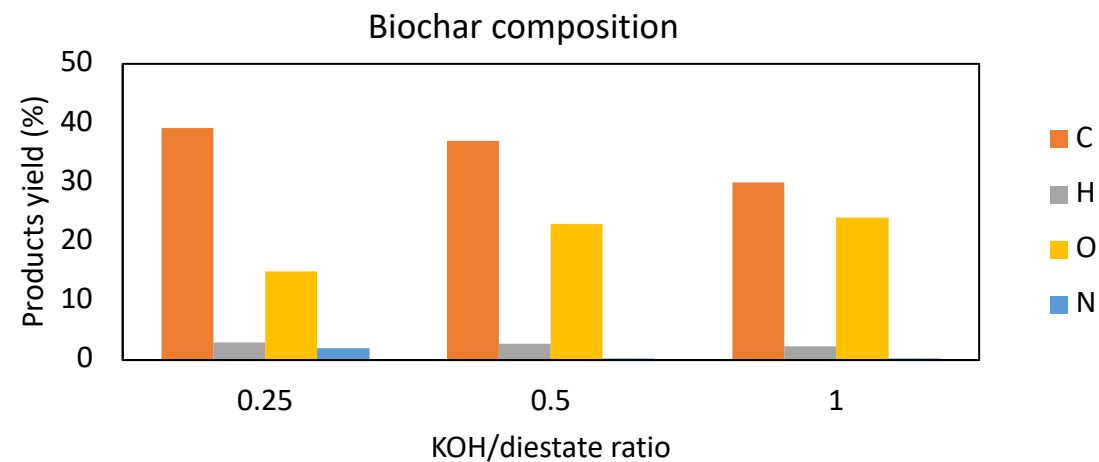
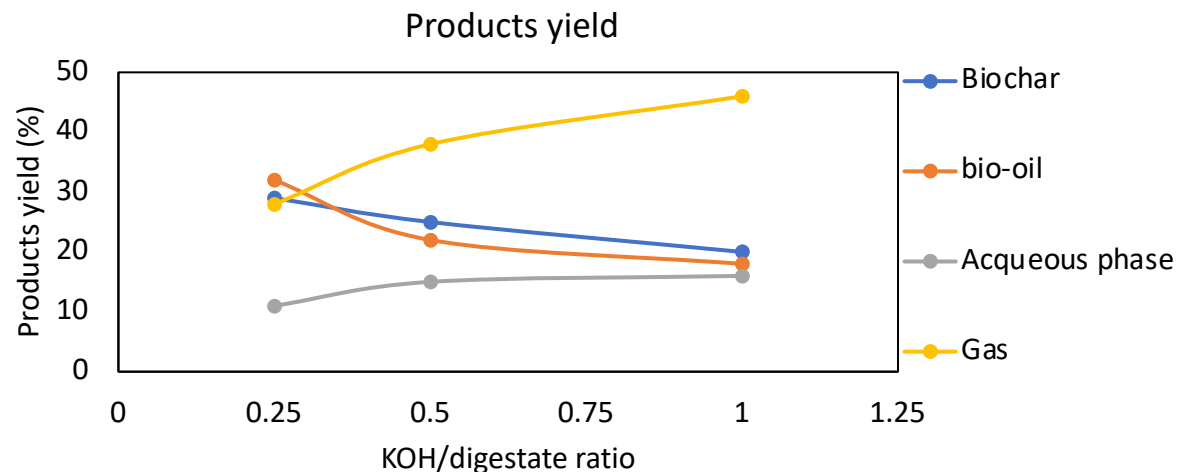


Biochar from digestate



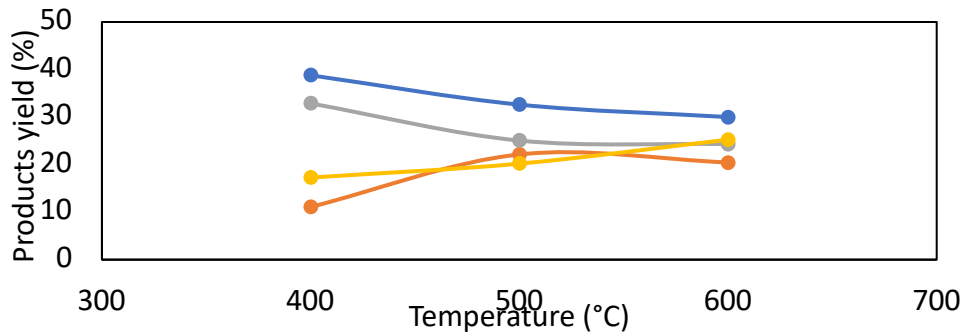
Slow pyrolysis : study of KOH effect

T = 600°C

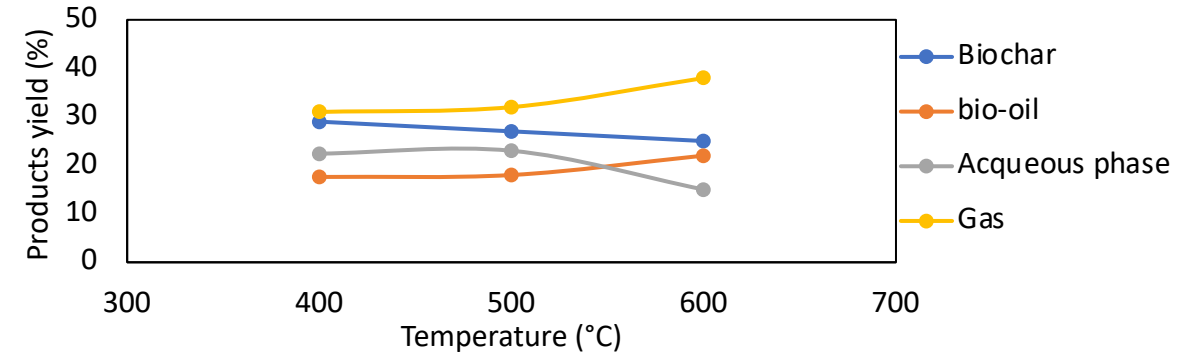


Slow pyrolysis: study of temperature effect

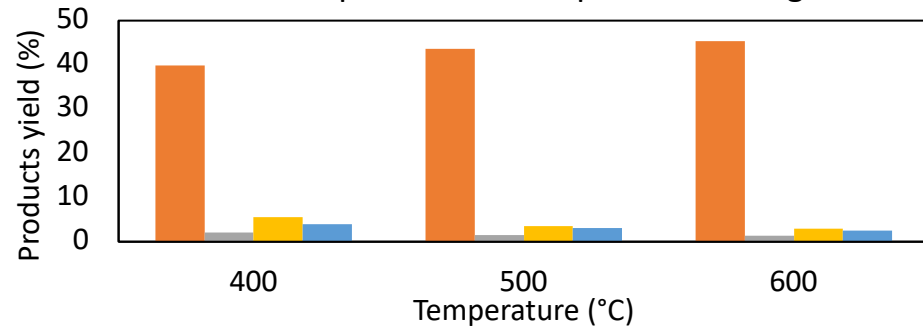
Products yield with non pre-treated digestate



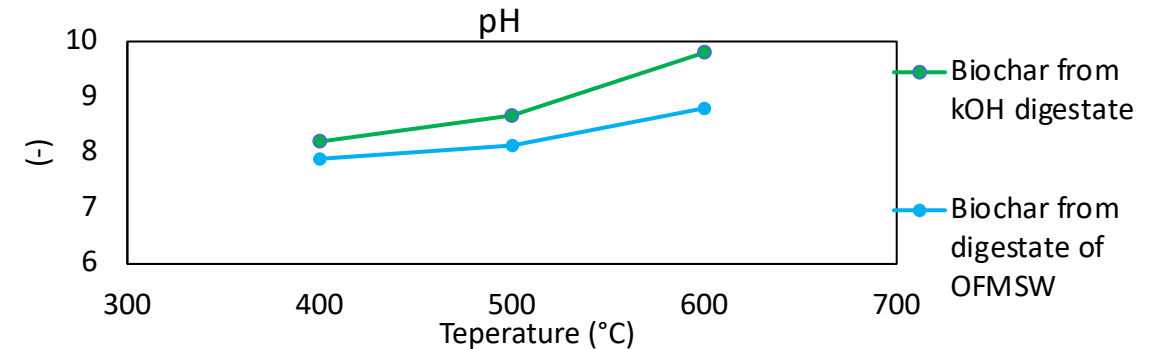
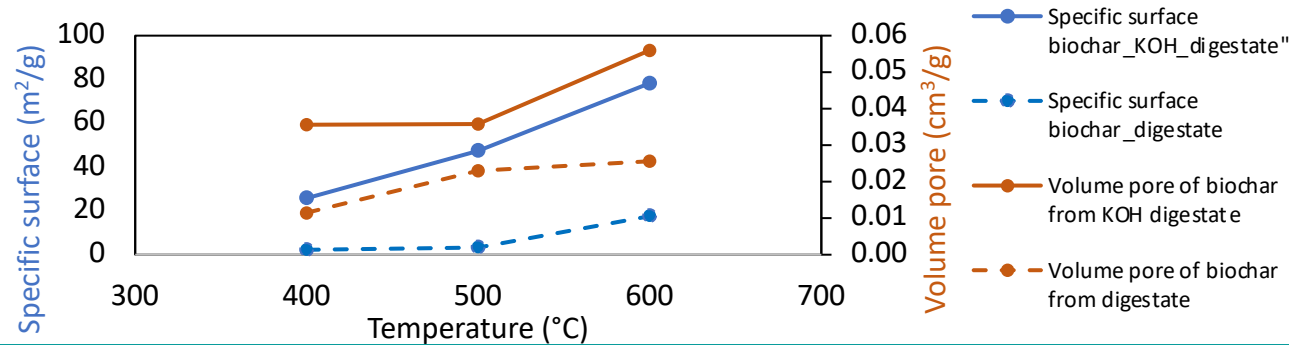
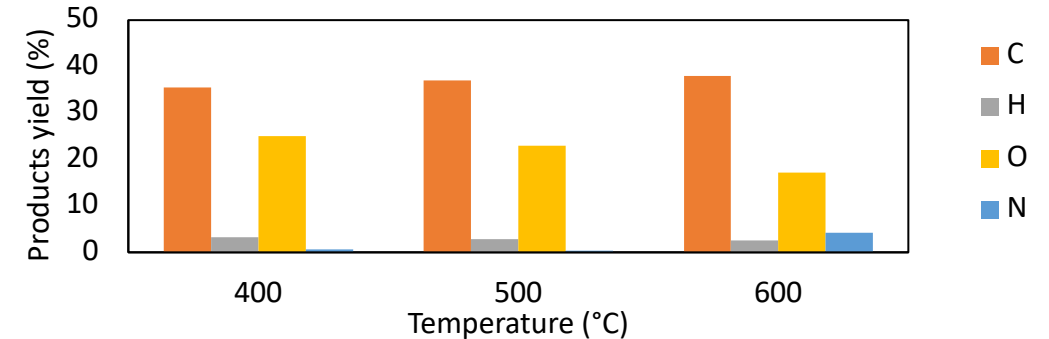
Products yield with KOH pre-treated digestate



Biochar composition of non pre-treated digestate

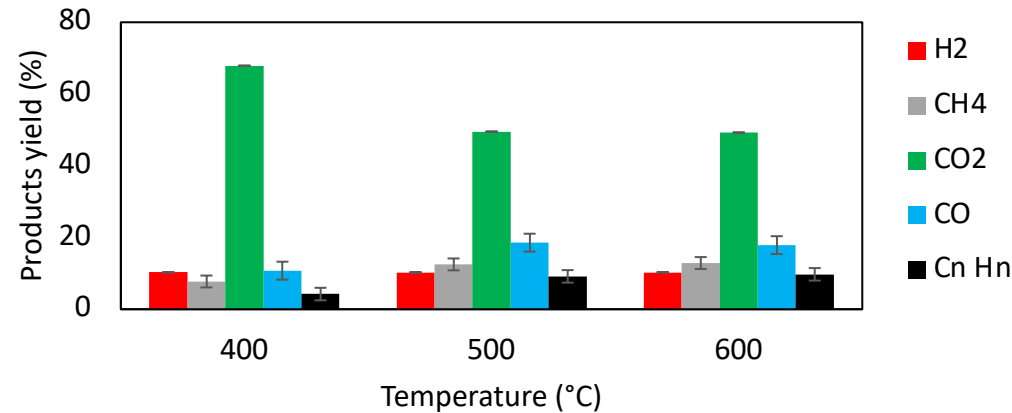


Biochar composition of KOH pre-treated digestate

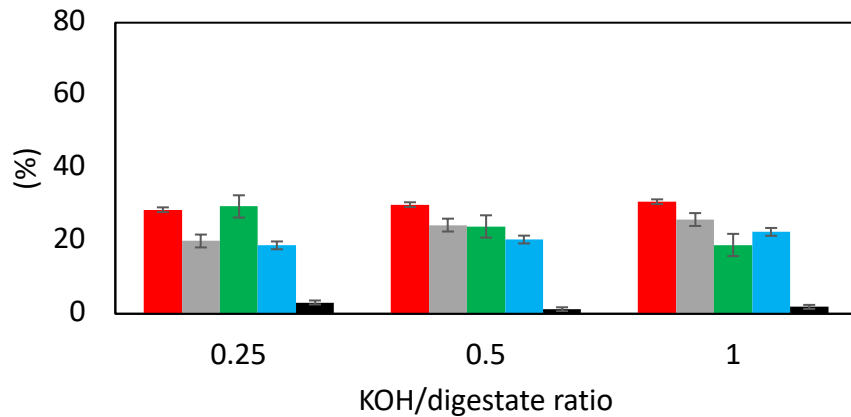


Slow pyrolysis: study of gas composition

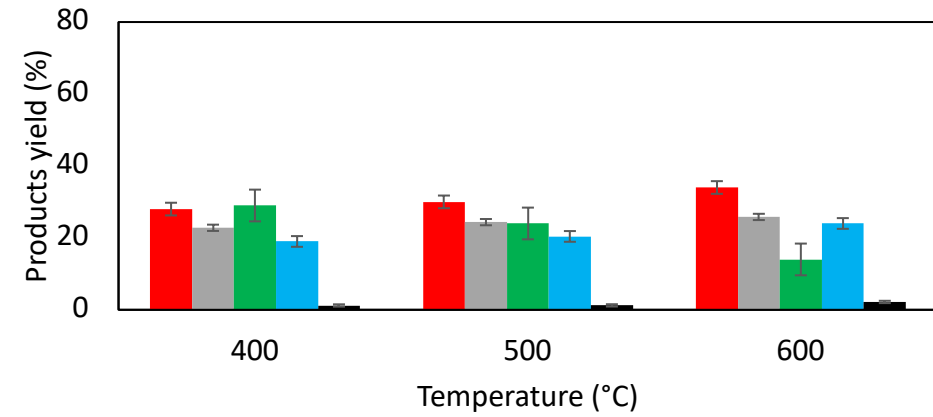
Gas composition of non pre-treated digestate



Gas composition of KOH pre-treated digestate



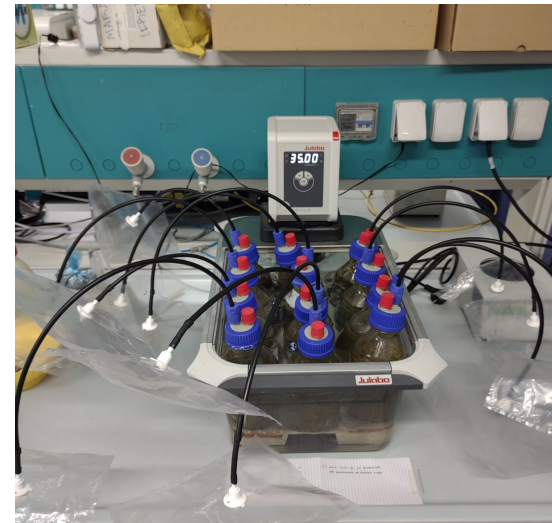
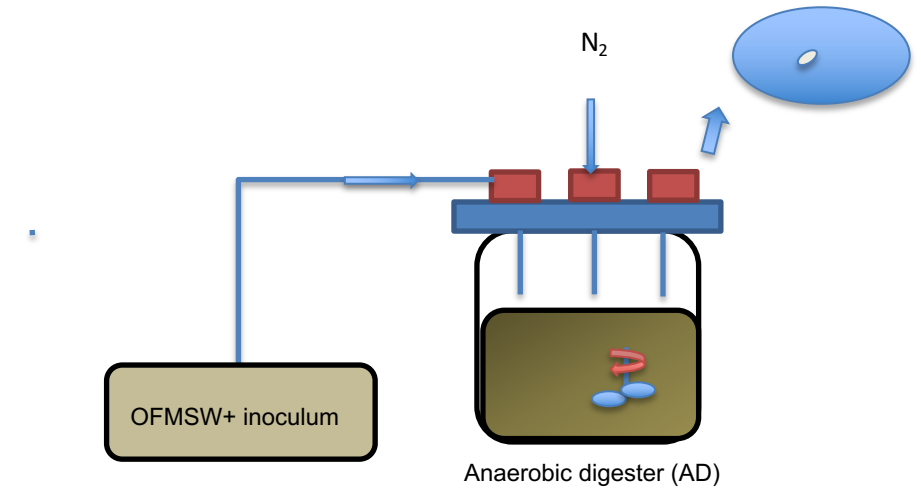
Gas composition of KOH pre-treated digestate



Anaerobic digestion with biochar: conditions

- Batch mode feed
- TS feed: 6 %
- S: OFMSW (Fossano, Italy)
- I: digestate from cow-agricultural waste
- S:I = 2:1
- T = 37 °C
- Volume = 500 mL
- **Biochar dose 5 and 10 g/L:**
 - KOH-biochar (BA): KOH/digestate = 1:2
 - Biochar from digestate (B)
- Tests in triplicate

(Ovi et al., 2022) <https://doi.org/10.1016/j.fuel.2022.123188>



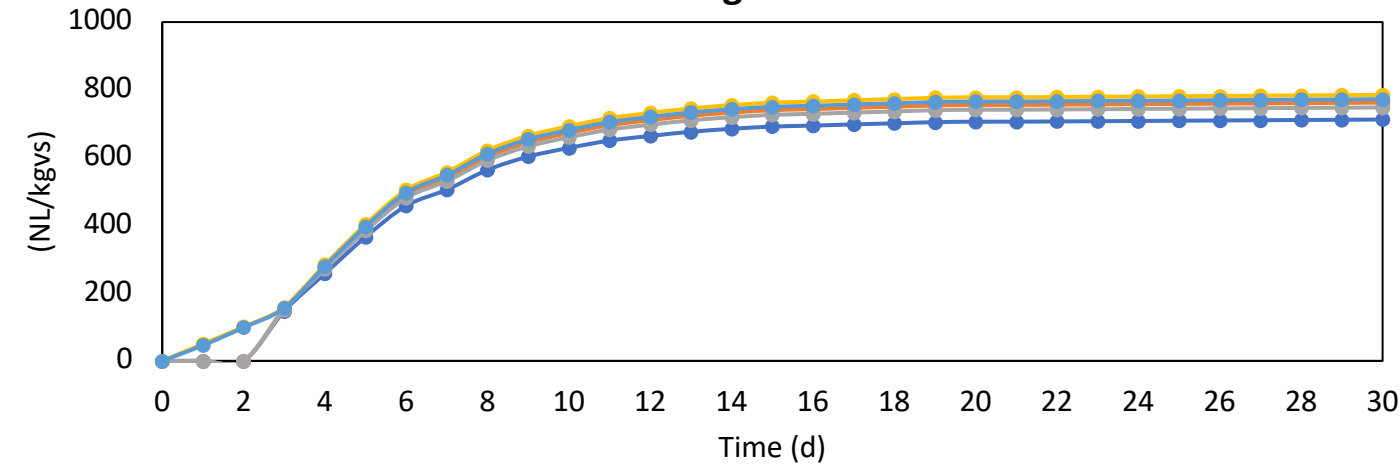
Biochar from
KOH-pre-treated
digestate



Biochar from
digestate

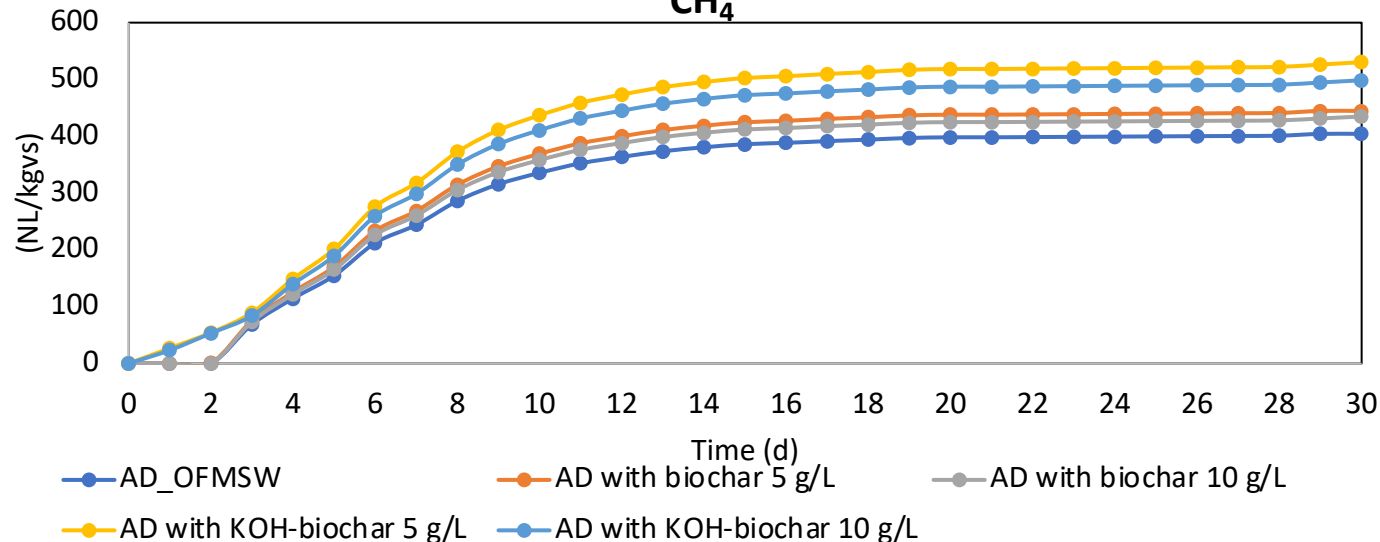
Anaerobic digestion with biochar: performances

Biogas

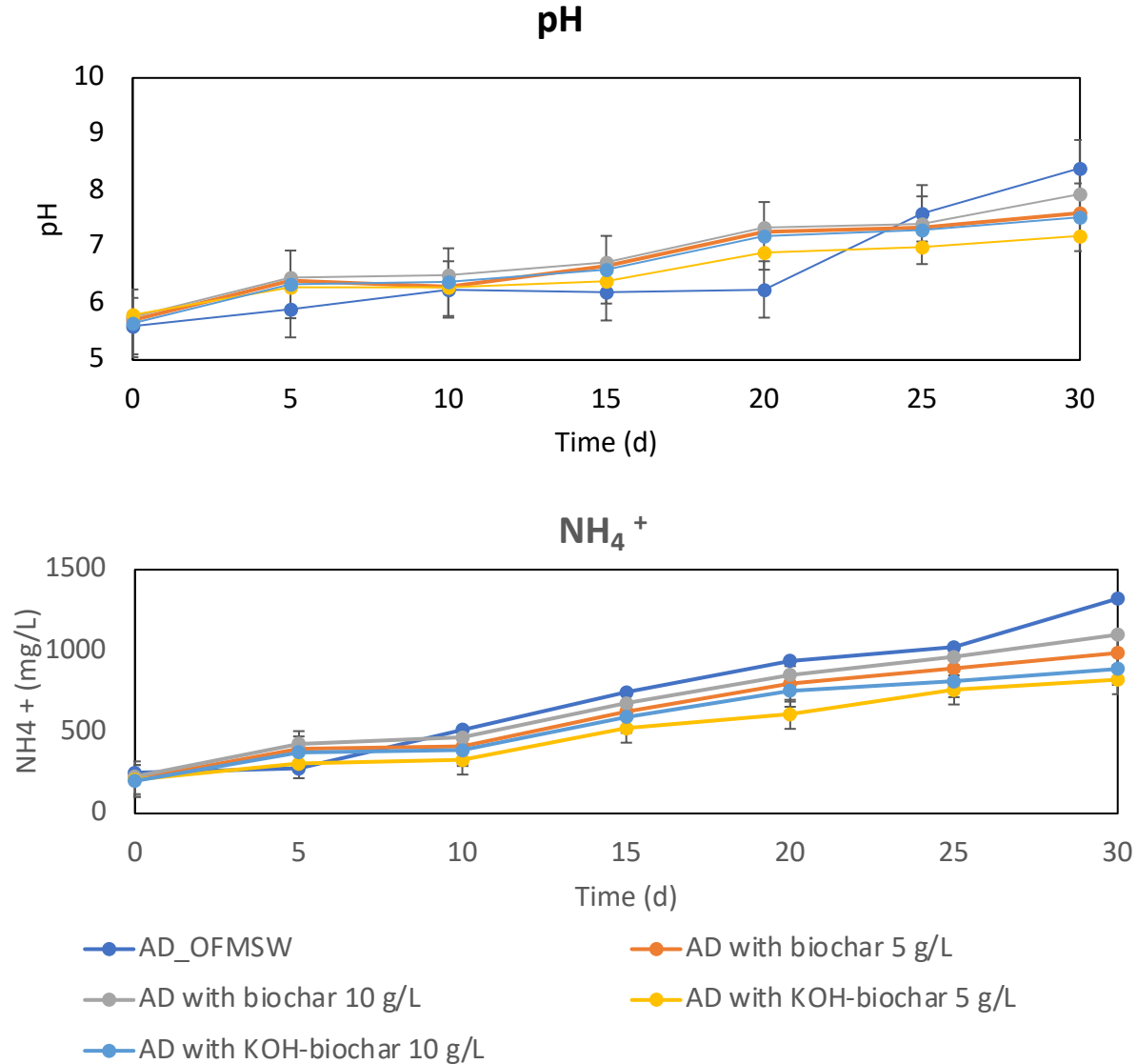


- The biogas yields did not change significantly.
- The CH_4 yield increased with the addition of KOH-pre-treated biochar.
- The AD with KOH-pre-treated biochar at 5 g/L reached + 24 % CH_4 compared to AD without biochar.
- The dose 5 g/L performed better than 10 g/L

CH_4



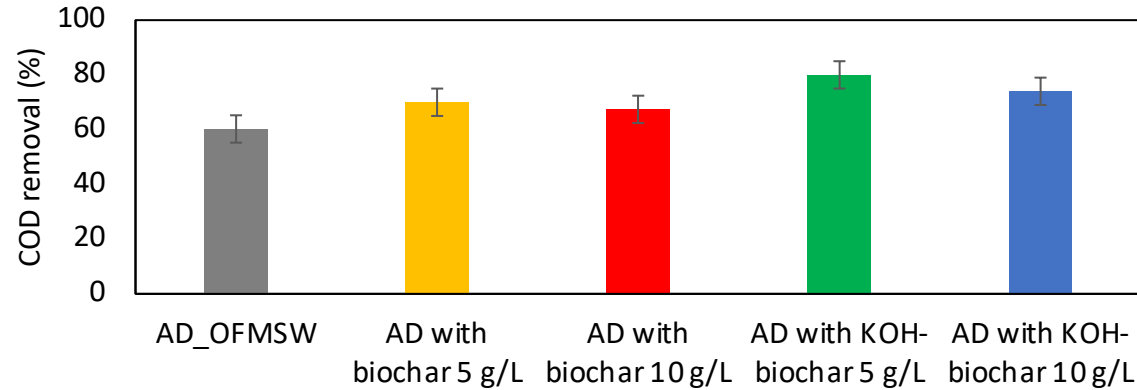
Anaerobic digestion with biochar performances



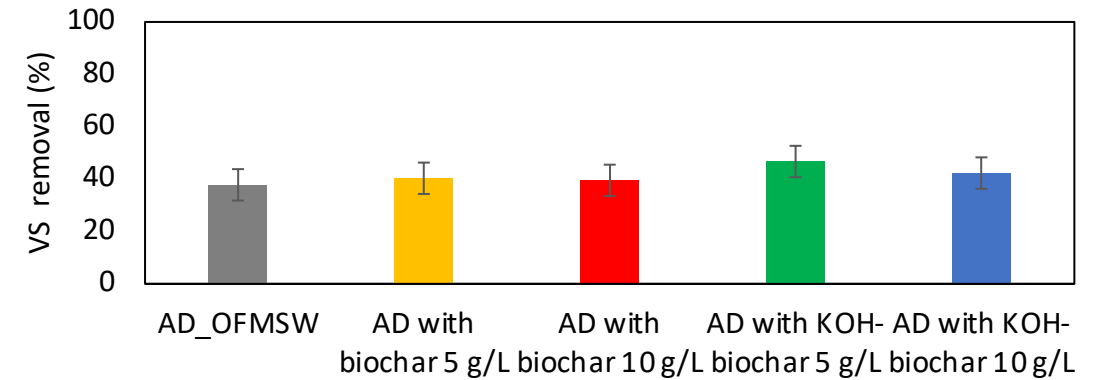
- The addition of biochar keep the pH in the desirable range for AD : 6.5-8.
- The addition of biochar keep the ammonia concentration below 1200 mg/L.
- KOH has strong $\text{NH}_4^+ / \text{NH}_3$ adsorption capacity.
- The highest performance was reached by 5 g/L
- KOH-pre-treated biochar has alkaline groups on its surface, which alleviate acid inhibition in the system.

Anaerobic digestion with biochar performances

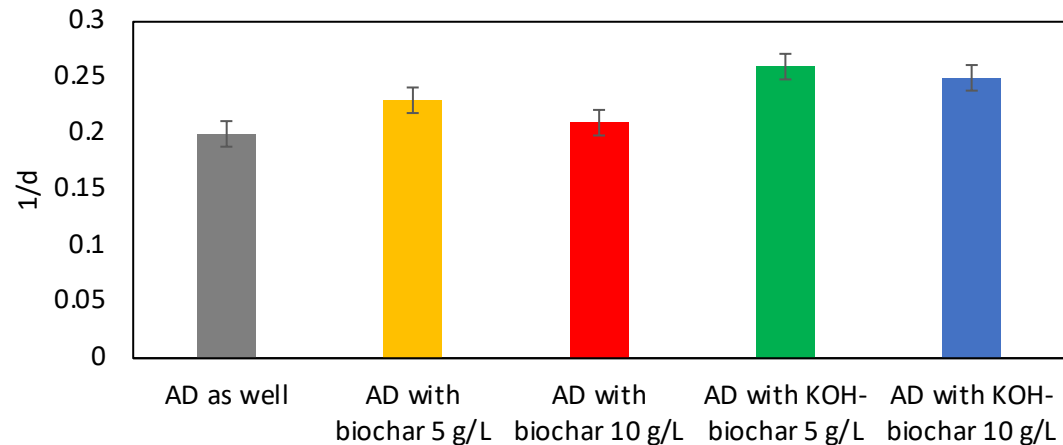
COD removal



VS removal



kd



- COD degradation and VS removal indicated the microbial behaviour.
- Kinetic disintegration improved with KOH-pre-treated biochar due to the faster biodegradation.

Conclusions and future perspectives

- ❖ KOH-digestate derived biochar reached higher surface area and pore volume by increasing the KOH/digestate ratio and pyrolysis temperature
- ❖ The optimal biochar in AD was the biochar derived from digestate pre-treated with KOH at 1:2 ratio at 600 °C at 5 g/L
- ❖ The 5 g/L dose of biochar reached higher performance than 10 g/L both with and without KOH pre-treated biochar.
- ❖ Environmental analysis will be performed.

Thank you for
the attention



References

1. Wei Chen, Meng Gong , Kaixu Li , Mingwei Xia, Zhiqun Chen, Haoyu Xiao , Yang Fang , Yingquan Chen Haiping Yang, Hanping Chen. Insight into KOH activation mechanism during biomass pyrolysis: Chemical reactions between O-containing groups and KOH. 2023. Applied Energy 278 (2020) 115730 .
<https://doi.org/10.1016/j.apenergy.2020.115730>
2. Debnath Ovi, Soon Woong Chang, Jonathan W.C. Wong, Davidraj Johnravindar, Sunita Varjani , Jae Hoon Jeung, Woo Jin Chung, Anand Thirupathi, Balasubramani Ravindran. 2022.Effect of rice husk and palm tree-based biochar addition on the anaerobic digestion of food waste/sludge. Fuel 315 (2022) 12318.
<https://doi.org/10.1016/j.fuel.2022.123188>